

# Laureatz Technochem Pvt Ltd.

Date: 15.06.2021

To,

**Member Secretary, Industry - II,**  
**Ministry of Environment, Forest & Climate Change,**  
**Vayu Wing, Indira Paryavaran Bhavan,**  
**Jor Bagh Road, Jor Bagh, New Delhi – 110003.**

Sir,

**Sub:** Submission of updated application to obtain Environmental Clearance for the proposed project "Manufacturing of Active Pharmaceutical Ingredients (API's)" at Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka-585221.

**Ref:** 1. Online application dated 25-03-2021 with Proposal No. IA/KA/IND2/206839/2021.

2. Proceedings of 9<sup>th</sup> Expert Appraisal Committee (Industry-3 Sector) meeting held during April 12-13, 2021.

Sl No.	Observations	Reply
1	The Notification dated 27.03.2020 is only for API not for intermediates. If the proposal is for API & Intermediate both, please apply for TOR. PP needs to submit the undertaking that the products are related to API only.	As per Ministry of Environment, Forest and Climate Change Notification dated 27 <sup>th</sup> March 2020 & 15 <sup>th</sup> Oct 2020, the project involves manufacturing of Active Pharmaceutical Ingredients (API's) which is under 5(f) category and hence application is being submitted under B2 Category Project. The undertaking letter is attached along with the covering letter.
2	The information filled in Form I/PFR/Reports is vagues/insufficient to address the environmental concern; accordingly, PP needs to revise the Form-1/PFR/EMP and other Reports.	The revised Form I, PFR and EMP are uploaded in the portal.
3	EMP is not adequate and not addressing the concern of Environment. Consultant has not read the provisions of the EIA Notification and applied the proposal in hurry without addressing the concern of	Environmental management Plan has been updated as per the provisions of the EIA Notification 2006 and copy of the same has been uploaded in the portal.

# Laureatz Technochem Pvt Ltd.

	EMP. Revised EMP needs to be submitted.	
4	Details of Raw material and its linkage and its mitigation measure during transportation needs to be submitted	The list of raw materials along with the quantities are attached as ANNEXURE-4. The project site is located with road distance of 180 km from Hyderabad and all the raw materials required for the projects will be obtained from thereby road. Storage, handling and transportation of raw materials with mitigation measures are detailed in EMP report.
5	As per the Ministry OM No. 22-23/2019-IA.III, dated 28.01.2021, the PP/Consultant needs to submit the details of pollution load i.e. quantity and quality, including composition, of emissions, discharges and waste (hazardous, solid & industrial) generation from the activities for further deliberations before the EAC.	As per the MoEF & CC OM No. 22-23/2019-IA.III, dated 28.01.2021, we have provided the information of product wise pollution loads includes, Water & Effluent details with effluent characteristics, Hazardous Solid waste details, Emission details, Gaseous emission details and Solvent Vapour loss details in the EMP report.
6	Details accreditation of Consultants under QCI/NABET along with certificate and disclosure of Consultant needs to be uploaded.	M/s. AM Enviro Engineers, Bengaluru is located at No. 14/1, 2 <sup>nd</sup> Floor, HARIKRUPA, Pattalamma Temple Street, Basavanagudi, Bengaluru – 560 004 and has been accredited as Category A organization under QCI-NABET scheme for Accreditation of EIA Consultant Organizations Versions 3 for preparing EIA/EMP reports with Certificate No. NABET/EIA/1922/IA0056. The copy of NABET Certificate is attached as ANNEXURE-11 and consultant disclosure is detailed in Chapter-6 of EMP report.
7	Details of land conversion documents needs to be uploaded.	The proposed project is in KIADB notified Industrial area. Hence land conversion is not applicable. KIADB land Gazette notification copy is attached as ANNEXURE-9.
8	All old CTEs/CTOs/ HW Authorization to be uploaded to verify the violation, if any.	The proposed project is a Greenfield Project. Hence, old CTEs/CTOs/ HW Authorization are not applicable.
9	PP got land on 20.03.2021. However, CETP & TSDF NOC has obtained on 18.03.2021. Please provide the details.	M/s. Laureatz Technochem Pvt Ltd proposed for API manufacturing unit at Kadechur Industrial area, Yadagir Taluk & District, Karnataka, and

# Laureatz Technochem Pvt Ltd.

		<p>accordingly requested KIADB, to allot 2 acre of land with Application dated 07-10-2020, KIADB confirmed the land and issued the demand notice to pay initial payment with letter dated <b>KIADB/HO/Allot/Secy-3/11436 /2020-21 dated:22-01-2021</b> With continuation of the demand notice, M/s. Laureatz Technochem paid the initial payment to KIADB on 20-02-2021, approached with written letter to KIADB on 06-03-2021 for allotment of land and parallelly approached M/s. Mother Earth Environ Tech Pvt. Ltd to have membership for CETP and TSDF facility. KIADB took time to issue the allotment letter but M/s. Mother Earth Environ Tech Pvt Ltd processed and issued the CETP and TSDF membership agreement one day earlier than the allotment letter.</p> <p>M/s. Laureatz Technochem Pvt Ltd. has submitted a letter to MoEF regarding the same subject, and it is attached along with the revised application.</p>
10	<p>On examination it is observed by the Ministry that the Consultant has submitted many applications with same type of data and in-adequate information in Form-I, PFR &amp; EMP. Please revise all the application as per provisions of the EIA Notification, 2006.</p>	<p>The revised application is submitted in the portal.</p>

In view of the above, we are requesting you to issue us the environmental clearance at the earliest.

**Enclosures:**

1. Form1, PFR, EMP report, additional attachments.

Thanking You,

Yours Faithfully,

For M/s. Laureatz Technochem Pvt. Ltd

  
Authorized Signatory



End: as above

Plot 147, Sri Sai Nilayam, Pragathi Nagar, Kokarapally, Hyderabad - 500090, Telangana, India  
 CIN: U71999TG2017PTC116085, GSTIN: 36AADCL2975P1Z1

Email: laureatz.sri@gmail.com, Phone: +91991407373

# **ENVIRONMENTAL MANAGEMENT PLAN**

*PREPARED FOR*

**“MANUFACTURING OF ACTIVE  
PHARMACEUTICAL INGREDIENTS (API)”**

**AT**

**PLOT NO. 62, KADECHUR INDUSTRIAL AREA, YADAGIR  
TALUK & DISTRICT, KARNATAKA.**

**NEW PROJECT BY**

**M/s. LAUREATZ TECHNOCHEM PVT LTD**

**PLOT NO. 147, SRI SAI NILAYAM, PRAGATHI NAGAR,  
KUKATPALLI, (NEAR JNTU), HYDERABAD, TELANGANA-500090**

*Prepared By*



**AM ENVIRO ENGINEERS**

**[ISO 9001-2015 CERTIFIED COMPANY]**

**(QCI/NABET Accreditation No. NABET/EIA/1922/IA0056)**

**No. 14/1, 2nd Floor, HARIKRUPA, Pattamma Temple Street,**

**Basavanagudi, Bengaluru - 560 004**

**Ph. No. : 080 2657 6577**

**DOCUMENT NO. AMEE/IND/EMP/49**



# Quality Council of India

National Accreditation Board for  
Education & Training



## CERTIFICATE OF ACCREDITATION

### AM Enviro Engineers

No.14/1, Harikrupa, Patalamma Temple Street, Basavanagudi, Bangalore,  
Karnataka-560004

Accredited as Category - A organization under the QCI-NABET Scheme for Accreditation of EIA Consultant Organizations: Version 3 for preparing EIA/EMP reports in the following sectors:

Sl. No	Sector Description	Sector (as per)		Cat.
		NABET	MoEFCC	
1.	Mining of minerals - opencast mining only	1	1 (a) (i)	B
2.	Metallurgical industries (secondary – ferrous only)	8	3 (a)	B
3.	Pesticides industry and pesticide specific intermediates (excluding formulations)	17	5 (b)	A
4.	<b>Synthetic organic chemicals industry</b> (dyes & dye intermediates; bulk drugs and intermediates <b>excluding</b> drug formulations; synthetic rubbers; basic organic chemicals, other synthetic organic chemicals and chemical intermediates)	21	5 (f)	A
5.	Building and construction projects	38	8 (a)	B
6.	Townships and Area development projects	39	8 (b)	B

**Note: Names of approved EIA Coordinators and Functional Area Experts are mentioned in IA AC Minutes dated February 21, 2020 on QCI-NABET website.**

*The Accreditation shall remain in force subject to continued compliance to the terms and conditions mentioned in NABET's letter of accreditation bearing no. QCI/NABET/ENV/ACO/20/1271 dated March 12, 2020. The accreditation needs to be renewed before the expiry date by AM Enviro Engineers, Bangalore following due process of assessment.*

Sr. Director, NABET  
Dated: March 12, 2020

Certificate No.  
NABET/EIA/1922/IA0056

Valid till  
Dec 30, 2022

For the updated List of Accredited EIA Consultant Organizations with approved Sectors please refer to QCI-NABET website.



# AM ENVIRO ENGINEERS

(Environmental Engineers and Consultants)  
(ISO 9001-2015 Certified Organization)



HeadOffice: #14/1, 2nd Floor, HARIKRUPA, Patalamma Temple Street, Basavanagudi, Bangalore-560004

## Declaration by the Head of the accredited consultant organization/ authorized person

I, **Mr. Mahadevaswamy P.** hereby, confirms and certify that the application and EMP report has been prepared by us on behalf of AM ENVIRO ENGINEERS for proposed "Active Pharmaceutical Ingredients (API's) manufacturing unit" by M/s. LAUREATZ TECHNOCHEM PVT LTD (Proposal No: IA/KA/IND2/206839/2021) located at Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka - 585221.

### Signature and Date:

**Name:** Mr. Mahadevaswamy P

**Date:** 18/06/2021

**Designation:** CEO

1.	<b>Name of the Accredited Consultant Organisation</b>	M/s. AM ENVIRO ENGINEERS, BENGALURU
2.	<b>Address of the Accredited Consultant Organisation</b>	No. 14/1, 2 <sup>nd</sup> Floor, HARIKRUPA, Patalamma Temple Street, Basavanagudi, Bengaluru - 560 004 Ph: 080-26576577 mail ID: <a href="mailto:admin@amee.in">admin@amee.in</a> Website: <a href="http://www.amee.in">www.amee.in</a>
3.	<b>Accreditation number</b>	NABET/EIA/1922/IA0056
4.	<b>Sector of Accreditation</b>	5 (f) Synthetic Organic Chemical Manufacturing Unit
5.	<b>Category of Accreditation (Eligible for Category A / Eligible for Category B)</b>	Accredited as "Category A"
6.	<b>Validity of Accreditation (date up to which the Accreditation is valid)</b>	Valid till - Dec 30, 2022

# Laureatz Technochem Pvt Ltd.

Date: 15.06.2021

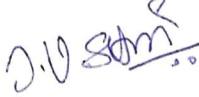
## LETTER OF UNDERTAKING

We, M /s. Laureatz Technochem Pvt. Ltd hereby declare that we have hired the Environmental Consultant M/s. AM Enviro Engineers, Bangalore to prepare the EMP report for the proposed project "Manufacturing of Active Pharmaceutical Ingredients (API)" located at Plot No. 62, Kadechur Industrial area, Yadgir Taluk & District, Karnataka. The content (Information and data) as given by us and mentioned by the consultant in the EMP report are factually correct with full knowledge of the undersigned.

Thanking you,

Yours faithfully

For M/s. Laureatz Technochem Pvt. Ltd



Authorized Signatory



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### LIST OF ANNEXURES

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3	PROCESS DESCRIPTION OF PROPOSED PRODUCTS
4	LIST OF RAW MATERIALS
5	TSDF AGREEMENT COPY
6	CETP AGREEMENT COPY
7	RISK ASSESSMENT REPORT
8	ALLOTMENT LETTER
9	KIADB GAZETTE NOTIFICATION COPY
10	LAYOUT PLAN
11	NABET ACCREDITATION CERTIFICATE

## 1.0 INTRODUCTION

### 1.1 PURPOSE OF THE REPORT

M/s. Laureatz Technochem Pvt. Ltd has proposed for establishment of new API manufacturing industry at Plot No. 62, Kadachur industrial area, Yadagir Taluk & District, Karnataka. As per the EIA notification vide gazette no. S.O. 1533 dated 14<sup>th</sup> September 2006, the proposed project comes under activity 5 (f) "Synthetic organic chemicals industry" of Category- "B".

The Karnataka - Telangana interstate boundary is at 2.64 Km in South direction from the proposed project site. Hence the proposed project has to obtain environmental clearance from MoEF & CC.

Ministry of Environment, Forest and Climate Change categorized Active Pharmaceutical Ingredients manufacturing units as 'B2' for a period up to 30<sup>th</sup> March 2021 as per the notification dated 27<sup>th</sup> March 2020 and OM dated 15<sup>th</sup> Oct 2020, as an interim measure to handle the Novel Corona Virus (COVID-19) outbreak.

In this context, to submit the application to obtain environmental clearance under B2 category as per the EIA notification 2006, Environmental management plan has been prepared.

### 1.2 DETAILS OF PROJECT PROPONENT

M/s. Laureatz Technochem Pvt. Ltd is a private limited firm and is promoted by Mr. T.V.Srihari and T.Ramani. Mr T.V.Srihari, is a Chemical Engineer and also a Postgraduate in Economics. He has vast experience of over 34 years in the field of Pharma industry by serving major Pharma players like Natco Pharma, SMS Pharma, Lupin group (Concept Labs), TTK Pharma, Neuland Labs, Clinfield India, JBF Industries, Phalanx Labs etc. He is having rich experience in the fields of manufacturing, (exposed to number of drugs synthesis), R&D, process engineering,



more than 20 of his inventions were patented, plant design and implementation of various projects from green field to manufacturing. He worked in various management levels like Director in Phalanx Labs, Vice-President (Technical) in SMS Pharmaceuticals Limited, General Manager (Technical) in Natco Pharma Limited, as Senior Manager in JBF Industries limited, middle management level Lupin group (Concept Laboratories), TTK Pharma, Clinfields India Limited, Neuland Laboratories Ltd. etc. He participated in various global pharmaceutical meets, exhibitions and international Green chemistry seminars. He is a member of green chemistry organization.

Mrs. Ramani Tadimalla, aged about 57 years is a Graduate in arts from Andhra University. Mrs. Ramani is an expert in deploying the best of the leadership practices with Results Based Measurement being the core theme. Played an effective role as Strategy Expert; as the prime negotiator with all the stakeholders. Mrs. Ramani brings in 15+ years of experience as a Strategy Specialist. She learned the ethics and techniques to promote her own firm.

### **1.3 LOCATION OF THE PROJECT**

M/s. Laureatz Technochem Pvt. Ltd is located at Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka. The Project site is close to Yadagir Raichur road which is at a distance of 1 km towards South-West side and the nearest railway station is Chegunta railway station at 3.7 km towards SW. The nearest airport is Rajiv Gandhi International Airport located at a distance of 140.9 km from the site towards North East. The maximum elevation above Mean Sea level of the project site is 363 m. The project site co-ordinates ranges from Latitude - 16.516923° to 16.517494° and Longitude- 77.313713° to 77.314952°.



TABLE-1.1: ENVIRONMENTAL SETTINGS

Particulars	Details		
	Corners	Latitude	Longitude
Plant site co-ordinates (Latitude & Longitude)	A	16°31'2.95"N	77°18'49.37"E
	B	16°31'0.98"N	77°18'49.39"E
	C	16°31'0.93"N	77°18'53.80"E
	D	16°31'2.90"N	77°18'53.83"E
Temperature	Max. 42°C, Min. 26°C		
Present land-use	KIADB land (Industrial area)		
Average rainfall	850 mm per year		
Nearest Highway	NH-167 (Yadgir - Raichur Road) - 1 km (SW)		
Nearest Railway station	Chegunta Railway Station - 3.7 km (SW)		
Nearest Airport	Rajiv Gandhi International Airport, Shamshabad -140.9 Km (NE)		
Nearest Water body	Seasonal Nala - 50 m (W) Kadechur lake - 1.5 km (NE) Bhima river - 8.7 km (SW) Krishna river - 12.3 km (SW)		
Nearest Village	Kadechur - 1.2 Km (E) Shattihalli - 2.5 km (NW)		
Nearest Town/City	Yadgir city - 33.6 Km (NW)		
Seismic Zone	Seismic zone-II as per IS-1893 (Part-1) - 2002		
Interstate boundary	Karnataka - Telangana Interstate Boundary - 2.64 Km (S)		



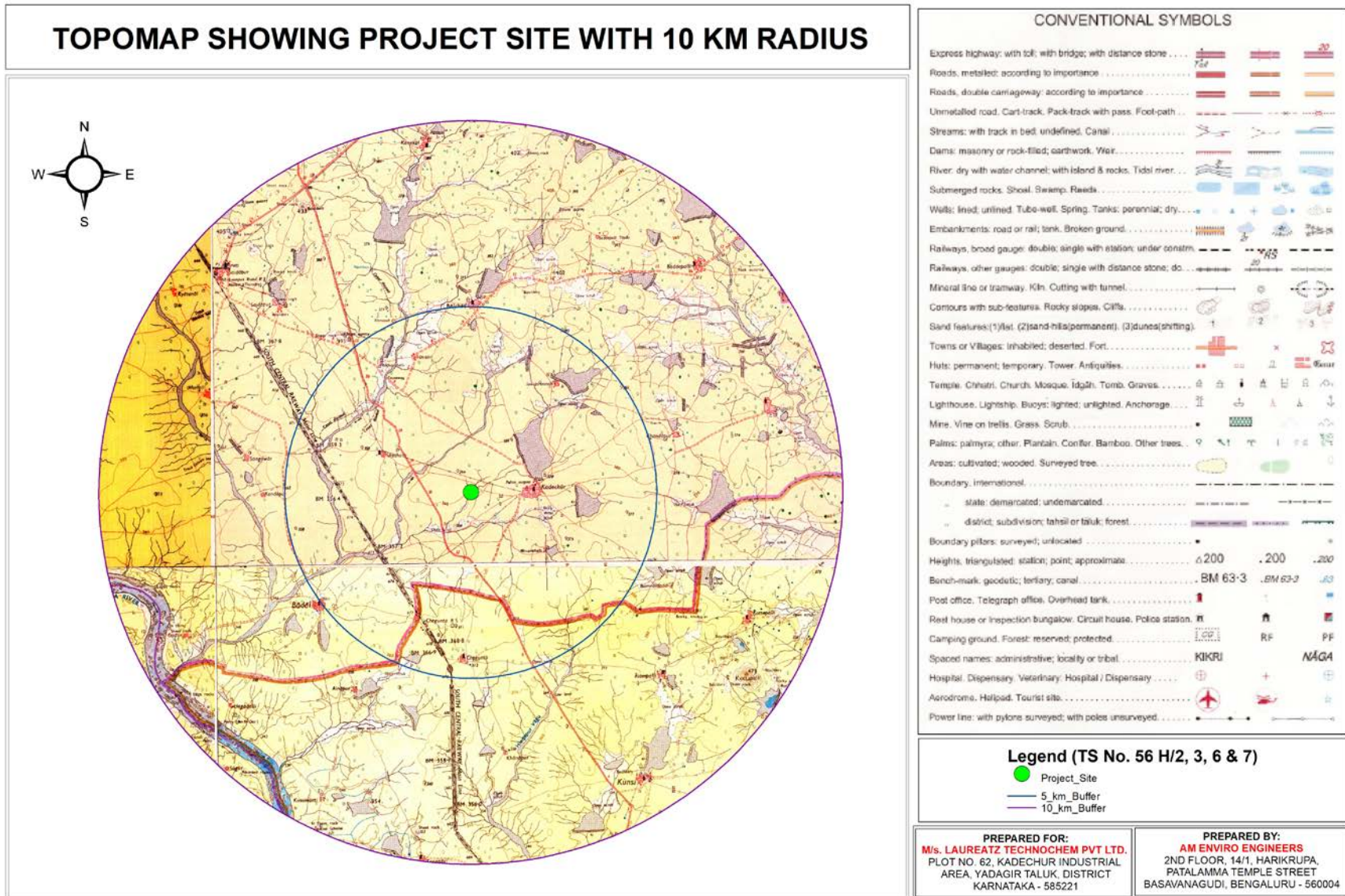


FIGURE - 1.1: TOPOMAP (1:50,000) WITH 10 KM RADIUS DEMARICATION

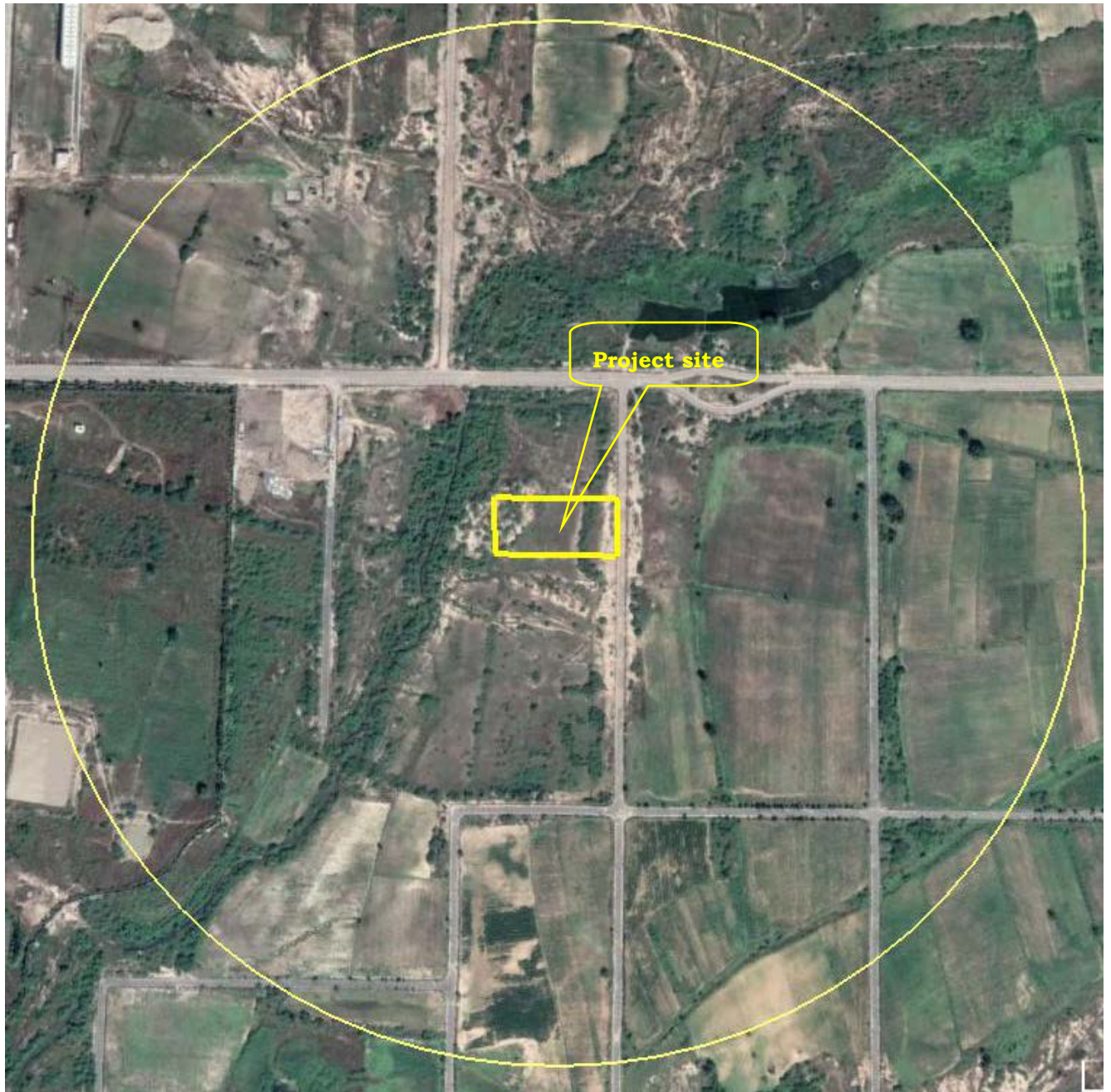


FIGURE: 1.2: GOOGLE IMAGE SHOWING 500 M RADIUS AROUND THE SITE

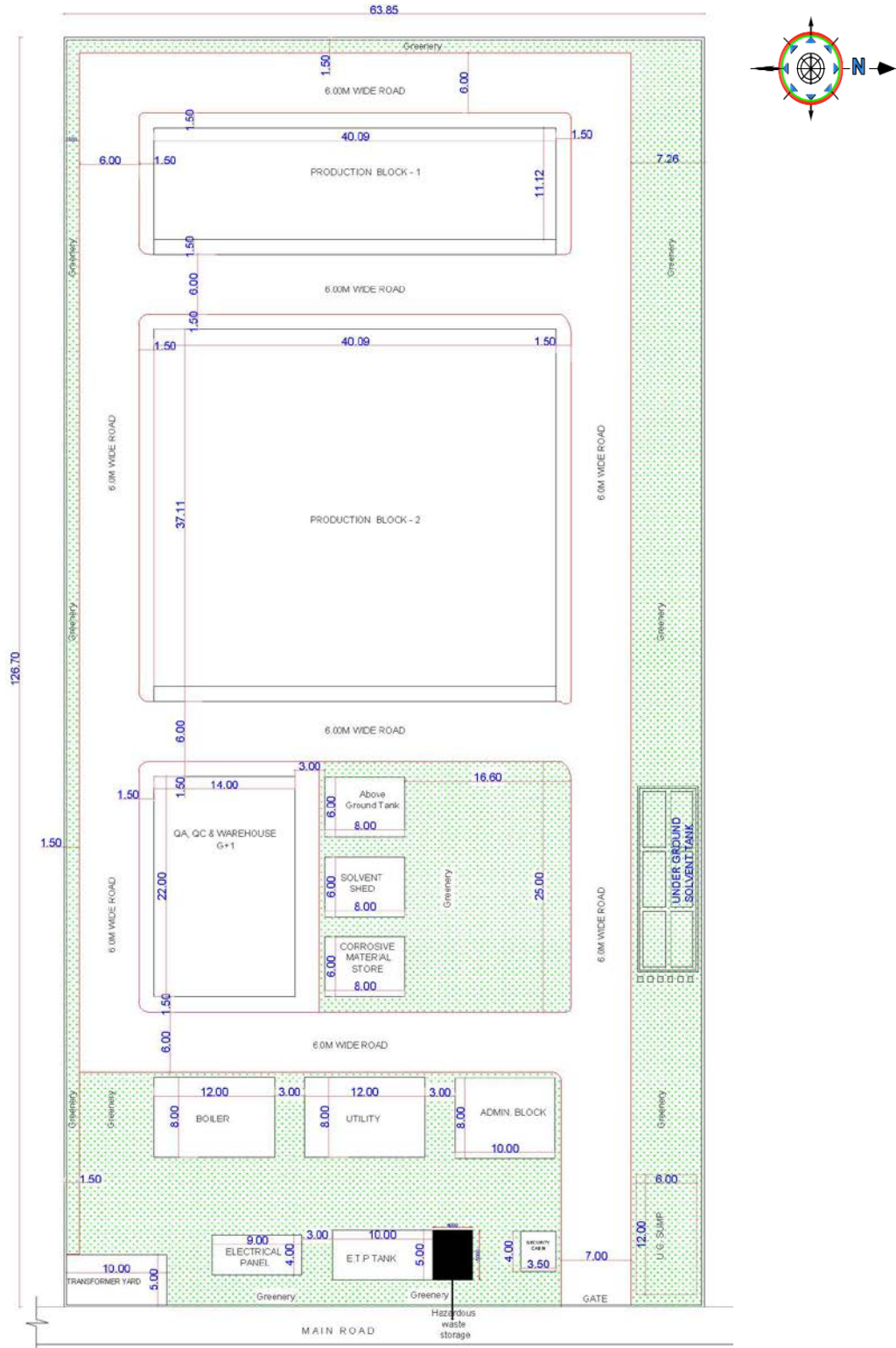


FIGURE - 1.3: LAYOUT PLAN OF THE PROPOSED PROJECT SITE



FIGURE-1.4: PHOTOS OF THE PROJECT SITE

#### 1.4 BRIEF DESCRIPTION OF THE PROJECT

KIADB has allotted 2.0 acres of land to M/s. Laureatz Technochem Pvt. Ltd at Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka in the year of 20-03-2021. The industry is proposing for manufacturing of API of 48 TPM capacity.

The project falls in the activities listed under the EIA notification- 2006 hence does require prior Environmental Clearance under the EIA notification 2006. The proposed project is covered under activity 5 (f) "Synthetic organic chemicals industry" of Category- "B" of MoEF as per the EIA notification vide gazette no. S.O. 1533 dated 14<sup>th</sup> September 2006. As per the MoEF notification dated 27<sup>th</sup> March 2020 & 15<sup>th</sup> Oct 2020, Pharmaceutical industries are categorized as 'B2' accordingly application has been submitted to MoEF & CC.

The Karnataka - Telangana interstate boundary is at 2.64 Km in South direction from the proposed project site. Hence the proposed project has to obtain environmental clearance from MoEF & CC.

#### 1.5 IMPORTANCE OF THE PROJECT

The drugs demand in India is increasing rapidly due to rapid growth of population. The requirement addition at the present rate will not be able to meet the projected demand and would result in a large drug deficit. To mitigate the gap between demands and supply Govt. of India is facilitating large scale capacity additions at shorter time through public and private investments. India with its large talented manpower, cost effective chemical synthesis, legal & financial framework is poised to become sourcing destination of drugs to the global market.



## CHAPTER - 2

## 2.0 PROJECT DESCRIPTION

## 2.1 TYPE OF PROJECT

M/s. Laureatz Technochem Pvt. Ltd has proposed for establishment of new API manufacturing industry at Kadachur industrial area, Yadagir Taluk & District, Karnataka. As per the EIA notification vide gazette no. S.O. 1533 dated 14<sup>th</sup> September 2006, the proposed project comes under activity 5 (f) "Synthetic organic chemicals industry" of Category- "B" of MoEF.

## 2.2 NEED FOR THE PROJECT

India with its large talented manpower, cost effective chemical synthesis, legal & financial framework is poised to become sourcing destination of API's to the global market. Global economic progress and social wellbeing depend a lot on health, both human and animal. Therefore, M/s. Laureatz Technochem Pvt. Ltd wants to help make a difference in these two areas by ability to compete, innovate and perform. Industry strategies revolve around the changing requirements of customers and partners, and we comply with evolving standards of regulators.

## 2.3 PROJECT MAGNITUDE

The total production capacity from the proposed project is 48 TPM. The list of the proposed products is given in below table.

TABLE - 2.1: LIST OF PROPOSED PRODUCTS WITH CAPACITY

S. No	Name of Products	Qty. in TPM	CAS No.	Therapeutic Use
1.	Adefovir	2	142340-99-6	To treat chronic (long-term) hepatitis B infection
2.	Bortezomib	1	179324-69-7	Multiple myeloma
3.	Capecitabine	5	154361-50-9	Anti-Cancer
4.	Clopidogrel Bisulphate	5	120202-66-6	Cardiovascular
5.	Dapagliflozin	2	461432-26-8	Anti-diabetic



6.	Dapoxetine Hydrochloride	2	129938-20-1	Inhibitor
7.	Darunavir Ethanolate	3	635728-49-3	Antiviral
8.	Empagliflozin	2	864070-44-0	Anti-diabetic
9.	Etodolac	1	41340-25-4	Anti-inflammatory
10.	Etoricoxib	15	202409-33-4	Anti-inflammatory
11.	Famotidine	3	76824-35-6	To treat gastritis
12.	Imatinib Mesylate	1	152459-95-5	Anti-Cancer
13.	Irinotecan HCl	1	136-572-09-3	Topoisomerase I inhibitors
14.	Ivabradine HCl	2	148849-67-6	To treat heart disease
15.	Lenalidomide	1	191732-72-6	To treat anemia
16.	Linezolid	5	165800-03-3	Antibiotic
17.	Mesalamine	10	89-57-6	Ulcerative colitis
18.	Olmесartan Medoximil	1	144689-63-4	Anti-hypertension
19.	Pantoprazole Sodium	8	138786-67-1	To treat gastritis
20.	Piroctone Olamine	5	68890-66-4	Antifungal
21.	Ramipril	5	87333-19-5	To treat high blood pressure
22.	Risperidone	2	106266-06-2	Schizophrenia
23.	Sacubitril	2	149709-62-6	Chronic heart failure and reduced ejection fraction
24.	Sparfloxacin	5	110871-86-8	Antibiotic
25.	Tadalafil	5	171596-29-5	To treat erection problems
26.	Tamsulosin hydrochloride	1	106463-17-6	To treat Benign Prostatic Hyperplasia (BPH)
27.	Telmisartan	5	144701-48-4	Anti-hypertensive
28.	Thalidomide	1	50-35-1	To treat a skin condition and cancer
29.	Triclabendazole	3	68786-66-3	Anthelmintics
30.	Zoledronic acid	1	165800-06-6	To treat high levels of calcium
	<b>Total (6 products)</b>	<b>48</b>		

**Note: From the above list of products, any 6 products will be manufactured at a given point of time.**



TABLE-2.2: LIST OF PROPOSED BY-PRODUCTS

S.No	Name of the Product	Name of the By Product	Quantity in Kgs/Day
1	Capecitabine	Peridine Hydrochloride	59.69
2	Famotidine	Potassium chloride	53.14
3	Piroctone Olamine	Aluminium hydroxide solution	1452.5
4	Pantoprazole Sodium	Potassium Sulphate	60
		Ammonium Phosphate	35
		Sodium Acetate	110
		Ammonium Chloride	72.25
5	Telmisartan	Sodium phosphate	251

TABLE-2.3: SALIENT FEATURES OF PROPOSED MANUFACTURING OF API'S

Description	Details
Project Name	Manufacturing of Active Pharmaceutical Ingredients (API)
Proponent	M/s. Laureatz Technochem Pvt. Ltd
Total Site Area	8089.8 Sq.m (2.0 acres)
Greenbelt area	2694.3 Sq.m (33.3%)
Land	KIADB land
Products capacity	48 TPM (6 products)
Man power	55 no's
Total Water required	135.3 KLD (Fresh water - 83.1 KLD )
Effluent generation	67.6 KLD (Domestic sewage - 2.1 KLD)
Treatment Plant Capacity	Sent to CETP, Kadechur
Source of water	KIADB
Cooling tower capacity	2 X 150 TR, 1 X 300 TR
Power	500 KVA
Boiler	1 X 4 TPH (Briquettes/Coal)
Scrubbers	2 X 500 cfm & 1 X 1000 cfm (Two stage)
Thermic fluid heater	2,00,000 Kcal/hr. (Briquettes/Coal)
Power Source	GESCOM
Power Back up	1X 250 KVA
Project cost	6.6 Crores

## 2.4 PROCESS DESCRIPTION

Process description of the proposed product along with route of synthesis, flow diagram & material balance is attached as ANNEXURE -3.

## 2.5 RAW MATERIAL REQUIREMENT

### 2.5.1 MAJOR RAW MATERIALS

Many raw materials are required for the chemical synthesis processes that are used by the industry. During transportation of the raw materials, the procedures given in the MSDS will be followed and the list of raw materials is enclosed as ANNEXURE -4. The mode of transportation is through roads.

### (I). STORAGE, HANDLING AND TRANSPORTATION OF RAW MATERIALS & PRODUCTS

Raw materials are stored in containers in the storage area, products are stored in product house. Raw materials are transported through trucks to the plant and within the plant small vehicles such as forklifts are used to move the raw materials. Products are transported through vehicles according to the requirement and capacity of the customer requirement.

#### a) STORAGE

Industry will provide adequate and proper storage facilities for all the raw materials and finished products. Corrosive substances will be stored away from the moisture. Solid raw material will be stored in covered area and liquid raw material will be stored in closed horizontal tank. Hazardous chemicals and solid wastes will be stored away from other plant activities. The storage yard of chemicals will be isolated and it will be equipped with all necessary safety measures.

### 2.5.2. SOLVENT REQUIREMENTS

Solvents are of immense importance in Pharmaceutical Industry. Various solvents are stored and handled every day in different stages of manufacturing. In the proposed API manufacturing facility of M/s. Laureatz Technochem Pvt. Ltd, utmost care will be taken



from the design stage to minimize losses and also hazards. Steps will be taken from the receipt to final disposal are as follows. Dedicated fresh solvent storage facility will be provided to meet uninterrupted supply of different solvents to the various process areas. The fresh solvents used during the course of processing get contaminated and come out of the process units with impurities. These solvents are recovered and reused after purification.

The basic points considered in the design, installation and operation of solvent storage and handling facility are

1. Solvent storage capacity required for each solvent.
2. Solvents stored in tanks & drums.
3. Capacity of Unloading/loading facility for each solvent.
4. Sizing of tank, pump and pipeline.
5. Preparation of basic P & ID for storage and transfer
6. Tank farm lay out design.

All the solvents are highly flammable and hence pose potential fire hazard. These solvents stored in the storage area fall under the purview of Petroleum Act and Rules, which are implemented by chief controller of explosives (CCOE). The layout and design of solvent storage area shall conform to the latest petroleum rules and PESO guidelines.

The fresh solvent requirement will be depended on generation of distillation loss. The details of solvent consumption and loss details are given below.



TABLE-2.4: PROPOSED SOLVENT USAGE, LOSSES AND RECOVERY

Sl. No	Product Name	Qty/month in kg	Qty/day in kg	No of batches per day	Solvent	Qty. in kg/day				
						Solvent input	Solvent Recovery	Solvent Loss	Solvent in Wastewater	Solvent in residue
1.	Adefovir	2000	66.67	4.76	DMF	333.35	309.54	14.29	0	9.52
		2000	66.67	4.76	Toluene	333.35	285.72	14.29	19.05	14.29
2.	Bortezomib	1000	33.33	3.33	N-Heptane	10	9.67	0.33	0	0
		1000	33.33	3.33	THF	43.33	40.83	2.17	0.33	0
		1000	33.33	3.33	MDC	148.3	141.21	4.09	0	3
		1000	33.33	3.33	Diisopropyl Ether	79.5	74.3	3.53	1.67	0
		1000	33.33	3.33	IPA	16.67	15.84	0.33	0	0.5
		1000	33.33	3.33	Methanol	100	88.5	5.83	1.67	4
		1000	33.33	3.33	DMF	50	47.5	0.1	0	2.4
		1000	33.33	3.33	Ethyl Acetate	66.67	63.33	2.67	0	0.67
		1000	33.33	3.33	n-Heptane	123.33	117.33	4.5	0	1.5
3.	Capecitabine	5000	166.7	6.67	MDC	6733.4	6400.13	133.34	0	200
		5000	166.7	6.67	Ethyl acetate	5666.7	5386.77	113.34	0	166.67
		5000	166.7	6.67	Methanol	2000.0	1900.04	40	26.67	33.33
4.	Clopidogrel Bisulphate	5000	166.7	3.33	Methylene Dichloride	999.96	949.96	50	0	0
		5000	166.7	3.33	Acetonitrile	166.66	159.99	6.67	0	0
		5000	166.7	3.33	Toluene	2283.2	2193.24	90	0	0
		5000	166.7	3.33	Isopropyl alcohol	333.32	319.99	13.33	0	0
		5000	166.7	3.33	Methanol	129.99	123.32	6.67	0	0
		5000	166.7	3.33	n-Hexane	833.3	789.97	40	3.33	0



		5000	166.7	3.33	MEK	483.31	459.98	23.33	0	0
		5000	166.7	3.33	Acetone	483.31	459.98	20	0	3.33
5.	Dapagliflozin	2000	66.67	1.33	MDC	400.02	380.02	13.33	0	6.67
		2000	66.67	1.33	Toluene	546.69	506.69	20	10.67	9.33
		2000	66.67	1.33	Methanol	400.02	373.35	13.33	6.67	6.67
		2000	66.67	1.33	N-Hexane	126.67	120.01	2.66	2.67	1.33
		2000	66.67	1.33	THF	333.35	306.68	13.33	6.67	6.67
		2000	66.67	1.33	Acetonitrile	400.02	378.69	20	0	1.33
		2000	66.67	1.33	MDC	400.02	380.02	20	0	0
6.	Dapoxetine HCl	2000	66.67	0.83	Methanol	995.00	943.00	40.00	2.00	10.00
		2000	66.67	0.83	Ethyl acetate	1170.7	1112.18	58.54	0	0
7.	Darunavir Ethanolate	3000	100.0	1.00	N-Methyl-2- Pyrrolidinone	224.88	211.39	8.99	4.5	0
		3000	100.0	1.00	Ethyl acetate	1094.4	1039	53.45	2	0
		3000	100.0	1.00	Ethanol	329.83	313.44	14.39	2	0
8.	Empagliflozin	2000	66.67	0.67	Toluene	400.02	366.69	13.33	10.67	9.33
		2000	66.67	0.67	Methanol	400.02	366.69	16.66	10	6.67
		2000	66.67	0.67	THF	400.02	366.69	13.33	10.67	9.33
		2000	66.67	0.67	Acetonitrile	200.01	183.34	10	4.67	2
		2000	66.67	0.67	MDC	200.01	183.34	10	0	6.67
9.	Etodolac	1000	33.33	0.17	Methanol	124.99	122.95	5	0	1.2
10.	Etoricoxib	15000	500.0	5.00	EDC	1250	1190	25	0	35
		15000	500.0	5.00	Hexane	1000	950	20	0	30
		15000	500.0	5.00	Toluene	2500	2375	50	25	50
		15000	500.0	5.00	THF	6000	5700	120	45	135
11.	Famotidine	3000	100.0	1.00	Acetone	170	161	8	0	1
		3000	100.0	1.00	Methanol	39	37	1	1	0



12.	Imatinib Mesylate	1000	33.33	0.67	IPE	133.33	126.66	2.67	0	4
		1000	33.33	0.67	Methanol	1072	1017	21.57	12.66	20.77
		1000	33.33	0.67	n-Butanol	666.67	633.34	13.33	5.33	14.67
		1000	33.33	0.67	IPA	166.67	158	3.34	5.33	0
		1000	33.33	0.67	MDC	533.33	506.67	10.66	0	16
		1000	33.33	0.67	Ethyl acetate	80	76	1.33	2.67	0
13.	Irinotecan HCl	1000	33.33	3.33	MDC	100	95	2	0	3
		1000	33.33	3.33	Di isopropyl ether	100	95	2	0	3
		1000	33.33	3.33	Iso propyl alcohol	166.67	158.33	3.33	3.33	1.68
		1000	33.33	3.33	N-methyl-2-Pyrrolidine	133.33	126.67	2.66	0	4
14.	Ivabradine HCl	2000	66.67	1.33	MDC	40	38	0.8	0	1.2
		2000	66.67	1.33	Acetone	40	38	0.8	0.4	0.8
		2000	66.67	1.33	DMSO	13.33	12.67	0.26	0.4	0
		2000	66.67	1.33	MIBK	20	19	0.4	0	0.6
		2000	66.67	1.33	IPA	40	31.67	0.66	0	7.67
		2000	66.67	1.33	DMF	26.67	25.33	0.54	0	0.8
15.	Lenalidomide	1000	33.33	1.33	Methanol	53.33	50.67	1.06	0.8	0.8
		1000	33.33	1.33	Dichloromethane	20	19	0.4	0	0.6
		1000	33.33	1.33	Hexane	40	38	0.8	0	1.2
16.	Linezolid	5000	166.7	1.67	MIBK	2000.0	1908.37	91.67	0	0
		5000	166.7	1.67	MDC	2666.7	2533.38	133.34	0	0
		5000	166.7	1.67	Methanol	2083.3	1955.04	95	33.34	0
		5000	166.7	1.67	Ethyl acetate	1000.0	950.02	50	0	0
17.	Mesalamine	10000	333.3	10.01	Aniline	260.26	203.2	57.06	0	0
18.	Olmesartan Medoximil	1000	33.33	0.33	THF	233.31	221.64	4.67	3.67	3.33
		1000	33.33	0.33	Ethyl acetate	116.66	110.99	2.34	1	2.33



		1000	33.33	0.33	Di isopropyl ether	33.33	31.66	1.67	0	0
		1000	33.33	0.33	IPA	199.98	189.98	6.67	0	3.33
		1000	33.33	0.33	MDC	399.96	379.96	8	0	12
		1000	33.33	0.33	Acetone	166.65	156.65	3.34	3.33	3.33
19.	Pantoprazole Sodium	8000	266.7	1.33	Acetone	1333.3	1259.97	66.66	2.67	4
		8000	266.7	1.33	Toluene	1066.6	1002.64	53.33	4.67	6
		8000	266.7	1.33	MDC	2933.2	2790.6	140	0	2.67
		8000	266.7	1.33	Methanol	499.99	442.66	50	3.33	4
		8000	266.7	1.33	Methanol	666.65	613.32	26.67	4	16
		8000	266.7	1.33	Chloroform	1399.9	1333.3	66.67	0	0
20.	Piroctone Olamine	5000	166.7	0.83	Methanol	2500.0	2331.71	124.17	31.25	12.92
		5000	166.7	0.83	EDC	833.35	791.68	41.67	0	0
		5000	166.7	0.83	Ethyl acetate	833.35	783.35	37.5	0	12.5
21.	Ramipril	5000	166.7	0.33	Ethyl acetate	200	190	10	0	0
		5000	166.7	0.33	Ethanol	216.67	206	10.67	0	0
22.	Risperidone	2000	66.67	0.13	MIBK	40	38	2	0	0
		2000	66.67	0.13	DMF	3.33	2.93	0.27	0	0.13
		2000	66.67	0.13	IPA	66.67	62.94	3.33	0	0.4
23.	Sacubitril	2000	66.67	0.67	Toluene	466.69	446.69	10	0	10
		2000	66.67	0.67	Acetone	266.68	253.35	6.66	0	6.67
		2000	66.67	0.67	Methanol	266.68	253.35	6.66	0	6.67
24.	Sparfloxacin	5000	166.7	1.67	Toluene	2333.3	2200.04	116.67	16.67	0
		5000	166.7	1.67	Ethanol	4305.7	4064.05	213.9	163.9	0
25.	Tadalafil	5000	166.7	1.67	DMSO	250.01	238.34	6.67	2.5	2.5
		5000	166.7	1.67	Methanol	250.01	238.34	6.67	2.5	2.5
26.	Tamsulosin HCl	1000	33.33	0.17	Methanol	149.99	142.49	5	0	2.5
		1000	33.33	0.17	Ethyl acetate	83.33	79.17	2.5	0.83	0.83



		1000	33.33	0.17	n-Hexane	83.33	79.17	3.33	0	0.83
		1000	33.33	0.17	Ethanol	149.99	142.49	5	0	2.5
27.	Telmisartan	5000	166.7	1.67	Methanol	4491.5	4338.17	221.65	29.49	3.33
		5000	166.67	1.67	Chloroform	533.31	506.65	26.66	0	0
		5000	166.7	1.67	MDC	1999.9	1896.59	100	0	3.33
		5000	166.7	1.67	Acetone	749.97	711.64	36.66	0	1.67
		5000	166.7	1.67	n-Hexane	166.66	158.33	8.33	0	0
28.	Thalidomide	1000	33.33	0.33	N,N-DMF	33.33	29	3.33	0.67	0.33
29.	Triclabendazole	3000	100.0	0.20	Methanol	3100	2945	62	78.95	48
		3000	100.0	0.20	Toluene	500	475	10	7	8
		3000	100.0	0.20	Ethyl acetate	500	475	10	0	15
30.	Zoledronic acid	1000	33.33	3.33	Ethyl acetate + Toluene	466.66	433.33	33.33	0	0
		1000	33.33	3.33	Chloro benzene	133.33	100	33.33	0	0



Synthetic Organic Chemicals involves the use of various chemicals and organic solvents either directly as reactant or for extraction of a product of interest from the reaction mixture. The chemicals required for the process are bought from the local markets. Mode of transportation of all raw materials and finished products for / from the project site through road. The list of solvents & hazardous and other chemicals with their storage capacity for the manufacture of above products are presented in below table.

**TABLE-2.5: LIST OF SOLVENTS & STORAGE CAPACITY**

Sl. No.	Solvent Name	Maximum storage (KL)	Physical status	Storage	Storage pressure & temp
1	Methanol	25	Liquid	Tanks	Ambient
2	MDC	25	Liquid	Tanks	Ambient
3	Ethyl Acetate	25	Liquid	Tanks	Ambient
4	Toluene	20	Liquid	Tanks	Ambient
5	THF	20	Liquid	Tanks	Ambient
6	Ethanol	20	Liquid	Tanks	Ambient
7	Acetone	15	Liquid	Drums	Ambient
8	Hexane	15	Liquid	Drums	Ambient

These materials are procured and stored in tankers and drums. They will be procured based on the production requirement.

During transportation of the raw material the procedures given in the MSDS will be followed. M/s. Laureatz Technochem Pvt. Ltd is not proposing use of banned chemicals and Hazardous chemicals in the proposed project.

## 2.6 RESOURCE REQUIREMENT

### 2.6.1 WATER REQUIREMENT

During operation phases water for the proposed project will be procured through KIADB water supply. Total water requirement during operation phase is estimated at 135.3 KLD (Fresh water-83.1 KLD), out of which approximately 2.5 KLD water required for domestic consumption, 10.7 KLD for gardening and remaining 122.1 KLD for industrial use. Wastewater generation is 67.6 KLD including domestic wastewater of 2.1



KLD. The effluents will be segregated into High TDS of 37.1 KLD and Low TDS streams of 30.5 KLD. The effluents generated from industrial process, after primary treatment will be sent to CETP, Kadechur. Domestic sewage will be passed to Septic tank followed by multigrade filter and the treated water will be reused for gardening purpose.



TABLE-2.6: CONSOLIDATED POLLUTION LOAD

S. No	Name of Products	Quantity per Month	Quantity per Day	Quantity in kgs/day													
				Water input	Water in Effluent	Effluents per day						Process Organic residues	Inorganic Residue	Total S.W	Spent carbon	Spent Catalyst	Process Emission
						TDS Load	Total Organics in effluents	COD load in Kgs	HTDS	LTDS	Total Effluents						
1	Adefovir	2000	66.67	238.1	238.1	47.95	20.86	31.29	306.9	0	306.9	16	0	16	0	0	0
2	Bortezomib	1000	33.33	1400	1408.77	97.43	17.4	26.1	949.47	574.13	1523.6	91.33	0	91.33	0	0	25.81
3	Capecitabine	5000	166.67	3333.3	3342.12	176.13	26.67	40	3544.9	0	3544.92	482.53	0	482.53	66.67	0	41.29
4	Clopidogrel Bisulphate	5000	166.67	5833.3	6184.5	236.07	3.33	7.47	6423.9	0	6423.9	593.67	72.53	666.2	21	0	64.94
5	Dapagliflozin	2000	66.67	1133.3	1117.69	220.08	29.37	73.12	1367.1	0	1367.15	38.53	0	38.53	0	0	16.94
6	Dapoxetine Hydrochloride	2000	66.67	2437.5	2441.02	87.17	235	375.83	2763.2	0	2763.18	10.13	0	10.13	11.67	0	0
7	Darunavir Ethanolate	3000	100	554.72	554.72	55.12	4	8.96	613.84	0	613.84	85.36	0	85.36	0	0	0
8	Empagliflozin	2000	66.67	1333.3	1314	62.35	46.09	69.14	731.11	691.33	1422.44	41.43	0	41.43	0	0	43.8
9	Etodolac	1000	33.33	66.67	219.2	0	1	2.24	0	73.1	73.1	4.04	11.19	15.23	0	0	0
10	Etoricoxib	15000	500	10500	10218.2	730.25	114.95	255.45	9518.4	1544.9	11063.4	558.65	0	558.65	10	0	545.25
11	Famotidine	3000	100	825	863.11	24.4	25.8	36.55	874	39.31	913.31	0	2.4	2.4	3	0	12.1
12	Imatinib Mesylate	1000	33.33	1400	1404.31	39.35	25.33	38	1126.3	342.67	1468.99	62.96	1.33	64.29	3.33	0	9.07
13	Irinotecan HCl	1000	33.33	83.33	83.33	0	3.33	5	86.67	0	86.67	16.13	0	16.13	0	0	4.2
14	Ivabradine	2000	66.67	133.33	136.4	21.01	0.8	1.52	155.15	3.07	158.21	26.63	35.99	62.61	1.33	0	0
15	Lenalidomide	1000	33.33	13.33	15.91	13.89	0.4	0.6	30.2	0	30.2	3.63	0	3.63	0.33	0.33	10.73
16	Linezolid	5000	166.67	3833.3	3876	142	89.5	89.32	2667	1440.5	4107.5	264.17	0	264.17	16.67	0	0
17	Mesalamine	10000	333.33	4904.9	4904.9	480.48	0	0	5385.4	0	5385.39	142.14	393.39	535.54	50.05	0	0
18	Olmesartan Medoximil	1000	33.33	455.56	447.78	45.56	8.89	13.33	502.22	0	502.22	32.67	52.89	85.56	0	0	2.12
19	Pantoprazole Sodium	8000	266.67	5066.6	5144.09	135.2	28	45.77	2315.6	2991.6	5307.29	108.11	0	108.11	13.33	0	88.48
20	Piroctone Olamine	5000	166.67	3316.6	1908	70.42	26.42	39.63	1584	420.83	2004.83	46.25	16.67	62.92	4.17	0	108.09
21	Ramipril	5000	166.67	50	57.38	0	0	0	0	57.38	57.38	3.95	0	3.95	3.33	0	0
22	Risperidone	2000	66.6667	13.33	13.33	1.47	0	0	14.8	0	14.8	0.93	0	0.93	1.33	0	9.62
23	Sacubitril	2000	66.67	400	400	12.67	0	0	412.67	0	412.67	82.67	0	82.67	0	0	7.33
24	Sparfloxacin	5000	166.67	4166.7	4174.57	124.9	136.7	291.22	4436.2	0	4436.17	15.73	0	15.73	16.67	0	69.92
25	Tadalafil	5000	166.67	200	201.2	0	13.2	20	0	214.4	214.4	10.17	0	10.17	0	0	15.95
26	Tamsulosin hydrochloride	1000	33.33	500	500	0	1.67	3.03	0	501.67	501.67	34.54	0	34.54	0	0	7.11
27	Telmisartan	5000	166.67	5383.3	5179.28	198.33	103.5	127.3	4766.7	1097.8	5864.45	139.73	0	139.73	16.67	5	13.88
28	Thalidomide	1000	33.33	233.33	233.33	9	0.67	2.09	243	0	243	2.57	0	2.57	1.67	0	9.1
29	Triclabendazole	3000	100	1500	1516.73	45.46	70.19	71.31	667.71	964.67	1632.38	37.63	0	37.63	0	2	49.4
30	Zoledronic acid	1000	33.33	266.67	266.67	170	47.67	53.86	484.33	0	484.33	25.67	0	25.67	16.67	0	0
	<b>Total (6 products)</b>	<b>48000</b>	<b>1600</b>	<b>35854.9</b>	<b>35805.5</b>	<b>2041.34</b>	<b>749.84</b>	<b>1212.24</b>	<b>34075.5</b>	<b>2642.73</b>	<b>36718.2</b>	<b>2180.89</b>	<b>582.66</b>	<b>2763.55</b>	<b>187.73</b>	<b>7.33</b>	<b>926.08</b>

TABLE-2.7: WATER CONSUMPTION &amp; EFFLUENT GENERATION WITH TREATMENT MECHANISM

Sl. No.	Purpose	Fresh Water (KLD)	Recycled water (KLD)	Total Water requirement (KLD)	Effluent generation (KLD)	Treatment method
1	Process	51.1	-	51.1	36.7	Sent to CETP, Kadechur
2	Scrubbing	3	-	3	3	
3	RO reject	-	-	-	15.3	
4	Boiler	23.5	-	23.5	3.4	
5	Cooling tower	-	41.5	41.5	4.1	
6	Washing	3	-	3	3	
7	Domestic Usage	2.5	-	2.5	2.1	Septic tank followed by multigrade filter
8	Gardening	-	10.7	10.7	-	-
<b>Total</b>		<b>83.1</b>	<b>52.2</b>	<b>135.3</b>	<b>67.6</b>	

### 2.6.2 POWER REQUIREMENT

Overall Power demand during operation phase is 500 KVA. The supply of power is met through GESCOM supply. Diesel generators set of 1X250 KVA will be provided as power backup in case of power failure.

### 2.6.3 PROJECT COST

The overall project cost for the proposed project is 6.6 Crores.

TABLE 2.8: BREAKUP OF THE PROJECT COST

Particulars	Amount (Rs. Crores)
Land	1.39
Building, civil work	2.60
Plant & Machinery -Mechanical, Utilities, etc.	1.86
Furniture, Fixtures and other assets	0.40
Preliminary Preoperative	0.15
Miscellaneous	0.20
<b>Total</b>	<b>6.60</b>



## 2.7 LAND REQUIREMENT

M/s Laureatz Technochem Pvt. Ltd acquired the KIADB land. The present land use is industrial. The land use break up for various activities within the facility is given below.

**TABLE-2.9: LAND USE DETAILS**

Sl no	Description	Area (Sqmt)	Area in percentage (%)
1	Ground coverage area	2725.5	33.7
2	Green belt area	2694.3	33.3
3	Roads Area	2670.0	33.0
	<b>Total</b>	<b>8089.8</b>	<b>100</b>

## 2.8 RESOURCE OPTIMIZATION AND RECYCLING

After the reaction is complete the solvents are recovered in a distillation unit. The residue from the distillation unit is collected in a container and sent to co processing. The recovered solvents are collected in drums, labeled and analyzed. Then they are reused (recycled) for the process.

Chemical synthesis produces majority of drugs currently available in the market. Chemical synthesis consists of four steps - reaction, separation, purification, and drying. Large volume of solvents are used during chemical syntheses, extractions, and solvent interchanges. The bulk drug manufacturing process utilizes various process equipment and chemical methods. Sources of emissions include dryers, reactors, distillation units, storage and transfer of materials, filtration, extraction, centrifugation, and crystallization. Chemical synthesis consists of one or more batch reactions followed by separation and purification steps utilizing organic and inorganic reactants, solvents, and catalysts, and is solvent-intensive. Waste streams generated are numerous and complex due to the raw materials used and the varied nature of operations. Organic synthesis generates a mother liquor containing unconverted reactants, byproducts, and residual product in a solvent or aqueous base, as well as acids, bases, metals, etc.

In the proposed project in the stage of separation, there are by products which are generated and which will be recovered by considering the market values. Mainly By



product recovery reduces the load on effluent treatment plant and it can be reused so that the fresh raw material consumption will reduce.

**TABLE-2.10: LIST OF BY-PRODUCTS**

S.No	Name of the Product	Name of the By Product	Quantity in Kgs/Day
1	Capecitabine	Peridine Hydrochloride	59.69
2	Famotidine	Potassium chloride	53.14
3	Piroctone Olamine	Aluminium hydroxide solution	1452.5
4	Pantoprazole Sodium	Potassium Sulphate	60
		Ammonium Phosphate	35
		Sodium Acetate	110
		Ammonium Chloride	72.25
5	Telmisartan	Sodium phosphate	251

As a green chemistry initiative, industry will be using palladium carbon in the hydrogenation reaction in the place of raney nickel.

In the proposed project, conservation has adequately addressed and hence, water consumption is optimized. All process effluent will be sent to CETP. M/s. Laureatz Technochem Pvt. Ltd obtained CETP and TSDF agreement (M/s. Mother Earth Environ Tech Pvt. Ltd) dated 18.03.2021 for discharge of Wastewater and hazardous waste generated from the industry. Treated water is available from the CETP for non-portable purposes; it will be procured and used for cooling tower make up which will be around 41.5 KLD and for gardening which will be around 10.7 KLD. So that the fresh water consumption will be 83.1 KLD.

## 2.9 WASTE MANAGEMENT

The various types of waste from different units of the proposed plant are described underneath:

### 2.9.1 LIQUID WASTE GENERATION & UTILIZATION AND DISPOSAL

Water is used both for process operations as well as for other non-process purposes. However, the use and discharge practices and the characteristics of the wastewater will vary depending on the operations conducted at the facility. Process wastewater



includes water used for reaction, water used to clean process equipment and floors. Non-process wastewater includes no contact cooling water (e.g., used in heat exchangers), no contact ancillary water (e.g., boiler blow down, bottle washing), sanitary wastewater and wastewater from other source. The wastewater generated will be sent to CETP after primary treatment.

TABLE-2.11: EFFLUENT DETAILS

S. NO	Unit	HTDS (KLD)	LTDS (KLD)	Waste water Generation in KLD	Treatment Method
1	Process	34.1	2.6	36.7	Sent to CETP, Kadechur
2	Washings	-	3	3	
3	Boiler Blow Down	-	3.4	3.4	
4	Cooling towers Blow Down	-	4.1	4.1	
5	Scrubber System	3	-	3	
6	RO reject	-	15.3	15.3	
7	Domestic	-	2.1	2.1	Septic tank followed by multigrade filter
	<b>Total</b>	<b>37.1</b>	<b>30.5</b>	<b>67.6</b>	-

### 2.9.2 SOLID WASTE GENERATION & UTILIZATION AND DISPOSAL

Both non-hazardous and hazardous wastes are generated during all stages of pharmaceutical manufacturing. These wastes can include off- specification or obsolete raw materials or products, spent solvents, reaction residues, used filter media, still bottoms, used chemical reagents, dusts from filtration or air pollution control equipment, raw material packaging wastes, and laboratory wastes.

TABLE-2.12: SOLID &amp; HAZARDOUS WASTE DETAILS

S. No	Category of the HW	Name of the Hazardous Waste	Quantity	Disposal Method
<b>Hazardous waste generation from plant</b>				
1	5.1	Waste oils & Grease/ Used Mineral oil	0.2 KL/ Annum	Agencies authorized by KSPCB
2	5.2	Oil Soaked Cotton	2 Kgs/month	KSPCB authorized Vendor
3	20.3	Distillation Residue	830 kgs/ day	Store in secured manner and hand over to authorized cement industry for Co-processing
4	28.1	Process Residues & Waste	2764 Kgs/day	Store in secured manner and hand over to authorized cement industry for Co-processing/TSDF
5	28.2	Spent Catalyst	7.3 kgs/day	Store in secured manner and hand over to authorized recycler
6	28.3	Spent Carbon + Hyflow	188 Kgs/Day	Store in secured manner and hand over to authorized cement industry for Co-processing
7	28.4	Off Specification Products	1 TPM	Store in secured manner and hand over to authorized cement industry for Co-processing/TSDF
8	28.5	Date expired products	500 Kgs/Month	Store in secured manner and hand over to authorized cement kiln for Co-processing/ TSDF
9	33.1	Detoxified- Container & Container Liners of Hazardous Chemicals and Wastes	250 No's/Month	After complete detoxification, shall be disposed to the outside agencies.
10	33.2	Contaminated cotton rags or other cleaning materials	25 Kgs/month	Store in secured manner and hand over to KSPCB Authorized Vendor
11	A1160	Used Lead Acid batteries	2 No's/Annum	Returned back to dealer/ Supplier
<b>Other &amp; Miscellaneous Solid Wastes</b>				
12	--	Coal ash	1120 kgs/ day	Sent to Brick Manufacturers



13		Briquette ash	2860 kgs/ day	Sent to fertilizer industries
14	--	Residues from Scrubber	143 kg/day	Shall be stored in secured manner & handed over to TSDF.
15	--	Used PPE	5 Kgs/ Month	Sent to authorized vendor
16	--	E- Waste	150 Kgs/ Annum	Authorized recyclers
17	--	Plastic Waste	200 Kgs/ Annum	Authorized recyclers
18	--	Metal Scrap	3 TPA	Sale to outside agencies/ recyclers
19	--	Used Filters (HEPA filters, Oil Filters etc.)	25 Nos /year	Sent to TSDF
20	--	Used / Discarded RO Membranes	0.2 TPA	Sent to TSDF

## 2.10 PROPOSED SCHEDULE FOR APPROVAL AND IMPLEMENTATION

The industry will take necessary approvals from the consented authority and start the construction immediately after obtaining Environmental Clearance.

**TABLE 2.13: TIME FRAME FOR COMPLETION OF THE PROJECT**

Details of work	Aug 2021 to July 2022	Dec 2021 to April 2022
Building and construction work	12 months	
Erection of reactors and service facilities		12 months
<b>Total</b>	<b>24 months</b>	



**CHAPTER - 3****ENVIRONMENTAL IMPACTS & PROPOSED MITIGATION MEASURES****3.1 ENVIRONMENTAL SCENARIO FOR THE PROJECT**

Every developmental activity interacts with the environment and leaves some environmental impact. Some environmental impacts associated with the current project are also inevitable. As per good manufacturing practices, such environmental impacts arising out of the project are identified well in advance and the consequences are assessed for incorporating the preventive/mitigation measures through a precautionary approach.

The proposed project would create impacts on the environment in two distinct phases:

Phase 1: During the construction phase which may be regarded as temporary or short – term

Phase 2: During the operation stage which will have marginal impact.

**3.2 ANTICIPATED IMPACTS AND MITIGATION MEASURES CONSTRUCTION PHASE**

Environmental impacts during the construction phase can be attributed to the site preparation, excavation of trenches, erection & mechanical fabrication, construction activities, transportation etc. The potential for environmental impact during construction phase on most of the environmental components, is temporary, and the environment returns back to its previous status on completion of the construction. State of the art technology will be adopted for control of pollution during project execution phase, whenever and wherever applicable.

All construction activities generally cause disruptions to the pre project environmental quality. The following environmental protection measures shall be incorporated as part of terms and conditions of contract for implementation by the contractor or the authority as appropriate. Recommendations made to minimize impacts during construction phase are delineated below:



TABLE-3.1: IMPACTS DURING CONSTRUCTION PHASE

S. No.	Environmental parameter	Impacts	Mitigate measures
1	Water	Short term negative impacts due to water consumption & sewage disposal	<p>Water requirement for construction phase will be very minor and for short period and will be fulfilled by KIADB through tankers. Thus, there will not be any significant impact on water environment.</p> <ul style="list-style-type: none"> <li>• The wastewater generation will be from the domestic activities. Domestic effluent will be disposed of through mobile Septic tank followed by soak pit.</li> <li>• Greenbelt development will have positive impact on ground water table.</li> <li>• Measures will be implemented to prevent seepage of liquid materials into ground where it could contaminate groundwater and soil. <ul style="list-style-type: none"> <li>✓ Ensure prompt cleaning up of accidental spillages</li> <li>✓ Measures will be followed to prevent the contamination of hydrological features by diesel, grease, oil, etc. derived from the working area</li> <li>✓ The machinery / equipment will be maintained in a good operating condition</li> <li>✓ Specially designated areas will be created for vehicle maintenance</li> <li>✓ Storm water will be routed through the drain after passing through the siltation tank to avoid carrying of sand.</li> </ul> </li> <li>• Provisions will be made to ensure the construction vehicles stick to the access track to prevent mud &amp; dirt being deposited on roads.</li> <li>• All mud &amp; dirt deposited on the roads from the construction activities will be cleaned.</li> <li>• Adopting good construction and engineering</li> </ul>

			practices will help in mitigating the water pollution.
2	Air	Short term negative impacts because of dust emission due to site cleaning, road laying, earthwork, transportation & construction	<p>As the project, changes will be carried out within the premises, very negligible site cleaning will be required.</p> <ul style="list-style-type: none"> <li>• Construction confined to proposed project site will be carried out as per the requirement.</li> <li>• The emissions will be temporary and confined within proposed project boundary. It is not expected to contribute significantly to the ambient air quality.</li> <li>• However, the unit will take following measures for control of dust emissions: <ul style="list-style-type: none"> <li>✓ Use of plastic cover sheet while transporting raw material at site</li> <li>✓ The heights, from which materials will be dropped, will be the minimum practical height to limit fugitive dust generation.</li> <li>✓ Use of water sprinkling system at site for dust suppression</li> <li>✓ Provision of barricade sheet of steel sheet/ tin sheet of minimum 3m heights to protect the surrounding area from the dust</li> <li>✓ All transportation vehicles will be suitably covered with tarpaulin &amp; overloading of the vehicles will be avoided.</li> <li>✓ PUC certified vehicles will be used to avoid the exhaust emission.</li> </ul> </li> <li>• The construction activity will be carried out during day time only.</li> <li>• Greenbelt development will have significant impact in reduction of dust dispersion.</li> </ul>
3	Land	Short term negative impact due to change in top layer of soil	Project construction will be carried out within the premises. Therefore no change will occur in land use pattern as well as there will not be any significant topographical change. However, temporary change in top layer of soil will be occurred but the construction activity will help in fixation of soil, thereby reducing the soil



			<p>erosion.</p> <ul style="list-style-type: none"> <li>• Top soil to be generated during construction activity will be preserved and used for the green belt development. Other excavated earth from the construction activity will be used for the backfilling and leveling in low laying area.</li> <li>• Greenbelt development will have significant impact in reduction of the soil erosion.</li> </ul>
4	Noise	Short term negative impact due to increase in noise level by site cleaning, road laying, earthwork, transportation & construction activities	<p>The noise impacts due to construction activities will be local; limited to the premises and for very short period of time.</p> <ul style="list-style-type: none"> <li>• The noise generated from construction machinery will be kept low by keeping the moving parts serviced and properly lubricated.</li> <li>• The construction activity will be carried out during day time only.</li> <li>• Vehicular movement carrying raw materials will be avoided during night time.</li> <li>• The vehicles will be regularly maintained and optimum use of the same will be made.</li> <li>• Adequate PPE's (ear plugs, ear muffs, helmet, mask etc.) will be provided to the workers.</li> <li>• PUC certified vehicles will be used.</li> <li>• Greenbelt development will have significant impact in reduction of the noise.</li> </ul>
5	Socio-economic environment	Short term positive impact by employment generation	<p>Temporary employment will be generated due to construction activities and related services like transportation of construction materials, mechanical erections etc.</p> <p>Proper facility for domestic water supply, sanitation, domestic fuel and other essential community services shall be made available to the construction workers.</p>
6	Ecology	Long term positive impact due to green	Unit will provide greenbelt area in premises which will have positive impact on local flora & fauna.

		belt development	
--	--	---------------------	--

### 3.3 ANTICIPATED IMPACTS AND MITIGATION MEASURES DURING OPERATIONAL PHASE

Several control measures have been incorporated in the process technology to minimize the generation of wastes and subsequent environmental impacts during the operational phase. Strict adherence to these pollution prevention and control measures shall moderate the environmental impacts to the minimum possible level during operational phase. In general, the environmental management plan during operational phase of the plant shall be directed to the following:

- It shall be ensured that all the pollution control / environment management systems are commissioned before the commencement of operation of the project.
- Wherever possible, the control systems shall be interlinked with the operational units, so that failure of the control system shall shut down the respective operational unit.
- Regular performance evaluation of the control systems shall be undertaken to ensure their optimum performance.
- Preventive maintenance schedule of the control systems will be matching with that of the respective operational unit.
- Regular monitoring for various components of environment shall be undertaken to ensure effective functioning of pollution control measures as well as to safe guard against any unforeseen changes in environment.
- Efforts shall be made to ensure the maximum utilization of wastes generated.

A program of vegetation reinstatement should be undertaken to compensate for loss of vegetation cover during construction phase.

During the operational phase, there will not be any significant impacts on various environmental components. The various accidental spillage/emission which can lead to emergencies are not covered in the present study.



## 3.3.1 MANAGEMENT OF AIR ENVIRONMENT

The main raw materials required for the proposed project are various chemicals, solvents, etc., for production of Synthetic Organic Chemicals, Briquettes/Coal for boilers & and Diesel for DG sets. The main sources of pollution envisaged from the proposed project are as follows.

- Process emissions
- Boiler & DG set emissions
- Details of process, boiler and DG set emissions as follows

TABLE-3.2: PROPOSED AIR EMISSIONS AND CONTROL METHOD

Sl. No	Stack attached to	Fuel used	Fuel consumption	Number of stacks	Stack/s height	Emissions	Air pollution control unit
1	Process section	-	-	3	10 m AGL	Acid mist, NH <sub>3</sub> , HBr, HF, HI, C <sub>2</sub> H <sub>5</sub> , O <sub>2</sub> , CO <sub>2</sub> , H <sub>2</sub>	Scrubber (3 no's)
<b>D.G. sets</b>							
2	1 X 250 KVA	HSD (L/hr)	52	1	4 m AGL	SO <sub>x</sub> , NO <sub>x</sub> , PM	Acoustic Measures
<b>Boiler</b>							
3	1 X 4 TPH	Briquettes (TPD)	11	1	30 m AGL	SO <sub>2</sub> , NO <sub>x</sub> , PM	Multi cyclone separators
		Coal (TPD)	8				
<b>Thermic Fluid Heater</b>							
5	Thermic Fluid Heater - 2,00,000 Kcal/Hr	Coal /Briquette (TPD)	2	1	15 m AGL	SO <sub>2</sub> , NO <sub>x</sub> , SPM,	Chimney
			3				

## a. Fugitive Emissions from Solvents Handling &amp; Recovery and Mitigation Measures

Various types of solvents are used in the Synthetic Organic Chemicals process. Fugitive emissions are expected from the reactors in the workroom, storage tanks area and as well as from handling area. Product wise solvent usage, losses and recovery are estimated based on the material balance.

Industry proposed several steps to minimize the solvent vapour emanations and recovery procedures. To control fugitive emission from process/ reaction, all reactors will be equipped with two stage condensers – primary condenser and secondary condenser. For effective condensation of vapour during reaction and distillation, primary condenser will be provided chilled water and secondary condenser will be provided chilled brine of as utility. Solvents and chemicals are handled in closed loop to avoid emission to atmosphere. Chemicals are stored under controlled temperatures to avoid evaporation during storage.

**Solvent management for effective recovery:**

- ✓ Reactor and solvent handling pump will have mechanical seals to prevent leakage.
- ✓ Condensers will be provided with sufficient Heat Transfer Area and residence time so as to achieve maximum recovery.
- ✓ Solvents will be stored in a separate space specified with all safety measures.
- ✓ Proper earthing will be provided in all the electrical equipment wherever solvent handling is done.
- ✓ Low boiling solvents storage tanks are insulated
- ✓ Entire plant where solvents are used, the equipment's/pumps/fittings will be of flame proof.

**Mitigation Measures**

To control the fugitive emissions generated during various operations in the industry, the following mitigation measures will be adopted.

- ✓ All reactors will be provided by double condensers.
- ✓ Mechanical seals will be provided for all the reactors for improving emission control measures.
- ✓ Mother liquors will be collected in closed drums.
- ✓ Wherever possible, pressure nutch filters (PNF) will be used in place of centrifuges to reducing the solvent emissions.



### Process Emissions and Mitigation Measures

Manufacturing of Synthetic Organic Chemicals will result in gaseous emissions. Maximum Process emissions with their quantities and treatment method are presented in Table 3.3. Gaseous emissions will be scrubbed in multi stages with water /caustic / solution based on the characteristics of gases.

**TABLE-3.3: PROPOSED PROCESS EMISSIONS AND CONTROL METHOD**

S. No	Name of the Gas	Quantity in Kg/Day	Treatment Method	Disposal Method
1	Hydrogen chloride	609.7	Scrubbed by using water media	Generated Dil. HCl will be reused within the industry
2	Ammonia	27.5		Generated NH <sub>4</sub> OH will be reused within the industry
3	Sulphur dioxide	80.1	Scrubbed by using C.S. Lye solution	Residues from the reaction will be sent to TSDF
4	Hydrogen Bromide	21.3		
5	Hydrogen Fluoride	3.3		
6	Hydrogen Iodide	19.9		
7	Pentane	9.2	Dispersed into atmosphere	-
8	Oxygen	104.8		
9	Carbon dioxide	259.2		
10	Hydrogen	20.2	Dispersed into atmosphere through flame arrester	-

#### b. Flue gas emissions and mitigation measures

During operational stage of the plant, Particulate Matter (PM), Sulphur dioxide (SO<sub>2</sub>) and Oxides of Nitrogen (NO<sub>x</sub>) emissions would be the major criteria air pollutants. However, the emission concentrations are insignificant.

Stack emissions in this unit are from boilers and DG sets, which will be released to atmosphere at elevated level at considerable level. DG sets will be used as standby during power failure.



TABLE 3.4: EMISSION CHARACTERISTICS DETAILS OF BOILER

Particulars	Units	4.0 TPH Boiler	
		Briquettes	Coal
Type of Fuel	--	Briquettes	Coal
Coal Consumption	TPD	11	8
Ash Content	%	26	14
Sulphur Content	%	0.002	1.5
No. of Stacks	No	1	
Height of stack	M	30	
Diameter of Stack	M	0.3	
Temperature of Flue Gas	°C	120	
Velocity of Flue Gas	m/s	9.5	
<b>Emission Details</b>			
Particulate Matter as PM	gm/sec	5.5	3.3
Sulphur dioxide as SO <sub>2</sub>	gm/sec	0.004	0.9
Oxides of Nitrogen as NO <sub>x</sub>	gm/sec	0.006	0.7
<b>Pollution Control Details</b>			
Pollution control equipment	Multi Cyclone separator		

TABLE 3.5: STACK EMISSION DETAILS OF DG SET

Capacity in KVA	Emission of PM in gm/sec	Emission of SO <sub>2</sub> in gm/sec	Emission of NO <sub>x</sub> in gm/sec	Stack dia. in m	Flue Gas Temp. in °C	Stack Height in (m)	Flue gas Velocity in m/sec
250 KVA	0.014	0.11	0.48	0.3	140	4m AGL	14

TABLE 3.6: STACK EMISSION DETAILS FOR THERMIC FLUID HEATER

Particulars	Units	Thermic fluid heater	
		Coal	Briquette
Thermo pack Boiler Capacity	Kcal/hr.	2,00,000	
Type of Fuel	--	Coal	Briquette
Fuel Consumption per Day	TPD	2	3
Stack Temperature	°C	190	192
Velocity	m/sec	5.3	5.3
Stack Height	m	15	15
Stack Diameter	m	0.2	0.2
Ash content	%	0.14	0.26
Sulphur Content	%	1.3	0.001
Emission of PM	gm/ sec	0.8	1.4
Emission of SO <sub>2</sub>	gm/ sec	0.2	0.001
Emission of NO <sub>x</sub>	gm/ sec	0.2	0.002

### 3.3.2 MANAGEMENT OF WATER ENVIRONMENT

With respect to water environment; three aspects are generally considered in study, availability & requirement of water, wastewater generation and its disposal.

**Water Requirement:** Total water requirement for the proposed project is 135.3 KLD, out of which fresh water requirement is 83.1 KLD which will be met from KIADB.

Unit will regularly check and maintain water consumption records for the proposed project. The area falls in industrial zone, specifically chemical & pharmaceutical industries and looking to the lot of sub-surface pollution in and around the area and proposed handling of hazardous chemicals by the unit, it is not advisable to recharge aquifer directly through the recharge well. Rain water can also be stored and utilized for plantation and other purposes. Thus, it is suggested to collect, store and utilize the rain water for plantation and other industrial purposes. Water balance chart is presented below.



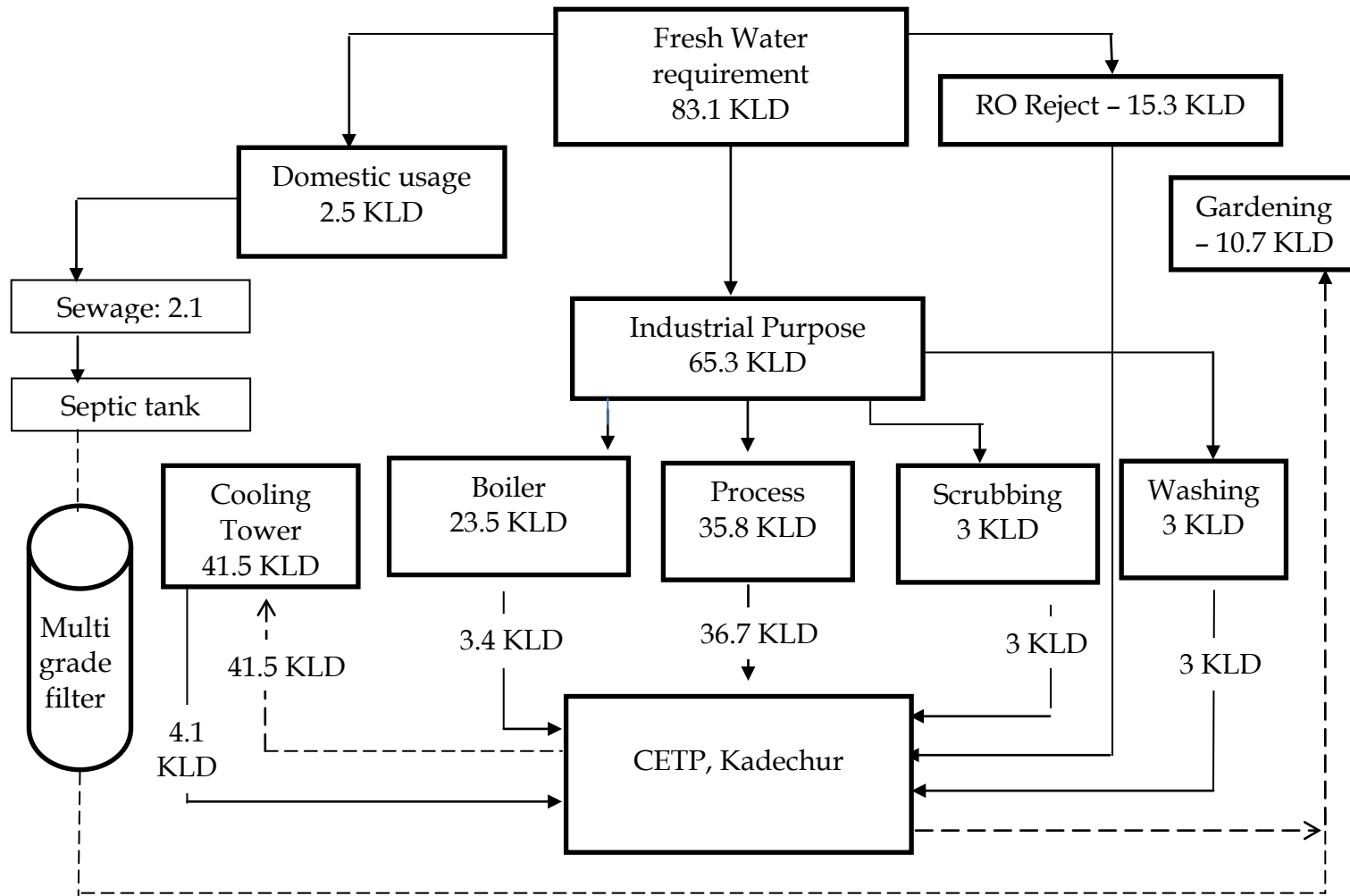


FIGURE 3.1: WATER BALANCE CHART

Hence, there will not be any adverse impact on water environment due to water availability and water requirement for the proposed project.

#### Wastewater generation:

Two different streams of effluent will be generated and will be sent to CETP, Kadechur.

S. NO	Unit	HTDS (KLD)	LTDS (KLD)	Waste water Generation in KLD	Treatment Method
1	Process	34.1	2.6	36.7	Sent to CETP, Kadechur
2	Washings	-	3	3	
3	Boiler Blow Down	-	3.4	3.4	
4	Cooling towers Blow Down	-	4.1	4.1	
5	Scrubber System	3	-	3	
6	RO reject	-	15.3	15.3	
7	Domestic	-	2.1	2.1	Septic tank followed by multigrade filter
	<b>Total</b>	<b>37.1</b>	<b>30.5</b>	<b>67.6</b>	-

#### Disposal of Effluent:

Effluent generated from industry will be collected in Equalization tank of capacity 75 KL and Neutralization tank of capacity 75 KL and later will be sent to CETP, Kadechur. Separate drains for storm water and wastewater collection will be provided. Open drains for storm water shall be provided and be kept neat and clean all the time and free of any cross connection from process source.

TABLE: 3.7: UNTREATED WATER CHARACTERISTICS

SL. NO.	PARAMETER	EXPECTED RANGE
1	pH	5-9
2	TSS	200 - 8,000 mg/L
3	TDS	500 - 56,000 mg/L
4	COD	600- 34,000 mg/L
5	BOD	500 - 12,000 mg/L



TABLE: 3.8: CETP TREATED WATER CHARACTERISTICS

SL. NO.	PARAMETER	CHARACTERISTIC RANGE
1	pH	6.5-8.0
2	TSS	Nil
3	TDS	<250 mg/L
4	COD	<50 mg/L
5	BOD	<30 mg/L

The wastewater generated from the industrial process and utilities is sent to CETP, Kadachur. There will not be any discharge of wastewater on the land. Domestic sewage will be passed to Septic tank followed by multigrade filter and the treated water will be reused for gardening purpose. Besides, there will be separate storm water and industrial wastewater drains to eliminate chances of mixing of rainwater with wastewater. Hazardous wastes will be stored, managed and handled as per hazardous wastes rules. All bulk chemicals and fuel storage areas will be provided with dyke wall/bunds to eliminate chances of any spillages/leakages entering into the storm water drain. No significant adverse impact on the surface and ground water or soil quality is envisaged in view of the proposed mitigation measures.

#### DETAILS OF RAIN WATER HARVESTING

To control soil erosion by storm water management and rain water harvesting to utilize the same for industrial uses, facility has been proposed after assessing the potential at the project. Details as follows.

1. Production Block - 1,2 of 1934 sqm
2. Ware house of 308 sqm

The total area of 2242 Sqmt.

Rainfall intensity in Yadagir - 850 mm/year

By considering 45 days of rainfall average rainfall =  $850/45 \text{ days} = 18.8 \text{ mm/day}$

Harvestable rainfall from the rooftop area  $Q = C I A$

Where, C is runoff coefficient.

I is intensity of rainfall in mm.



A is area in Sqm.

Total rainfall =  $(0.9 \times 2242 \times 18.8)/1000 = 38 \text{ m}^3/\text{day}$

**It is proposed to have roof water collection tank of capacity 80 cum.**

### **RUNOFF CALCULATIONS**

I. Runoff from Roads & Paved Area =  $(0.7 \times 2670 \times 18.8)/1000 = 35.1 \text{ m}^3/\text{day}$

II. Runoff from Landscape Area =  $(0.25 \times 2694.3 \times 18.8) /1000 = 12.6 \text{ m}^3/\text{day}$

Total runoff from hard paved and landscape area =  $48 \text{ m}^3/\text{day}$

**Runoff from Landscape, Roads & Paved Area will pass through the Oil & grease trap and Siltation tank and let in to external storm water drain.**

### **3.3.3 MANAGEMENT OF NOISE ENVIRONMENT**

- The sources of intermittent noise generating equipment will be provided with appropriate acoustic barriers so that the noise level within 100 m of these facilities when in operation will be less than 70 dBA.
- Walls and ceilings of building will be lined with sound absorbing materials, wherever required
- Sheet metal casting and housing will be insulated with sound absorbing materials
- Noise generating sources and their platforms will be maintained properly to minimize noise vibrations generated by them
- Personnel working near the noisy machines in different plant locations, will be provided with well-designed ear muffs / plugs (effective noise reduction 10-15 dBA).
- Green belt will be developed to act as a noise barrier.
- Noise barriers/ shields in the form of walls, beams will be provided around the units wherever found feasible
- Training to personnel will be imparted to generate awareness about effects of noise and importance of using PPEs.

### **3.3.4 IMPACT OF TRAFFIC**

During industrial activities, mainly emission of dust and gases from movement of vehicles and industrial activity is expected. Cement roads will be developed internally at the project site. However, following measures will be taken to reduce / contain such emissions:



- Transport vehicles and construction equipment's / machineries will be properly maintained to reduce air emissions.
- Vehicles and equipment's will be periodically checked for pollutant emissions against stipulated norms.
- Idle running of vehicles will be minimized during material loading / unloading operations.

### **3.3.5 SOLID WASTE MANAGEMENT**

All process waste is considered as hazardous waste and segregated into process organic residues, Inorganic salts and spent carbon. The organic residues and spent carbon will be disposed to cement units, for use as alternate fuel either in the solid or liquid form as recommended by CPCB. Inorganic salts will be sent to landfill at TSDF, for incineration. Hazardous/Solid waste will be segregated, detoxified and collected in the HDPE drums/bags and will be stored in the covered and raised platform with leachate collection system till its disposal. All wastes including hazardous & non-hazardous wastes will be disposed through the method approved/ permitted by the competent authority.

Hence, issues of impacts on land due to the solid/hazardous waste are not envisaged. In addition to these mitigation measures, proponent will be dedicated to maintain healthy greenbelt, which can have beneficial impact to land use, land cover and for prevention of erosion of topsoil.

### **3.3.6 MANAGEMENT OF SOCIO-ECONOMIC FACTORS**

Local people will be employed as far as possible to avoid migration of people from outside the study area.

### **3.3.7 GREEN BELT DEVELOPMENT**

The main purpose of green belt designing is to make the greenery work as barrier to the project site. Even, otherwise as per normal practice, the green belt provision is made around the permanent installations, subject to varying degrees of green belt thickness in the context of usual wind direction, its velocity and intensity in that specific area.

An ideal green belt always imparts scenic beauty besides providing roosting/perching place for birds and ground surface for naturally available reptiles, other flora and fauna species, to make the area more natural and hazard free.



**PROPOSED AFFORESTATION**

The industry proposes to develop green belt. With respect to the proposed activities more species are proposed and details are as follows.

**TABLE 3.9: LIST OF PROPOSED SPECIES**

<b>TREES</b>			
1	Indian cork tree	<i>Millingtonia hortensis</i>	82
2	Country gooseberry	<i>Phyllonthus ocidus</i>	89
3	Indian coral tree	<i>Erythrina variegata</i>	77
4	Teak	<i>Tectona grandis</i>	81
5	Beat Tree	<i>Aegle marmelos</i>	75
6	Neem tree	<i>Azadirachta indica</i>	63
7	Custard apple	<i>Anona squomosa</i>	67
8	Indian Tulip tree	<i>Spathodea companulata</i>	75
<b>TOTAL</b>			<b>609</b>
<b>SHRUBS</b>			
1	Firebush	<i>Hamelia patens</i>	40
2	Hibiscus	<i>Hibiscus rosa-sinensis</i>	36
3	Sky flower	<i>Duranta erecta</i>	35
4	Jungle geranium	<i>Ixora chinensis</i>	50
5	Scarlet bush	<i>Hamelia patens</i>	38
6	Australian Wattle	<i>Acacia catechu</i>	30
7	Golden showers	<i>Carissa spmarum</i>	30
<b>TOTAL</b>			<b>259</b>
<b>GRAND TOTAL</b>			<b>868</b>

**TABLE 3.10: IMPLEMENTATION PROGRAMME FOR GREENBELT DEVELOPMENT**

<b>Plan Period</b>	<b>Area (sq.m)</b>	<b>No. of Trees &amp; Shrubs</b>	<b>Trees &amp; Shrubs</b>
August - October, 2021	696	252	Teak, Custard apple, Scarlet bush, Hibiscus, Australian Wattle
November -December 2021, January 2022	668	197	Indian cork tree, Indian Tulip tree, Firebush
February - April, 2022	645	225	Indian coral tree, Neem tree, Jungle geranium, Sky flower
May - July, 2022	686	194	Beat tree, Country gooseberry, Golden showers
<b>Total</b>	<b>2695</b>	<b>868</b>	



### 3.3.8 HEALTH AND SAFETY

Following measures will be adopted in the plant:

- Regular inspection and maintenance of pollution control systems.
- All measures related to safety such as safety appliances, training, safety awards, posters, slogans will be undertaken.
- The workers exposed to noisy sources will be provided with ear muffs/plugs.
- Adequate facilities for drinking water and toilets will be provided to the employees.
- The fire and safety equipment will be properly utilized and maintained regularly.
- The health of the workers will be regularly checked by a well-qualified doctor and proper records will be kept for each worker.

### 3.3.9. RISK ASSESSMENT

#### a. Identification of Hazards

- Hazard identification is the most critical step in the risk assessment. This is because to identify the hazards, experience, detailed process knowledge, engineering codes, checklist, HAZOPs etc is required.
- Hazard identification is carried out to ascertain the controls required and available in order to mitigate the risk of exposure to the hazards. This would substantially help in overcoming costly errors and prolonged delays that may be caused due to the design changes that may be required on a later date.
- Hazard assessment is carried out at the equipment design stage and the control / mitigation measures are put in place overcome them to avoid costly errors at a later stage.
- Hazard assessment in our plant is carried out examining the, material storage, type of operations, locations to find out the facilities in place to overcome the risks of exposure to the hazards.
- After a critical analysis of the chemicals used, stored, defined safe operating procedures and the different manufacturing processes, the following table lists the safety measures / installations in place and mitigation measures to overcome the hazards.



Following are the Hazards identified in proposed project activities:

- Fire Hazards
- Spillage of Hazardous chemicals which leads to Air pollution
- Explosion Hazards
- Toxic gas release
- Noise

**TABLE:3.11 LIST OF SOLVENTS**

S.NO	NAME OF THE SOLVENT	PHYSICAL STATE	MODE OF STORAGE	MAX. INVENTORY IN KL.	NATURE OF HAZARD	NFPA RATING
1.	Methanol	Liquid	Tank	25	Flammable	H: 1 F: 3 R: 0
2.	MDC	Liquid	Tank	25	Harmful	H: 2 F: 1 R: 0
3.	Ethyl Acetate	Liquid	Tank	25	Flammable	H: 1 F: 3 R: 0
4.	Toluene	Liquid	Tank	20	Flammable	H: 2 F: 3 R: 0
5.	THF	Liquid	Tank	20	Flammable	H: 2 F: 3 R: 1
6.	Ethanol	Liquid	Tank	20	Flammable	H: 3 F: 2 R: 0
7.	Acetone	Liquid	Drums	15	Flammable	H: 1 F: 3 R: 0
8.	Hexane	Liquid	Drums	15	Flammable	H: 2 F: 3 R: 0



**b. Handling Precautions**

- Use in a closed system under argon or nitrogen.
- Do not get in eyes, on skin or clothing.
- Do not breathe vapors or mist.
- Store in a cool place. Keep container closed.
- Keep away from sources of ignition, water, air, acids and oxidizing agents
- In case of fire, do not use water or carbon dioxide

**c. Emergency Preparedness**

- On Site Emergency Plan
- Training & Awareness

**d. Safe Practices [Handling, Storage, Transportation And Unloading Of Chemicals]****Drums**

Liquid Raw materials will be transferred from the drums to the day tank situated at the production block with the help of leak proof drum pumps / pumps / Vacuum through pipe lines from day tank to reaction vessel unloading by gravity.

**Storage Tanks**

Solvent will be transferred to the day tank situated at the production block with the help of mechanical seal pump through pipe lines from the tank, from day tank to reaction vessel unloading by gravity.

Tank is connected to chilled water circulated condenser with reflux system.

**Measures to Avoid Evaporation**

- Keep containers tightly closed.
- Keep away from heat, spark & flame
- Keep away from sources of ignition
- Store in a cool, dry, well-ventilated area away from incompatible substances.



### Safety Systems

- Designated areas with proper indication & safety signs.
- Double earthing systems
- Flame arrestor to the vent
- Flame proof transferring pumps
- Handling precautions/SOP protocol
- Pressure Gauges
- Level indicators
- Flame proof lighting to storage yard

### Transportation / Unloading

Highly inflammable chemicals will be transported by road. Therefore, adequate safety precautions for transportation are followed. During transportation of hazardous chemicals, MSDS & TREM card will be provided to driver. As per Motor Vehicle Rules, PESO rules and Factory Rules all safety precautions will be followed during transportation of hazardous chemicals.

The following safety precautions are suggested during transportation of toxic, inflammable and corrosive chemicals in tankers, while loading and unloading, transportation and meeting the emergencies arising out of leakages and spillages of hazardous materials:

- Park the vehicle at designated place.
- Stop the engine.
- Check-up spark arrester.
- Provide earthing to tanker securely.
- Ensure that fireman is available near the place with proper equipment's.
- Connect the piping properly
- Before start unloading, check that, there should not be any leakage.
- In case of leakage, immediately attend the leakages & rectify it.
- After unloading is over, close the lid properly.



- Vehicle to be started only after removal of all pipelines connected with tanker.

### **Safety Instructions For Transportation Of Hazardous Materials**

- The name of the chemical along with pictorial sign denoting the dangerous goods should be marked on the vehicle and the packing material.
- The name of the transporter, his address and telephone number should be clearly written on the road tanker and on the vehicle.
- The tanker or vehicle should not be used to transport any material other than what is written on it.
- Only trained drivers and cleaners should transport hazardous chemicals.
- The transporter and the manufacturer must ensure the safe transportation of the material.
- The Tanker / Vehicle should be checked for its fitness and safe condition before loading.
- During loading and unloading, the tanker/vehicle should be braked and isolated against any movement, while loading/unloading, use safety appliances.
- The tanker / vehicle should not be overloaded beyond the weight permitted by R.T.O.
- Check for leakages from the line connections / containers before starting and Stopping the filling operations.
- Drive the vehicles carefully, especially in crowded localities and on Bumpy roads.
- Do not apply sudden break.
- The tanker / vehicle should not be parked for long time on the way and especially in crowded places. Park the vehicle away from residential areas

### **Spill Control**

- For all plants spill control procedures will be displayed. Spillage shall be controlled as per concerned spill control procedure.
- Unprotected personnel up wind will be kept upwind.
- Like any spilled materials to contain. Absorb spilled liquid by dry absorbent



clay or vermiculite.

- Collect most of the contaminated absorbent with shovel for further disposal/incineration.
- If spill of material directly on the ground, dig up and remove saturated soil for disposal/incineration.
- Inactivate poisonous chemical with suitable method.

#### **e. Effect And Consequence Analysis**

- In a plant handling hazardous chemicals, the main hazard due to storage, handling and use of these chemicals. If these chemicals are released into the atmosphere, they may cause damage due to resulting fires or vapor clouds last over pressures depend upon the reactivity class of material between two explosive limits.

#### **Operating Parameters**

- Potential vapor release for the same material depends significantly on the operating conditions especially for any liquefied gas, operating conditions are very critical to assess the damage potential.
- If we take up an example of ammonia, if it is stored at ambient temperature say 30°C, and then the vapor release potential of the inventory is much higher as compared to the case if it is stored at 0°C.

#### **Inventory**

- Inventory analysis is commonly used in understanding the relative hazards and short listing of release scenarios.
- Inventory plays an important role in regard to the potential hazard.
- Larger the inventory of a vessel or a system, larger the quantity of potential release.
- The potential vapor release [source strength] depends upon the quantity of liquid release, the properties of the materials and the operating conditions [pressure, temperature].



- If all these influencing parameters are combined into a matrix and vapor source strength estimated for each release case, a ranking should become a credible exercise.

### **Loss of Containment**

- Plant inventory can get discharged to environment due to Loss of Containment.
- Certain features of materials to be handled at the plant need to be clearly understood to firstly list out all significant release cases and then to short list release scenarios for a detailed examination.
- Liquid release can be either instantaneous or continuous.
- Failure of a vessel leading to an instantaneous outflow assumes the sudden appearance of such a major crack that practically all of the contents above the crack shall be released in a very short time.
- The more likely event is the case of liquid release from a hole in a pipe connected to the vessel. The flow rate will depend on the size of the hole as well as on the pressure, which was present, in front of the hole, prior to the accident. Such pressure is basically dependent on the pressure in the vessel.
- The vaporization of released liquid depends on the vapor pressure and weather conditions. Such consideration and others have been kept in mind both during the initial listing as well as during the short listing procedure.

**Detailed risk assessment report is attached as ANNEXURE- 7**



**CHAPTER - 4****4.0 ENVIRONMENTAL MONITORING PROGRAM****4.1 INTRODUCTION**

Environmental monitoring is an essential tool for sustainable development & ensuring effective most implementation & monitoring of environmental management plan & mitigation measures. It is also very essential to keep updating the environmental management system for effective conservation of environment along with ongoing project activities/operation. It provides exact idea for mitigation measures to be implemented as it is linked with actual distraction of environmental quality due to the project activities. Hence, monitoring of critical parameters of environmental quality is very essential in the routine activity schedule of project operation.

**4.2 OBJECTIVES OF MONITORING**

An Environmental Monitoring Programme shall be scheduled for the following major objectives:

- Assessment of the changes in environmental conditions, if any, during the project operation/activities.
- Monitoring & tracking the effectiveness of Environment Management Plan & implementation of mitigation measures planned.
- Identification of any significant adverse transformation in environmental condition to plan additional mitigation measures.

**4.3 MONITORING SCHEDULE**

Environmental Monitoring Schedules are prepared covering various stages of project advancement such as constructional phase and regular operational phase.

**4.3.1 MONITORING SCHEDULES DURING CONSTRUCTIONAL PHASE**

Environmental impacts during the construction phase can be attributed to the site preparation activity and the mobilization of workforce. The impacts of the construction phase on the environment would be basically of transient nature and



are expected to wear out gradually on completion of the construction programme. However, once the construction of the project is completed and its operations started, these operation stage impacts would overlap the impacts due to the construction activities.

Environmental attributes Monitoring schedules during construction phase will be as per the CFE issued from KSPCB and EC issued from MoEF&CC.

#### 4.3.2 MONITORING SCHEDULES DURING OPERATION PHASE

The control measures that will be undertaken during the operation phase to mitigate the impacts that may be caused during the operation of the project are as follows:

- Periodic monitoring of the environmental attributes to check the adequacy and effectiveness of the pollution control measures employed.
- The major sources of emission are D.G sets, boiler stack, production block (reactor) scrubber stacks which will be of adequate height to disperse the pollutants. Adequate green belt has been developed to mitigate the pollution arising due to movement of vehicles. Regular monitoring of DG-Stack and Ambient air quality will be carried out.
- Effluent will be sent to CETP for further treatment.
- Noise pollution will be curbed by using proper acoustic enclosures for D.G sets and reactors, thereby the ambient noise levels will be maintained below the CPCB limits of 75 dB for industrial areas. Personal protective equipment's will be provided to those workers who work in areas of high noise.
- Rainwater harvesting system has been designed to utilize the underground water system sustainably.
- Proper maintenance of greenbelt will be ensured.
- Adequate safety measures conforming to the occupational health and safety policy will be taken to prevent accidents/hazards to the workers.

Proposed monitoring schedule for environmental parameters is given in following table.



**TABLE 4.1: PROPOSED MONITORING SCHEDULE FOR ENVIRONMENTAL PARAMETERS**

SI No	ATTRIBUTE	PARAMETERS	FREQUENCY OF MONITORING
1.	Stack Monitoring	SPM, SO <sub>2</sub> , NO <sub>x</sub> and process emissions	Every Month or as specified by State pollution Control Board
2.	Ambient air quality within premises	PM <sub>10</sub> , PM <sub>2.5</sub> SO <sub>2</sub> , NO <sub>x</sub> , VOC	Every Month or as specified by State pollution Control Board
3.	Ambient air quality outside premises	PM <sub>10</sub> , PM <sub>2.5</sub> SO <sub>2</sub> , NO <sub>x</sub> ,	Once in a year or as specified by State pollution Control Board
4.	Water monitoring	Ph, Temp., TDS, TSS, Hardness, BOD, COD, heavy metals, etc.	Once in a year or as specified by State pollution Control Board
5.	Noise monitoring within premises	Noise levels	Every Month or as specified by State pollution Control Board
6.	Noise monitoring outside premises	Noise levels	Every Month or as specified by State pollution Control Board

#### 4.4 SITE SPECIFIC BASELINE DATA

##### 4.4.1 LAND ENVIRONMENT

The main objective of this section is to provide environmental baseline status of the proposed project site so that temporal changes due to the proposed development on the surroundings can be assessed.



TABLE 4.2: PHYSICO-CHEMICAL CHARACTERISTICS OF THE SOIL

Parameters with units	Results
<b>Physical properties:</b>	
<b>Description: brown colored soil.</b>	
Coarse sand, (%)	38
Fine sand, (%)	22
Silt, (%)	28
Clay, (%)	12
Colour	Brown
<b>Chemical properties:</b>	
pH (1:2)	7.30
Electrical conductivity, (1:2) ( $\mu\text{S}/\text{cm}$ )	74
Moisture content, %	1.8
Organic matter, (%)	1.26
Chloride as Cl, mg/kg	16.0
Magnesium as Mg, mg/kg	1814
Available Nitrogen as N, mg/kg	102.8
Available Phosphorus as P, mg/kg	44.2
Available Potassium as K, mg/kg	132.2
Copper as Cu, mg/kg	24.2
Mercury as Hg, mg/kg	<0.05
Cadmium as Cd, mg/kg	1.24
Selenium as Se, mg/kg	<0.05
Arsenic as As, mg/kg	<0.05
Lead as Pb, mg/kg	4.6
Zinc as Zn, mg/kg	1.6
Manganese as Mn, mg/kg	9.4
Cyanide as Cn, mg/kg	BDL

#### 4.4.2 WATER ENVIRONMENT

Industrialization at any region is contingent on the availability of sufficient water resources as there would be a continuous requirement of water for various industrial activities. The potential for exploitation and contamination of either or both surface and ground water resources in the project area would increase through discharge of effluents. In order to identify the possible impacts on water environment due to the major industrial development project, the available water resources have been collected and analyzed to assess the existing quality to represent the baseline status of water environment.



TABLE 4.3: WATER TEST RESULTS

Sl. No	Parameter	Results	Maximum Desirable Limit IS 10500 : 2012	Maximum Permissible Limit IS 10500 : 2012
1	Color (hazen units)	<5.0	5	15
2	Odor	Agreeable	Agreeable	Agreeable
3	Taste	Agreeable	Agreeable	Agreeable
4	Electrical Conductivity, $\mu\text{s}/\text{cm}$	838	-	-
5	pH Value	7.30	6.5 - 8.5	No relaxation
6	Turbidity, NTU	0.5	1	5
7	Chloride as Cl, mg/L	62.92	250	1000
8	Total hardness as $\text{CaCO}_3$ , mg/L	120	200	450
9	Calcium as Ca, mg/L	26.4	75	200
10	Magnesium as Mg, mg/L	14.84	30	100
11	Total Dissolved Solids, mg/L	394	500	2000
12	Sulphate as $\text{SO}_4$ , mg/L	14.84	200	400
13	Fluoride as F, mg/L	0.8	1.0	1.5
14	Chromium as $\text{Cr}^+$ , mg/L	BDL	0.05	No relaxation
15	Residual Free Chlorine, mg/L	BDL	0.2	1
16	Alkalinity as $\text{CaCO}_3$ , mg/L	106.4	200	450
17	Nitrates as $\text{NO}_3$ , mg/L	7.34	45	No relaxation
18	Copper as Cu, mg/L	BDL	0.05	1.5
19	Iron as Fe, mg/L	BDL	0.3	No relaxation
20	Manganese as Mn, mg/L	BDL	0.1	0.3
21	Phenolic compounds as $\text{C}_6\text{H}_5\text{OH}$ , mg/L	Absent	0.001	0.002
22	Mercury as Hg, mg/L	BDL	0.001	No relaxation
23	Cadmium as Cd, mg/L	BDL	0.003	No relaxation
24	Selenium as Se, mg/L	BDL	0.01	No relaxation
25	Arsenic as As, mg/L	BDL	0.01	No relaxation
26	Cyanide as CN, mg/L	Absent	0.05	No relaxation
27	Lead as Pb, mg/L	BDL	0.01	No relaxation
28	Zinc as Zn, mg/L	BDL	5	15
29	Anionic detergents as MBAS, mg/L	Absent	0.20	1.0
30	Aluminium as Al, as mg/L	BDL	0.03	0.2
31	Boron as B, mg/L	BDL	0.5	1.0
32	Coliform Organism / 100ml	<1	Less than 1	IS 1622 - 1981
33	Escherichia coli / 100ml	<1	Absent	IS 1622 - 1981

Note: BDL for Cr: 0.005, Cu: 0.01, Fe: 0.1, Mn: 0.01, Hg: 0.001, Cd:0.003, Se:0. 0.01, As:0.01, Pb:0.01, Al:0.005, B:0.5,Zn: 0.01, CN:0.05



#### 4.4.3 AIR ENVIRONMENT

The major objective of baseline air monitoring is to evaluate the existing air quality of the area. Formulation of baseline Ambient Air Quality (AAQ) data of the study area occupies a significant role in assessing the conformity to standards of the ambient air quality during the construction and operation of the proposed project. The ambient air quality has been monitored for all the parameters as per NAAQS notified on 16th September, 2009. The major air pollutants monitored on 24 hourly bases are, Particulate matter (PM10 and PM2.5  $\mu\text{g}/\text{m}^3$ ), Sulfur dioxide and oxides of Nitrogen. Sampling and analysis of the above variables is according to the guidelines of Central Pollution Control Board.

**TABLE 4.4: AMBIENT AIR QUALITY RESULTS**

Sl.No	Test Parameters	Results	Limits (As Per NAAQS)
1	Particulate Matter PM10, $\mu\text{g}/\text{m}^3$	64.26	100
2	Particulate Matter PM2.5, $\mu\text{g}/\text{m}^3$	24.20	60
3	Nitrogen Dioxide NO <sub>x</sub> , $\mu\text{g}/\text{m}^3$	28.20	80
4	Sulphur dioxide as SO <sub>2</sub> , $\mu\text{g}/\text{m}^3$	18.26	80

#### 4.4.4 NOISE ENVIRONMENT

The objective of noise pollution survey in the study area was to assess the impact of noise generated by the existing noise sources in the region especially on the human settlements. The noise levels of a region can be estimated from the cumulative noise pressure levels considering all the noise pollution sources in the region and the prevailing environmental conditions.

Noise Level Stipulated by KSPCB for Residential area is 55 dB (A) (During day time) and 45 dB(A) (During night time), For Commercial area 65 dB (A) (During day time) and 55 dB(A) (During night time), For Industrial area 75 dB (A) (During day time) and 70 dB(A) (During night time)



TABLE 4.5: MEASURED AMBIENT NOISE LEVELS

Location	Results			KSPCB Limit
	Parameter			
	L min Result	L max Result	Leq Result	
North Side Boundary Area	52.1	54.6	53.35	75 dB (A) (During day time)
South Side Boundary Area	52.9	54.8	53.85	
East Side Boundary Area	51.5	54.8	53.05	
West Side Boundary Area	51.9	52.8	52.35	



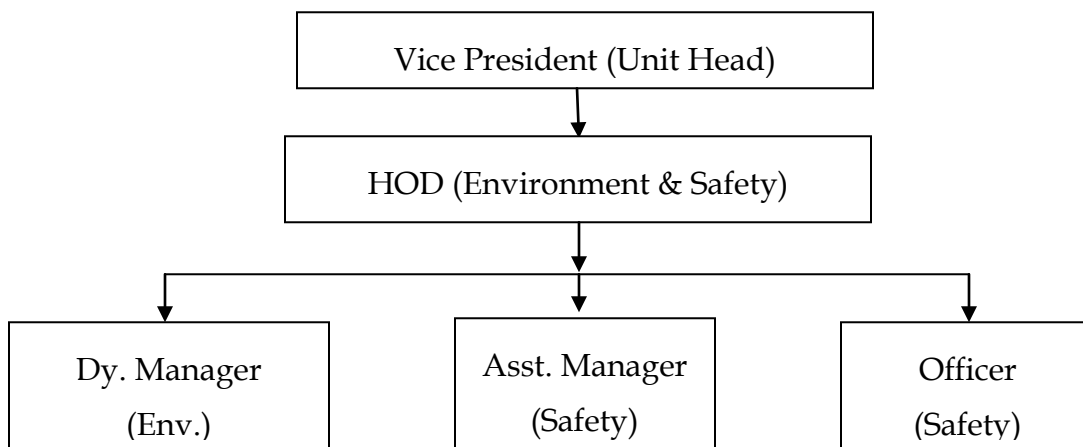
TABLE 4.6: ENVIRONMENTAL MONITORING PLAN &amp; COST

	Item	Parameter	Frequency	Location	Unit cost per sampling & Analysis (Rs)	Samples per year (No)	Cost per year (Rs)
1	Air quality	PM <sub>10</sub> , PM <sub>2.5</sub> , SO <sub>2</sub> , NO <sub>x</sub> , O <sub>3</sub> , Pb, CO, NH <sub>3</sub> , C <sub>6</sub> H <sub>6</sub> , BaP, As, Ni	Monthly	3 locations around periphery of site	6500	36	2,34,000
2	Indoor Air quality	PM <sub>10</sub> , PM <sub>2.5</sub> , SO <sub>2</sub> , NO <sub>2</sub>	Monthly	3 locations	3500	36	1,26,000
3	Ambient Noise	Equivalent Noise Level	Monthly	3 locations around periphery of site	500	36	18,000
4	Exhaust from DG set	SO <sub>2</sub> , SPM	Monthly	Stacks of 1X 250 KVA	2500	12	30,000
5	Boiler emissions	PM, SO <sub>2</sub> , CO, NO <sub>x</sub>	Monthly	1 no 4 TPH	2500	12	30,000
6	Wastewater Analysis	p <sup>H</sup> , BOD, COD, TSS, TDS	Monthly	Process, Washings, Boiler Blow Down, Cooling Towers Blow Down, Scrubbing System, Domestic	2500	12	30,000
<b>Total Cost during Operation per Year</b>							<b>4,68,000</b>



#### 4.5 ENVIRONMENTAL MANAGEMENT CELL

In addition to preparing an EMP, it is also necessary to have a permanent organizational set up to ensure its effective implementation. Hence, M/s. Laureatz Technochem Pvt. Ltd will create a team consisting of officers from various departments to co-ordinate the activities concerned with management and implementation of the environmental control measures. This team undertakes the activity of monitoring the stack emissions, ambient air quality, noise level etc. either departmentally or by appointing external agencies wherever necessary. Regular monitoring of environmental parameters is being carried - out to find out any deterioration in environmental quality and also to take corrective steps, if required, through respective internal departments.



**FIGURE 4.1: ORGANOGRAM OF ENVIRONMENTAL MANAGEMENT CELL**

The cell will also be responsible for monitoring of the plant safety and safety related systems which include:

Checking of safety related operating conditions.

Visual inspection of safety equipment's.

Preparation of a maintenance plan and documentation of maintenance work specifying different maintenance intervals and the type of work to be performed.



**Other responsibilities of the cell will include:**

Conduct and submit annual Environmental Audit. KSPCB registered agency will be retained to generate the data in respect of air, water, noise, soil and meteorological data and prepare the Environmental Audit report. Timely renewal of Consolidated Consents & Authorization (CC & A) will also be taken care of.

Submitting environmental monitoring report to KSPCB. Data monitored by the cell will be submitted to the Board regularly and as per the requirement of KSPCB. The cell will also take mitigative or corrective measures as required or suggested by the Board.

Keeping the management updated on regular basis about the conclusions / results of monitoring activities and proposes measures to improve environment preservation and protection.

Conducting regular safety drills and training programs to educate employees on safety practices. A qualified and experienced safety officer will be responsible for the identification of the hazardous conditions and unsafe acts of workers and advise on corrective actions, organize training programs and provide professional expert advice on various issues related to occupational safety and health.

Conducting safety and health audits to ensure that recommended safety and health measures are followed.



## CHAPTER - 5

## 5.0 PROJECT BENEFITS

## 5.1 PROPOSED BUDGETORY PROVISIONS FOR EMP

Adequate budgetary provisions have been made by management for execution of environmental management plans. The details of total capital and recurring (per annum) for environmental pollution control measures are given in following table.

TABLE 5.1: TOTAL CAPITAL AND RECURRING COST

S. No.	Description	Amount in lakhs	
		Investment cost	Maintenance cost
1	Pollution Control equipment's (Scrubber, Multi Cyclone separators)	35	10
2	Rainwater Harvesting system	5	2
3	Green Belt Development	10	2
4	Occupational health and safety	5	1
5	Storm water drains and fire management	20	2
6	Environmental laboratory	5	0.5
	<b>TOTAL</b>	<b>80</b>	<b>17.5</b>



## 5.2 CORPORATE ENVIRONMENTAL RESPONSIBILITY

In accordance with O.M. F. No. 22-65/2017-IA.III dated 30<sup>th</sup> September 2020 issued by MoEF&CC by suppressing the CER notification dated 1<sup>st</sup> May 2018, Government of India, the industry is willing to allocate amount of Rs. 7 Lakhs in 5 years against each of the activities and the time frame within which such activities will be completed as below.

1 <sup>st</sup> Year	2 <sup>nd</sup> Year	3 <sup>rd</sup> year	4 <sup>th</sup> year	5 <sup>th</sup> year	Total	Proposed CER activities
2 Lakh	2 Lakh	1 Lakh	1 Lakh	1 Lakh	7 Lakhs	<ul style="list-style-type: none"> <li>• Providing sanitation facility to Kudlur government school</li> <li>• Providing drinking water facility to Kudlur Village</li> </ul>

## 5.3 EMPLOYMENT POTENTIAL

The manpower is one of the main resource requirements to operate and maintain the plant in a better and efficient way. Total 55 personnel of working employees will be required in the plant.

## 5.4 FINDINGS

The following findings are to be mentioned:

- The Project will have no significant environmental impacts during operations.
- Project risks will be minimized through rigorous enforcement of international design and operational standards.
- The environmental and safety aspects of the Project are straightforward and well understood.



## 5.5 CONCLUSIONS

The project can cause significant impacts only during construction phase due to the various activities involved during that phase. However, strict adherence to the mitigative measures as identified under the EMP, strengthened by adequate environmental monitoring and auditing and good operating practices, including the special operation methods as prescribed, will go a long way in effectively reducing the impacts as to negligible levels.

During operation phase of the project, none of the routine activities will cause any noticeable impact on any component of the environment, including the socio-economic component. Provision of green belt and rain water harvesting, storm water management shall further facilitate in overall scenario management of Environment.

Thus, it can be concluded on a positive note that after the implementation of the mitigation measures and Environmental Management Plan, the proposed project shall have negligible impact on environment and will benefit the local people and economy.



## CHAPTER 6

## DISCLOSURE OF CONSULTANT

## 6.1 DECLARATION BY CONSULTANT DEVELOPING EMP REPORT

M/s. AM Enviro Engineers, Bengaluru is a prominent provider of environmental consulting to wide range of clients. Our comprehensive range of diversified services includes obtaining environmental clearance from SEIAA/MoEF, CRZ clearance from MoEF, preparation of EIA/EMP and approval/authorization from KSPCB.

TABLE-6.1: DISCLOSURE OF CONSULTANT

<b>Project proponent</b>	<b>M/s. Laureatz Technochem Pvt. Ltd</b>
<b>Project site</b>	New API manufacturing industry at Plot No. 62, Kadachur industrial area, Yadagir Taluk & District, Karnataka.
<b>Type of project</b>	Manufacturing of API
<b>Category of project as per EIA notification</b>	5 (f) of Category-B2, "Synthetic organic chemicals industry"
<b>EIA consultant organization</b>	<b>M/s. AM ENVIRO ENGINEERS Bengaluru</b>
<b>Contact information</b>	No. 14/1, 2 <sup>nd</sup> Floor, HARIKRUPA, Pattalamma Temple Street, Basavanagudi, Bengaluru - 560 004
<b>Status of accreditation with NABET</b>	<b>Certificate No. NABET/EIA/1922/IA0056.</b>



# **PRE-FEASIBILITY REPORT**

*PREPARED FOR*

**“MANUFACTURING OF ACTIVE  
PHARMACEUTICAL INGREDIENTS (API)”**

**AT**

**PLOT NO. 62, KADECHUR INDUSTRIAL AREA, YADAGIR  
TALUK & DISTRICT, KARNATAKA.**

**NEW PROJECT BY**

**M/s. LAUREATZ TECHNOCHEM PVT LTD**

**PLOT NO. 147, SRI SAI NILAYAM, PRAGATHI NAGAR,  
KUKATPALLI, (NEAR JNTU), HYDERABAD, TELANGANA-500090**

*Prepared By*



**AM ENVIRO ENGINEERS**

**[ISO 9001-2015 CERTIFIED COMPANY]**

**(QCI/NABET Accreditation No. NABET/EIA/1922/IA0056)**

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**DOCUMENT NO. AMEE/IND/EMP/49**

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## 1. EXECUTIVE SUMMARY

M/s. Laureatz Technochem Pvt. Ltd has been allotted an area of 2.0 acres by KIADB for “Manufacturing of Active Pharmaceutical Ingredients (API)” at Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District of Karnataka State. The proposed total production capacity of API is of 48 TPM.

**TABLE 1.1: SALIENT FEATURES OF THE PROJECT**

Sl. No.	Description	Details
1.	Name of the project	Manufacturing of Active Pharmaceutical Ingredients (API) by M/s. Laureatz Technochem Pvt. Ltd
2.	Location of the project	Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka State
3.	Total land requirement for the project	8089.8 Sqmt (2 Acres)
4.	Total water requirement & Source	Total water requirement - 135.3 KLD (Fresh water - 83.1 KLD ) Source: KIADB water
5.	Total Power requirement & Source	Power requirement: 500 KVA Source: GESCOM DG: 1X 250 KVA
6.	Rehabilitation and Resettlement	No R & R issue is involved
7.	Manpower	55 no's
8.	Estimated cost of the project	6.6 Crores



## 2. INTRODUCTION OF THE PROJECT/BACKGROUND INFORMATION

### i. Identification of project and project proponent.

M/s. Laureatz Technochem Pvt. Ltd is proposed to establish the API manufacturing unit at Kadechur Industrial Area, Yadagir Taluk & District of Karnataka state with a total capacity of 48 TPM.

#### Details of Project Proponent:

M/s. Laureatz Technochem Pvt. Ltd is a private limited firm and is promoted by Mr. T.V.Srihari and T.Ramani. Mr T.V.Srihari, is a Chemical Engineer and also a Postgraduate in Economics. He has vast experience of over 34 years in the field of Pharma industry by serving major Pharma players like Natco Pharma, SMS Pharma, Lupin group (Concept Labs), TTK Pharma, Neuland Labs, Clinfield India, JBF Industries, Phalanx Labs etc. He is having rich experience in the fields of manufacturing, (exposed to number of drugs synthesis), R&D, process engineering, more than 20 of his inventions were patented, plant design and implementation of various projects from green field to manufacturing. He worked in various management levels like Director in Phalanx Labs, Vice-President (Technical) in SMS Pharmaceuticals Limited, General Manager (Technical) in Natco Pharma Limited, as Senior Manager in JBF Industries limited, middle management level Lupin group (Concept Laboratories), TTK Pharma, Clinfields India Limited, Neuland Laboratories Ltd. etc. He participated in various global pharmaceutical meets, exhibitions and international Green chemistry seminars. He is a member of green chemistry organization.

Mrs. Ramani Tadimalla, aged about 57 years is a Graduate in arts from Andhra University. Mrs. Ramani is an expert in deploying the best of the leadership practices with Results Based Measurement being the core theme. Played an effective role as Strategy Expert; as the prime negotiator with all the stakeholders. Mrs. Ramani brings in 15+ years of experience as a Strategy Specialist. She learned the ethics and techniques to promote her own firm.



**ii. Brief description of nature of the project**

Drug discovery for therapeutic use to improve the human health is a fast changing field. To keep pace with international developments, Indian pharmaceutical industry needs to constantly upgrade their product portfolio and production volumes. Under similar circumstances, M/s. Laureatz Technochem Pvt. Ltd proposed for manufacturing of Active pharmaceutical ingredients. The project area comes under notified Industrial Area. Hence the project falls under item no-5(f) of schedule to EIA notification, dated 14th September 2006.

**iii. Need for the project and its importance to the country or region**

The drugs demand in India is increasing due to rapid growth of population. The requirement addition at the present rate will not be able to meet the projected demand and would result in a large drug deficit. To mitigate the gap between demands and supply Govt. of India is facilitating large scale capacity additions at shorter time through public and private investments. India with its large talented manpower, cost effective chemical synthesis, legal & financial framework is poised to become sourcing destination of bulk drugs to the global market.

**iv. Demand and supply gap**

Over the years, the production of bulk drug has made significant progress. The drug & pharmaceutical industry in India meets around 70% of the country's demand for bulk drugs, pharmaceutical formulations, chemicals, tablets, capsules, orals and injectibles. There are about 250 large Pharmaceuticals manufacturers and suppliers and about 8000 Small Scale Pharmaceutical & Drug Units which form the core of the pharmaceutical industry in India (including 5 Central Public Sector Units). These bulk drugs and pharmaceuticals manufacturers produce the complete range of pharmaceutical formulations i.e. medicines ready for consumption by patients and about 350 bulk drugs i.e. chemicals having therapeutic value and used for production of pharmaceutical formulations. (Source: pharmaceutical-india.com)



**v. Imports v/s. Indigenous production**

Today, the pharmaceutical industry manufactures the entire range of therapeutic products and is capable of producing raw materials for the manufacture of a wide range of drugs from the basic stage as well as a range of pharmaceutical machinery and equipment. Apart from building up domestic capacity, leading Indian companies have established marketing and manufacturing activities in a large number of countries including USA and countries of Europe as well as expanded through acquisitions in these countries. The sector has therefore evolved from being dominated by multinational companies in the 1950's to some imports and indigenous manufacturing in the 1970's and then protected by the legislative provisions of the older Patents Act 1970, to significant indigenous production and subsequent exports. The Act of 1970 excluded product patents on pharmaceuticals, allowing the mushrooming of a vigorous generics industry in India which could meet not only domestic demand for drugs at lower prices but could also export cheaper drugs to other Third World countries. Further, the government policies restricted imports of finished formulations, imposed high tariff rates and introduced strict price control regulation through the 1970 Drugs Price Control Order. The multi-national companies are now looking at India not only for its traditional strengths in manufacturing but also as a highly attractive location for research and development (R&D), particularly in the conduct of clinical trials and other services. The consumption potential offered by more than one billion inhabitants, rising affluent customers and the changing lifestyles offer huge potential domestically for the sector. Currently, the Indian pharmaceutical industry is one of the world's largest and most developed, ranking 4th in volume terms and 13th in value terms. The country accounted for 8 percent of global production and 2 percent of world markets in pharmaceuticals. Most of the domestic pharmaceutical drug requirements are met by the domestic industry. In the segment of Active Pharmaceutical Ingredients (APIs) India ranks third in the world producing about 500 different APIs. (Source: Pharmexcil.org)

**vi . Export Possibility**

The company has no plans to export its products outside the country. All the products produced are requirement of domestic market.

**vii. Domestic/ Export Markets**

Over 60 per cent of India's bulk drug production is exported. India's pharmaceutical exports are to the tune of Rs 87 billion, of which formulations contribute nearly 55 per cent and the rest 45 per cent comes from bulk drugs.

**viii. Employment generation (direct and indirect) due to the project**

M/s. Laureatz Technochem Pvt. Ltd has planned to have employees about 55 no's to operate the unit.



### 3. PROJECT DESCRIPTION

**i. Type of project including interlinked and interdependent project if any**

To cater the needs of the market, M/s. Laureatz Technochem Pvt. Ltd has proposed to establish Active Pharmaceutical Ingredients (API) manufacturing unit at Plot No. 62, Kadachur Industrial area, Yadagir Taluk & District, Karnataka.

There are no interlinked or interdependent projects.

**ii. Location (map showing general location, specific location, and project boundary & Project site layout) with coordinates**

The project site is located at Kadachur Industrial area, Yadagir Taluk & District, Karnataka State. The project site co-ordinates ranges from Latitude - 16.516923° to 16.517494° and Longitude- 77.313713° to 77.314952°. The location map showing is as shown below.



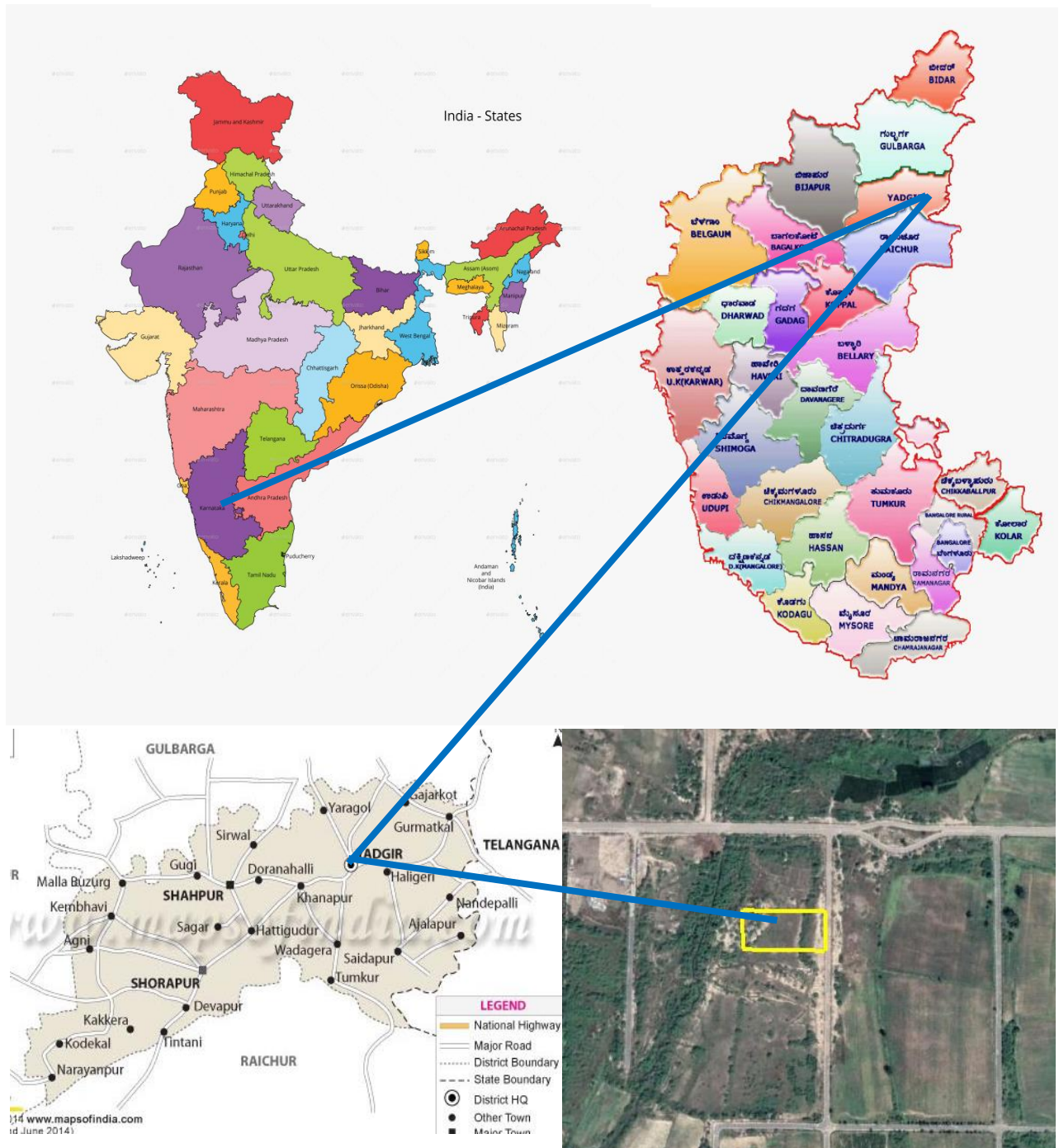


FIGURE 3.1: LOCATION MAP

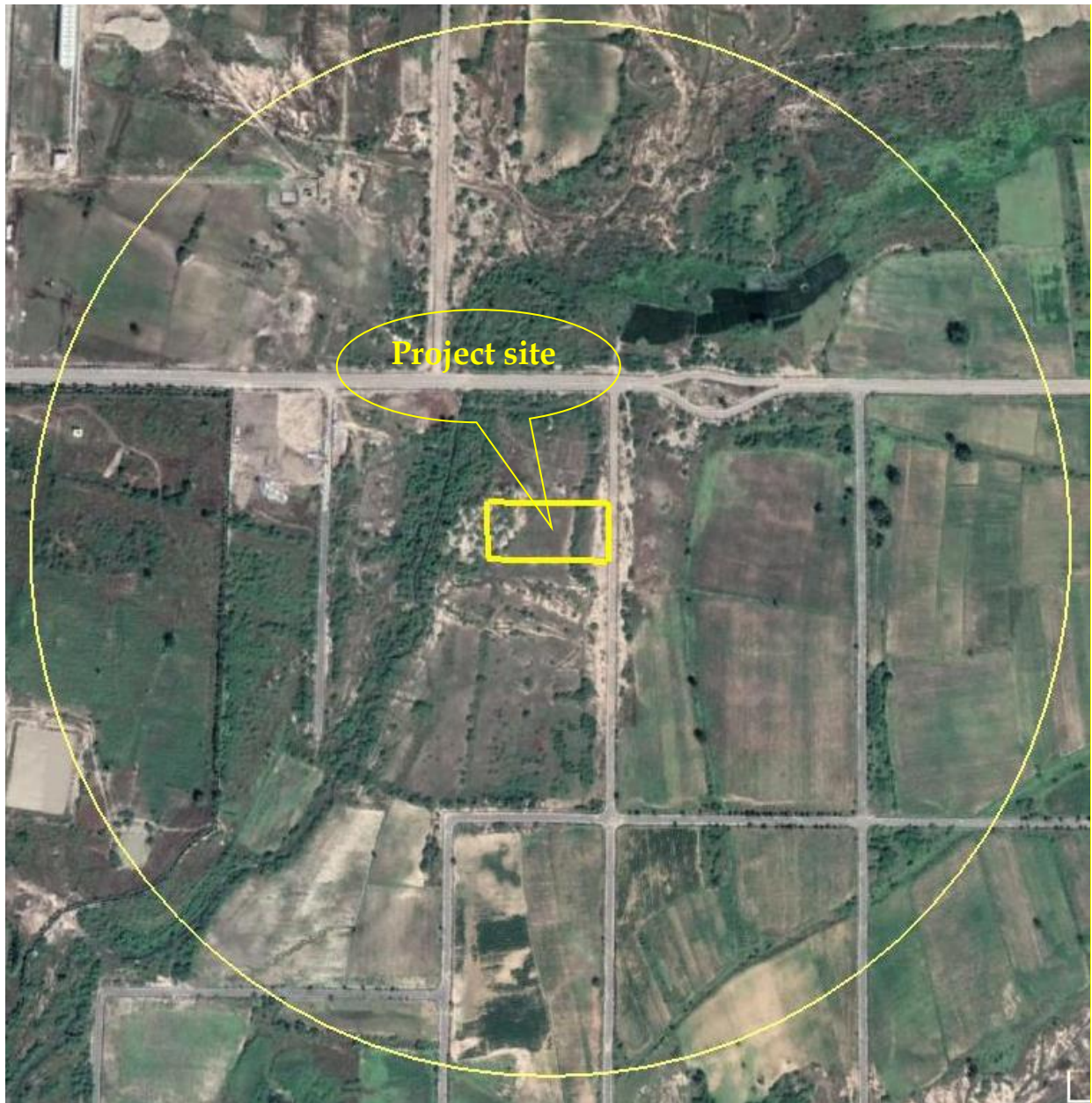


FIGURE: 3.2 GOOGLE IMAGE SHOWING 500 M RADIUS FROM THE PROJECT SITE

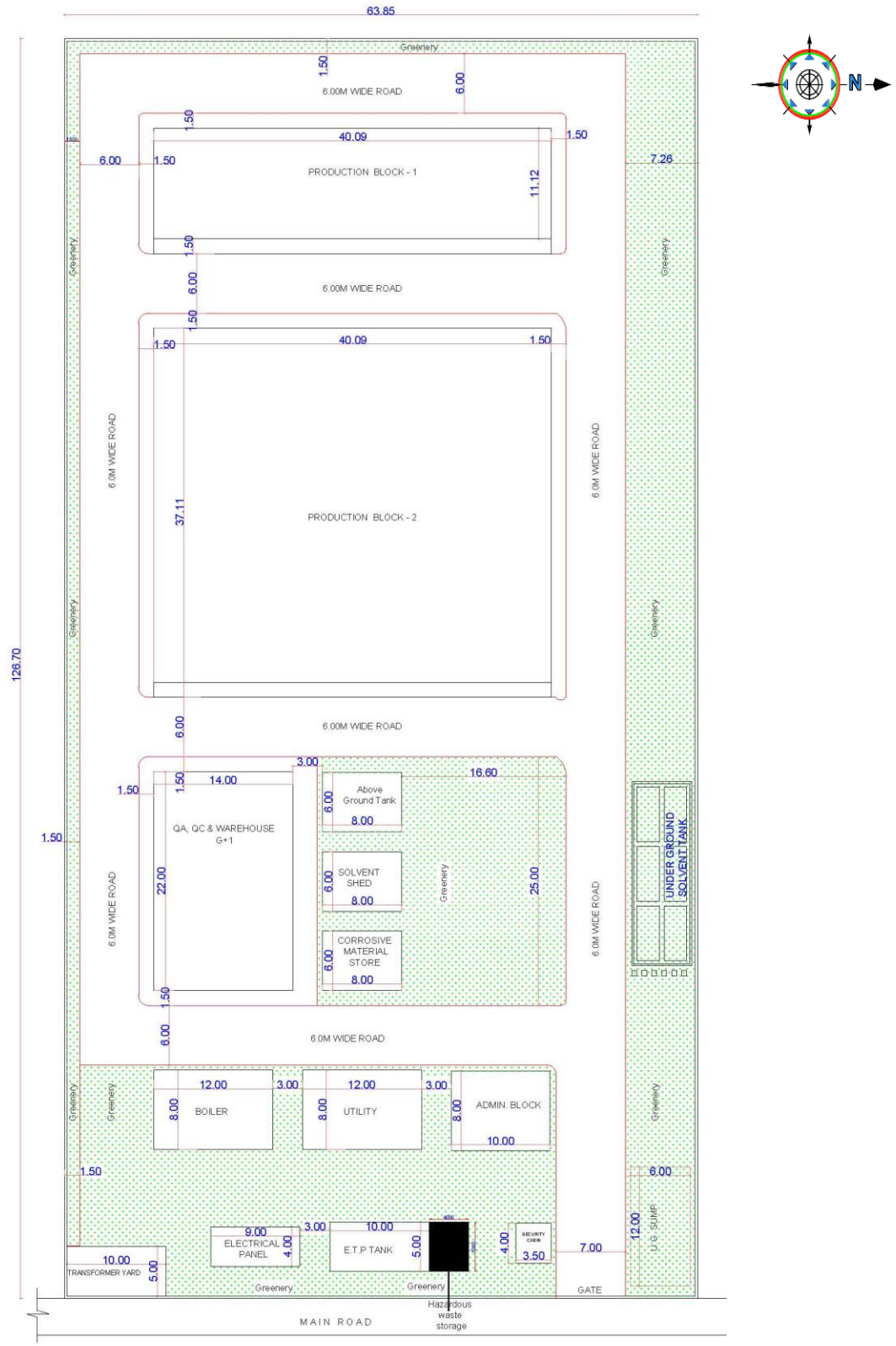


FIGURE: 3.3 LAYOUT PLAN OF THE PROJECT SITE

**iii. Details of alternate sites considered and the basis of selecting the proposed site, particularly the environmental considerations gone into should be highlighted**

There is no any alternate site as the proposed site is acquired.

Since the project is located in Kadechur Industrial area, Yadagir Taluk & District, Karnataka and the site has distinct advantages such as accessibility to road, electricity and water supply. The following factors which influence the site selection have been very favourable to select this site.

- The plant site is located within the Industrial Estate.
- Land requirement for the proposed project is 2 acres which is in notified KIADB Industrial area
- Topographically, the area is generally plain.
- The area is not covered by any notified forests.
- No clearance of existing land & vegetation.
- Proximity of National Highways and railways station, Transport of raw materials and manufactured drugs.

**TABLE 3.1: DETAILS OF ENVIRONMENTAL SETTINGS**

Particulars	Details		
	Corners	Latitude	Longitude
Plant site co-ordinates (Latitude & Longitude)	A	16°31'2.95"N	77°18'49.37"E
	B	16°31'0.98"N	77°18'49.39"E
	C	16°31'0.93"N	77°18'53.80"E
	D	16°31'2.90"N	77°18'53.83"E
Temperature	Max. 42°C, Min. 26°C		
Present land-use	KIADB land (Industrial area)		
Average rainfall	850 mm per year		
Nearest Highway	NH-167 (Yadgir - Raichur Road) - 1 km (SW)		
Nearest Railway station	Chegunta Railway Station - 3.7 km (SW)		
Nearest Airport	Rajiv Gandhi International Airport, Shamshabad -140.9 Km (NE)		



Nearest Water body	Seasonal Nala - 50 m (W) Kadechur lake - 1.5 km (NE) Bhima river - 8.7 km (SW) Krishna river - 12.3 km (SW)
Nearest Village	Kadechur - 1.2 Km (E) Shattihalli - 2.5 km (NW)
Nearest Town/City	Yadgir city - 33.6 Km (NW)
Seismic Zone	Seismic zone-II as per IS-1893 (Part-1) - 2002
Interstate boundary	Karnataka - Telangana Interstate Boundary - 2.64 Km (S)

#### iv. Size or magnitude of operation

The total production capacity from the proposed project is 48 TPM. The list of the proposed products is given in below table.

**TABLE 3.2: LIST OF PROPOSED PRODUCTS WITH CAPACITY**

S. No	Name of Products	Qty. in TPM	CAS No.	Therapeutic Use
1.	Adefovir	2	142340-99-6	To treat chronic (long-term) hepatitis B infection
2.	Bortezomib	1	179324-69-7	Multiple myeloma
3.	Capecitabine	5	154361-50-9	Anti-Cancer
4.	Clopidogrel Bisulphate	5	120202-66-6	Cardiovascular
5.	Dapagliflozin	2	461432-26-8	Anti-diabetic
6.	Dapoxetine Hydrochloride	2	129938-20-1	Inhibitor
7.	Darunavir Ethanolate	3	635728-49-3	Antiviral
8.	Empagliflozin	2	864070-44-0	Anti-diabetic
9.	Etodolac	1	41340-25-4	Anti-inflammatory
10.	Etoricoxib	15	202409-33-4	Anti-inflammatory
11.	Famotidine	3	76824-35-6	To treat gastritis
12.	Imatinib Mesylate	1	152459-95-5	Anti-Cancer
13.	Irinotecan HCl	1	136-572-09-3	Topoisomerase I inhibitors
14.	Ivabradine HCl	2	148849-67-6	To treat heart disease
15.	Lenalidomide	1	191732-72-6	To treat anemia
16.	Linezolid	5	165800-03-3	Antibiotic
17.	Mesalamine	10	89-57-6	Ulcerative colitis



18.	Olmesartan Medoximil	1	144689-63-4	Anti-hypertension
19.	Pantoprazole Sodium	8	138786-67-1	To treat gastritis
20.	Piroctone Olamine	5	68890-66-4	Antifungal
21.	Ramipril	5	87333-19-5	To treat high blood pressure
22.	Risperidone	2	106266-06-2	Schizophrenia
23.	Sacubitril	2	149709-62-6	Chronic heart failure and reduced ejection fraction
24.	Sparfloxacin	5	110871-86-8	Antibiotic
25.	Tadalafil	5	171596-29-5	To treat erection problems
26.	Tamsulosin hydrochloride	1	106463-17-6	To treat Benign Prostatic Hyperplasia (BPH)
27.	Telmisartan	5	144701-48-4	Anti-hypertensive
28.	Thalidomide	1	50-35-1	To treat a skin condition and cancer
29.	Triclabendazole	3	68786-66-3	Anthelmintics
30.	Zoledronic acid	1	165800-06-6	To treat high levels of calcium
	<b>Total (6 products)</b>	<b>48</b>		

**Note:** From the above list of products, any 6 products will be manufactured at a given point of time.

**TABLE 3.3: LIST OF PROPOSED BY-PRODUCTS**

S.No	Name of the Product	Name of the By Product	Quantity in Kgs/Day
1	Capecitabine	Peridine Hydrochloride	59.69
2	Famotidine	Potassium chloride	53.14
3	Piroctone Olamine	Aluminium hydroxide solution	1452.5
4	Pantoprazole Sodium	Potassium Sulphate	60
		Ammonium Phosphate	35
		Sodium Acetate	110
		Ammonium Chloride	72.25
5	Telmisartan	Sodium phosphate	251

The process description for the proposed products along with route of synthesis, flow diagram, material balances are attached as ANNEXURE - 3.

- v. Raw material required along with estimated quantity likely source marketing area of final product/s, mode of transport of raw material and

**finished product**

The list of raw materials along with quantities is attached as ANNEXURE -4. The raw materials will be sourced from local market and also from the different suppliers across the world. The raw materials and finished products will be transported through road.

**vii. Resource optimization/recycling and reuse envisaged in the project if any should be briefly outlined**

After the reaction is complete the solvents are recovered in a distillation unit. The residue from the distillation unit is collected in a container and sent for co-processing. The recovered solvents are collected in drums, labelled and analysed. Then they are reused (recycled) for the process.

In the proposed project, conservation has adequately addressed and hence, water consumption is optimized. All process effluent and domestic sewage will be sent to CETP.

**viii. Availability of water its source, energy/power requirement and source should be given.**

**TABLE 3.4: WATER CONSUMPTION & EFFLUENT GENERATION WITH TREATMENT MECHANISM**

Sl. No.	Purpose	Fresh Water (KLD)	Recycled water (KLD)	Total Water requirement (KLD)	Effluent generation (KLD)	Treatment method
1	Process	51.1	-	51.1	36.7	Sent to CETP, Kadechur
2	Scrubbing	3	-	3	3	
3	RO reject	-	-	-	15.3	
4	Boiler	23.5	-	23.5	3.4	
5	Cooling tower	-	41.5	41.5	4.1	
6	Washing	3	-	3	3	
7	Domestic Usage	2.5	-	2.5	2.1	Septic tank followed by multigrade filter
8	Gardening	-	10.7	10.7	-	-
<b>Total</b>		<b>83.1</b>	<b>52.2</b>	<b>135.3</b>	<b>67.6</b>	



The total fresh water demand for proposed project is 83.1 KLD, which is met by KIADB. Power demand is 500 KVA which is met by GESCOM.

**ix. Quantity of wastes to be generated (liquid & solid) and scheme for their management/disposal**

The various types of waste from different units of the proposed plant are described underneath:

**a) Liquid Waste:**

All the products require water during the process. The wastewater generated from the plant is 67.6 KLD and will be sent to CETP.

**TABLE 3.5: EFFLUENT DETAILS**

S. NO	Unit	HTDS (KLD)	LTDS (KLD)	Waste water Generation in KLD	Treatment Method
1	Process	34.1	2.6	36.7	Sent to CETP, Kadechur
2	Washings	-	3	3	
3	Boiler Blow Down	-	3.4	3.4	
4	Cooling towers Blow Down	-	4.1	4.1	
5	Scrubber System	3	-	3	
6	RO reject	-	15.3	15.3	
7	Domestic	-	2.1	2.1	Septic tank followed by multigrade filter
	<b>Total</b>	<b>37.1</b>	<b>30.5</b>	<b>67.6</b>	-

**b) Solid Waste Generation & Utilization and Disposal**

The details of solid and hazardous waste generated along with the mode of disposal is detailed in below table.

TABLE 3.6: HAZARDOUS &amp; SOLID WASTE DETAILS

S. No	Category of the HW	Name of the Hazardous Waste	Quantity	Disposal Method
<b>Hazardous waste generation from plant</b>				
1	5.1	Waste oils & Grease/ Used Mineral oil	0.2 KL/Annum	Agencies authorized by KSPCB
2	5.2	Oil Soaked Cotton	2 Kgs/month	KSPCB authorized Vendor
3	20.3	Distillation Residue	830 kgs/ day	Store in secured manner and hand over to authorized cement industry for Co-processing
4	28.1	Process Residues & Waste	2764 Kgs/ day	Store in secured manner and hand over to authorized cement industry for Co-processing/TSDF
5	28.2	Spent Catalyst	7.3 kgs/ day	Store in secured manner and hand over to authorized recycler
6	28.3	Spent Carbon + Hyflow	188 Kgs/Day	Store in secured manner and hand over to authorized cement industry for Co-processing
7	28.4	Off Specification Products	1 TPM	Store in secured manner and hand over to authorized cement industry for Co-processing/TSDF
8	28.5	Date expired products	500 Kgs/Month	Store in secured manner and hand over to authorized cement kiln for Co-processing/ TSDF
9	33.1	Detoxified- Container & Container Liners of Hazardous Chemicals and Wastes	250 No's/Month	After complete detoxification, shall be disposed to the outside agencies.
10	33.2	Contaminated cotton rags or other cleaning materials	25 Kgs/month	Store in secured manner and hand over to KSPCB Authorized Vendor
11	A1160	Used Lead Acid batteries	2 No's/Annum	Returned back to dealer/ Supplier



Other & Miscellaneous Solid Wastes				
12	--	Coal ash	1120 kgs/day	Sent to Brick Manufacturers
13	--	Briquette ash	2860 kgs/day	Sent to fertilizer industries
14	--	Residues from Scrubber	143 kg/day	Shall be stored in secured manner & handed over to TSDF.
15	--	Used PPE	5 Kgs/ Month	Sent to authorized vendor
16	--	E- Waste	150 Kgs/ Annum	Authorized recyclers
17	--	Plastic Waste	200 Kgs/ Annum	Authorized recyclers
18	--	Metal Scrap	3 TPA	Sale to outside agencies/ recyclers
19	--	Used Filters (HEPA filters, Oil Filters etc.)	25 Nos /year	Sent to TSDF
20	--	Used / Discarded RO Membranes	0.2 TPA	Sent to TSDF

TABLE 3.7: PROCESS EMISSION DETAILS

S. No	Name of the Gas	Quantity in Kg/Day	Treatment Method	Disposal Method
1	Hydrogen chloride	609.7	Scrubbed by using water media	Generated Dil. HCl will be reused within the industry
2	Ammonia	27.5		Generated NH <sub>4</sub> OH will be reused within the industry
3	Sulphur dioxide	80.1	Scrubbed by using C.S. Lye solution	Residues from the reaction will be sent to TSDF
4	Hydrogen Bromide	21.3		
5	Hydrogen Fluoride	3.3		
6	Hydrogen Iodide	19.9		
7	Pentane	9.2	Dispersed into atmosphere	-
8	Oxygen	104.8		
9	Carbon dioxide	259.2		
10	Hydrogen	20.2	Dispersed into atmosphere through flame arrester	-



TABLE 3.8: STACK EMISSION DETAILS FOR PROPOSED BOILERS

Particulars	Units	4.0 TPH Boiler	
		Briquettes	Coal
Type of Fuel	--	Briquettes	Coal
Coal Consumption	TPD	11	8
Ash Content	%	26	14
Sulphur Content	%	0.002	1.5
No. of Stacks	No	1	
Height of stack	M	30	
Diameter of Stack	M	0.3	
Temperature of Flue Gas	°C	120	
Velocity of Flue Gas	m/s	9.5	
Emission Details			
Particulate Matter as PM	gm/sec	5.5	3.3
Sulphur dioxide as SO <sub>2</sub>	gm/sec	0.004	0.9
Oxides of Nitrogen as NO <sub>x</sub>	gm/sec	0.006	0.7
Pollution Control Details			
Pollution control equipment	Multi Cyclone separator		

TABLE 3.9: STACK EMISSION DETAILS FOR PROPOSED DG SETS

Capacity in KVA	Emission of PM in gm/sec	Emission of SO <sub>2</sub> in gm/sec	Emission of NO <sub>x</sub> in gm/sec	Stack dia. in m	Flue Gas Temp. in °C	Stack Height in (m)	Flue gas Velocity in m/sec
250 KVA	0.014	0.11	0.48	0.3	140	4m AGL	14

TABLE 3.10: STACK EMISSION DETAILS FOR THERMIC FLUID HEATER

Particulars	Units	Thermic fluid heater	
		Coal	Briquette
Thermo pack Boiler Capacity	Kcal/hr.	2,00,000	
Type of Fuel	--	Coal	Briquette
Fuel Consumption per Day	TPD	2	3
Stack Temperature	°C	190	192
Velocity	m/sec	5.3	5.3
Stack Height	m	15	15
Stack Diameter	m	0.2	0.2
Ash content	%	0.14	0.26
Sulphur Content	%	1.5	0.002
Emission of PM	gm/ sec	0.8	1.4
Emission of SO <sub>2</sub>	gm/ sec	0.2	0.001
Emission of NO <sub>x</sub>	gm/ sec	0.2	0.002



**x. Schematic representations of the feasibility drawing which give information of EIA purpose**

Ministry of Environment, Forest and Climate Change categorized active pharmaceutical ingredients manufacturing units as 'B2' for a period up to 30<sup>th</sup> March 2021 as per the notification dated 27<sup>th</sup> March 2020 and OM dated 15<sup>th</sup> Oct 2020, as an interim measure to handle the Novel Corona Virus (COVID-19) outbreak. In this context, EIA study has been excepted and Environmental management plan has been prepared.



#### 4. SITE ANALYSIS

**(i) Connectivity:**

The plant site is well connected by road to the major national and state highway network. The approach road to the site would have to be suitably laid by making it a two-lane road suitable for movement of heavy loads involved including the construction materials.

The Project site is close to Yadagir Raichur road which is at a distance of 1 km towards South - West side and the nearest railway station is Chegunta railway station at 3.7 km towards SW. The nearest airport is Rajiv Gandhi International Airport located at a distance of 140.9 km from the site towards North East.

**(ii) Land Form, Land use and Land ownership:**

M/s. Laureatz Technochem Pvt. Ltd acquired 2 acres of land at KIADB notified industrial area.

**(iii) Topography (along with map):**

Topographically, the site is plain and devoid of rocky outcrops and does not have any forests. No significant cutting or filling activities are required for land development activities. Entire site area is under industrial occupation and no cultivation land exists. No clearance of existing land, vegetation or buildings is involved. The project site is located at the Northern part of Karnataka. The elevation in the project site is 363 meter above mean sea level. An area covering 10 km radius, with project site as centre, topo sheet has been prepared and shown subsequently.



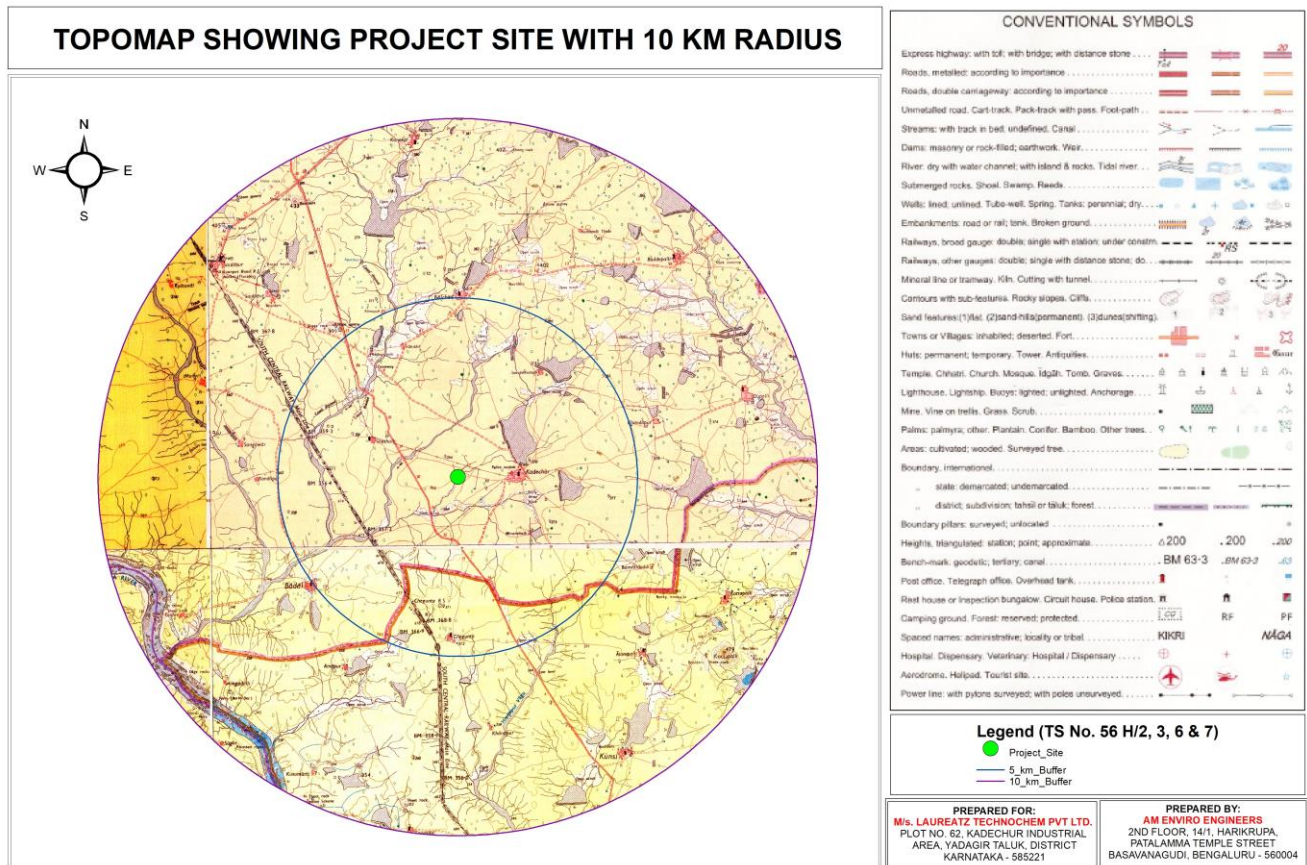


FIGURE: 4.1 TOPOMAP COVERING 5 KM & 10 KM RADIUS FROM THE PROJECT SITE

(iv) Existing land use pattern (agriculture, non-agriculture, forest, water bodies (including area under CRZ)), shortest distances from the periphery of the project to periphery of the forests, national park, wild life sanctuary, eco sensitive areas, water bodies (distance from the HFL of the river), CRZ, In case of notified industrial area, a copy of the gazette:

The district is bounded by Gulbarga district in the north, Bijapur district in west, Raichur district in south and Telangana in the east. The existing land use patter is industrial and the project site is in the KIADB notified industrial area. There are no reserved forests, national parks, wild life sanctuary and CRZ regions within 10 km radius. There is no HFL from the periphery of the project site. There are no eco-sensitive locations within 10 Km from the site.

**(v) Existing Infrastructure:**

There is no existing infrastructure and utilities in the proposed project site.

**(vi) Soil Classification:**

Soils: The vast stretch of fertile black soil of the district is known for bumper red gram and jowar Crops and the district is also referred to as the “Daal bowl” of the state. The soil types in the taluk are deep black, medium black soil, shallow soil and lateritic soil. The thickness of deep & medium black soil varies from 0.5 to 3.6 m. Infiltration rate of shallow, medium and deep black soil is moderate to poor. Infiltration rate of medium black soil recorded in the district is 2.5 cm/hr.

**(vii) Climatic data from secondary sources:**

Climatic Conditions of the site based on IMD, Bangalore are as followed: Average

Annual Maximum Temperature: 42°C

Average Annual minimum Temperature: 26°C

Average Annual Rainfall: 850 mm

**(viii) Social Infrastructure available**

For transportation, the project site is well connected to Raichur-Yadgir road at a distance of 1 km towards South West side & Chenguta railway station at a distance of 3.7 km. The nearest village is Kadechur at a distance of 1.2 km. Other basic infrastructures like primary, secondary and higher schools, colleges, Community and primary health care centres banks, temples, are located at Yadgir district which is at 33.6 km from the project site.

The impact of human settlement is expected to be positive, as apart from some people being directly employed, many others will get indirect employment.



## 5. PLANNING BRIEF

### i. Planning concept (type of industries, facilities, transportation etc) Town and Country Planning/Development authority Classification:

The proposed API manufacturing unit is located within the Kadechur Industrial Area, Yadagir Taluk & district of Karnataka State. The proposed site is earmarked by KIADB. No buildings or infrastructure is existing in proposed land. There is internal KAIDB road which is approach road to the project site. Approval from appropriate competent authority will be obtained.

### ii. Population Projection:

Not applicable.

### iii. Land use planning (breakup along with green belt etc):

TABLE 5.1: LANDUSE DETAILS

Sl no	Description	Area (Sqmt)	Area in percentage (%)
1	Ground coverage area	2725.5	33.7
2	Green belt area	2694.3	33.3
3	Roads Area	2670.0	33.0
	<b>Total</b>	<b>8089.8</b>	<b>100</b>

### iv. Assessment of Infrastructure Demand (Physical & Social): Service Buildings

M/s. Laureatz Technochem Pvt. Ltd proposed to establish API manufacturing unit at Kadechur industrial area, Yadgir Taluk and District. The project facility includes building blocks of production, raw material storage, office building and finished product storage area and other facilities. The project is proposed at KIADB industrial area which is developed in terms of roads and electricity supply. There is water source available to the project from the nearby Bhima river.

### v. Roads

Approach road to project site is formed.

### vi. Amenities/Facilities:

M/s. Laureatz Technochem Pvt. Ltd proposed to establish API manufacturing unit at Kadachur industrial area, Yadgir Taluk and District. The project facility includes building blocks of production, raw material storage, office building and finished product storage area and other facilities.

## 6. PROPOSED INFRASTRUCTURE

- i. **Industrial Area:** The proposed project is manufacturing of API and will take place in KIADB Industrial area.
- ii. **Residential Area:** NA.
- iii. **Greenbelt:** 2694.3 Sqmt (33.3%)
- iv. **Social Infrastructure:** Necessary support infrastructure will be provided as per the requirement of the project.
- v. **Connectivity:** Project site is well connected by an asphalted road and near National highway NH-167 (Raichur-Yadagir Road) just 1 km (SW) away from the Factory entrance.
- vi. **Drinking Water Management:** The water demand is met from KIADB (Karnataka Industrial Areas Development Board). The requirement of water for the unit is for domestic, industrial purposes and landscape development.
- vii. **Sewerage system:** The wastewater generated from Boiler blow down, cooling tower blow down and domestic sewage will be sent to CETP.
- viii. **Industrial waste management:**
  - a. **Air Environment:**

The major air pollution sources from the industry are DG sets, boilers, scrubber stack connected to process sections. These sources will be provided with control systems with stacks of adequate height so as to disperse the emanating flue gases containing SPM, oxides of sulfur, nitrogen and process emissions free from acid/alkali and Volatile organic carbons without affecting the ground level concentrations and also dedicated scrubbers will be provided exclusively to the process section with adequate stack height



as per the regulatory requirements.

**i. Sources:**

Boilers: The industry is proposing for Briquettes/Coal fired Boilers of capacity 1 X 4TPH.

D.G. sets: Diesel generator of 1X250 KVA capacity will be installed to serve as an alternative source of power supply to this unit.

**ii. Mitigative measures:**

1. Process emission will be connected to scrubber with a stack attached.
2. The vapours will be collected through exhaust system consisting of hood, duct and vacuum fan and then vented out.
3. Stack will be provided to D.G. sets.
4. Boilers are connected with multi cyclone separator.
5. Plantation of green trees around the factory building and premises to control the intensity of noise to the surrounding area.
6. Use of PPE's

**b. Noise Environment:**

**i. Sources:**

Generators, Reactors, Compressors, Fans

**ii. Mitigative measures:**

1. Acoustic barriers or shields to the machineries.
2. Vibration free foundations for machineries
3. Acoustical walls and roofs to the building where such machineries are installed.
4. Segregation of machineries having high noise level in isolated buildings.
5. Sound control measures to steam vents.
6. Proper maintenance of machineries especially oiling and greasing of bearing and gears etc.
7. Avoiding vibration of machineries with proper design of machineries such as speed, balancing etc.

8. Use of personnel protective such as ear muff and ear plugs for persons working in such locations.
9. Plantation of green trees around the factory building and premises to control the intensity of noise to the surrounding area.

**c. Water Environment:** The water demand is met from KIADB (Karnataka Industrial Areas Development Board). The requirement of water for the unit is for domestic, industrial purposes and landscape development. The total fresh water requirement for the industry is 83.1 KLD.

**i. Sources:**

- Process water
- Cooling tower blow down
- Floor wash
- Boiler blow down

**ii. Mitigative measures:**

1. Rain water harvesting plan will be executed effectively & a storage reservoir of adequate capacity will be provided to hold rainwater.
2. Recycle of process water including steam condensate.
3. Control of water taps, washings, leakages from pump glands and flanged joints.
4. Floor cleaning with water will be replaced with dry cleaning.

**d. Hazardous waste management:**

**i. Sources:**

Used oil, Spent carbon, Polythene bags, Used fiber drums, etc.

**ii. Mitigative measures:**

1. Used oil shall be collected in leak proof containers & disposed to Central Pollution Control Board / Karnataka State Pollution Control Board registered authorized recyclers.
2. The solid from the bottom of the neutralization tank will have a selling potentiality. In such case, this solid will be sold to the parties who have a license from



handling the same, other waste will be sent to TSDF.

3. The boiler ash will be given to the brick manufactures by which we can be sure of safe disposal system.
- ix. **Solid waste management:** Oil soaked cotton wastes, discarded containers, etc are the solid wastes generated and it will be stored in secured manner & handed over to the Karnataka State Pollution Control Board authorized recyclers.
  - x. **Power Requirements and Supply and Source:** The total power requirement of the proposed plant is about 500 KVA, which will be met from GESCOM.

## 7. REHABILITATION & RESETTLEMENT (R & R) PLAN

There is no human settlement or structures at the project site. Thus no R & R issue is involved.

## 8. PROJECT SCHEDULE AND COST ESTIMATE

- i. **Likely date of start of construction and likely date of completion (Time schedule for the project to be given)**

The industry will take necessary approvals from the consented authority and start the construction immediately after obtaining Environmental Clearance and Consent For Establishment.

**TABLE 8.1: TIME FRAME FOR COMPLETION OF THE PROJECT**

Details of work	Aug 2021 to July 2022	Dec 2021 to April 2022
Building and construction work	12 months	
Erection of reactors and service facilities		12 months
<b>Total</b>	<b>24 months</b>	

- ii. **Estimated project cost along with analysis in terms of economic viability of the project.**

The overall project cost for the proposed API manufacturing unit is 6.6 Crores. The

breakup is given below.

**TABLE 8.2: BREAKUP OF THE PROJECT COST**

<b>Particulars</b>	<b>Amount (Rs. Crores)</b>
Land	1.39
Building, civil work	2.60
Plant & Machinery -Mechanical, Utilities, etc.	1.86
Furniture, Fixtures and other assets	0.40
Preliminary Preoperative	0.15
Miscellaneous	0.20
<b>Total</b>	<b>6.60</b>

## 9. ANALYSIS OF PROPOSAL

- i. **Financial and social benefits with special emphasis on the benefit to the local people including tribal population, if any, in the area**

The proposal will bring employment opportunities. It will also bring trade opportunities to the country.



# **ANNEXURE-1**

## **LIST OF PROPOSED PRODUCTS** **AND BY PRODUCTS**

**ANNEXURE-1**

**LIST OF PROPOSED PRODUCTS WITH CAPACITY**

<b>S. No</b>	<b>Name of Products</b>	<b>Qty. in TPM</b>	<b>CAS No.</b>	<b>Therapeutic Use</b>
1.	Adefovir	2	142340-99-6	To treat chronic (long-term) hepatitis B infection
2.	Bortezomib	1	179324-69-7	Multiple myeloma
3.	Capecitabine	5	154361-50-9	Anti-Cancer
4.	Clopidogrel Bisulphate	5	120202-66-6	Cardiovascular
5.	Dapagliflozin	2	461432-26-8	Anti-diabetic
6.	Dapoxetine Hydrochloride	2	129938-20-1	Inhibitor
7.	Darunavir Ethanolate	3	635728-49-3	Antiviral
8.	Empagliflozin	2	864070-44-0	Anti-diabetic
9.	Etodolac	1	41340-25-4	Anti-inflammatory
10.	Etoricoxib	15	202409-33-4	Anti-inflammatory
11.	Famotidine	3	76824-35-6	To treat gastritis
12.	Imatinib Mesylate	1	152459-95-5	Anti-Cancer
13.	Irinotecan HCl	1	136-572-09-3	Topoisomerase I inhibitors
14.	Ivabradine HCl	2	148849-67-6	To treat heart disease
15.	Lenalidomide	1	191732-72-6	To treat anemia
16.	Linezolid	5	165800-03-3	Antibiotic
17.	Mesalamine	10	89-57-6	Ulcerative colitis
18.	Olmesartan Medoximil	1	144689-63-4	Anti-hypertension
19.	Pantoprazole Sodium	8	138786-67-1	To treat gastritis
20.	Piroctone Olamine	5	68890-66-4	Antifungal
21.	Ramipril	5	87333-19-5	To treat high blood pressure
22.	Risperidone	2	106266-06-2	Schizophrenia
23.	Sacubitril	2	149709-62-6	Chronic heart failure and reduced ejection fraction
24.	Sparfloxacin	5	110871-86-8	Antibiotic
25.	Tadalafil	5	171596-29-5	To treat erection problems
26.	Tamsulosin hydrochloride	1	106463-17-6	To treat Benign Prostatic Hyperplasia (BPH)
27.	Telmisartan	5	144701-48-4	Anti-hypertensive

28.	Thalidomide	1	50-35-1	To treat a skin condition and cancer
29.	Triclabendazole	3	68786-66-3	Anthelmintics
30.	Zoledronic acid	1	165800-06-6	To treat high levels of calcium
	<b>Total (6 products)</b>	<b>48</b>		

**Note:** From the above list of products, any 6 products will be manufactured at a given point of time.

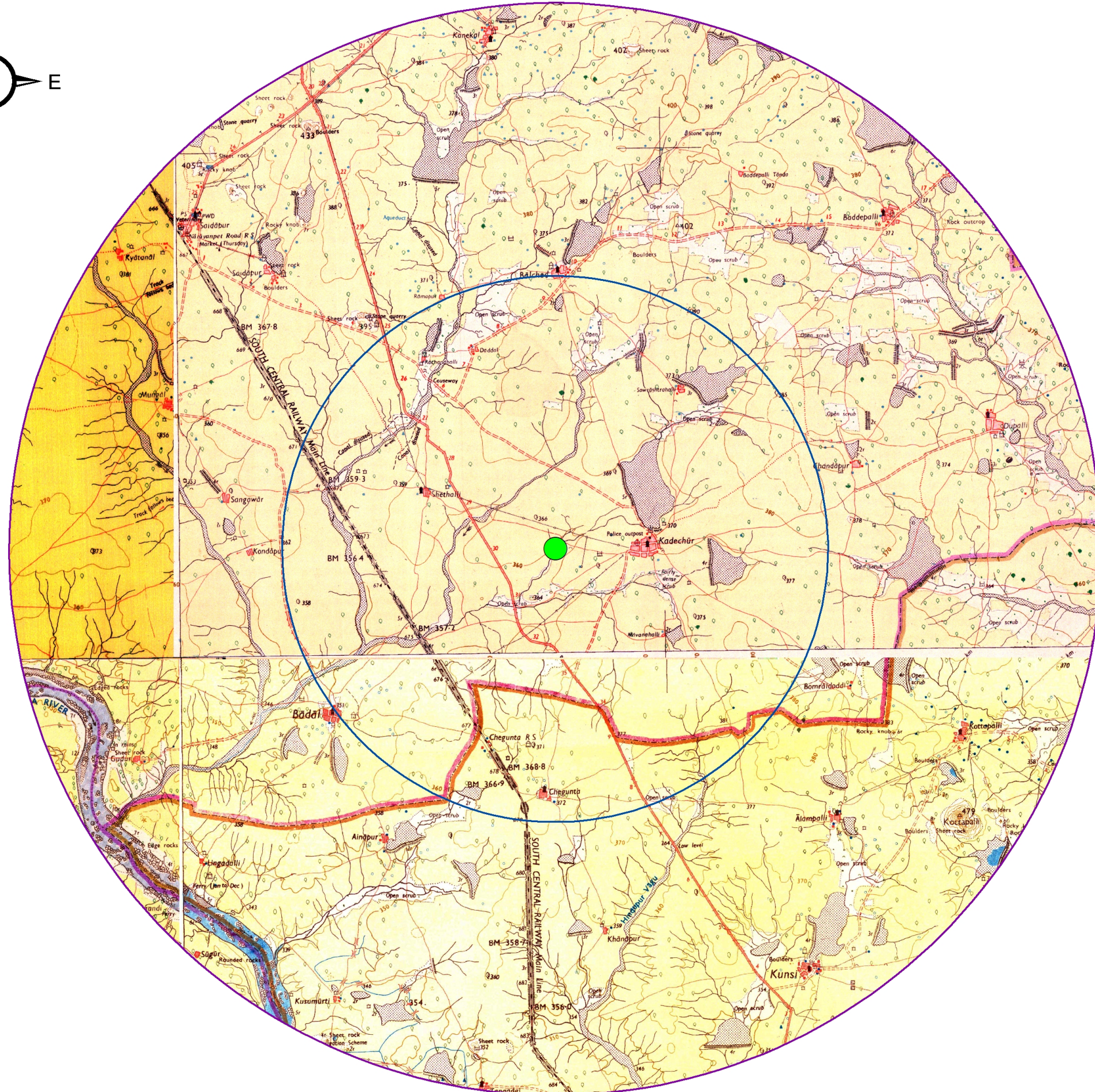
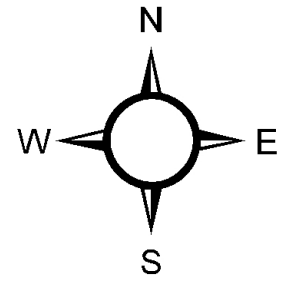
#### LIST OF PROPOSED BY-PRODUCTS

S.No	Name of the Product	Name of the By Product	Quantity in Kgs/Day
1	Capecitabine	Peridine Hydrochloride	59.69
2	Famotidine	Potassium chloride	53.14
3	Piroctone Olamine	Aluminium hydroxide solution	1452.5
4	Pantoprazole Sodium	Potassium Sulphate	60
		Ammonium Phosphate	35
		Sodium Acetate	110
		Ammonium Chloride	72.25
5	Telmisartan	Sodium phosphate	251

**ANNEXURE-2**

**TOPOSHEET**

# TOPOMAP SHOWING PROJECT SITE WITH 10 KM RADIUS



## CONVENTIONAL SYMBOLS

Express highway: with toll; with bridge; with distance stone			
Roads, metalled: according to importance			
Roads, double carriageway: according to importance			
Unmetalled road. Cart-track. Pack-track with pass. Foot-path			
Streams: with track in bed, undefined. Canal			
Dams: masonry or rock-filled; earthwork. Weir			
River: dry with water channel; with island & rocks. Tidal river			
Submerged rocks. Shoal. Swamp. Reeds			
Wells: lined; unlined. Tube-well. Spring. Tanks: perennial; dry			
Embankments: road or rail; tank. Broken ground			
Railways, broad gauge: double; single with station; under constr.			
Railways, other gauges: double; single with distance stone; do			
Mineral line or tramway. Kin. Cutting with tunnel			
Contours with sub-features. Rocky slopes. Cliffs			
Sand features: (1)flat. (2)sand-hills(permanent). (3)dunes(shifting)			
Towns or Villages: inhabited; deserted. Fort			
Huts: permanent; temporary. Tower. Antiquities			
Temple. Chhatri. Church. Mosque. Idgah. Tomb. Graves			
Lighthouse. Lightship. Buoys: lighted; unlighted. Anchorage			
Mine. Vine on trellis. Grass. Scrub			
Palms: palmyra; other. Plantain. Conifer. Bamboo. Other trees			
Areas: cultivated; wooded. Surveyed tree			
Boundary, international			
state: demarcated; undemarcated			
district: subdivision; tahsil or taluk; forest			
Boundary pillars: surveyed; unlocated			
Heights, triangulated: station; point; approximate			
Bench-mark: geodetic; tertiary; canal			
Post office. Telegraph office. Overhead tank			
Rest house or inspection bungalow. Circuit house. Police station			
Camping ground. Forest: reserved; protected			
Spaced names: administrative; locality or tribal			
Hospital. Dispensary. Veterinary. Hospital / Dispensary			
Aerodrome. Halipad. Tourist site			
Power line: with pylons surveyed; with poles unsurveyed			

## Legend (TS No. 56 H/2, 3, 6 & 7)

- Project\_Site
- 5\_km\_Buffer
- 10\_km\_Buffer

**PREPARED FOR:**  
**M/s. LAUREATZ TECHNOCHEM PVT LTD.**  
 PLOT NO. 62, KADECHUR INDUSTRIAL  
 AREA, YADAGIR TALUK, DISTRICT  
 KARNATAKA - 585221

**PREPARED BY:**  
**AM ENVIRO ENGINEERS**  
 2ND FLOOR, 14/1, HARIKRUPA,  
 PATALAMMA TEMPLE STREET  
 BASAVANAGUDI, BENGALURU - 560004

# **ANNEXURE-3**

**PROCESS DESCRIPTION,**  
**ROUTE OF SYNTHESIS ALONG**  
**WITH MATERIAL BALANCE**

## 1. ADEFOVIR

### Process Description

#### Stage-1

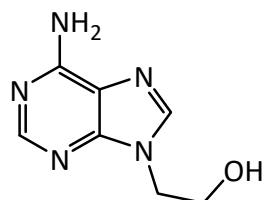
2-(6-Amino-9H-purin-9-yl) ethanol reacts with Diethyl P-Toluene sulfonyloxy methylphosphonate and Magnesium tert butoxide in presence of DMF to give Adefovir.

## ADEFOVIR

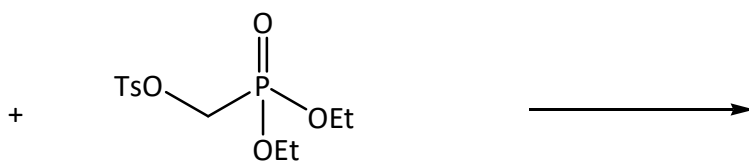
### Route of Synthesis

#### Stage-1

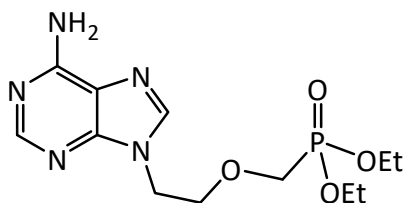
##### Step-A



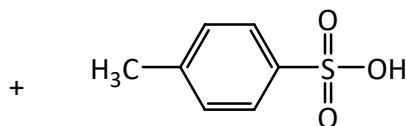
2-(6-Amino-9H-purin-9-yl)ethanol  
M.F:C<sub>7</sub>H<sub>9</sub>N<sub>5</sub>O  
M.Wt:179.18



Diethyl p-toluenesulfonyloxy methylphosphonate  
M.F:C<sub>12</sub>H<sub>19</sub>O<sub>6</sub>PS  
M.Wt:322.31

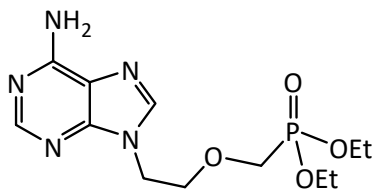


Diethyl ((2-(6-amino-9H-purin-9-yl)ethoxy)methyl)phosphonate  
M.F:C<sub>12</sub>H<sub>20</sub>N<sub>5</sub>O<sub>4</sub>P  
M.Wt:329.29



Paratoluene Sulphonic acid  
C<sub>7</sub>H<sub>8</sub>O<sub>3</sub>S  
172.20

## Step-B



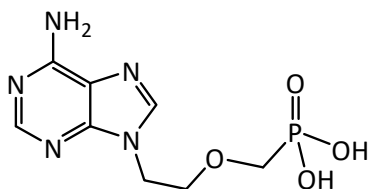
Diethyl ((2-(6-amino-9H-purin-9-yl)ethoxy)methyl)phosphonate

M.F:  $C_{12}H_{20}N_5O_4P$   
M.Wt: 329.29



Ammonium hydroxide  
 $2 \times 35.05 = 70.1$

$2 \times 36.5 = 73.0$



Adefovir

M.F:  $C_8H_{12}N_5O_4P$   
M.Wt: 273.19



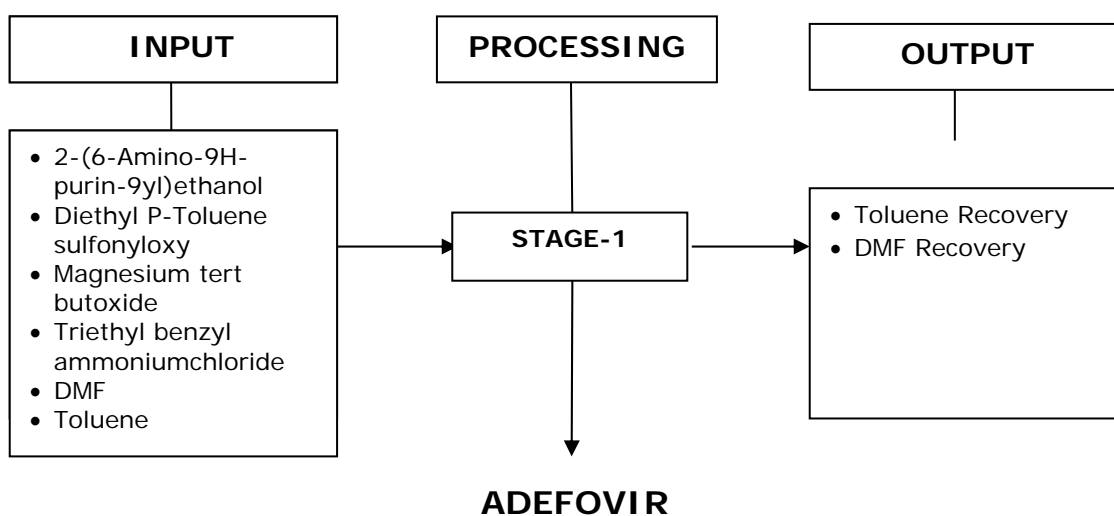
Ethanol

106.98

92.14

## ADEFOVIR

### Flow Chart:



## ADEFOVIR

### Material Balance

Material balance of Adefovir Stage-1 Batch Size: 14.0Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity In Kg
2-(6-Amino-9H-purin-9yl)ethanol	10.00	Adefovir	14.00
Diethyl P-Toluene sulfonyloxy methylphosphonate	18.00	DMF Recovery	65.00
Magnesium tert butoxide	3.00	DMF Loss	3.00
Triethyl benzyl ammoniumchloride	2.00	Toluene Recovery	60.00
DMF	70.00	Toluene Loss	3.00
Toluene	70.00	Effluent water	128.90
Hydrochloric acid	4.00	(water-100,p-Toluene sulphonic acid-9.62, Magnesium tert butoxide-3, triethyl benzyl ammonium chloride-2, ethanol-4.76, ammonium chloride-5.52, Toluene-4)	
Ammonium hydroxide	3.62	Organic Residue	6.72
Water	100.00	(Organic Impurities-1.72, DMF-2, Toluene-3)	
<b>Total</b>	<b>280.62</b>	<b>Total</b>	<b>280.62</b>

## 2. BORTEZOMIB

### Process Description:

#### Stage-1:

Isobutyl boronic acid reacts with Pinanediol in presence of Heptane to give Stage-1 Product.

#### Stage-2:

Stage-1 product reacts with Zinc chloride and n-hexyl Lithium in presence of THF and Sulphuric acid to give stage-2 product

#### Stage-3:

Stage-2 product reacts with 1,1,1,3,3,3-Hexamethyl-disilazane in presence of Tetra hydro furan and Di isopropyl ether to give stage-3 product

#### Stage-4:

Stage-3 product reacts with Trifluoro Acid in presence of Diisopropyl ether to give stage-4 product.

#### Stage-5:

L-phenyl Alanine undergoes chlorination with Thionyl chloride and methanol in presence of IPA to give Stage-5 product.

#### Stage-6:

Stage-5 product reacts with Pyrazine carboxylic acid in presence of Ethyl Acetate, N-Heptane, Acetone and sodium hydroxide to give stage-6 product

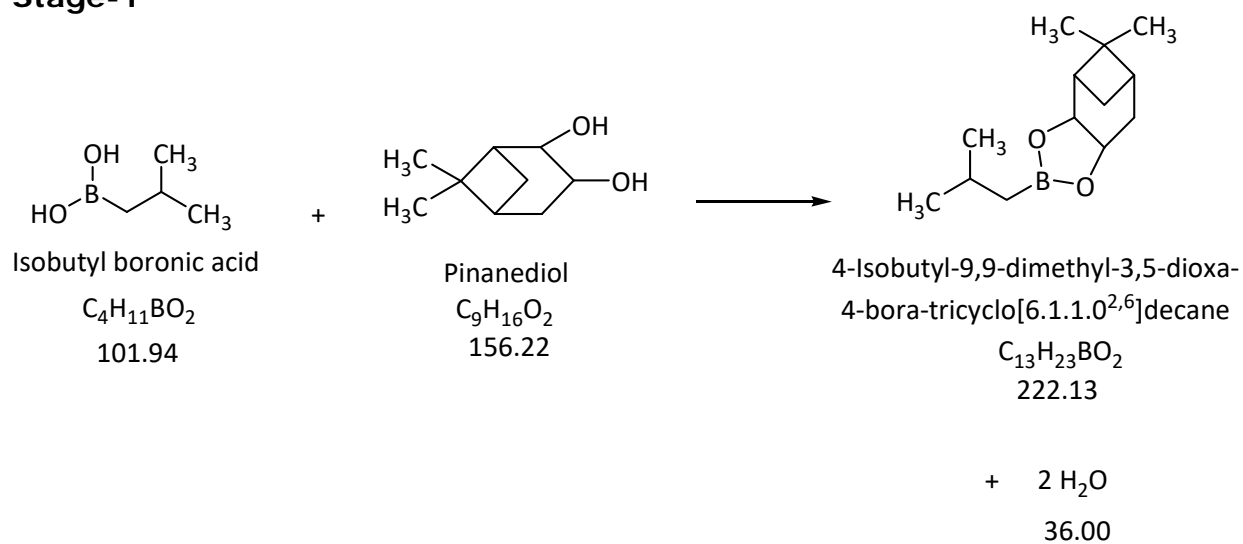
#### Stage-7:

Stage-6 product reacts with Stage-4 compound in presence of MDC and methanol to give Stage-7 product.

#### Stage-8:

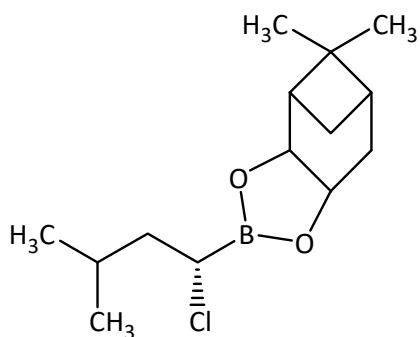
Stage-7 product reacts with Isobutyl boronic acid in presence of n-Heptane, MDC and Methanol to give Bortezomib.

**Route of Synthesis:  
Stage-1**



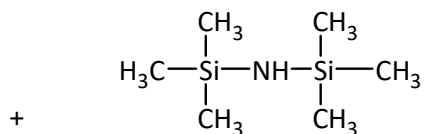


### Stage-3



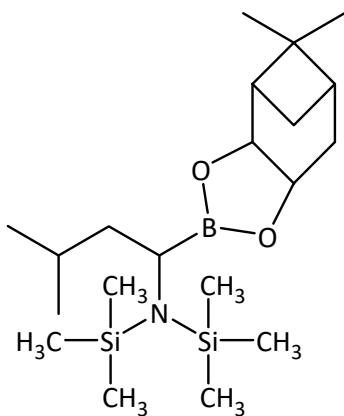
4-(1-Chloro-3-methyl-butyl)-9,9-dimethyl-3,5-dioxo-4-bora-tricyclo[6.1.1.0<sup>2,6</sup>]decane

$C_{14}H_{24}BClO_2$   
270.60



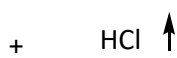
1,1,1,3,3,3-Hexamethyl-disilazane

$C_6H_{19}NSi_2$   
161.39



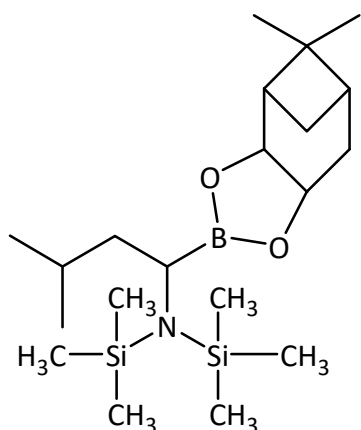
4-[1-(1,1,1,3,3,3-Hexamethyl-disilazan-2-yl)-3-methyl-butyl]-9,9-dimethyl-3,5-dioxo-4-bora-tricyclo[6.1.1.0<sup>2,6</sup>]decane

$C_{20}H_{42}BNO_2Si_2$   
395.53

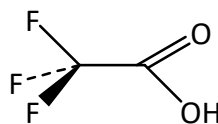


36.50

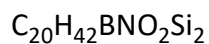
Stage-4



+

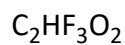


4-[1-(1,1,1,3,3,3-Hexamethyl-disilazan-2-yl)-  
3-methyl-butyl]-9,9-dimethyl-3,5-dioxa-4-bora-  
tricyclo[6.1.1.0<sup>2,6</sup>]decane

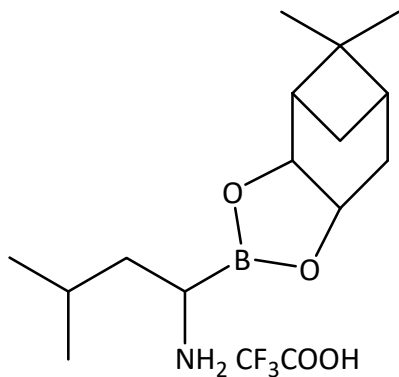


395.53

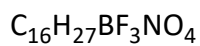
Trifluoro Acetic Acid



114.02

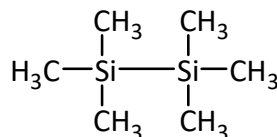


1-(9,9-Dimethyl-3,5-dioxa-4-bora-tricyclo  
[6.1.1.0<sup>2,6</sup>]dec-4-yl)-3-methyl-butylamine  
trifluoro-acetic acid

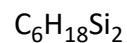


365.20

+

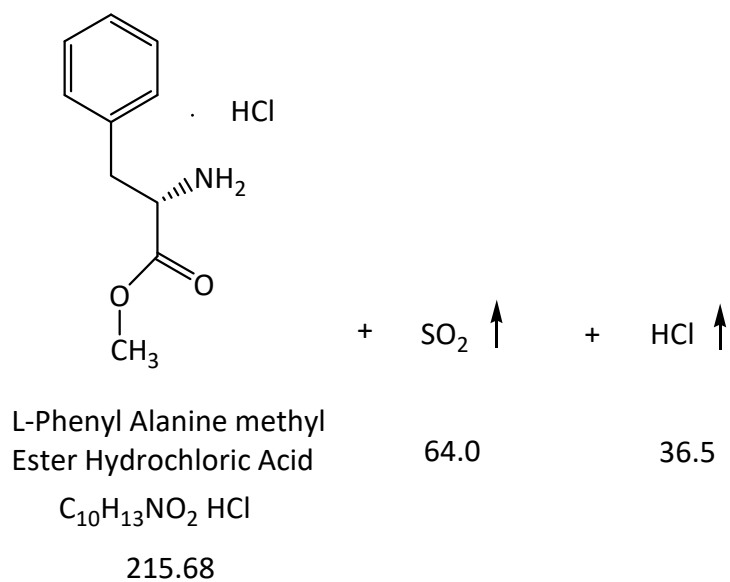
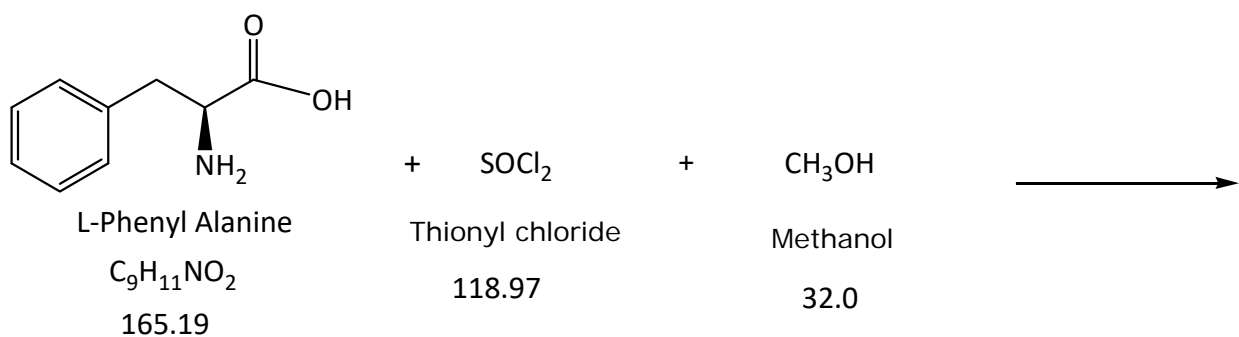


1,1,1,2,2,2-Hexamethyl-disilane

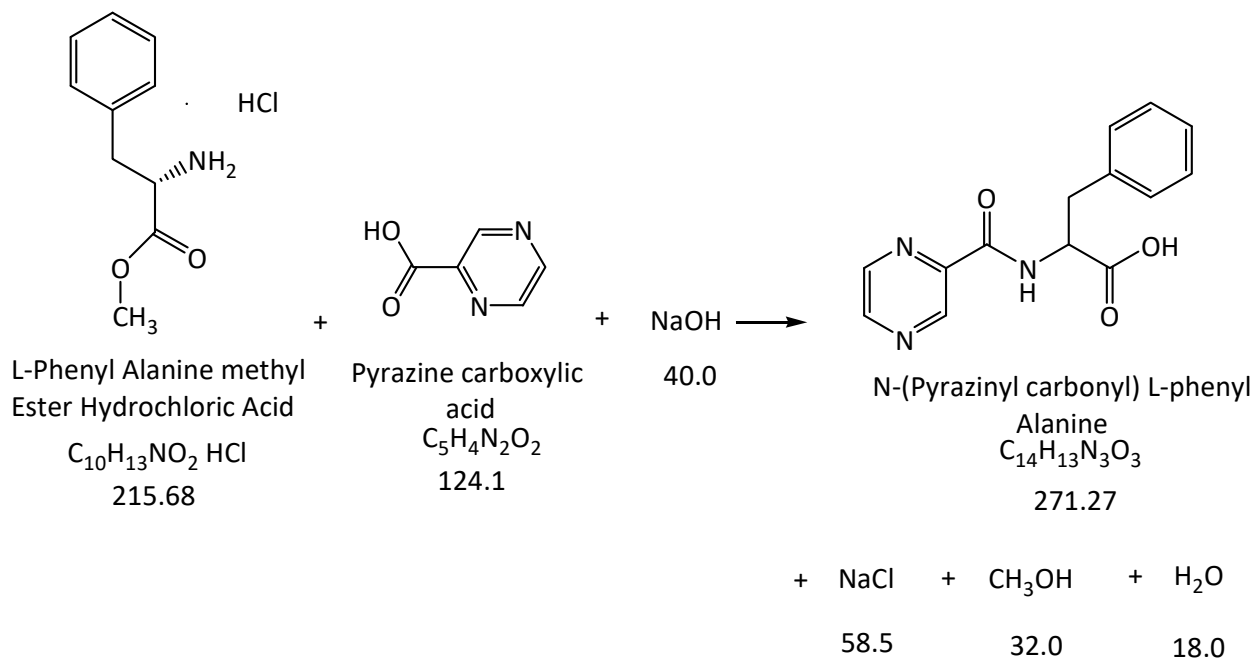


146.38

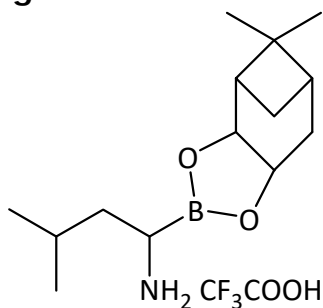
Stage-5



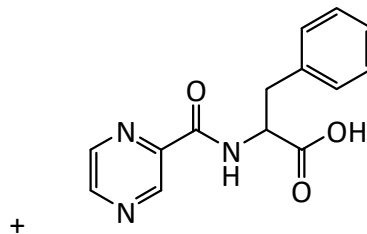
### Stage-6



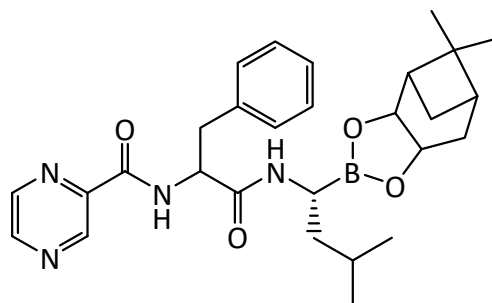
**Stage-7**



1-(9,9-Dimethyl-3,5-dioxa-4-bora-tricyclo[6.1.1.0<sup>2,6</sup>]dec-4-yl)-3-methyl-butylamine;trifluoro-acetic acid  
(Stage-4)  
 $C_{16}H_{27}BF_3NO_4$   
365.2



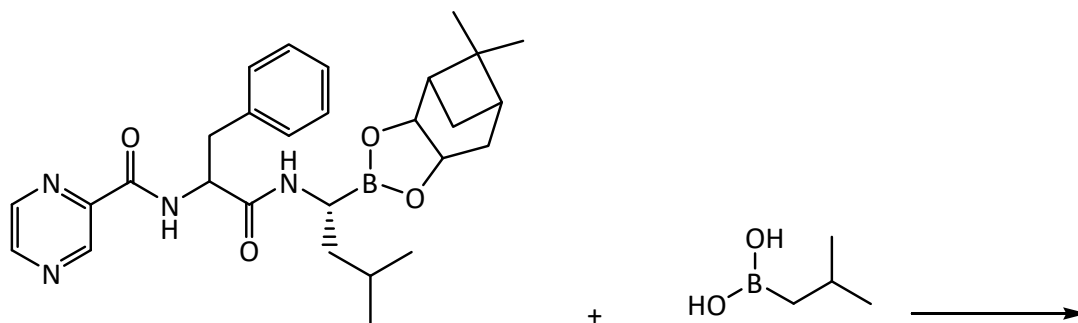
N-(Pyrazinyl carbonyl) L-phenyl  
Alanine  
(Stage-6)  
 $C_{14}H_{13}N_3O_3$   
271.27



Pyrazine-2-carboxylic acid {1-[1-(9,9-dimethyl-3,5-dioxa-4-bora-tricyclo[6.1.1.0<sup>2,6</sup>]dec-4-yl)-3-methyl-butylcarbamoyl]-2-phenyl-ethyl}-amide  
 $C_{28}H_{37}BN_4O_4$   
504.43

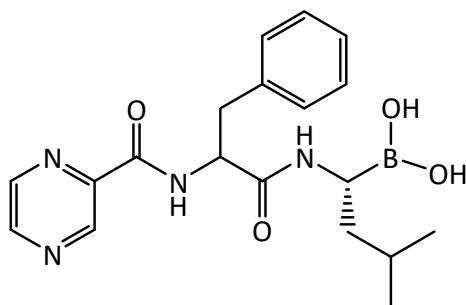
+  $CF_3COOH$  +  $H_2O$   
114.02      18.0

## Stage-8

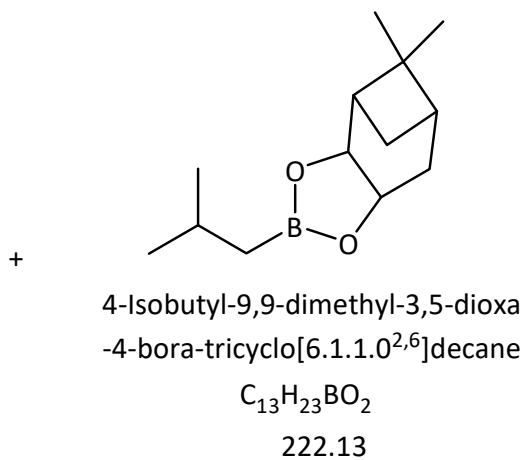


Pyrazine-2-carboxylic acid {1-[1-(9,9-dimethyl-3,5-dioxa-4-bora-tricyclo[6.1.1.0<sup>2,6</sup>]dec-4-yl)-3-methylbutylcarbamoyl]-2-phenyl-ethyl}-amide  
 $C_{28}H_{37}BN_4O_4$   
504.43

Isobutyl boronic Acid  
 $C_4H_{11}BO_2$   
101.94



Bortezomib  
 $C_{19}H_{25}BN_4O_4$   
384.24

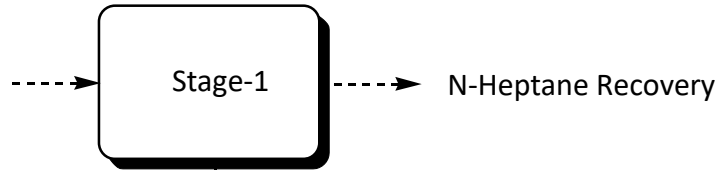


4-Isobutyl-9,9-dimethyl-3,5-dioxa-4-bora-tricyclo[6.1.1.0<sup>2,6</sup>]decane  
 $C_{13}H_{23}BO_2$   
222.13

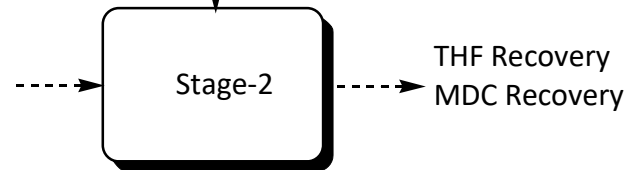
# BORTEZOMIB

## Flow chart:

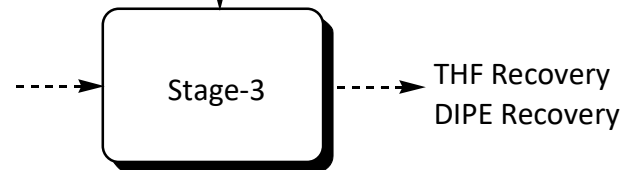
Iso Butyl Boronic Acid  
N-Heptane  
Pinanediol  
Sodium Chloride



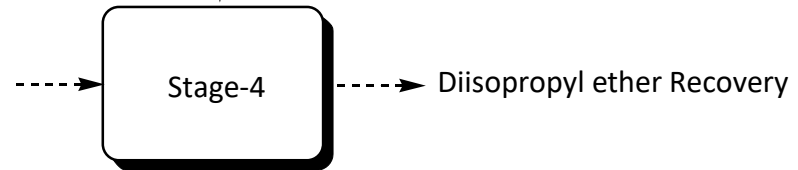
Stage-1  
Zinc Chloride  
THF  
N-Hexyl Lithium  
Di Iso Propyl Amine  
MDC  
Sulphuric acid



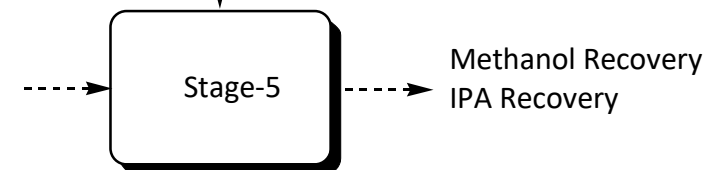
Stage-2  
HMDS  
THF  
N-Hexyl Lithium  
DIPE



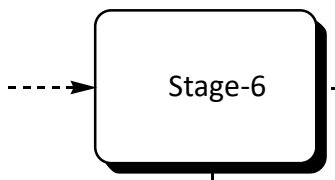
Stage-3  
Tri Fluoro Acetic Acid  
Diisopropyl Ether



L-Phenyl Alanine  
Thionyl Chloride  
Methanol  
IPA

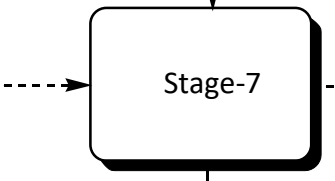


Pyrazine Carboxylic acid  
DMF  
N-Hydroxy Succinamide  
Di Cyclohexyl Carbodimide  
N-Methyl Morpholine  
Ethyl Acetate  
n-Heptane  
Acetone



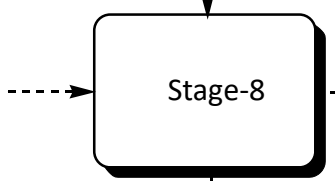
DMF Recovery  
Ethyl Acetate Recovery  
N-Heptane Recovery  
Acetone Recovery

N-Hydroxysucciniamide  
MDC  
Dicyclohexyl dicarbodimide  
Methanol  
Di isopropyl ethylamine  
Hydrochloric Acid  
Sodium bicarbonate



MDC Recovery  
Methanol Recovery

Bortezomib base  
Methanol  
N-Heptane  
Isobutyl boronic Acid  
MDC  
Sodium bicarbonate  
Hydrochloric Acid



Methanol Recovery  
MDC Recovery  
N-Heptane Recovery

**Bortezomib**

## BORTEZOMIB

### Material Balance:

MATERIAL BALANCE OF BORTEZOMIB STAGE 1 BATCH SIZE :10.0 KG			
NAME OF THE INPUT	QUANTITY IN KG	NAME OF THE OUT PUT	QUANTITY IN KG
Iso Butyl Boronic Acid	4.00	Stage-1	8.50
N-Heptane	3.00	• N-Heptane Recovery	2.90
Pinanediol	6.25	• N-Heptane Loss	0.10
		Effluent Water	11.48
Sodium Chloride	0.06	• Water-10.	
Water	10.00	• Generated water-1.42 • Sodium chloride-0.06	
		Organic residue	0.33
		• Process Residue-.0.33	
<b>Total</b>	<b>23.31</b>	<b>Total</b>	<b>23.31</b>

MATERIAL BALANCE OF BORTEZOMIB STAGE 2 BATCH SIZE :10.0 KG			
NAME OF THE INPUT	QUANTITY IN KG	NAME OF THE OUTPUT	QUANTITY IN KG
Stage-1	8.50	Stage-2	10.00
Zinc Chloride	5.50	THF Recovery	9.40
THF	10.00	THF Loss	0.50
N-Hexyl Lithium	1.25	MDC Recovery	11.88
Di Isopropyl amine	4.00	MDC Loss	0.62
MDC	12.50	Effluent Water – 49.57	
Sulphuric acid	4.00	• Water-40 • Zinc sulphate-6.18 • Ammonium chloride-2.04 • THF-0.1 • n-Hexyl Lithium-1.25	49.57
Water	40.00	Process Emission	
		Pentane – 2.76	2.76
		Organic residue – 1.02 (Process Residue-1.02)	1.02
<b>Total</b>	<b>85.75</b>	<b>Total</b>	<b>85.75</b>

<b>MATERIAL BALANCE OF BORTEZOMIB</b>			
<b>STAGE 3</b>			
<b>BATCH SIZE : 10.0KG</b>			
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KG</b>	<b>NAME OF THE OUT PUT</b>	<b>QUANTITY IN KG</b>
Stage-2	10.00	Stage-3	14.00
HMDS	6.00	THF Recovery	2.85
THF	3.00	THF Loss	0.15
N-Hexyl Lithium	3.50	DIPE Recovery	1.29
DIPE	1.35	DIPE Loss	0.06
		N-Hexyl Lithium Reuse	3.50
		Process Emission – 1.35 (Hydrogen chloride-1.35)	1.35
		Organic Residue – 0.65 (Process Residue-0.65)	0.65
Total	23.85	Total	23.85

<b>MATERIAL BALANCE OF BORTEZOMIB</b>			
<b>STAGE 4</b>			
<b>BATCH SIZE : 10.0 KG</b>			
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KG</b>	<b>NAME OF THE OUT PUT</b>	<b>QUANTITY IN KG</b>
Stage-3	14.00	Stage-4	12.00
Tri Fluoro Acetic Acid	4.25	Diisopropyl ether Recovery	21.00
Diisopropyl Ether	22.50	Diisopropyl ether Loss	1.00
DM Water	50.00	Effluent Water (Water-50,Hexamethyl disilane-5.18,DIPE-0.5)	55.68
		Organic residue	1.07
		Process residue – 1.07	
Total	90.75	Total	90.75

**MATERIAL BALANCE OF BORTEZOMIB  
STAGE 5  
BATCH SIZE :10.0KG**

<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KG</b>	<b>NAME OF THE OUT PUT</b>	<b>QUANTITY IN KG</b>
L-Phenyl Alanine	6.00	Stage-5	7.50
Thionyl Chloride	4.50	Methanol Recovery	2.85
Methanol	5.00	Methanol Loss	1.25
IPA	5.00	IPA Recovery	4.75
		IPA Loss	0.10
		Process Emission – 3.64 (Hydrogen chloride-1.32, Sulfurdioxide-2.32)	3.64
		Organic Residue – 1.60 (Process Residue-0.55 Distillation residue – 1.05 (IPA-0.15, Methanol – 0.9)	1.60
<b>Total</b>	<b>20.50</b>	<b>Total</b>	<b>20.50</b>

**MATERIAL BALANCE OF BORTEZOMIB  
STAGE 6  
BATCH SIZE :10.0 KG**

NAME OF THE INPUT	QUANTITY IN KG	NAME OF THE OUT PUT	QUANTITY IN KG
Stage-5	7.50	Stage-6	9.00
Pyrazine Carboxylic acid	4.50	• DMF Recovery	14.25
DMF	15.00	• DMF Loss	0.03
n-Hydroxy Succinamide	3.00	• Ethyl Acetate Recovery	19.00
Di Cyclohexyl Carbodimide	1.00	• Ethyl Acetate Loss	0.80
n-Methyl Morpholine	0.35	• n-Heptane Recovery	19.00
Ethyl Acetate	20.00	• n-Heptane Loss	1.00
n-Heptane	20.00	• Acetone Recovery	14.25
Acetone	15.00	• Acetone Loss	0.75
Sodium Hydroxide	1.50	Effluent Water – 168.11	168.11
Hydrochloric Acid	10.00	• Water-150, • Generated water-0.62, • Sodium chloride-2.03, • Methanol-1.11,HCl-10, • DCC-1 • n-Hydroxy Succinamide-3, • n-Methylmorpholine-0.35	
DM Water	150.00	Organic residue – 1.66	1.66
		• Process Residue-0.74 • Distillation Residue-0.92  (DMF-0.72,Ethyl acetate-0.2)	
Total	247.85	Total	247.85

**MATERIAL BALANCE OF BORTEZOMIB  
STAGE-7  
BATCH SIZE :10.0 KG**

NAME OF THE INPUT	QUANTITY IN KG	NAME OF THE OUT PUT	QUANTITY IN KG
Stage-4	12.00	Bortezomib Base	1.40
Stage-6	9.00	• MDC Recovery	14.25
N-Hydroxysucciniamide	0.25	• MDC Loss	0.30
MDC	15.00	• Methanol Recovery	9.50
Dicyclohexyl dicarbodimide	0.40	• Methanol Loss	0.20
Methanol	10.00	• Effluent Water	8.49
Di isopropyl ethylamine	0.45	Water-70, • Generated water-0.59 Sodium bicarbonate-0.2, • HCl-0.25,DIPA-0.45	71.49
Hydrochloric Acid	0.25	Organic Residue – 11.92	11.92
Sodium bicarbonate	0.20	• Process residue -11.17 • Trifluoro acetic acid-.3.75 • Distillation Residue-0.75  (Methanol-0.30,MDC-0.45)	
DM Water	70.00		
<b>Total</b>	<b>117.55</b>	<b>Total</b>	<b>117.55</b>

**MATERIAL BALANCE OF BORTEZOMIB  
STAGE 8  
BATCH SIZE- 10.0 KG**

<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KG</b>	<b>NAME OF THE OUT PUT</b>	<b>QUANTITY IN KG</b>
Bortezomib base	15.00	Bortezomib	10.00
Methanol	15.00	Methanol Recovery	14.20
N-Heptane	17.00	Methanol Loss	0.30
Isobutyl boronic Acid	3.25	MDC Recovery	16.20
MDC	17.00	MDC Loss	0.35
Sodium bicarbonate	0.19	N-Heptane Recovery	16.20
Hydrochloric Acid	0.06	N-Heptane Loss	0.35
Water	100.00	Effluent Water – 100.75 (Water-100,Sodium bicarbonate-0.19,HCl-0.06, Methanol-0.5)	100.75
		Organic Residue – 9.15 (Process residue-8.25 4-Isobutyl -9-9 dimethyl-3,5 – dioxo-a-bora-tricyclo decane- 6.60 Distillation Residue-0.9 (MDC-0.45,N-Heptane-0.45)	9.15
<b>Total</b>	<b>167.50</b>	<b>Total</b>	<b>167.50</b>

### 3. CAPECITABINE

#### **Process Description:**

#### **Stage-1:**

5-Deoxy-5-fluoro cytidine reacts with Chloro phenyl formate in presence of Pyridine and MDC to give Satge-1 compound.

#### **Stage-2:**

Satge-1 compound undergoes hydrolysis with sodium hydroxide in presence of MDC and HCl to give Satge-2 compound.

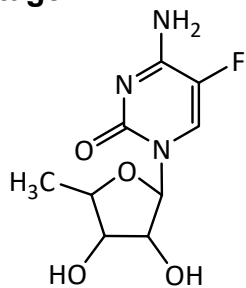
#### **Stage-3:**

Stage-2 compound undergoes purification in ethyl acetate to give Capecitabine

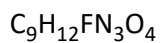
## CAPECITABINE

### Route of Synthesis:

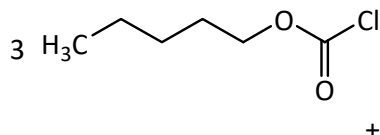
#### Stage-1



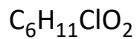
5-Deoxy-5-fluoro  
cytidine



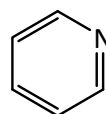
245.21



Chloro pentyl formate



3X150.6=451.8

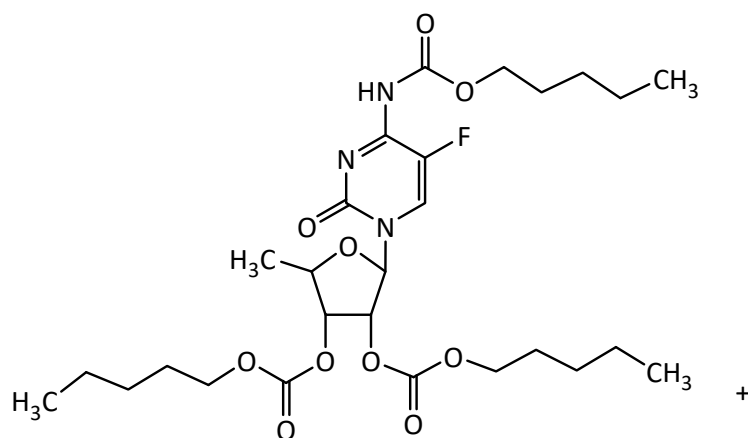


Pyridine

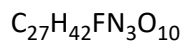


79.10

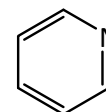
MDC, Ethyl Acetate,  $\rightarrow$



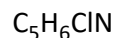
Carbonic acid 5-(5-fluoro-2-oxo-4-pentyloxy  
carbonylamino-2H-pyrimidin-1-yl)-2-methyl-4-pentyloxy  
carbonyloxy-tetrahydro-furan-3-yl ester pentyl ester



587.63



Pyridine  
Hydrochloride

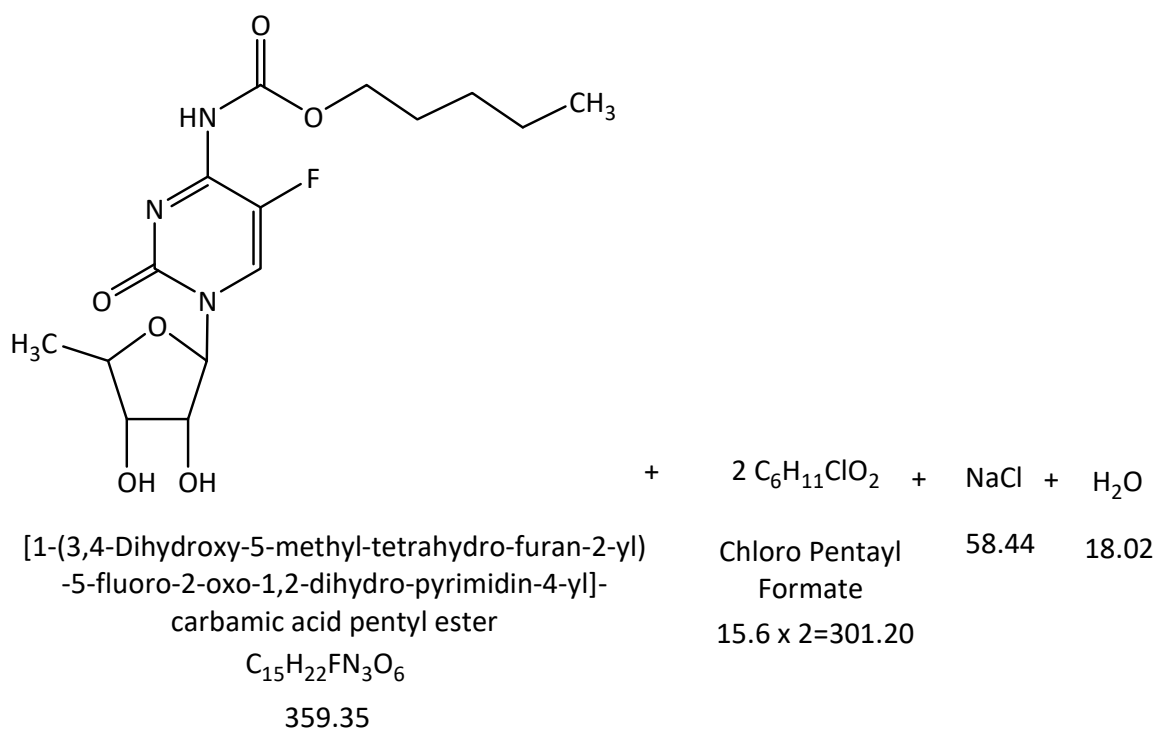
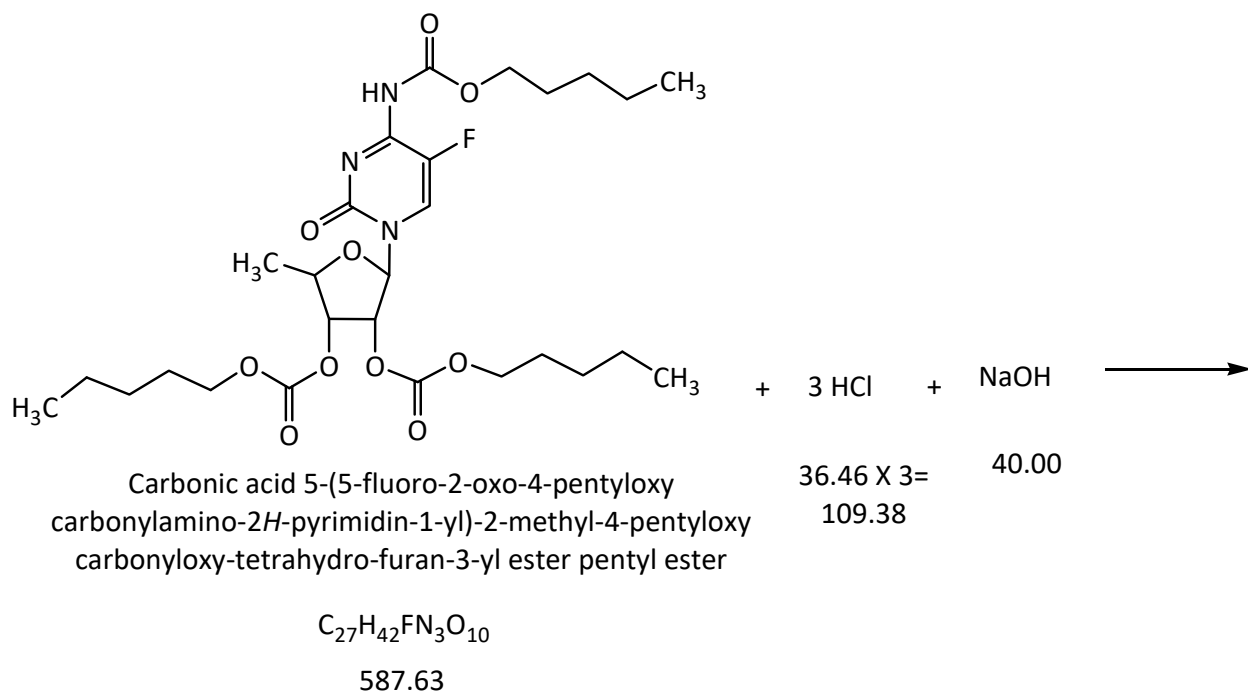


115.56

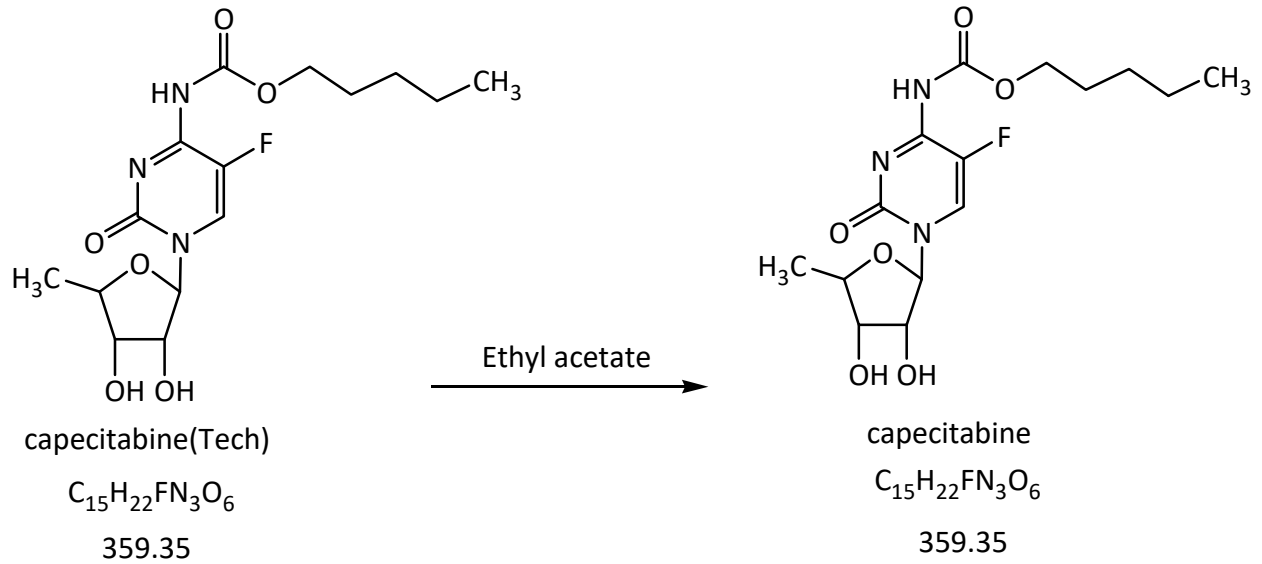
HCl + 2HCl  $\uparrow$

72.92

## Stage-2

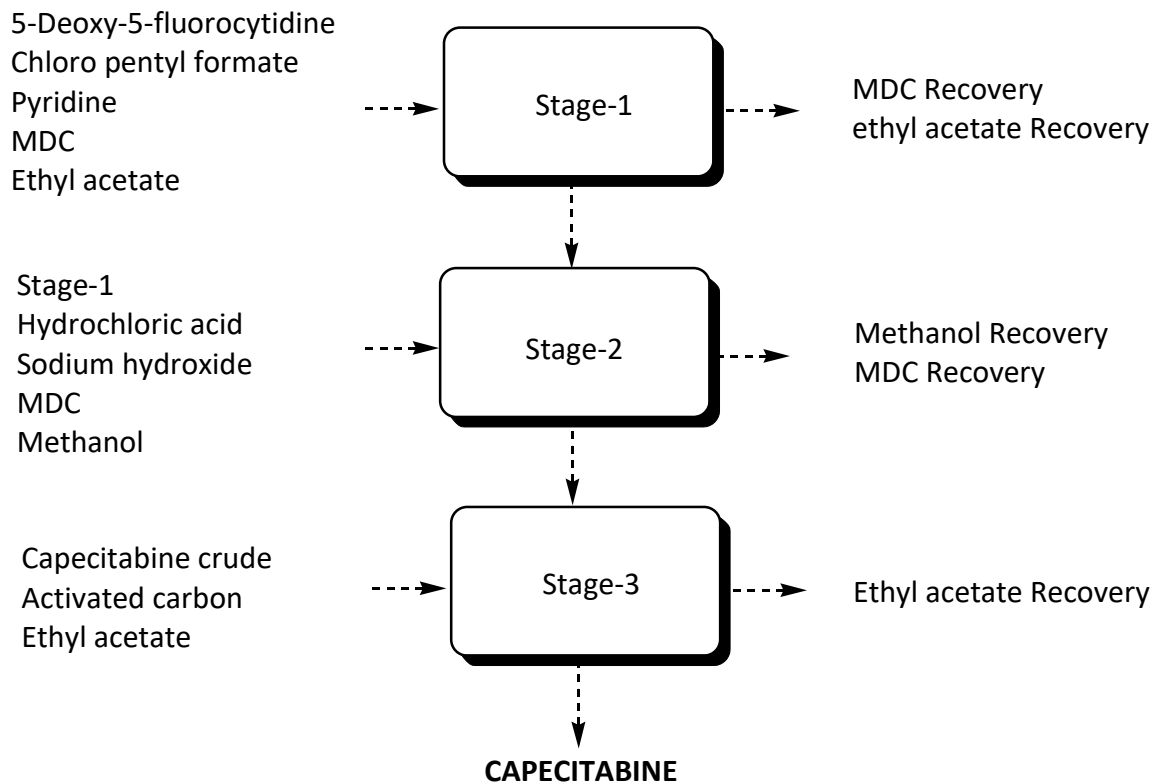


### Stage-3



## CAPECITABINE

### Flowchart:



## CAPECITABINE

### Material Balance:

Material Balance of Capecitabine Stage-1 Batch Size: 25.00Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
5-Deoxy-5-fluorocytidine	19.00	Stage-1	43.00
Chloro pentyl formate	35.00	MDC Recovery	627.00
Pyridine	6.25	MDC Loss	13.00
MDC	660.00	Ethyl acetate Recovery	333.00
Ethyl acetate	350.00	Ethyl acetate Loss	7.00
		By-product	8.95
		- 8.95)	0
		Process Emissions	6.19
		(Hydrogen chloride - 6.19)	0
		Organic Residue	32.11
		Process Residue-2.11, Distillation Residue-30 (MDC-20,Ethylacetate-10)	
<b>Total</b>	<b>1070.25</b>	<b>Total</b>	<b>1070.25</b>

Material Balance of Capecitabine Stage-2 Batch Size: 25.00Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	43.00	Stage-2	26.00
Hydrochloric acid	8.00	MDC Recovery	333.00
Sodium hydroxide	3.00	MDC Loss	7.00
MDC	350.00	Methanol Recovery	285.00
Methanol	300.00	Methanol Loss	6.00
Water	500.00	Effluent water (Water-500, generated water-1.318, Sodium chloride-4.42, Methanol-4)	531.73
		Chloro pentyl formate -22)	
		Organic Residue	15.27
		Process Residue-0.27, Distillation Residue-15 (MDC-10,Methanol-5)	
<b>Total</b>	<b>1204.00</b>	<b>Total</b>	<b>1204.00</b>

Material Balance of Capecitabine  
 Stage-3  
 Batch Size: 25.00Kg

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Capecitabine crude	26.00	Capecitabine (pure)	25.00
Activated carbon	10.00	Ethyl acetate Recovery	475.00
Ethyl acetate	500.00	Ethyl acetate Loss	10.00
		Spent carbon	10.00
		Organic Residue	25.00
		Process Residue-10 Distillation Residue-15 (Ethylacetate-15)	
<b>Total</b>	<b>536.00</b>	<b>Total</b>	<b>545.00</b>

## 4. CLOPIDOGREL BISULPHATE

### Process Description

#### Stage-1

Amino-(2-chloro-phenyl) acetic acid methyl ester Hydrochloride reacts with Sodium carbonate in presence of Dichloromethane as a solvent media to give Stage-1 as a product.

#### Stage-2

Stage-1 product reacts with Amino-(2-chloro-phenyl) acetic acid methyl ester and Isopropyl alcohol hydrochloride to give Stage-2 as a product.

#### Stage-3

Stage-2 Product reacts with Formaldehyde and Sodium carbonate in presence of Dichloromethane as a solvent media to give stage-3 as a product.

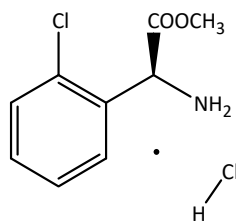
#### Stage-4

Stage-3 product reacts with Sulphuric acid in presence of Acetone as a solvent media to give Clopidogrel Bisulphate.

## CLOPIDOGREL BISULPHATE

### Route of Synthesis:

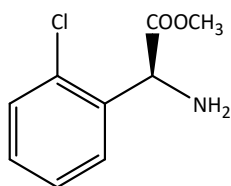
#### Stage-1:



Amino-(2-chloro-phenyl)  
-acetic acidmethyl ester  
Hydrochloride  
 $C_9H_{11}Cl_2NO_2$   
236.10



Sodium carbonate  
105.99



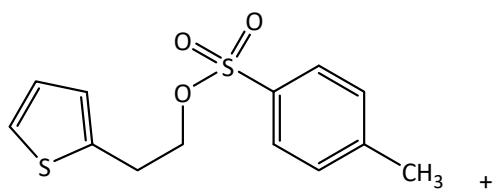
Amino-(2-chloro-phenyl)-acetic  
acid methyl ester  
 $C_9H_{10}ClNO_2$   
199.63



Sodium chloride  
58.5

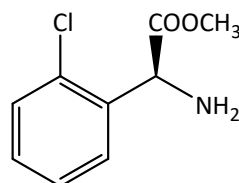
Sodium bicarbonate  
84.01

**Stage-2:**



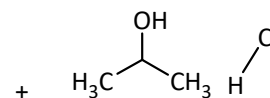
Toluene-4-sulfonic acid 2-thiophen-2-yl-ethyl ester

$C_{13}H_{14}O_3S_2$   
282.38



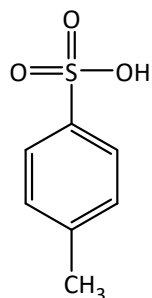
Amino-(2-chloro-phenyl)-acetic acid methyl ester

$C_9H_{10}ClNO_2$   
199.63



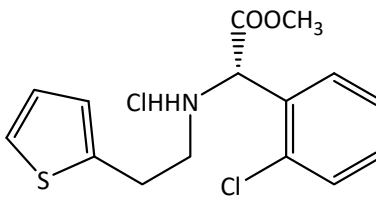
Isopropyl alcohol Hydrochloride

96.56



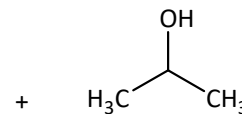
Toluene-4-sulfonic acid

$C_7H_8O_3S$   
172.20



(+)(2-Chloro-Phenyl)-(2-Thiophen-2-yl-Ethylamino)-Acetic Acid Methyl Ester Hydrochloride

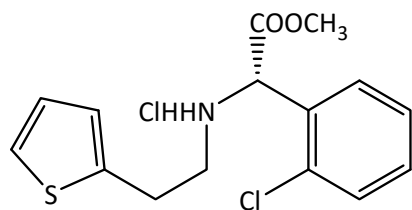
$C_{15}H_{17}Cl_2NO_2S$   
346.27



Isopropyl alcohol

60.10

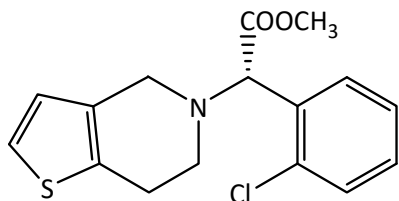
**Stage-3:**



(+)(2-Chloro-Phenyl)-(2-Thiophen-2-yl)  
-Ethylamino)-Acetic Acid Methyl Ester  
Hydrochloride  
 $C_{15}H_{17}Cl_2NO_2S$   
346.27

+ HCHO +  $Na_2CO_3$  +  $H_2O$   
Formaldehyde 105.99 18.00  
30.03

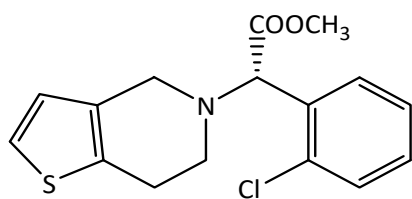
↓  
Dichloromethane



(2-Chloro-phenyl)-(6,7-dihydro-4H-thieno  
[3,2-c]pyridin-5-yl)-acetic acid  
methyl ester  
 $C_{16}H_{16}ClNO_2S$   
321.82

+ NaCl +  $NaHCO_3$  +  $2H_2O$   
Sodium chloride Sodium bicarbonate 36.0  
58.5 84.01

**Stage-4:**



(2-Chloro-phenyl)-(6,7-dihydro-4*H*-thieno  
[3,2-*c*]pyridin-5-yl)-acetic acid  
methyl ester

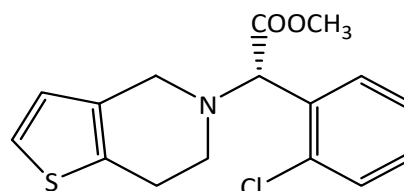
$C_{16}H_{16}ClNO_2S$

321.82



Sulphuric acid

98.08



$H_2SO_4$

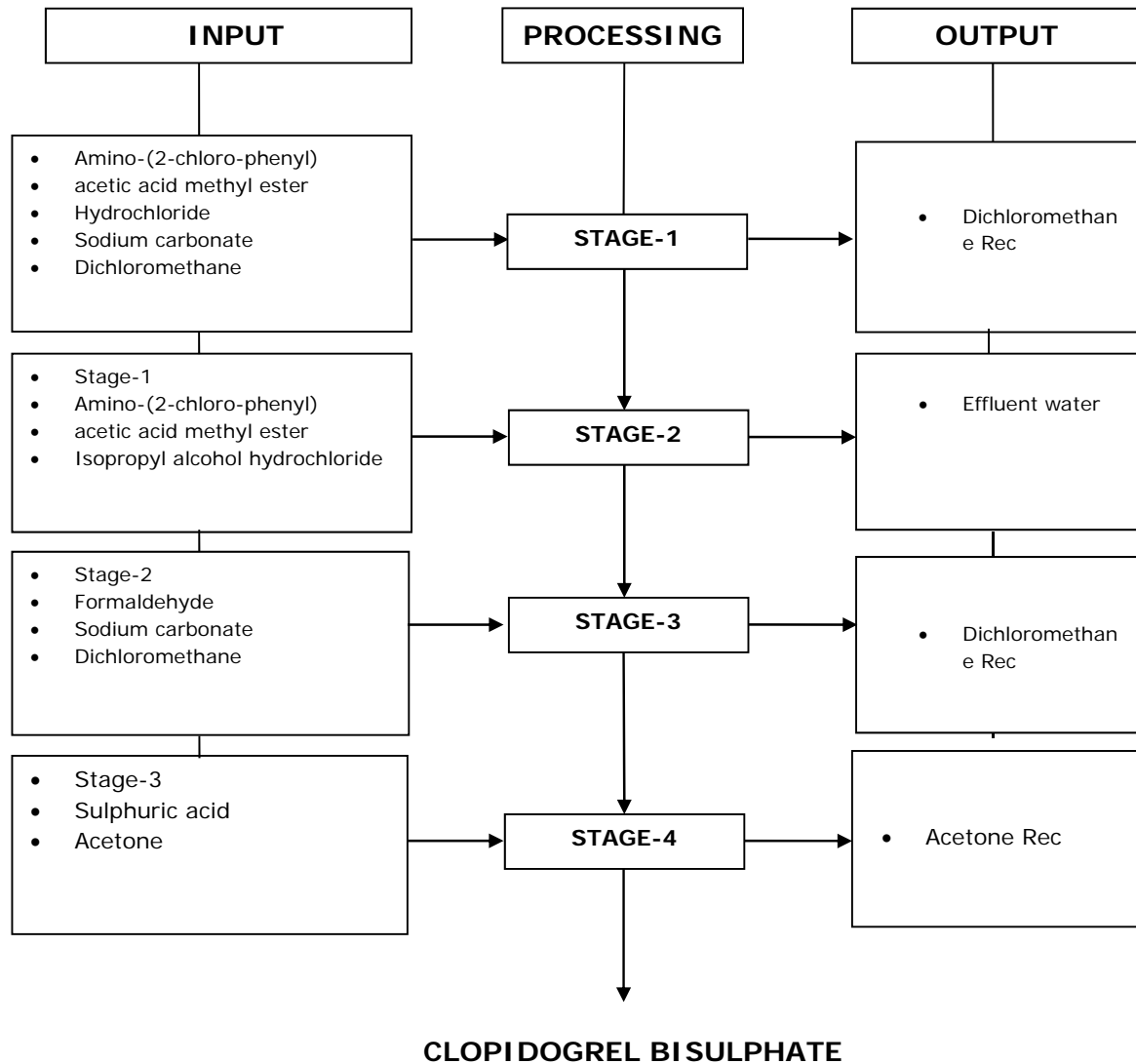
Clopidogrel bisulphate-II

$C_{16}H_{18}ClNO_6S_2$

419.90

# CLOPIDOGREL BISULPHATE

## Flow Chart:



## CLOPIDOGREL BISULPHATE

**Material Balance:**

<b>MATERIAL BALANCE OF CLOPIDOGREL BISULPHATE</b>			
<b>STAGE-1</b>			
<b>BATCH SIZE: 50.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Glycine methyl ester HCl	87.25	Stage-1	63.00
Methylene Dichloride	300.00	Methylene Dichloride Recovery	285.00
Sodium carbonates (20%)	140.00	Methylene Dichloride Loss	15.00
Sodium sulfate	9.00	Effluent water	1136.22
Water	1000.00	(water-986.7, Generated water-6.65, Sodium chloride-30.87, Water from Sodium carbonate-112)	
		Inorganic Residue	9.00
		(Sodium sulfate-9)	
		Process Emissions	11.62
		(Carbon dioxide-11.62)	
		Organic Residue	16.41
<b>Total</b>	<b>1536.25</b>	<b>Total</b>	<b>1536.25</b>

**MATERIAL BALANCE OF CLOPIDOGREL BISULPHATE**

**STAGE-2  
BATCH SIZE: 50.0 KGS**

INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-1	63.00	Stage-2	62.30
Tosylate	90.00	Acetonitrile Recovery	48.00
Acetonitrile	50.00	Acetonitrile Loss	2.00
Toluene	685.00	Toluene Recovery	658.00
Activated carbon	6.30	Toluene Loss	27.00
Isopropyl alcohol	100.00	Isopropyl alcohol Recovery	96.00
IPA.HCl (24%)	85.00	Isopropyl alcohol Loss	4.00
Methanol	25.00	Methanol Recovery	24.00
		Methanol Loss	1.00
		IPA Recovery	52.90
		Spent carbon	6.30
		Organic Residue	122.80
		(Paratoluene sulphonic acid-54.88, Organic impurities-67.92)	
<b>Total</b>	<b>1104.30</b>	<b>Total</b>	<b>1104.30</b>

**MATERIAL BALANCE OF CLOPIDOGREL BISULPHATE**

**STAGE-3  
BATCH SIZE: 50.0 KGS**

INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-2	62.30	Stage-3	44.75
Paraformaldehyde	21.42	n-Hexane Recovery	237.00
Liq.Ammonia solution	19.00	n-Hexane Loss	12.00
n-Hexane	250.00	Effluent water	790.95
Activated carbon	6.80	(Water-746.77, Sodium chloride-20.95, Generated water-3.23, Liq.Ammonia solution-19, n-Hexane-1)	
Sodium sulfate	12.76	Process Emissions	7.88
Sodium carbonate	19.00	(Carbon dioxide-7.88)	
DM Water	750.00	Inorganic Residue	12.76
		(Sodium sulfate-12.76)	0
		Spent carbon	6.80
		Organic Residue	29.14
<b>Total</b>	<b>1141.28</b>	<b>Total</b>	<b>1141.28</b>

**MATERIAL BALANCE OF CLOPIDOGREL BISULPHATE****STAGE-4  
BATCH SIZE: 50.0 KGS**

<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-3	44.75	Clopidogrel Bisulphate	50.00
Methyl ethyl ketone	145.00	MEK Recovery	138.00
Conc.H <sub>2</sub> SO <sub>4</sub>	14.00	MEK Loss	7.00
Acetone	145.00	Acetone Recovery	138.00
Methanol	14.00	Acetone Loss	6.00
		Methanol Recovery	13.00
		Methanol Loss	1.00
		Organic Residue	9.75
		(Unreacted stage-3-6.37,Organic impurities-2.38,Acetone-1)	
<b>Total</b>	<b>362.75</b>	<b>Total</b>	<b>362.75</b>

## 5. DAPAGLIFLOZIN

### Process Description:

#### Stage-1

Gluconolactone reacts with Trimethyl silane and N-Methyl morpholine in presence of MDC to give Stage-1 product.

#### Stage-2

Stage-1 reacts with 4-Bromo-1-chloro-2-(4-ethoxy benzyl) benzene and Methanol in presence of Toluene to give Stage-2 product.

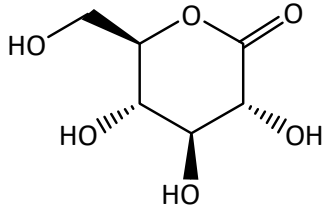
#### Stage-3

Stage-2 reacts with Triethylsilane in presence of MDC to give Stage-3 product.

# DAPAGLIFLOZIN

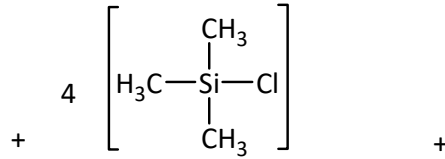
## Route of Synthesis

### Stage-1



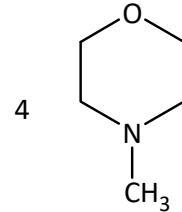
3,4,5-Trihydroxy-6-hydroxymethyl  
-tetrahydro-pyran-2-one

$C_6H_{10}O_6$   
178.14



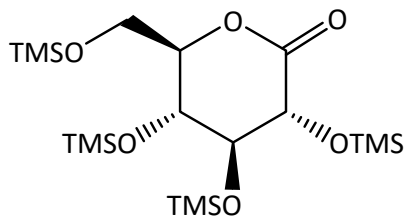
Trimethylsilyl Chloride

$C_3H_9ClSi$   
 $4 \times 108.64 = 434.56$



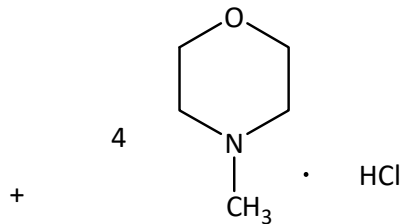
N-Methyl morpholine

$C_5H_{11}NO$   
 $4 \times 101.15 = 404.60$



3,4,5-Tris-trimethylsilyloxy  
-6-trimethylsilyloxymethyl  
-tetrahydro-pyran-2-one

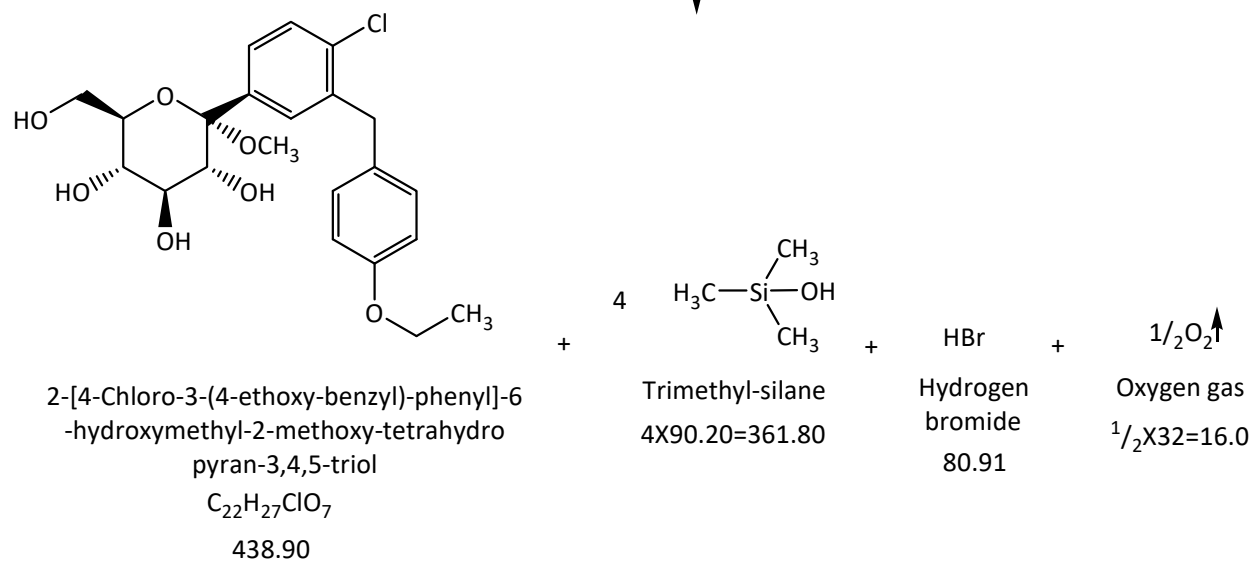
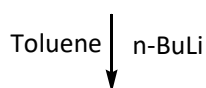
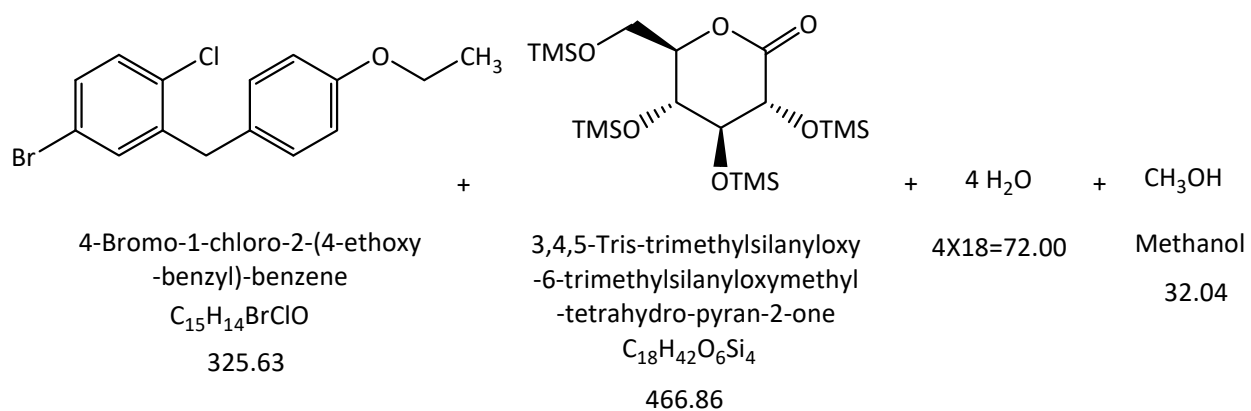
$C_{18}H_{42}O_6Si_4$   
466.86



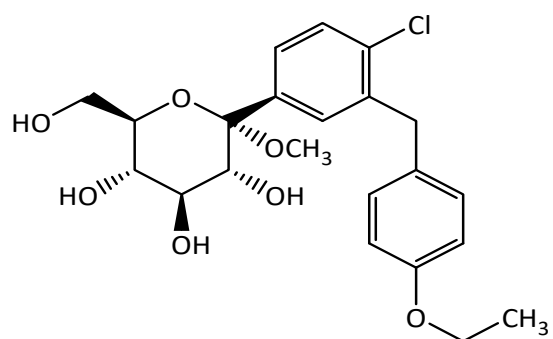
N-Methyl morpholine  
Hydrochloride

$C_5H_{12}ClNO$   
 $4 \times 137.61 = 550.44$

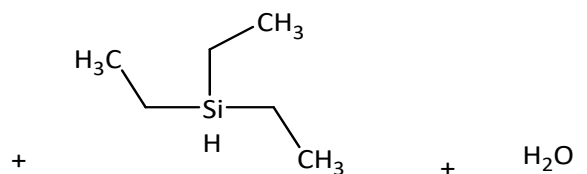
## Stage-2



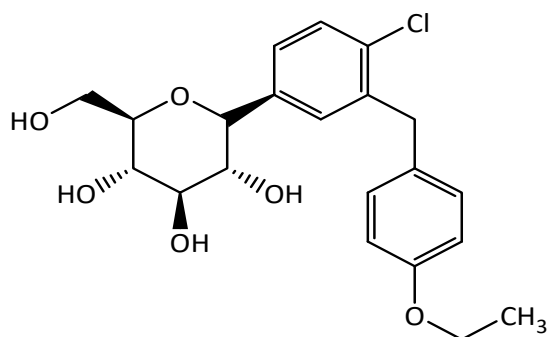
### Stage-3



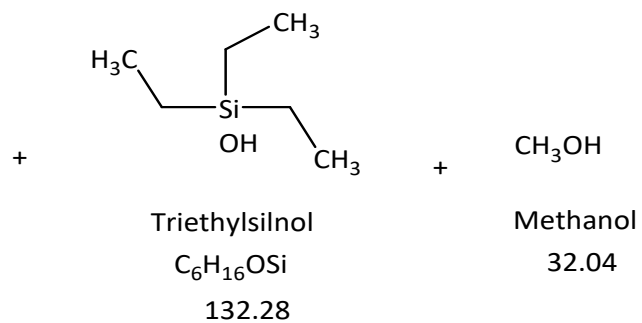
2-[4-Chloro-3-(4-ethoxy-benzyl)-phenyl]-6-hydroxymethyl-2-methoxy-tetrahydro pyran-3,4,5-triol  
 $C_{22}H_{27}ClO_7$   
438.90



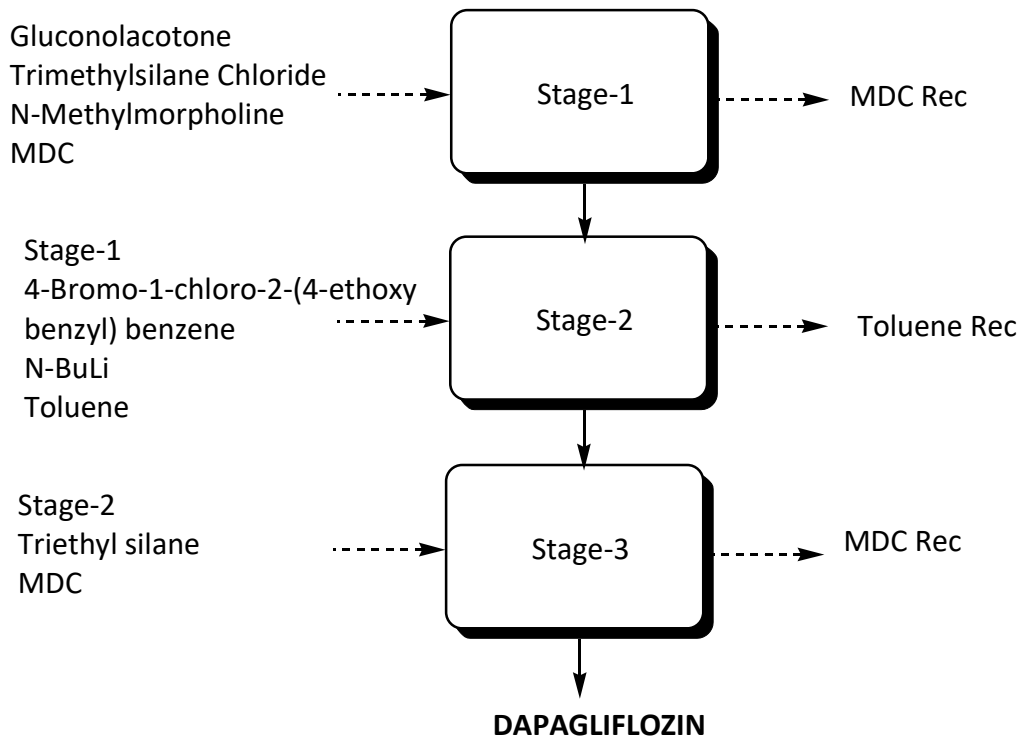
Triethylsilane  
 $C_6H_{16}Si$   
116.28



Dapagliflozin Tech  
 $C_{21}H_{25}ClO_6$   
408.87



## Flow Chart



## Material Balance

Material Balance of Dapagliflozin Stage-1 Batch Size: 50.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
3,4,5-trihydroxy-6-hydroxymethyl-tetrahydro-pyran-2-one	25.00	Stage-1	62.00
Trimethylsilane Chloride	59.00	MDC Recovery	285.00
N-Methylmorpholine	55.00	MDC Loss	10.00
MDC	300.00	Toluene Recovery	150.00
Toluene	160.00	Toluene Loss	5.00
Sod.Dihydrogen phosphate	2.00	Effluent water – 229.78 (Water-150, Sod. Di hydrogen phosphate-2, Sodium chloride-2, N-Methyl morpholine HCl-74.78 Toluene-3)	231.78
Sodium chloride	2.00		
Water	150.00	Organic Residue – 9.22 (Process residue -2.22 Distillation residue –7 MDC-5, Toluene – 2)	9.22
Total	753.00	Total	753.00

Material Balance of Dapagliflozin

Stage-2

Batch Size: 50.0Kgs

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	62.00	Stage-2	56.00
4-Bromo-1-chloro-2-(4-ethoxy benzyl) benzene	43.00	Methanol Recovery	280.00
N-BuLi	10.00	Methanol Loss	10.00
Methanol	300.00	Toluene Recovery	230.00
Toluene	250.00	Toluene Loss	10.00
THF	250.00	THF Recovery	230.00
n-Hexane	95.00	THF Loss	10.00
Water	400.00	n-Hexane Recovery	90.00
	0	n-Hexane Loss	2.00
	0	Effluent water	463.14
	0	(Water-390.53, Trimethyl silane-47.61, Toluene – 5, THF-5, n-Hexane – 2, Methanol-3, N-Buli-10)	
	0	Process Emissions	12.74
	0	(Oxygen-2.10, Hydrogen Bromide -10.64)	
	0	Organic Residue – 16.12	16.12
	0	(Process residue -3.12 ,Distillation residue - 1 Toluene-5, n-Hexane- 1, THF-5, Methanol-2)	
Total	1410.00	Total	1410.00

Material Balance of Dapagliflozin

Stage-3

Batch Size: 50.0Kgs

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	56.00	Dapagliflozin	50.00
Triethyl silane	15.000	Acetonitrile Recovery	284.00
Acetonitrile	300.00	Acetonitrile Loss	15.00
MDC	300.00	MDC Recovery	285.00
Sodium bicarbonate	6.00	MDC Loss	15.00
Sodium chloride	6.00	Effluent water (Water-297.74, Triethylsilnol-16.67, Methanol-4.03, , Sodiumbicarbonate-6, Sodiumchloride-6)	330.44
Water	300.00	Organic Residue – 3.56 (Process residue -2.56 Distillation residue – 1 (Acetonitrile-1))	3.56
<b>Total</b>	<b>983.00</b>	<b>Total</b>	<b>983.00</b>

## 6. DAPOXETINE HYDROCHLORIDE

### Process Description:

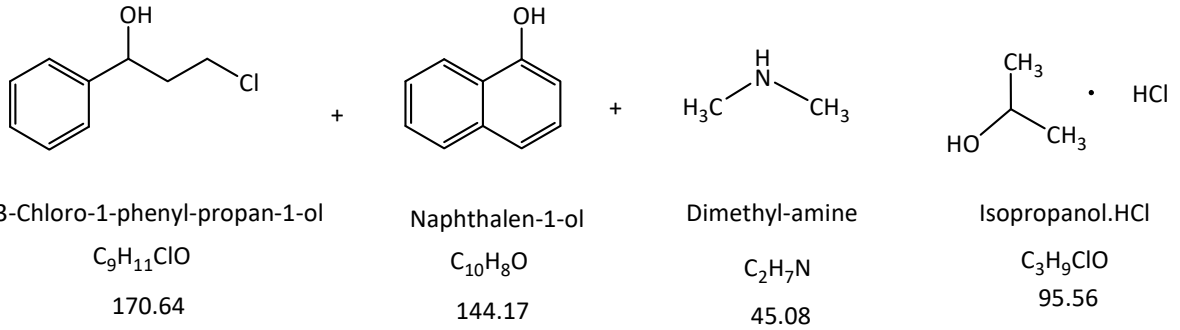
#### Stage-1

(S)-3-Chloro-1-phenyl propan-1-ol reacts with 1-Naphthol in the presence of Di methyl amine and Isopropanol HCl in the presence of Methanol as a solvent media to give Dapoxetine Hydrochloride as product.

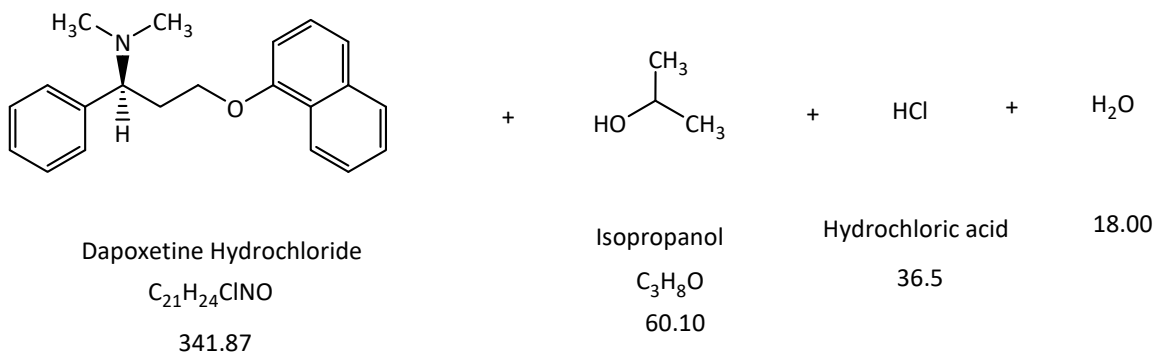
## DAPOXETINE HYDROCHLORIDE

### Route of Synthesis:

#### Stage -1:

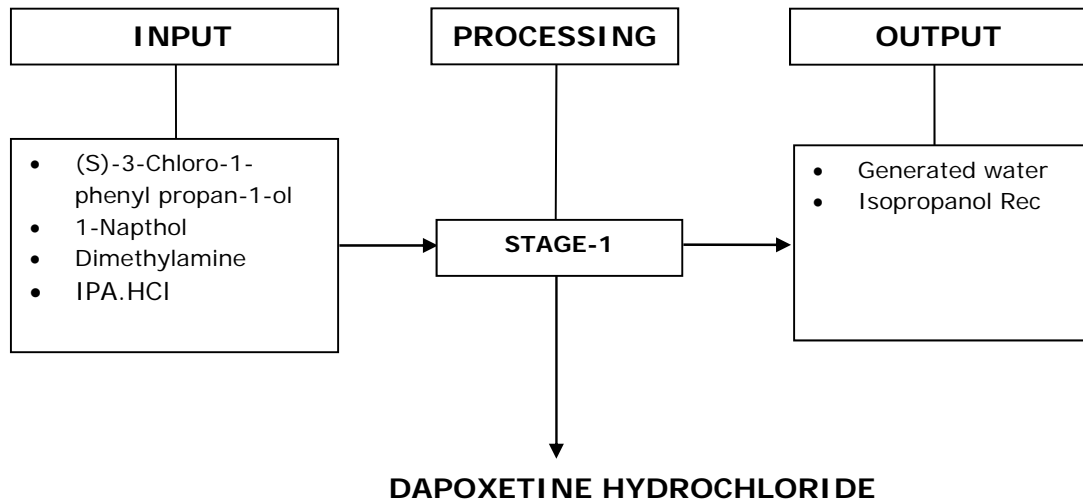


↓ Methanol



# DAPOXETINE HYDROCHLORIDE

## Flow Chart:



## DAPOXETINE HYDROCHLORIDE

### Material Balance:

MATERIAL BALANCE OF DAPOXETINE HYDROCHLORIDE			
STAGE-1			
BATCH SIZE: 80.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
(S)-3-Chloro-1-phenyl propan-1-ol reacts	40.00	Dapoxetine Hydrochloride	80.00
1-Naphthol	34.00	Methanol Recovery	943.00
Dimethylamine	10.56	Methanol Loss	40.00
IsopropanolHCl	22.4	Ethyl acetate Recovery	1334.75
Dimethyl sulfoxide	280.00	Ethyl acetate Loss	70.25
Sodium chloride	34.00	Effluent water	3315.82
Mesyl chloride	50.00	(Water-2925,Generated water-4.22,Isopropanol-14.08,Mesyl chloride-50, N,N-Dimethyl amino pyridine - 0.02,HCl-8.5,DMSO-280,Sodium chloride-32, Methanol-2)	0
Triethylamine	126.00	Triethylamine Recovery (For Reuse)	126.00
N,N-Dimethyl amino pyridine	0.02	Spent carbon	14.00
Methanol	995.00	Organic Residue	12.16
Ethyl acetate	1405.00	(Methanol-10)	
Activated carbon	14.00	Process residue- 2.16	
Water	2925.00		
<b>Total</b>	<b>5935.98</b>	<b>Total</b>	<b>5935.98</b>

## 7. DARUNAVIR ETHANOLATE

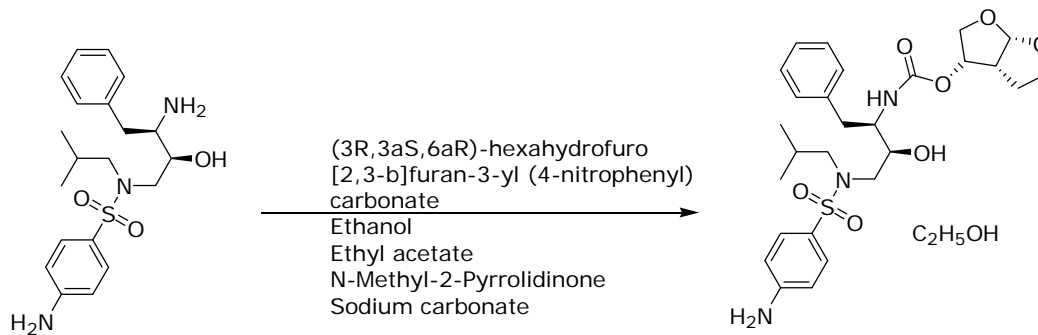
### Process Description

#### Stage-1

4-Amino-N-((2S,3S)-3-amino-2-hydroxy-4-phenylbutyl)-N-isobutylbenzenesulfonamide reacts with (3R,3aS,6aR)-Hexahydrofuro [2,3-b]furan-3-yl (4-nitrophenyl) carbonate in presence of Ethanol, N-Methyl-2-Pyrrolidinone, Sodium Carbonate and Sodium Chloride. After completion of reaction Ethyl Acetate and purified water were added to the reaction mass, organic layer was filtered and purified by using Ethanol to form the Darunavir Ethanolate.

### Route of synthesis

#### Stage-1



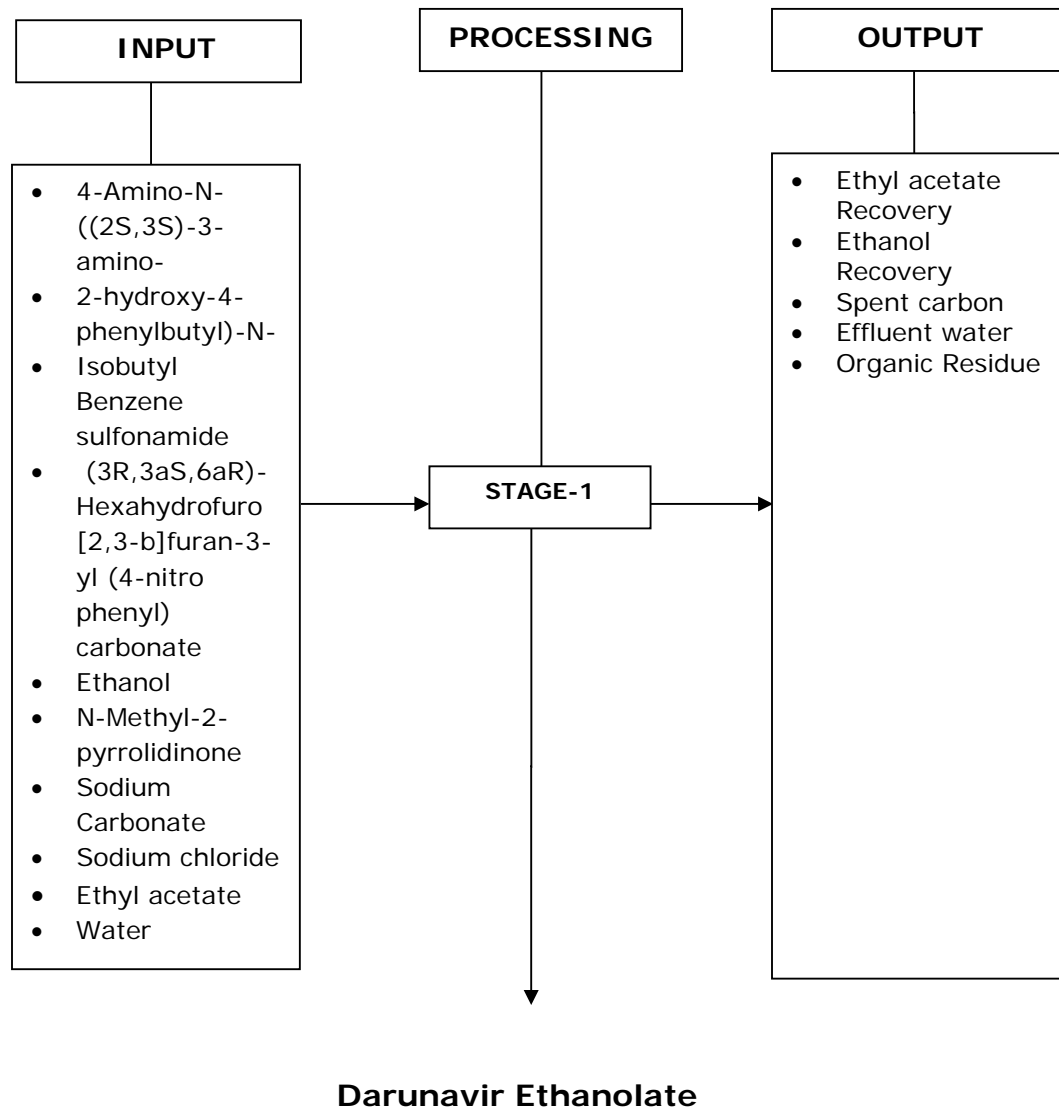
4-amino-N-((2S,3R)-3-amino-2-hydroxy-4-phenylbutyl)-N-isobutylbenzenesulfonamide

C<sub>20</sub>H<sub>29</sub>N<sub>3</sub>O<sub>3</sub>S  
391.53

**Darunavir Ethanolate**

C<sub>29</sub>H<sub>43</sub>N<sub>3</sub>O<sub>8</sub>S  
593.73

## Flow Chart



**Material Balance:**

<b>Material balance of Darunavir Ethanolate                      Stage-1                      Batch Size: 100.0Kg</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
(3R,3aS,6aR)-Hexahydrofuro [2,3-b]furan-3-yl (4-nitrophenyl) carbonate	83.95	Darunavir Ethanolate	100
4-Amino-N-((2S,3S)-3-amino-2-hydroxy-4-phenylbutyl)-N-isobutylbenzenesulfonamide	109.44	Solvent Recovery	0
Ethanol	329.83	• N-Methyl-2-Pyrrolidinone	211.39
Ethyl acetate	1094.45	• N-Methyl-2-Pyrrolidinone loss	8.99
N-Methyl-2-Pyrrolidinone	224.88	• Ethyl acetate	1039
Sodium Carbonate	29.98	• Ethyl acetate loss	53.45
Sodium Chloride	16.49	• Ethanol	313.34
Water	554.72	• Ethanol loss	14.392
		Effluent Water	613.84
		<ul style="list-style-type: none"> <li>• Sodium chloride-16.49</li> <li>• p- Nitrophenol-6.65</li> <li>• Sodium carbonate-29.98</li> <li>• N-methyl pyrrolidinon-4.5</li> <li>• Ethano-2</li> <li>• Ethyl acetate-2</li> <li>• Water -554.72</li> </ul>	0
		Organic residue	89.34
		<ul style="list-style-type: none"> <li>• Unreacted Organic impurities</li> <li>• Organic impurities Ethyl acetate</li> </ul>	0
<b>Total</b>	<b>2443.74</b>	<b>Total</b>	<b>2443.742</b>

## 8. EMPAGLIFLOZIN

### Process Description:

#### Stage-1:

2-Chloro-5-iodo-benzoic acid reacts with fluorobenzene in presence of Toluene to give stage-1 product.

#### Stage-2:

Stage-1 product reacts with Tetrahydro-furan-3-ol in presence of Toluene to give stage-2 product.

#### Stage-3:

Stage-2 product undergoes reduction with sodium borohydride in presence of THF and Aluminium chloride to give stage-3 product.

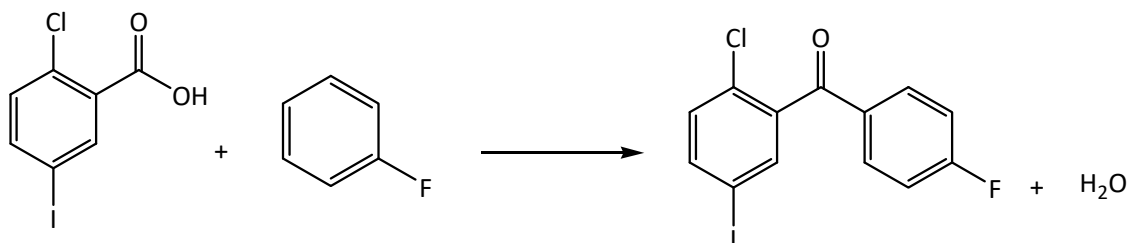
#### Stage-4:

Stage-3 product reacts with 3,4,5-Tris-trimethylsilyloxy-6-trimethylsilyloxymethyl-tetrahydro-pyran-2-one in presence of Acetonitrile, MDC and Methanol to give Empagliflozin.

## EMPAGLIFLOZIN

### Route of synthesis:

#### Stage-1



2-Chloro-5-iodo-  
benzoic acid

C<sub>7</sub>H<sub>4</sub>ClIO<sub>2</sub>

282.46

Fluoro-benzene

C<sub>6</sub>H<sub>5</sub>F

96.10

(2-Chloro-5-iodo-phenyl)-  
(4-fluoro-phenyl)-  
methanone

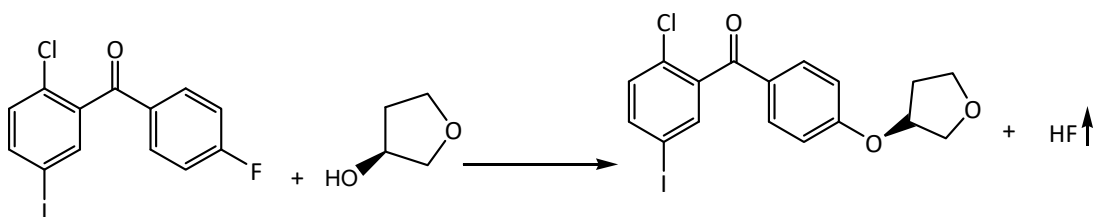
C<sub>13</sub>H<sub>7</sub>ClFIO

360.55

18.02

+ H<sub>2</sub>O

#### Stage-2



(2-Chloro-5-iodo-phenyl)-  
(4-fluoro-phenyl)-  
methanone

C<sub>13</sub>H<sub>7</sub>ClFIO

360.55

Tetrahydro-  
furan-3-ol

C<sub>4</sub>H<sub>8</sub>O<sub>2</sub>

88.11

(2-Chloro-5-iodo-phenyl)-[4-  
(tetrahydro-furan-3-yloxy)-  
phenyl]-methanone

C<sub>17</sub>H<sub>14</sub>ClIO<sub>3</sub>

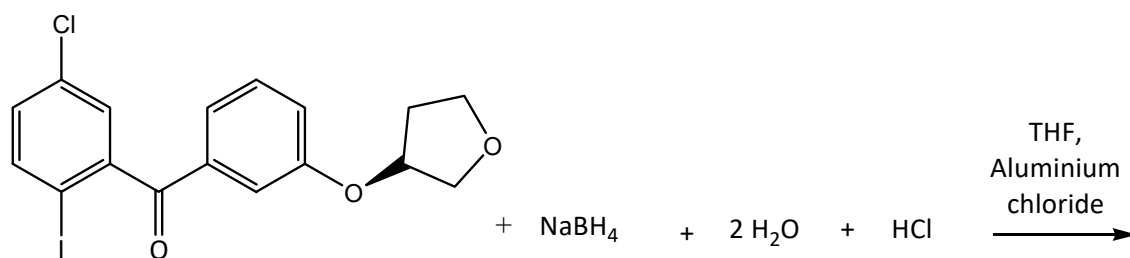
428.65

Hydrogen  
fluoride

20.01

+ HF↑

### Stage-3



(5-Chloro-2-iodo-phenyl)-  
[3-(tetrahydro-furan-3-yloxy)-  
phenyl]-methanone

$C_{17}H_{14}ClIO_3$

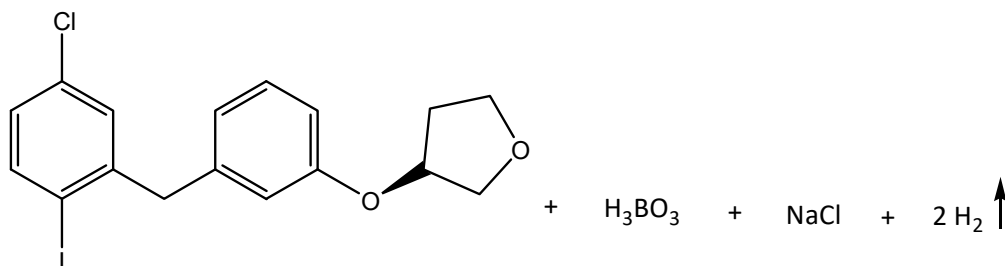
428.65

Sodium  
borohydride

36.03

36.46

37.83



3-[3-(5-Chloro-2-iodo-benzyl)-  
phenoxy]-tetrahydro-furan

$C_{17}H_{16}ClIO_2$

414.67

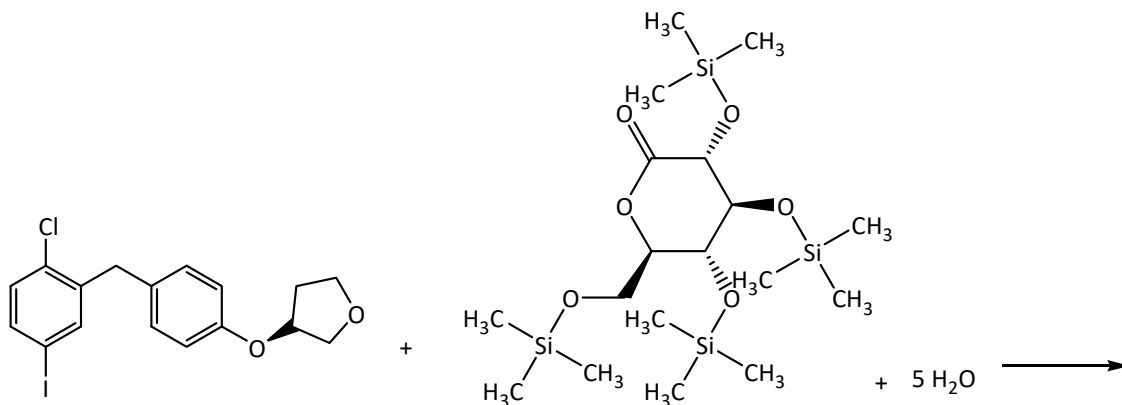
Boric acid

58.44

4.03

61.83

**Stage-4**



3-[4-(2-Chloro-5-iodo-benzyl)-  
phenoxy]-tetrahydro-furan

$C_{17}H_{16}ClIO_2$

414.67

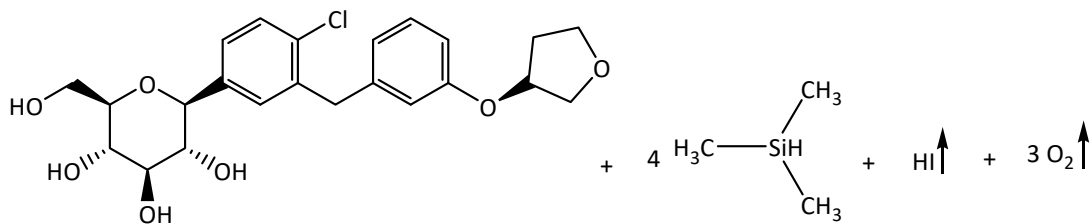
3,4,5-Tris-trimethylsilyloxy-  
6-trimethylsilyloxymethyl-  
tetrahydro-pyran-2-one

$C_{18}H_{42}O_6Si_4$

466.86

90.08

+ 5 H<sub>2</sub>O



Empagliflozin

$C_{23}H_{27}ClO_7$

450.91

Trimethyl silane

$C_{12}H_{40}Si_4$

4x74.20=296.8

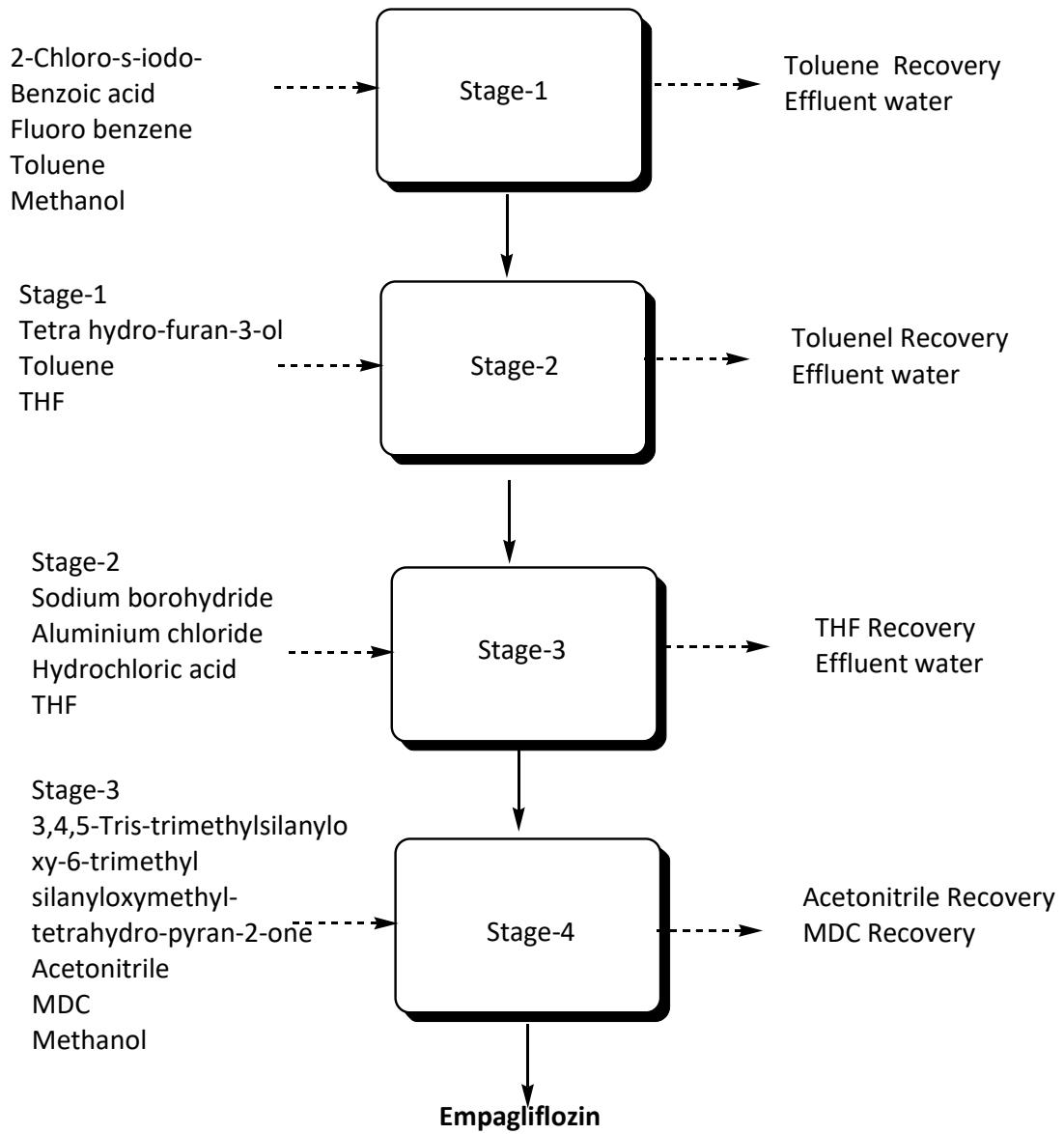
127.91

96.00

+ HI↑ + 3 O<sub>2</sub>↑

# EMPAGLIFLOZIN

## Flowchart:



## EMPAGLIFLOZIN

### Material Balance:

Material Balance of Empagliflozin Stage1 Batch Size: 100.0 Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
2-Chloro-s-iodo-Benzoic acid	72.00	Stage-1	90.00
Fluoro benzene	25.00	Toluene Recovery	275.00
Toluene	300.00	Toluene Loss	10.00
Methanol	300.00	Methanol Recovery	275.00
Water	500.00	Methanol Loss	10.00
		Effluent Water – 521 (Water- 500, generated water - 5, Toluene – 8, Methanol – 8)	521.00
		Organic Residue – 16 (process residue -2, Distillation residue – 14 Methanol- 7, Toluene -7)	16.00
<b>Total</b>	<b>1197.00</b>	<b>Total</b>	<b>1197.00</b>

Material Balance of Empagliflozin Stage 2 Batch Size: 100.0 Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	90.00	Stage-2	105.00
Tetra hydro-furan-3-ol	22.00	Toluene Recovery	275.00
Toluene	300.00	Toluene Loss	10.00
THF	300.00	THF Recovery	275.00
Water	500.00	THF Loss	10.00
		Effluent Water – 516 (Water- 500, Toluene – 8, THF – 8)	516.00
		Process emission (Hydrogen fluoride – 4.99)	4.99
		Organic Residue – 16.01 (process residue -2.01, Distillation residue – 14 THF- 7, Toluene -7)	16.01
<b>Total</b>	<b>1212.00</b>	<b>Total</b>	<b>1212.00</b>

Material Balance of Empagliflozin			
Stage 3			
Batch Size: 100.0 Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	105.00	Stage-3	100.00
Sodium borohydride	9.50	THF Recovery	275.00
Aluminium chloride	10.00	THF Loss	10.00
Hydrochloric acid	9.00	Effluent Water – (Water- 491, THF – 8, boric acid – 15.14, sodium chloride – 14.32, Aluminium chloride -10)	538.46
THF	300.00	Process emission (Hydrogen-1.)	1.00
Water	500.00	Organic Residue – 9.04 (process residue -2.04, Distillation residue – 7 THF- 7)	9.04
Total	933.50	Total	933.50

Material Balance of Empagliflozin			
Stage 4			
Batch Size: 100.0 Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-3	100.00	Empagliflozin	100.00
3,4,5-Tris-trimethylsilanyloxy-6-trimethylsilanyloxymethyl-tetrahydro-pyran-2-one	109.00	Acetonitrile Recovery	275.00
Acetonitrile	300.00	Acetonitrile loss	15.00
MDC	300.00	MDC recovery	275.00
Methanol	300.00	MDC Loss	15.00
Water	500.00	Methanol Recovery	275.00
		Methanol Loss	15.00
		Effluent Water – (Water- 475, Methanol-7, Acetonitrile – 7, Trimethylsilane -69.2)	558.20
		Process emission (Hydrogen Iodide – 29.84, Oxygen- 29.86.)	59.70

		Organic Residue – 21.10 (process residue -5.10 Distillation residue – 16 Acetonitrile -3, Methanol- 3, MDC-10)	21.10
Total	1609.00	Total	1609.00

## 9. ETODOLAC

### Process Description

#### Stage – 1

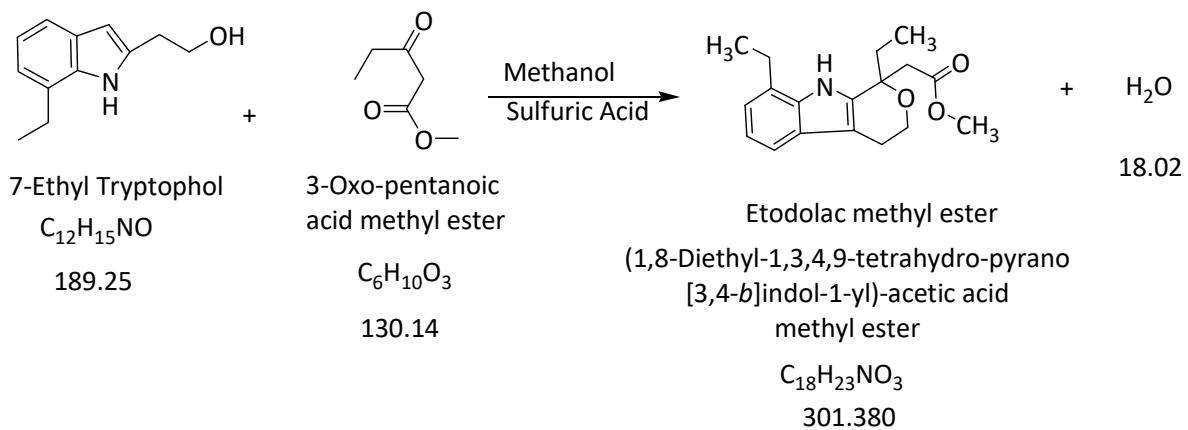
2(3a Ethyl-3aH- indol-3-yl)-ethanol reacts with 3-Oxo pentanoic acid methyl ester in presence of Methanol and Sulphuric acid to give stage -1 product

#### Stage – 2

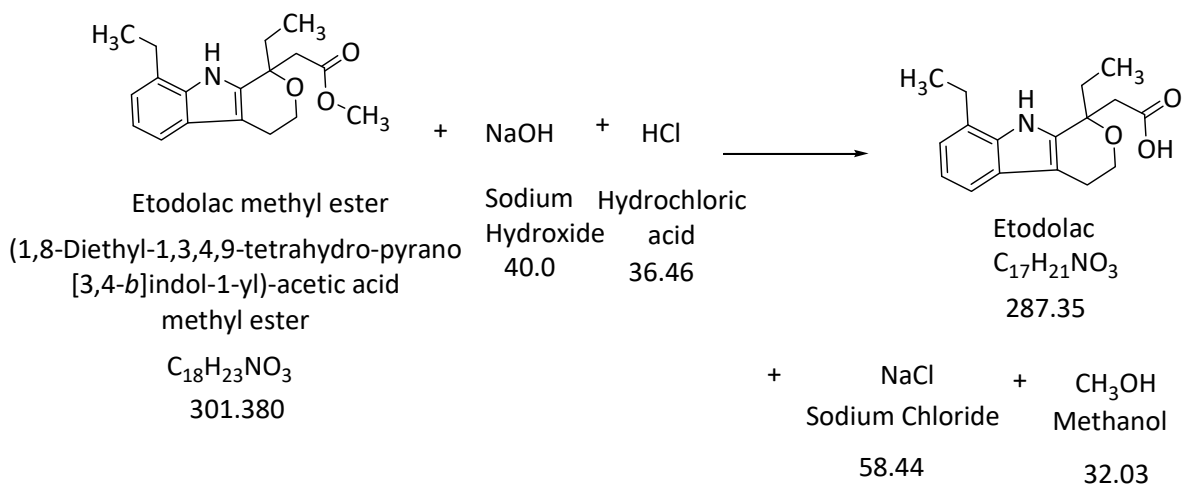
Stage -1 product undergoes Hydrolysis with Sodium hydroxide in presence of Water, Methanol and HCl to give **Etodolac** product

## Route of Synthesis:

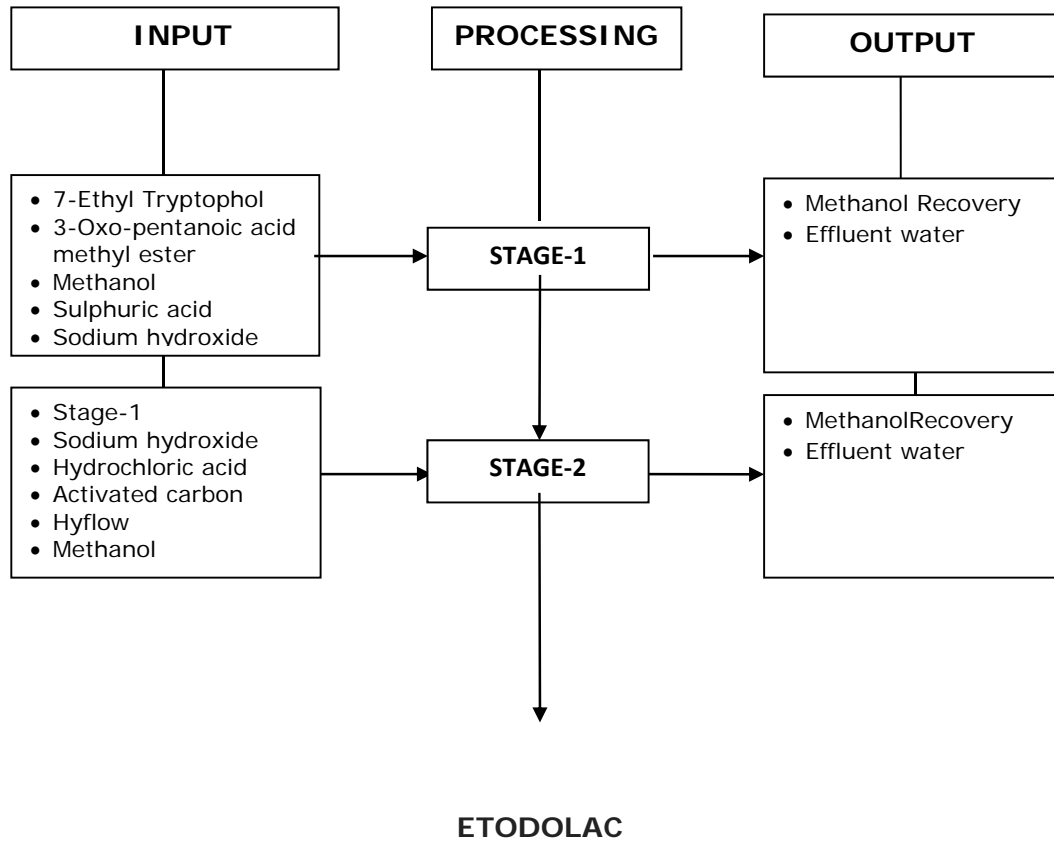
### Stage-1



### Stage-2



**Flow Chart:**



## ETODOLAC

### Material Balance:

MATERIAL BALANCE OF ETODOLAC			
STAGE-1			
BATCH SIZE: 200.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
7-Ethyl Tryptophol	160.00	Stage-1	234.00
3-Oxo-pentanoic acid methyl ester	110.00	Methanol Recovery	475.00
Methanol	500.00	Methanol Loss	20.00
Sulphuric acid	24.00	Effluent water	595.20
Sodium hydroxide	100.00	(Water-500, Generated water-15.20, Sodium hydroxide-80)	
Water	500.00	Inorganic Residue	44.00
		(Sodium sulphate)	
		Organic residue	25.80
		Process Residue-20.80 Distillation Residue-5 (Methanol)	
<b>Total</b>	<b>1394.00</b>	<b>Total</b>	<b>1394.00</b>

**MATERIAL BALANCE OF ETODOLAC****STAGE-2  
BATCH SIZE: 200.0 KGS**

<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-1	234.00	Etodolac	200.00
Sodium hydroxide	30.00	Methanol Recovery	262.80
Hydrochloric acid	28.00	Methanol Loss	10.00
Activated carbon	15.00	Effluent water	845.16
Hyflow	3.00	(Water-800, Sodium chloride- 45.16)	0
Methanol	250.00	Spent Carbon & Hyflow	18.00
Water	800.00	Organic residue	24.04
		Process residue -22.02 Distillation residue-2.2 (Metahnol)	
<b>Total</b>	<b>1360.00</b>	<b>Total</b>	<b>1360.00</b>

## 10. ETORICOXIB

### Process Description:

#### Stage-1

Thioanisole react with Acetyl chloride in presence of EDC as a solvent media to give as stage-1 as product.

#### Stage-2

Stage-1 product reacts with sulphur in presence of sodium hydroxide to give Stage-2 as a product.

#### Stage-3

Stage-2 product reacts with Methyl-6-methyl Nicotinate in presence of Tetra hydro furan as a solvent media to give Stage-3 as a product.

#### Stage-4

Chloro acetyl chloride reacts with Dimethyl formamide & Phosphorus oxychloride in presence of THF as a solvent media to give Stage-4 as a product.

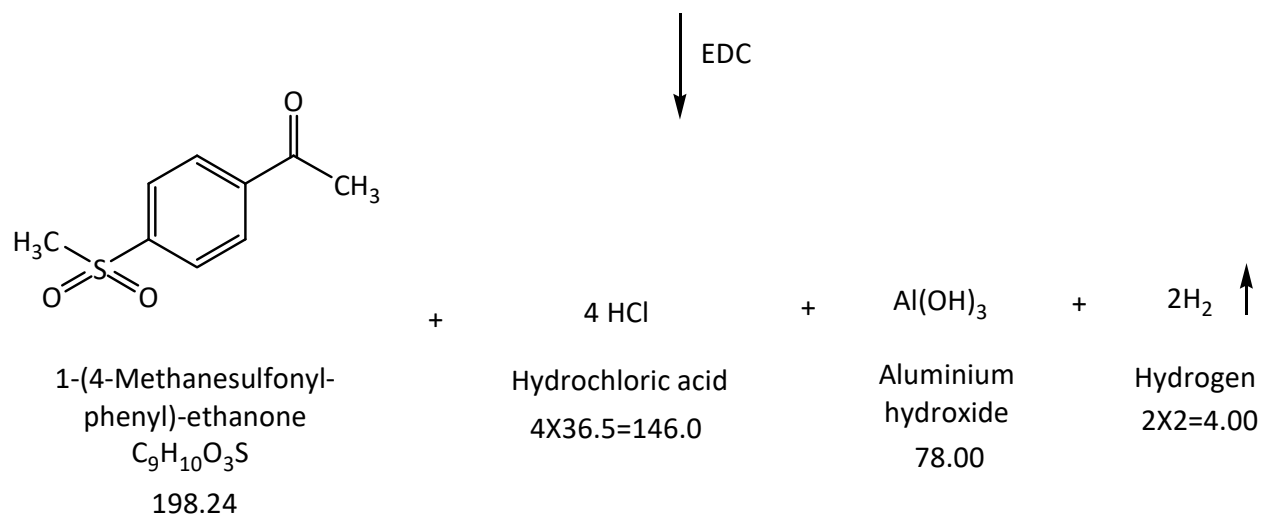
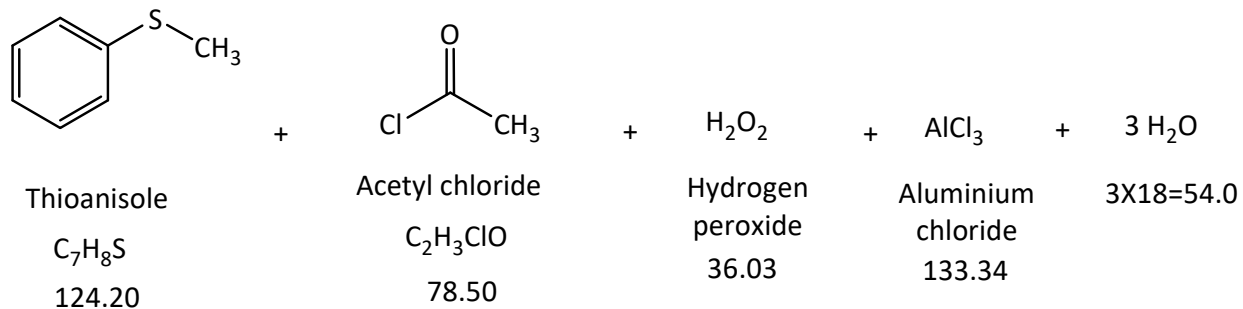
#### Stage-5

Stage-3 & Stage-4 product condensed in presence of toluene as a solvent media to give Etoricoxib as a product.

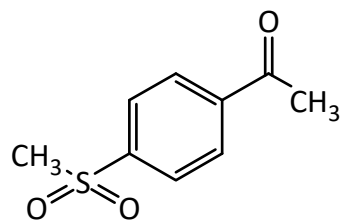
## ETORICOXIB

### Route of synthesis:

#### Stage-1:



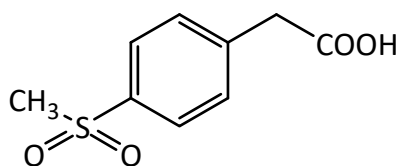
**Stage-2:**



1-(4-Methanesulfonyl-  
phenyl)-ethanone  
 $C_9H_{10}O_3S$   
198.24



Sulphur 32.06  
NaOH 40.00  
4 H<sub>2</sub>O 72.06

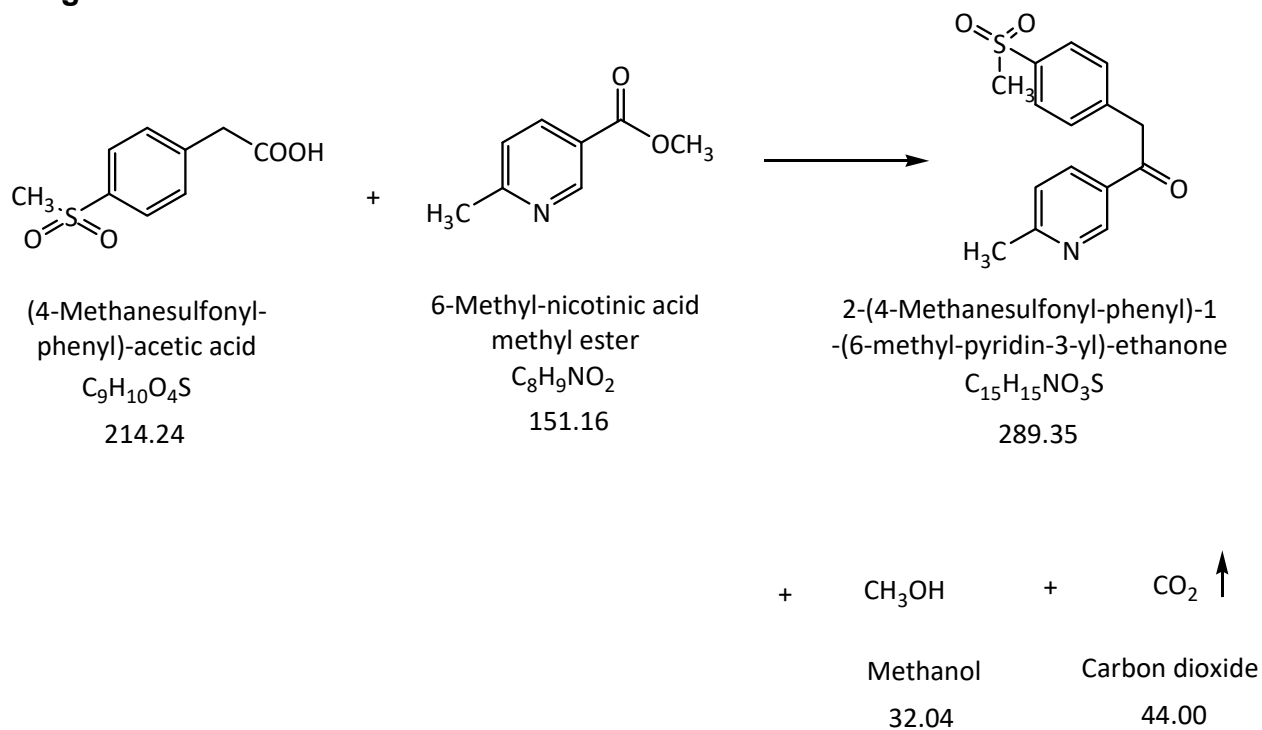


(4-Methanesulfonyl-  
phenyl)-acetic acid  
 $C_9H_{10}O_4S$   
214.24

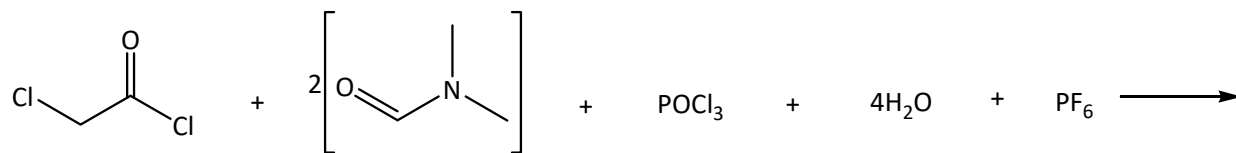


Sodium bi sulphate 120.06  
8.06

**Stage-3:**



**Stage-4:**



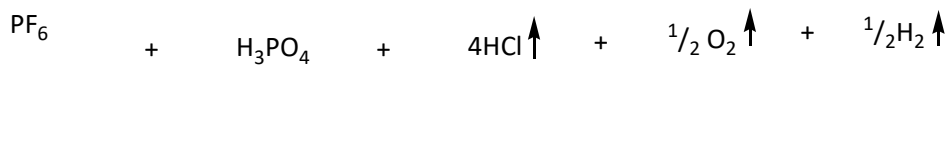
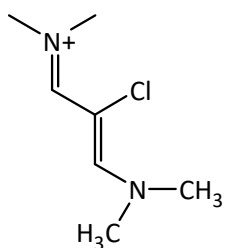
Chloroacetyl chloride  
 $\text{C}_2\text{H}_2\text{Cl}_2\text{O}$   
 112.94

Dimethyl formamide  
 $\text{C}_3\text{H}_7\text{NO}$   
 $2 \times 73.09 = 146.18$

Phosphorous  
 oxychloride  
 153.33

$4 \times 18 = 72.06$

Phosphorus  
 Hexafluoride  
 144.96



(2-Chloro-3-dimethylamino-allylidene)-dimethyl-ammonium salt of Phosphorus Hexafluoride  
 $\text{C}_7\text{H}_{14}\text{ClN}_2 \cdot \text{PF}_6$   
 306.62

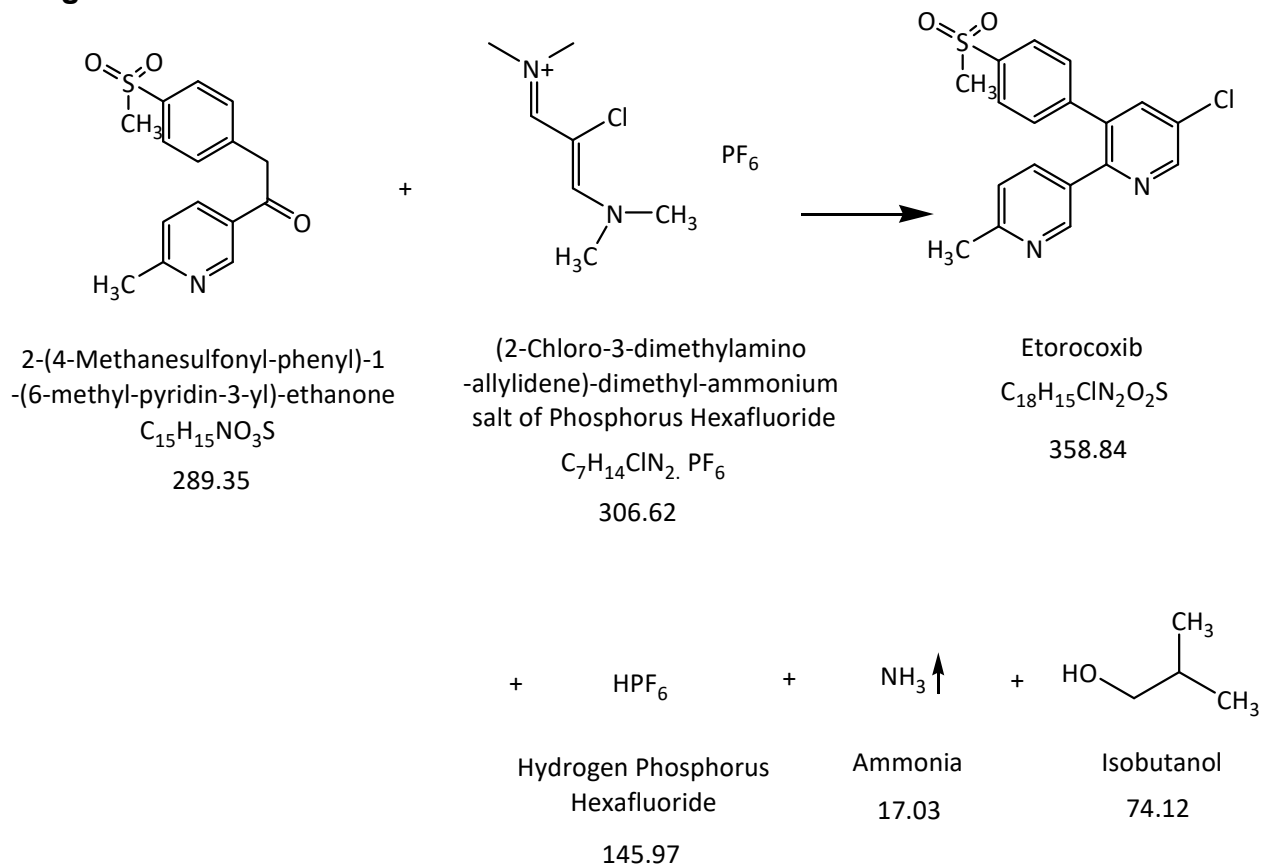
Phosphoric acid  
 98

Hydrogen chloride  
 $145.84$

Oxygen  
 $\frac{1}{2} \times 32 = 16.0$

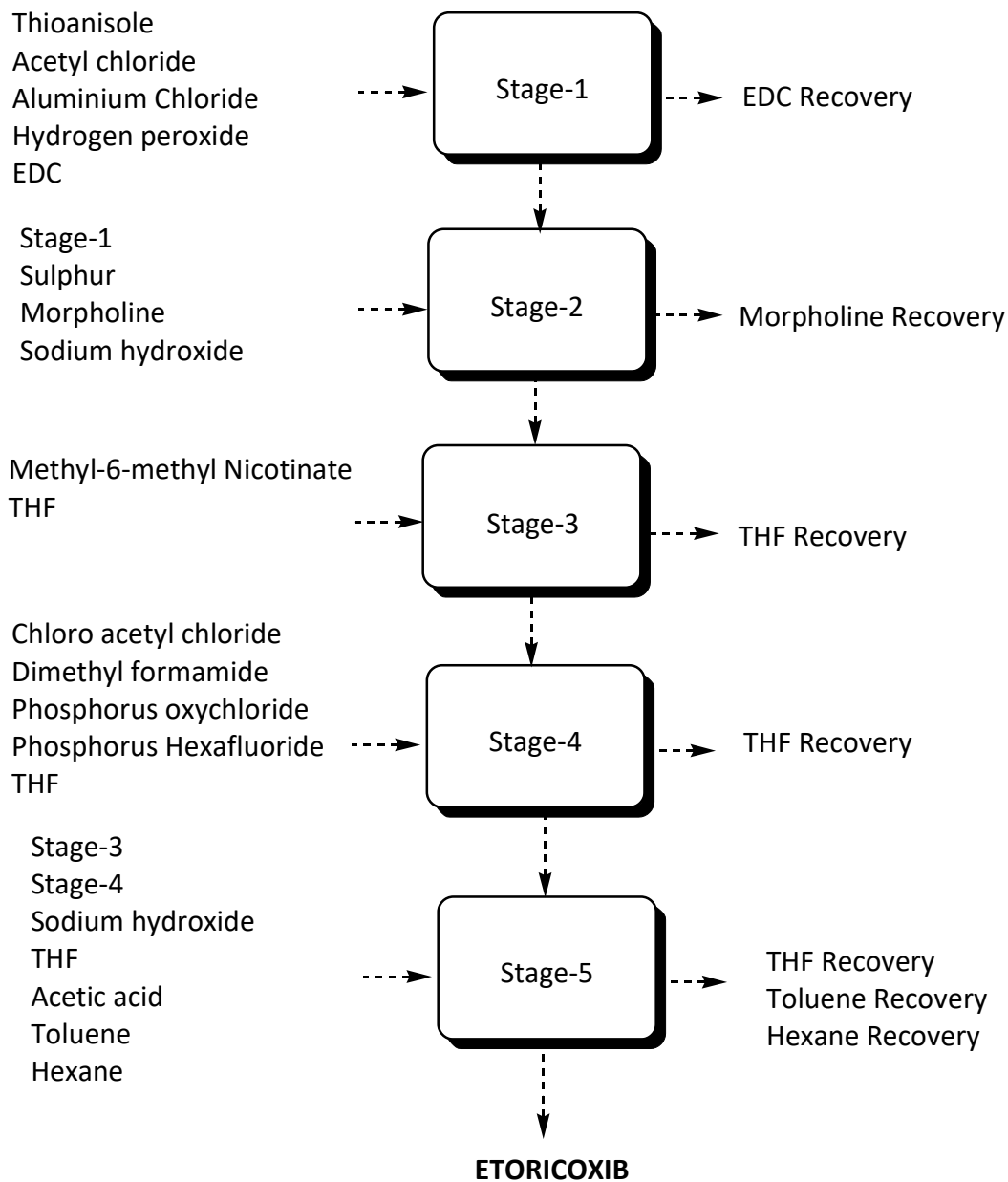
Hydrogen  
 $\frac{1}{2} \times 2 = 1.0$

**Stage-5:**



# ETORICOXIB

## Flow Chart:



## ETORICOXIB

### Material Balance:

Material Balance of Etoricoxib Stage-1 Batch Size:100.0Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Thioanisole	36.00	Stage-1	56.00
Acetyl chloride	23.00	EDC Recovery	238.00
Aluminium Chloride	39.00	EDC Loss	5.00
Hydrogen peroxide	10.50	Effluent water	506.95
EDC	250.00	(Water-484.35 , Aluminium hydroxide-22.6)	
Water	500.00	Process Emission	43.48
		(Hydrogen-1.16, Hydrogen chloride-42.32)	
		Organic Residue Process residue-2.07 Distillation Residue-7 (EDC)	9.07
<b>Total</b>	<b>858.50</b>	<b>Total</b>	<b>858.50</b>

Material Balance of Etoricoxib Stage-2 Batch Size:100.0Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	56.00	Stage-2	60.00
Sulphur	9.10	Effluent water	413.62
Sodium hydroxide	11.30	(Water-379.7,Sodium bisulphate- 33.92)	
Morpholine	10.00	Process Emission	2.26
Water	400.00	(Hydrogen)	
		Organic Residue Process residue-10.52 (Morpholine-10)	10.52
<b>Total</b>	<b>486.40</b>	<b>Total</b>	<b>486.40</b>

Material Balance of Etoricoxib Stage-3 Batch Size:100.0Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	60.00	Stage-3	81.00
Methyl-6-methyl Nicotinate	42.85	THF Recovery	285.00
THF	300.00	THF Loss	6.00
Water	300.00	Effluent water	308.99
		(Water-300,Methanol-8.99)	0
		Process Emission	12.32
		(Carbon dioxide)	0
		Organic Residue Process residue-0.54 Distillation Residue-9 (THF-9)	9.54
Total	702.85	Total	702.85

Material Balance of Etoricoxib Stage-4 Batch Size:100.0Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Chloro acetyl chloride	32.00	Stage-4	86.00
Dimethyl formamide	41.20	THF Recovery	285.00
Phosphorus oxychloride	43.50	THF Loss	6.00
Phosphorus Hexafluoride	41.00	Effluent water	408.38
THF	300.00	(Water-379.58,Phosphoric acid-27.8 ,THF-1)	
Water	400.00	Process Emissions	46.21
		(Oxygen-4.53,Hydrogen-0.28, Hydrogen chloride-41.4)	
		Organic Residue	26.11
		(Process residue-18.11, Distillation Residue-8 (THF-8)	
Total	857.70	Total	857.70

Material Balance of Etoricoxib  
Stage-5  
Batch Size:100.0Kg

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-3	81.00	Etoricoxib	100.00
Stage-4	86.00	THF Recovery	570.00
Sodium hydroxide	10.00	THF Loss	12.00
THF	600.00	Toluene Recovery	475.00
Acetic acid	20.00	Toluene Loss	10.00
Toluene	500.00	Hexane Recovery	190.00
Hexane	200.00	Hexane Loss	4.00
Activated carbon	2.00	Effluent water	574.73
Water	500.00	(water-500,Hydrogen phosphorus hexafluoride-40.94, Isobutanol-20.79,Toluene- 5,THF-8)	
		Spent carbon	2.00
		Process Emission	4.78
		(Ammonia)	
		Organic Residue	56.49
		(Process tresideu-30.49, Distillation Residue-26 (THF-10,Toluene-10,Hexane-6)	
Total	1999.00	Total	1999.00

## 11. FAMOTIDINE

### Process Description:

#### Stage-1

1, 3-Dichloro acetone reacts with Guanyl thiourea in the presence of Acetone as solvent media to give Stage-2 as product.

#### Stage-2

Stage-1 product reacts with Thiourea, N-Sulfamyl-3-chloropropionamide, Sodium hydroxide and acetic acid in the presence of Methanol as solvent media to give Stage-2 as product.

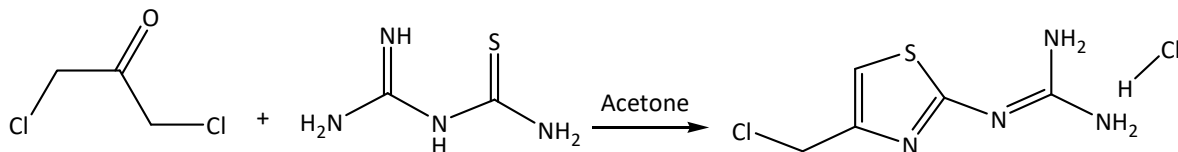
#### Stage-3

Stage-2 product reacts with ammonia in the presence of Methanol as solvent media to give Famotidine as product.

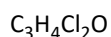
# FAMOTIDINE

## Route of Synthesis:

### Stage-1

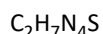


1,3-Dichloro acetone



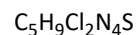
126.97

Guanyl thiourea

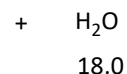


119.16

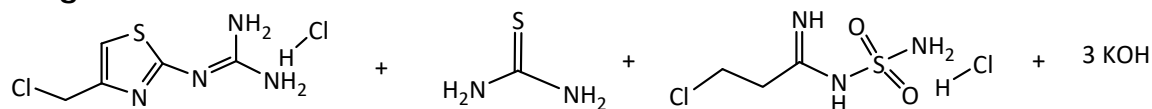
*N*-(4-Chloromethyl-thiazol-2-yl)  
-guanidine; hydrochloride



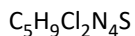
228.15



### Stage-2:



*N*-(4-Chloromethyl-thiazol-2-yl)  
-guanidine; hydrochloride



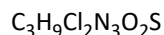
228.15

Thiourea



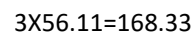
76.12

*N*-Sulfamyl-3-chloropropion  
amide Hydrochloride

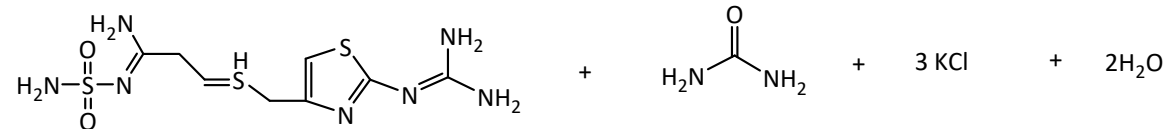


222.13

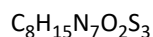
Potassium  
hydroxide



↓  
Methanol



*N*'-(aminosulfonyl)-3-[[[2-[(diaminomethylene)  
amino]-4-thiazolyl]methyl]thio]-  
propanamide acetate

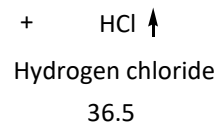


337.45

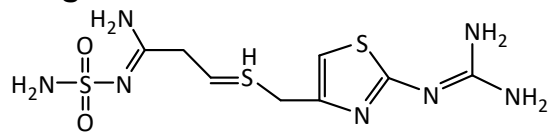
Urea  
60.06

Potassium chloride  
3 × 74.55 = 223.65

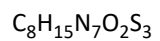
36.0



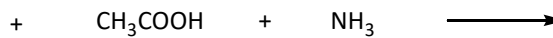
**Stage-3:**



N'-(aminosulfonyl)-3-[[[(2-[(diaminomethylene)amino]-4-thiazolyl)methyl]thio]propanamide



337.45



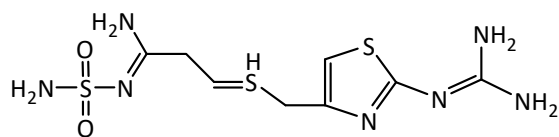
Acetic acid

60.05

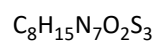
Ammonia

17.0

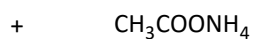
Methanol



Famotidine (Pure)



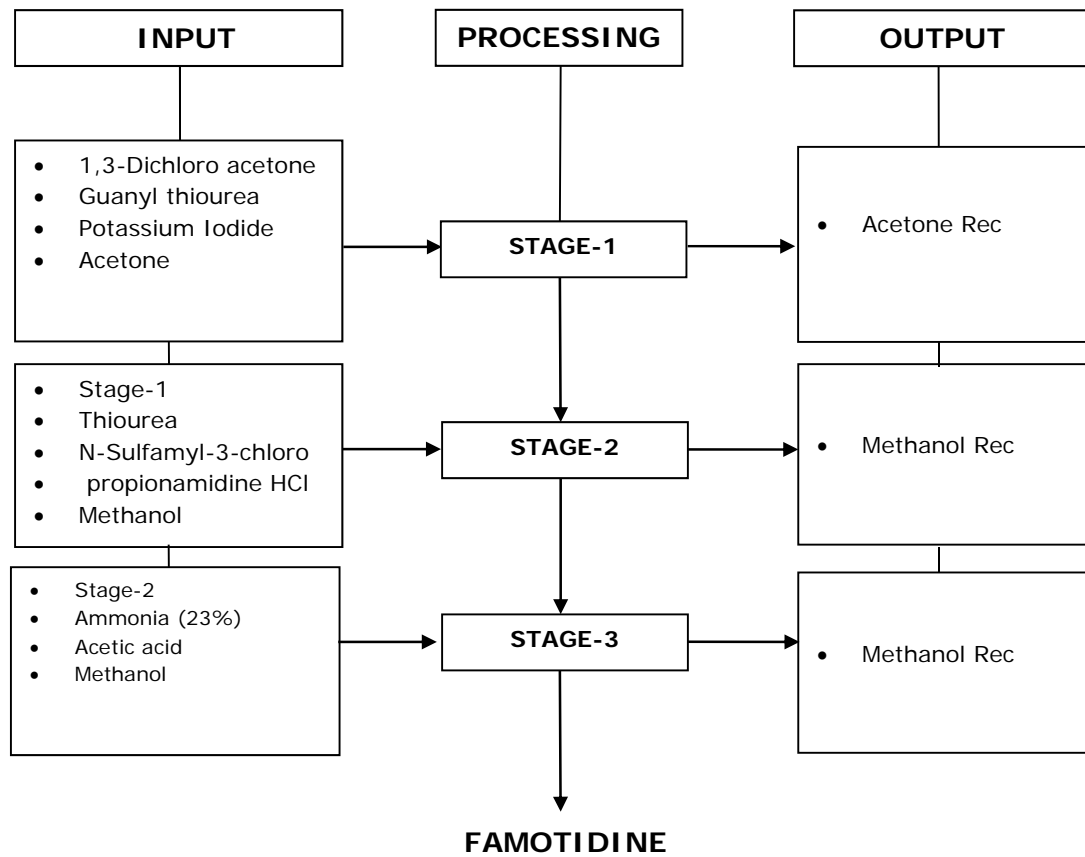
337.45



Ammonium formate

77.08

**Flow Chart:**



**Material Balance:**

<b>MATERIAL BALANCE OF FAMOTIDINE</b>			
<b>STAGE-1</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
1,3-Dichloro acetone	52.00	Stage-1	88.97
Guanyl thiourea	43.48	Acetone Recovery	161.00
Potassium Iodide	2.40	Acetone Loss	8
Acetone	170.00	Generated water	7.51
		Inorganic solid waste	1.40
		(Potassium Iodide)	
		Organic residue	1
<b>Total</b>	<b>267.88</b>	<b>Total</b>	<b>267.88</b>

<b>MATERIAL BALANCE OF FAMOTIDINE</b>			
<b>STAGE-2</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-1	88.97	Stage-2	125.70
Thiourea	25.13	Generated water	12.00
Sodium hydroxide	40.00	Byproduct	53.14
N-Sulfamyl-3-chloro propionamide HCl	68.64	(Potassium chloride )	
		Process Emission	12.10
		(Hydrogen chloride)	
		Urea Solution for Gardening	19.80
<b>Total</b>	<b>222.74</b>	<b>Total</b>	<b>222.74</b>

**MATERIAL BALANCE OF FAMOTIDINE****STAGE-3****BATCH SIZE: 100.0 KGS**

<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-2	125.70	Famotidine	100.00
Ammonia (23%)	17.30	Methanol Recovery	37.00
Acetic acid	5.00	Methanol Loss	1.00
Methanol	39.00	Effluent water	874.00
Activated carbon	3.00	(Water-825, Water from ammonia-18.6, Acetic acid-5, Ammonium acetate-24.4, Methanol-1)	
Water	825.00	Spent carbon	3.00
<b>Total</b>	<b>1015.00</b>	<b>Total</b>	<b>1015.00</b>

## 12. IMATINIB MESYLATE

### Process Description:

#### Stage-1:

o-Tolylamine undergoes nitration with nitric acid in presence of sulphuric acid to give stage-1 product.

#### Stage-2:

Stage-1 product reacts with cyanamide and nitric acid in presence of methanol to give Stage-2 product.

#### Stage-3:

Stage-2 product reacts with 3-dimethyl amino-1-pyridin-3-yl-propenone in presence of n-butanol to give Stage-3 product.

#### Stage-4:

Stage-3 product undergoes hydrogenation with hydrogen in presence of Palladium carbon and Methanol to give Stage-4 product.

#### Stage-5:

Stage-4 product undergoes condensation with 4-(4-methylpiperazin-1-yl)methyl benzoic acid dihydro chloride in presence of MDC to give stage-5 Imatinb product.

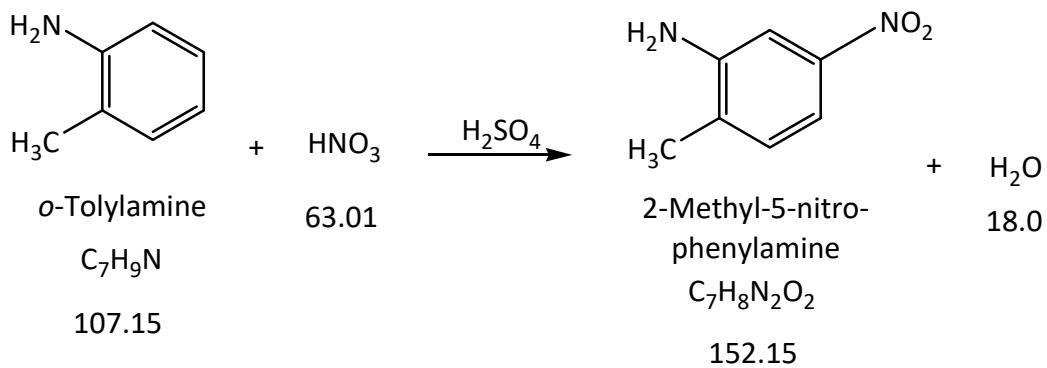
#### Stage-6:

Imatinib product undergoes salt formation with methane sulphonic acid in presence of methanol to give Imatinib Mesylate

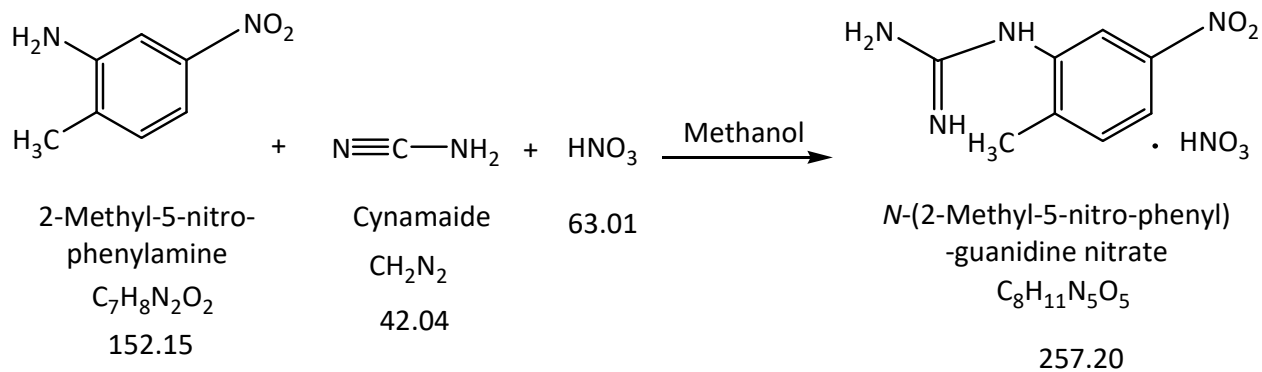
## IMATINIB MESYLATE

### Route of Synthesis:

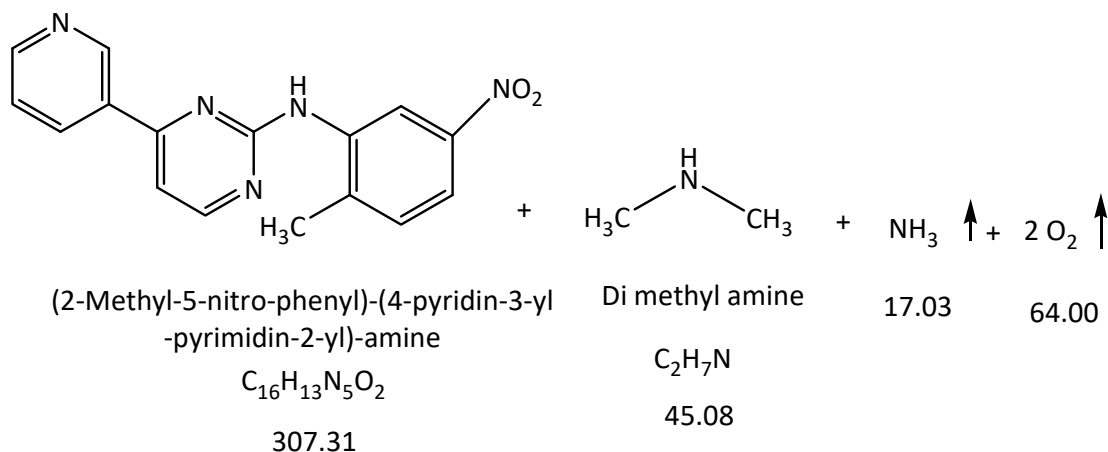
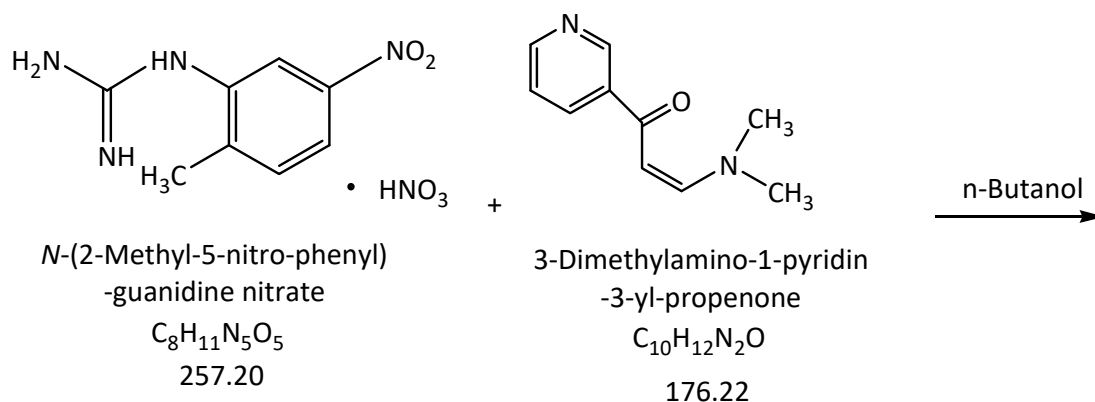
#### Stage-1



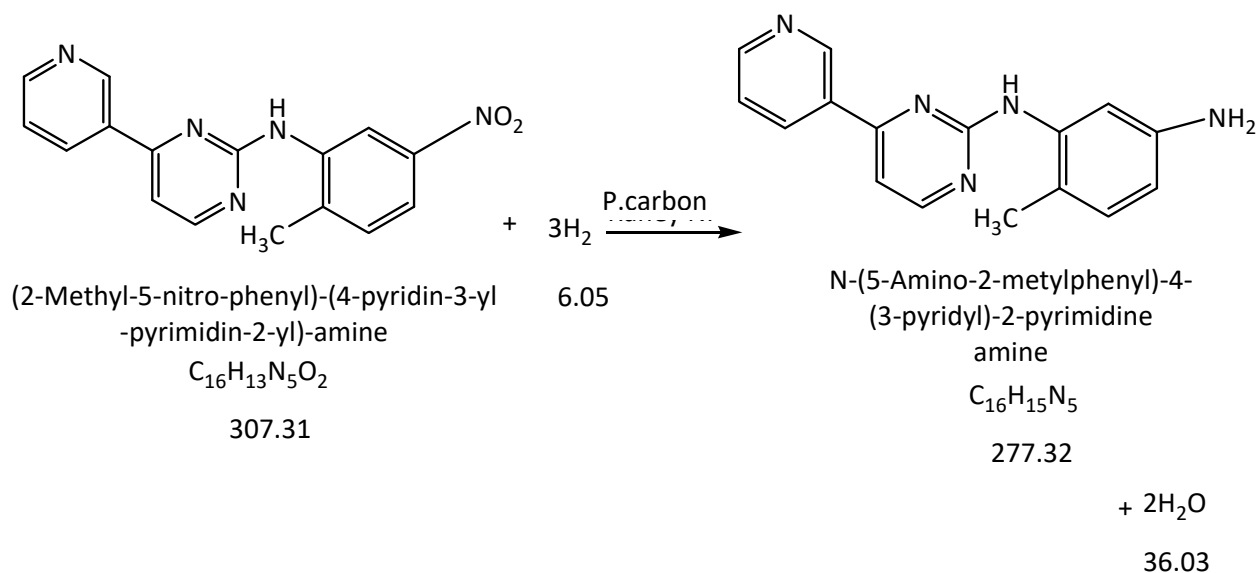
#### Stage-2



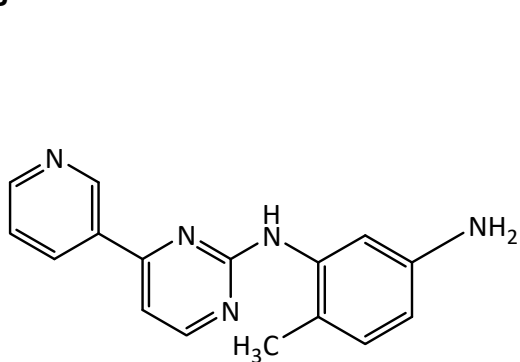
### Stage-3



### Stage-4



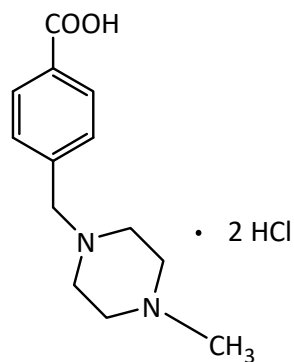
### Stage-5



N-(5-Amino-2-methylphenyl)-4-(3-pyridyl)-2-pyrimidine amine

$C_{16}H_{15}N_5$

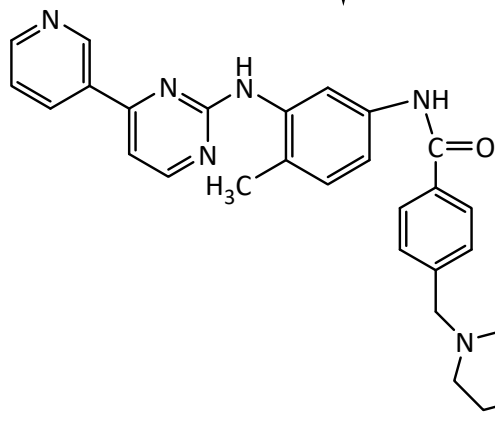
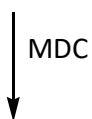
277.32



4-(4-Methylpiperazin-1-yl)methyl benzoic acid dihydrochloride

$C_{13}H_{18}N_2O_2 \cdot 2HCl$

307.22

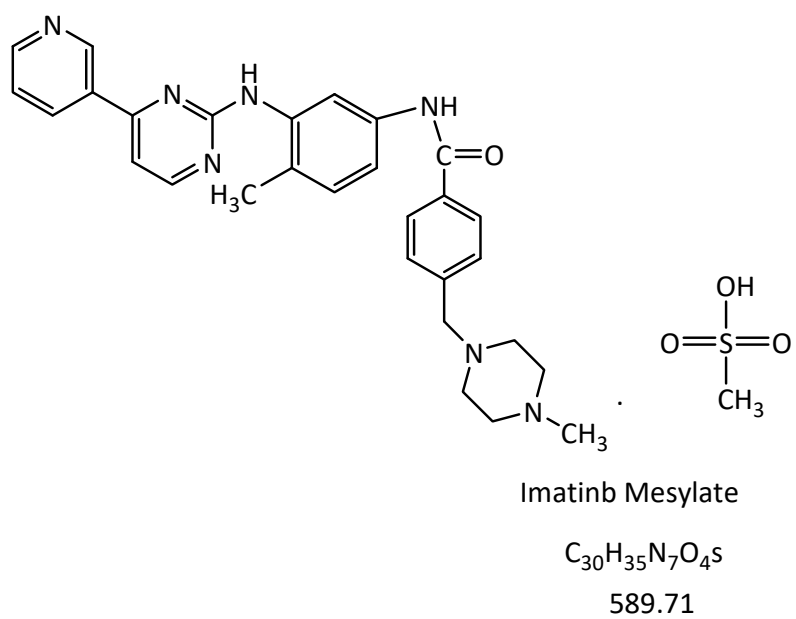
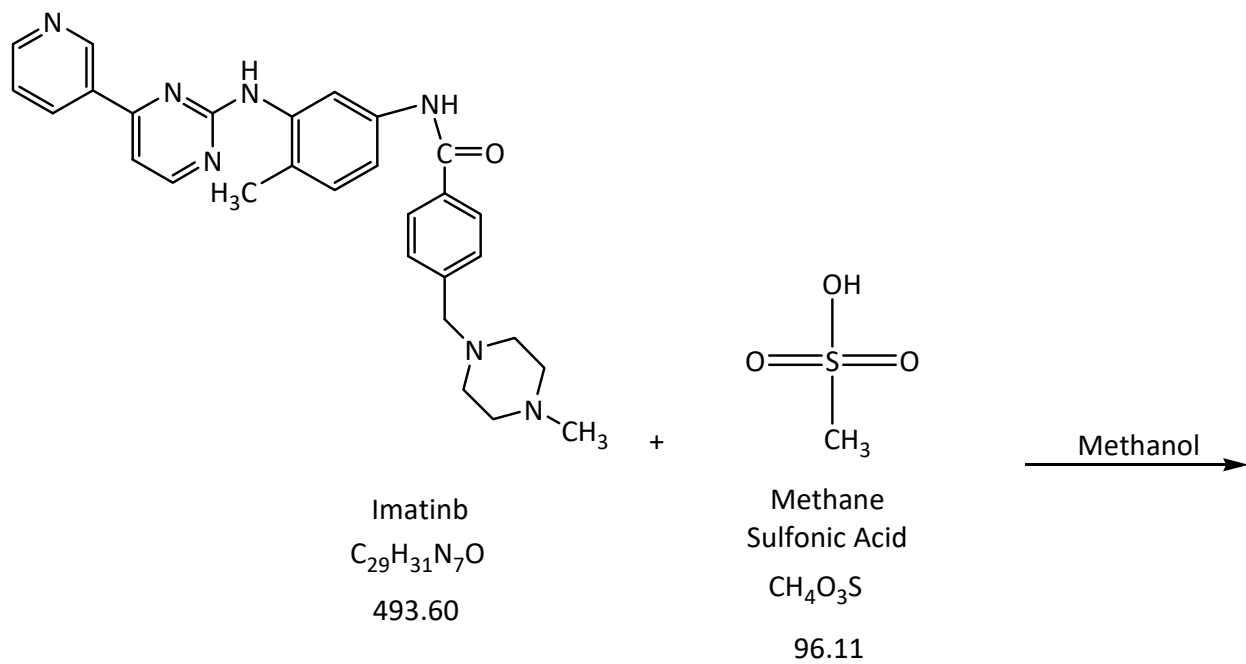


Imatinib

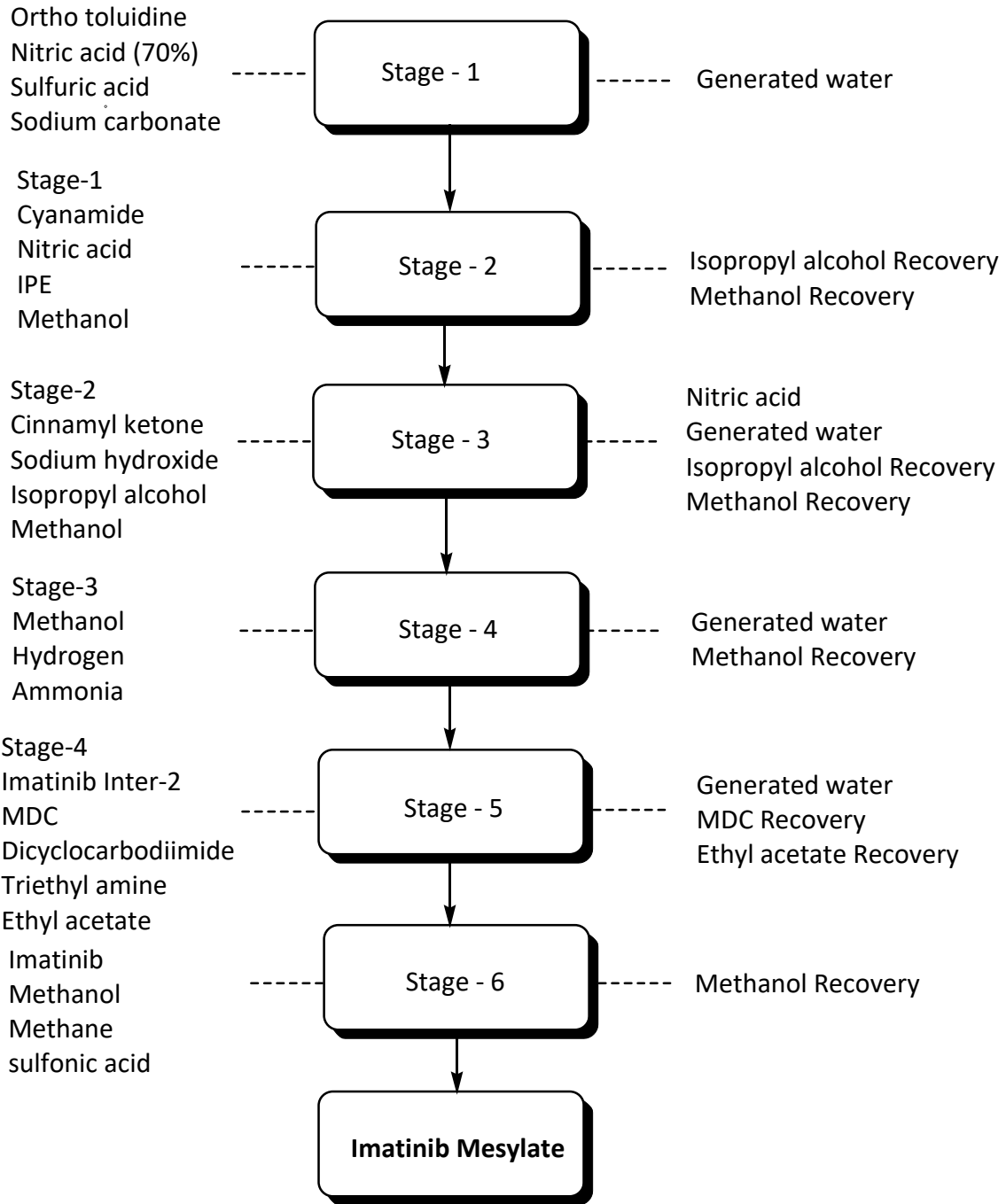
$C_{29}H_{31}N_7O$   
493.60

+ 2HCl↑ + H<sub>2</sub>O  
72.92 18.02

## Stage-6



## FLOW CHART OF IMATINIB MESYLATE



## IMATINIB MESYLATE

### Material Balance of Imatinib Mesylate

#### Stage-1

**Batch Size:50Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Ortho tolylamine	10.00	Stage-1	14.00
Nitric acid	6.00	Effluent water	526.70
Sulfuric acid	15.00	(Water-500, generated water-1.70, Sulfuric acid-15, Sodium carbonate-10)	
Sodium carbonate	10.00	Organic Residue	0.93
Water	500.00	(Process Residue-0.93)	
<b>Total</b>	<b>541.00</b>	<b>Total</b>	<b>541.00</b>

### Material Balance of Imatinib Mesylate

#### Stage-2

**Batch Size:50Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	14.00	Stage-2	23.00
Cyanamide	4.00	IPE Recovery	190.00
Nitric acid	6.00	IPE Loss	4.00
n-Butanol	600.00	Methanol Recovery	190.00
IPE	200.00	Methanol Loss	4.00
Methanol	200.00	n-Butanol Recovery	570.00
Water	500.00	n-Butanol Loss	12.00
		Effluent water	514.00
		(Water-500, Methanol-6, N-Butanol-8)	0
		Organic Residue	17.00
		Process residue-1, Distillation Residue-16 ( N-Butanol-10,IPE-6)	
<b>Total</b>	<b>1524.00</b>	<b>Total</b>	<b>1524.00</b>

**Material Balance of Imatinib Mesylate**  
**Stage-3**  
**Batch Size:50Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	23.00	Stage-3	27.00
n-Butanol	400.00	Isopropyl alcohol Recovery	237.00
3-dimethylamino-1-pyridin-3-yl propenone	15.75	Isopropyl alcohol Loss	5.00
Sodium hydroxide	6.00	Methanol Recovery	237.00
Isopropyl alcohol	250.00	Methanol Loss	5.00
Methanol	250.00	n-Butanol Recovery	380.00
Water	200.00	n-Butanol Loss	8.00
		Effluent water	220.03
		(Water-200, Dimethylamine-4.03, Methanol-8,IPA-8)	
		Process Emission	7.30
		(Ammonia-1.55,Oxygen-5.75)	
		Organic Residue	18.42
		Process Residue-6.42, Distillation Residue-12 (n-Butanol -12)	
<b>Total</b>	<b>1144.75</b>	<b>Total</b>	<b>1144.75</b>

**Material Balance of Imatinib Mesylate**  
**Stage-4**  
**Batch Size:50Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-3	27.00	Stage-4	24.00
Methanol	450.00	Methanol Recovery	427.00
Hydrogen	0.55	Methanol Loss	9.00
Palladium carbon	5.00	Palladium carbon reuse	5.00
Ammonia	20.00	Effluent water	527.16
Water	500.00	(Water-500, Generated water-3.16, Ammonia-20,Methanol-4)	
		Organic Residue	10.39
		Process Residue-0.39, Distillation Residue-10 (Methanol-10)	
<b>Total</b>	<b>1002.55</b>	<b>Total</b>	<b>1002.55</b>

**Material Balance of Imatinib Mesylate  
Stage-5  
Batch Size:50Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-4	24.00	Imatinib	42.00
Imatinib Intermediate-2 (4-(4-methyl piperazin-1-yl)methyl benzoic acid dihydrochloride)	26.60	MDC Recovery	760.00
MDC	800.00	MDC Loss	16.00
Dicyclocarbodiimide	10.00	Ethyl acetate Recovery	114.00
Ethyl acetate	120.00	Ethyl acetate Loss	2.00
Sodium sulphate	2.00	Effluent water	415.60
Water	400.00	(Water-400, generated water-1.6 Dicyclocarbodiimide-10, Ethyl acetate-4)	
		Inorganic solid waste	2.00
		(Sodium sulphate)	
		Process Emission	6.30
		(Hydrogen chloride)	
		Organic Residue	24.70
		(Process residue-.0.7, Distillation Residue-24 (MDC-24)	
<b>Total</b>	<b>1382.60</b>	<b>Total</b>	<b>1382.60</b>

**Material Balance of Imatinib Mesylate**  
**Stage-6**  
**Batch Size:50Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Imatinib	42.00	Imatinib Mesylate	50.00
Methanol	700.00	Methanol Recovery	665.00
Methane sulfonic acid	10.00	Methanol Loss	14.00
Activated carbon	5.00	Spent carbon	5.00
		Organic Residue	23.00
		(Process Residue-2, Distillation Residue-21 Methanol-21)	
<b>Total</b>	<b>757.00</b>	<b>Total</b>	<b>757.00</b>

## 13. IRINOTECAN HYDROCHLORIDE

### Process Description

#### Stage-1

##### Step-A

[1,4]Bipiperidiny-1'-carbonyl chloride Hydrochloride undergoes condensation with 4,11-Diethyl-4,9-dihydroxy-1,12-dihydro-4H-2-oxa-6,12a-diaza-dibenzo[b,h]fluorene-3,13-dione in presence of MDC, Diisopropylether & N-Methyl-2-pyrrolidone to give Step-A compound.

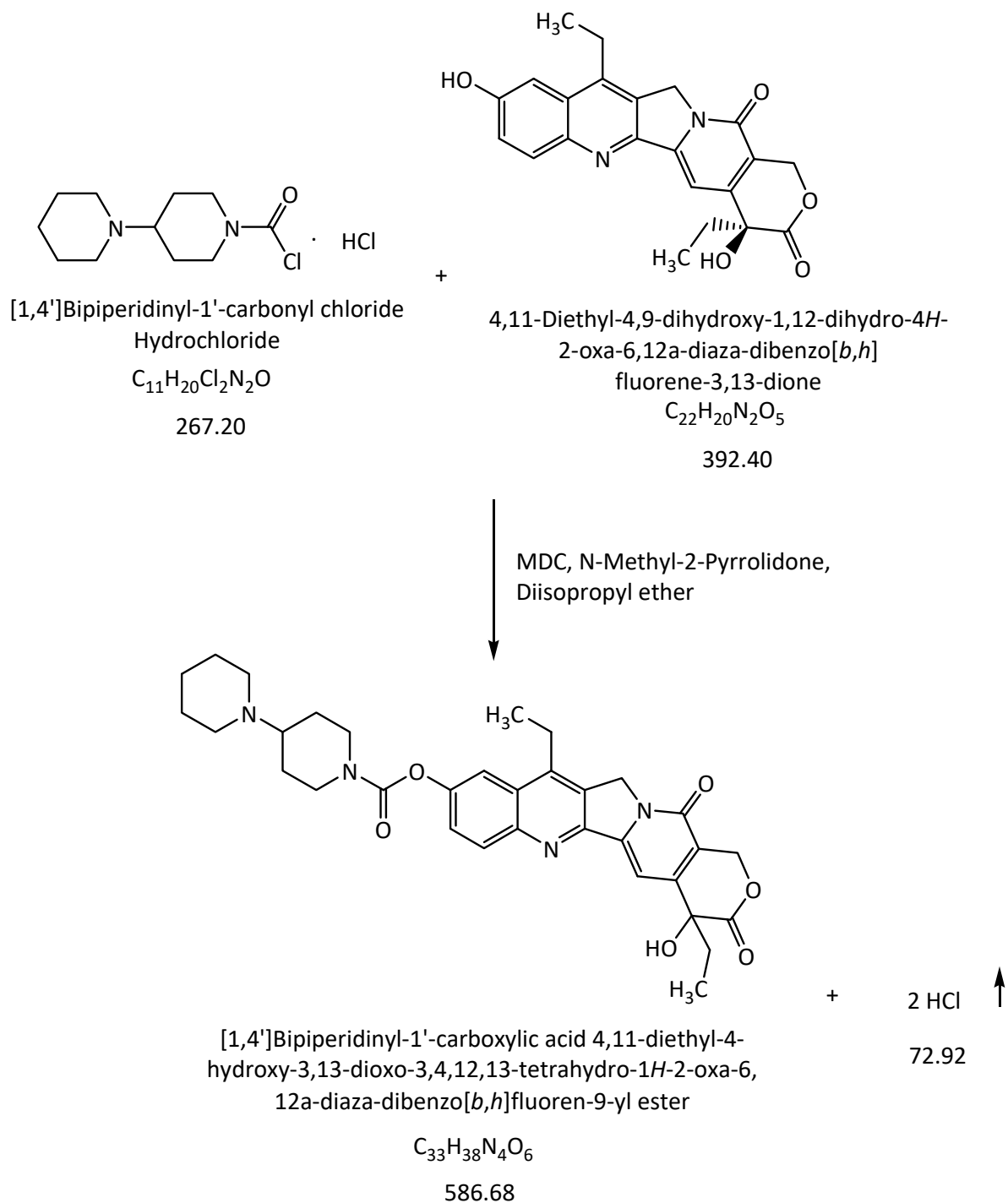
##### Step-B

Irinotecan Base (Step-A) undergoes salt formation with HCl in presence of IsoPropyl Alcohol to give irinotecan hydrochloride.

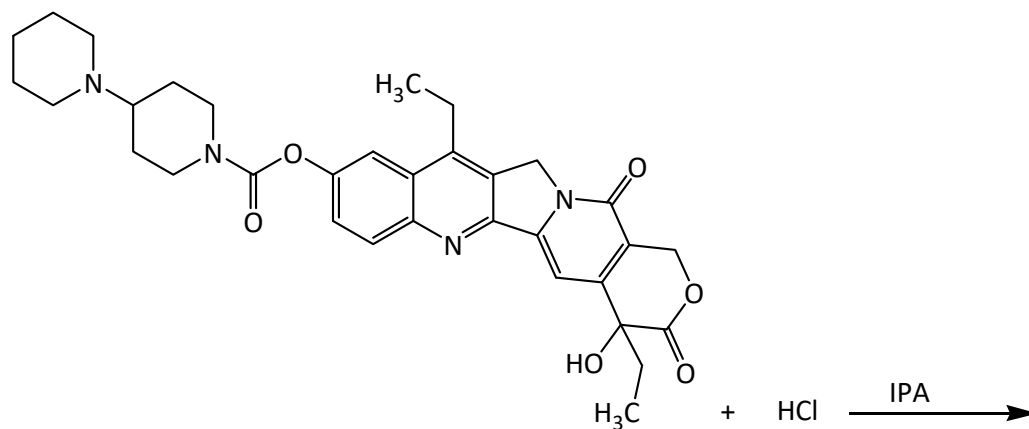
# IRINOTECAN HYDROCHLORIDE

Route of synthesis:

Stage-1  
Step -A



**Step-B**

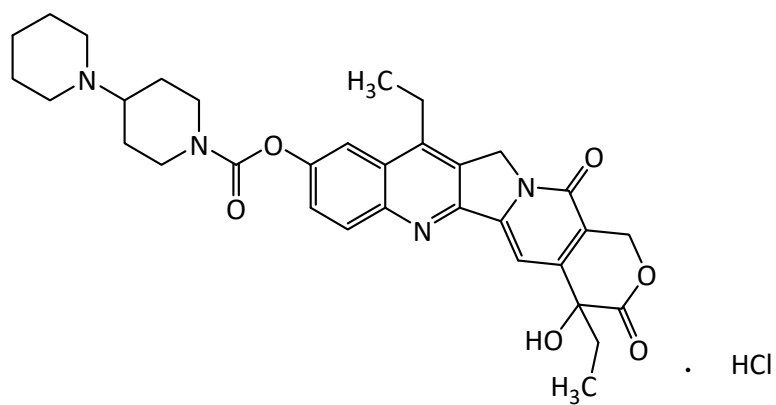


Irinotecan Base

$C_{33}H_{38}N_4O_6$

586.68

36.46



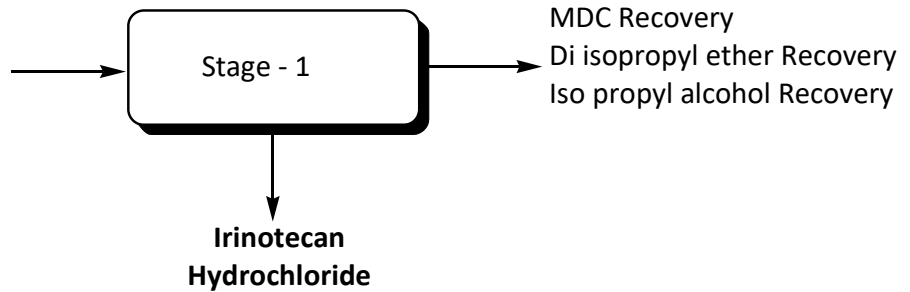
Irinotecan Hydrochloride

$C_{33}H_{38}N_4O_6 \cdot HCl$

623.14

## IRINOTECAN HYDROCHLORIDE

[1,4']Bipiperidiny-1'-carbonyl  
chloride Hydrochloride  
4,11-Diethyl-4,9-dihydroxy-1,12-  
dihydro-4H-2-oxa-6,12a-diaza-di  
benzo[b,h]fluorene-3,13-dione  
Methylene di chloride  
N-methyl-2-Pyrrolidine  
Di isopropyl ether  
Iso propyl alcohol  
Hydrochloric acid



## IRINOTECAN HYDROCHLORIDE

**Material balance:**

<b>Material Balance of Irinotecan Hydrochloride</b>			
<b>Stage-1</b>			
<b>Batch Size:10Kg</b>			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
[1,4']Bipiperidiny-1'-carbonyl chloride Hydrochloride	5.00	Irinotecan Hydrochloride	10.00
4,11-Diethyl-4,9-dihydroxy-1,12-dihydro-4H-2-oxa-6,12a-diaza-dibenzo[b,h]fluorene-3,13-dione	7.00	MDC Recovery	28.50
Methylene di chloride	30.00	MDC Loss	0.60
N-methyl-2-Pyrrolidine	40.00	Di isopropyl ether Recovery	28.50
Di isopropyl ether	30.00	Di isopropyl ether Loss	0.60
Iso propyl alcohol	50.00	Iso propyl alcohol Recovery	47.50
Hydrochloric acid	0.60	Iso propyl alcohol loss	1.00
Water	25.00	N-methyl-2-Pyrrolidine Recovery	38.00
		N-methyl-2-Pyrrolidine loss	0.80
		Effluent water (Water-25, IPA-1)	26.00
		Process emission (Hydrogen chloride)	1.26
		Organic Residue	4.84
		(Process Residue-1.34, Distillation Residue-3.5 (MDC-0.9, Di isopropyl ether -0.9, IPA-0.5, N-methyl-2-Pyrrolidine-1.2)	
<b>Total</b>	<b>187.60</b>	<b>Total</b>	<b>187.60</b>

## 14. IVABRADINE HYDROCHLORIDE

### Process Description:

#### Stage-1:

1,3-dihydro-7,8-dimethoxy-2-oxo-1H-3-benzazepine reacts with 3-chloro-1-bromo propane in presence of potassium hydroxide, MDC and Acetone to give stage-1 product.

#### Stage-2:

Stage-1 product reacts with Sodium Iodide in presence of MDC and Acetone to give stage-2 product.

#### Stage-3:

Stage-2 product reacts with 1-[(7S)-3,4-dimethoxybicyclo[4.2.0]octa-1,3,5-trien-7-yl]-N-methylmethanamine in presence of Potassium carbonate, DMSO and MIBK to give stage-3 product.

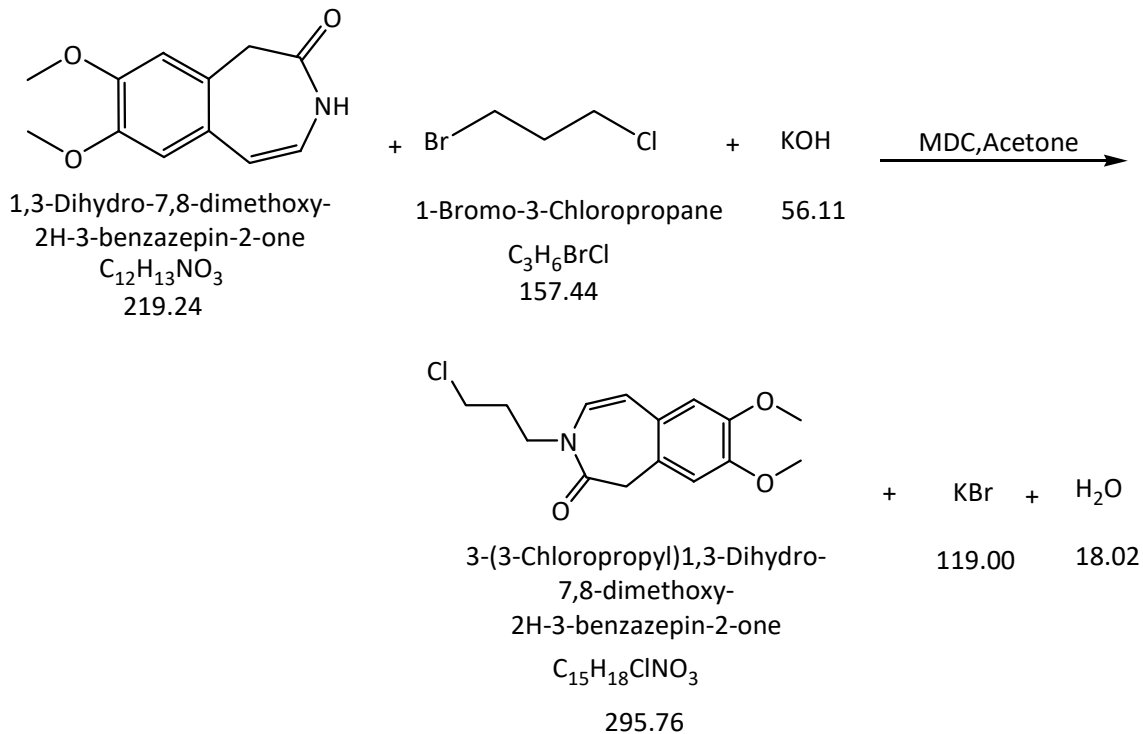
#### Stage-4:

Stage-3 product reacts with hydrogen gas in presence of Pd/C, IPA, DMF and HCl to give Ivabradine Hydrochloride.

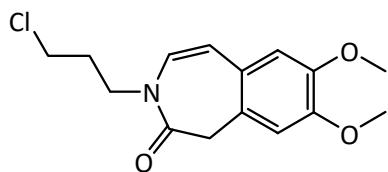
## IVABRADINE HYDROCHLORIDE

### Route of Synthesis:

#### Stage-1:



**Stage-2:**



3-(3-Chloropropyl)1,3-Dihydro-  
7,8-dimethoxy-  
2H-3-benzazepin-2-one

$C_{15}H_{18}ClNO_3$

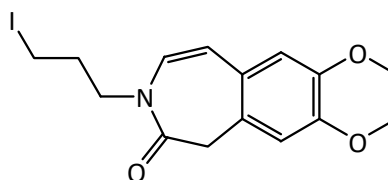
295.76

+ NaI

Acetone, MDC, Hyflow

Sodium Iodide

149.89



3-(3-iodopropyl)1,3-Dihydro-  
7,8-dimethoxy-  
2H-3-benzazepin-2-one

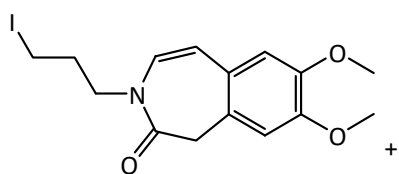
$C_{15}H_{18}INO_3$

387.21

+ NaCl

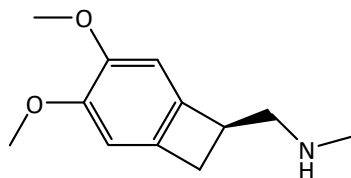
58.44

**Stage-3:**



3-(3-iodopropyl)-1,3-Dihydro-  
7,8-dimethoxy-  
2H-3-benzazepin-2-one

$C_{15}H_{18}INO_3$   
387.21

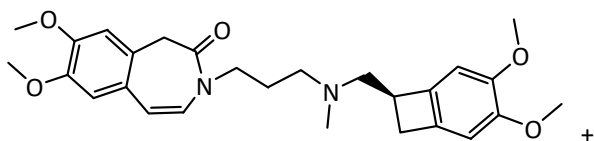


1-[(7S)-3,4-dimethoxybicyclo[4.2.0]  
octa-1,3,5-trien-7-yl]-N-methylmethanamine

$C_{12}H_{17}NO_2$   
207.27

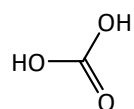
+  $K_2CO_3$  + HCl

138.21 36.46



3-{3-[(3,4-Dimethoxy-bicyclo[4.2.0]octa-1(6),  
2,4-trien-7-yl)methyl]-methyl-amino}-propyl-7,8-  
dimethoxy-1,3-dihydro-benzo[d]azepin-2-one

$C_{27}H_{34}N_2O_5$   
466.57



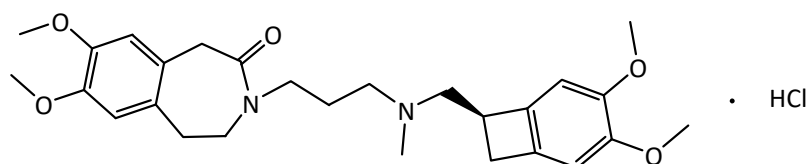
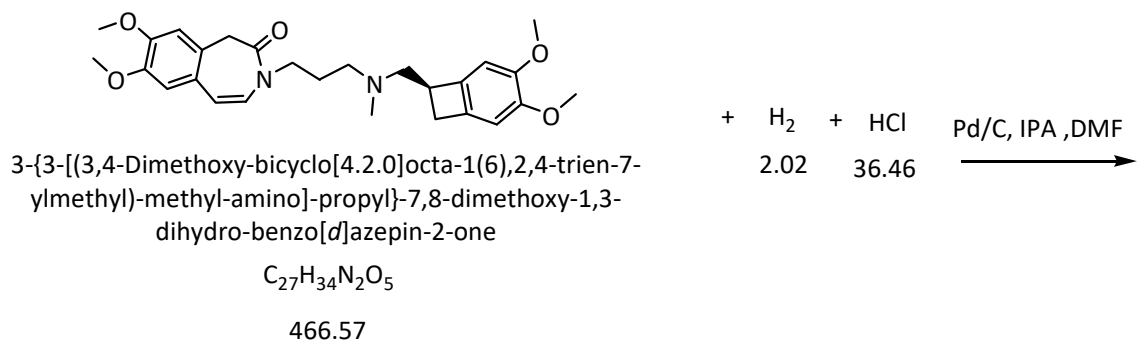
Carbonic acid

$CH_2O_3$   
62.02

+ KI + KCl

166.00 74.55

**Stage-4:**



IVABRADINE HYDROCHLORIDE

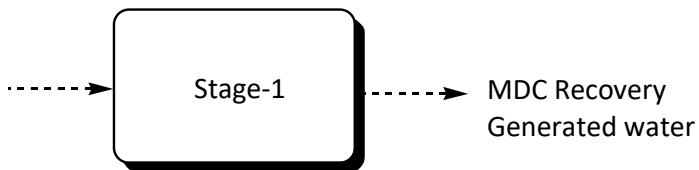
$C_{27}H_{37}ClN_2O_5$

505.05

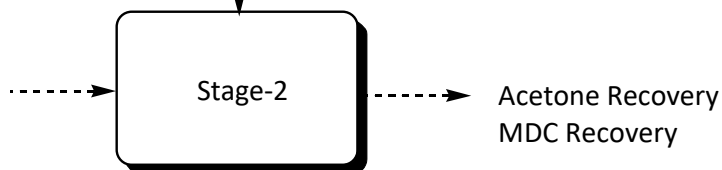
# IVABRADINE HYDROCHLORIDE

## Flowchart:

1,3-dihydro-7,8-dimethoxy-  
2-oxo-1H-3-benzazepine  
3-chloro-1-bromo propane  
Potassium Hydroxide  
Methylene dichloride  
Acetone  
Hyflow



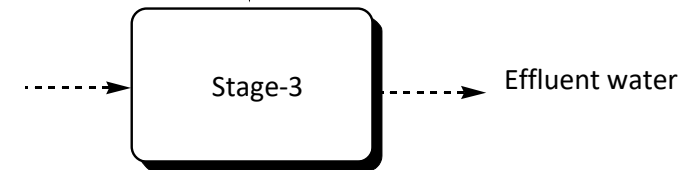
Stage-1  
Sodium Iodide  
Acetone  
Methylene dichloride  
Sodium sulphate anhydrous  
Hyflow



Stage-2  
1-[(7S)-3,4-dimethoxybicyclo[4.2.0]  
octa-1,3,5-trien-7-yl]-N-  
methylmethanamine  
Potassium carbonate  
Dimethyl sulphoxide  
Methyl iso butyl ketone  
Iso propyl alcohol  
Hydrochloric acid



Stage-3  
Hydrochloric acid in IPA  
5%palladium on Carbon  
Hydrogen  
Dimethylformamide



Ivabradine Hydrochloride

## IVABRADINE HYDROCHLORIDE

### Material Balance:

Material Balance of Ivabradine Hydrochloride Stage-1 Batch Size: 50.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
1,3-dihydro-7,8-dimethoxy-2-oxo-1H-3-benzazepine	28.00	Stage-1	36.00
3-chloro-1-bromo propane	20.50	Methylene dichloride recovery	14.25
Potassium Hydroxide	7.16	Methylene dichloride loss	0.30
Methylene dichloride	15.00	Inorganic Solid Waste (Potassium Bromide)	15.19
Acetone	20.00	Acetone recovery	19.00
Hyflow	0.50	Acetone loss	0.40
		Spent Hyflow	0.50
		Generated water	2.30
		Organic residue (Process Residue-2.17, Distillation Residue- (Acetone-0.6, MDC-0.45)	3.22
<b>Total</b>	<b>91.16</b>	<b>Total</b>	<b>91.16</b>

Material Balance of Ivabradine Hydrochloride Stage-2 Batch Size: 50.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	36.00	Stage-2	45.00
Sodium Iodide	19.00	Acetone recovery	9.50
Acetone	10.00	Acetone process loss	0.20
Methylene dichloride	15.00	Methylene dichloride recovery	14.25
Sodium sulphate anhydrous	0.50	Methylene dichloride process loss	0.30
Hyflow	0.50	Effluent water (Water-50 Sodium chloride-7.11, acetone-0.3)	57.41
Water	50.00	Inorganic solid waste (Sodium sulphate)	0.50
		Spent Hyflow	0.50
		Organic Residue (Process Residue-2.89, Distillation Residue-0.45 (MDC-0.45)	3.34
<b>Total</b>	<b>131.00</b>	<b>Total</b>	<b>131.00</b>

Material Balance of Ivabradine Hydrochloride Stage-3 Batch Size: 50.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	45.00	Stage-3	52.00
1-[(7S)-3,4-dimethoxybicyclo[4.2.0]octa-1,3,5-trien-7-yl]-N-methylmethanamine	24.00	Dimethyl sulphoxide recovery	9.50
Potassium carbonate	17.00	Dimethyl sulphoxide loss	0.20
Dimethyl sulphoxide	10.00	Methyl iso butyl ketone recovery	14.25
Methyl iso butyl ketone	15.00	MIBK loss	0.30
Iso propyl alcohol	10.00	Iso propyl alcohol recovery	9.50
Hydrochloric acid	5.00	Iso propyl alcohol loss	0.20
Water	50.00	Effluent water (Water-50, Potassium chloride-8.65, DMSO-0.3)	58.95
		Inorganic solid waste (Potassium iodide-19.29, Carbonic acid-7.20)	26.49
		Organic residue – 4.61 (Process residue-3.86, Distillation Residue-0.75 (MIBK-0.45, IPA-0.30)	4.61
Total	176.00	Total	176.00

Material Balance of Ivabradine Hydrochloride Stage-4 Batch Size: 50.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-3	52.00	Ivabradine Hydrochloride	50.00
Hydrochloric acid in IPA	20.00	Isopropyl alcohol recovery	14.25
5%palladium on Carbon	0.50	Isopropyl alcohol loss	0.30
Hydrogen	0.25	Dimethylformamide recovery	19.00
Dimethylformamide	20.00	Dimethylformamide loss	0.40
	0	Organic residue (Process Residue- 2.75 Distillation Residue-1.05 (IPA-5.45, DMF-0.6)	8.80
Total	92.75	Total	92.75

## 15. LENALIDOMIDE

### Process Description:

#### Stage-1:

2-Bromomethyl-3-nitro-benzoic acid reacts with 3-amino-piperidine-2,6-dione in presence of methanol and MDC to give stage-1 product.

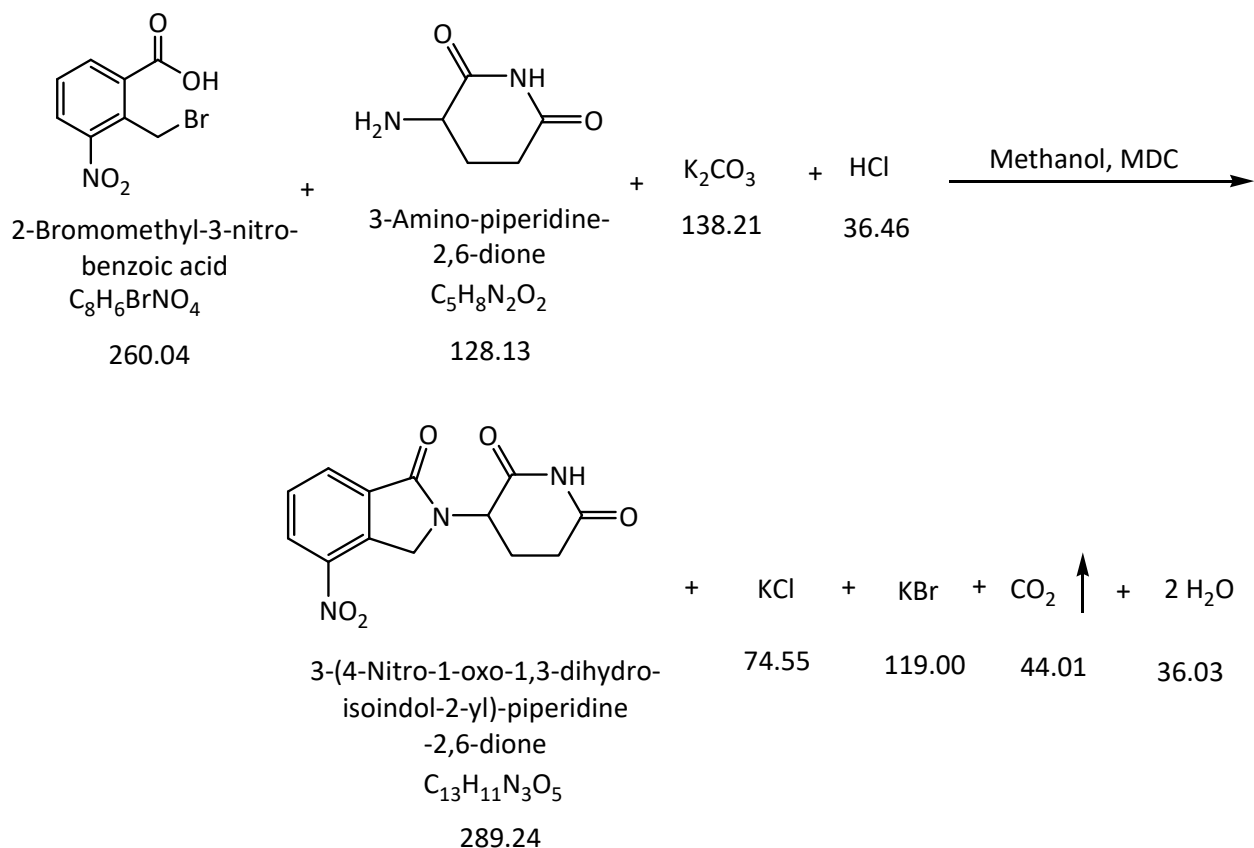
#### Stage-2:

Stage-1 product undergoes Hydrogenation with hydrogen in presence of Methanol and Pd/c to give Lenalidomide.

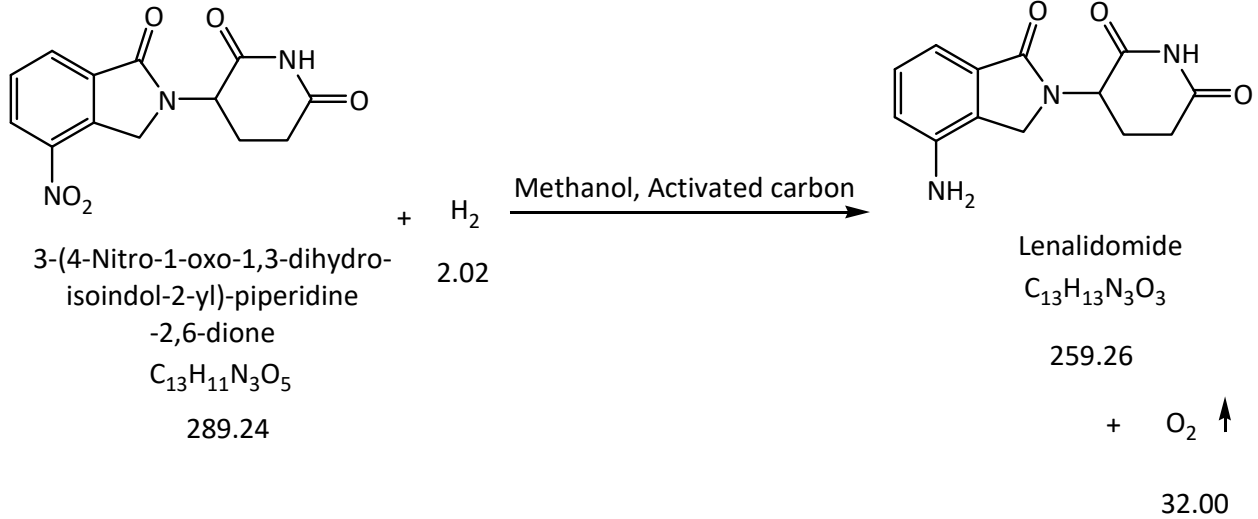
## LENALIDOMIDE

### Route of synthesis:

#### Stage-1



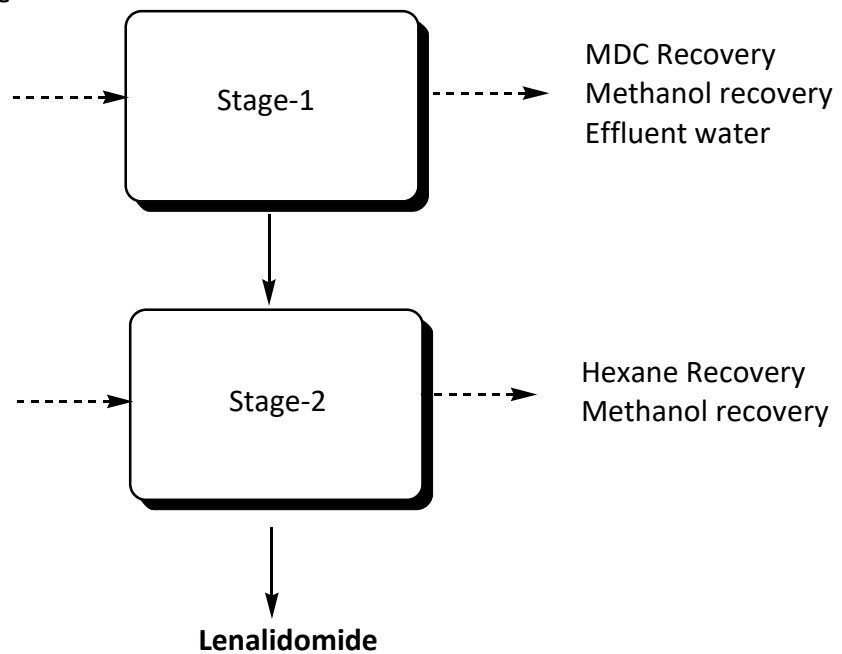
## Stage-2



## LENALIDOMIDE

### Flowchart:

2-(bromomethyl)-3-nitrobenzoic acid  
3-aminopiperidine-2,6-dione  
Hydrochloric acid  
Potassium Carbonate  
Methanol  
Dichloromethane

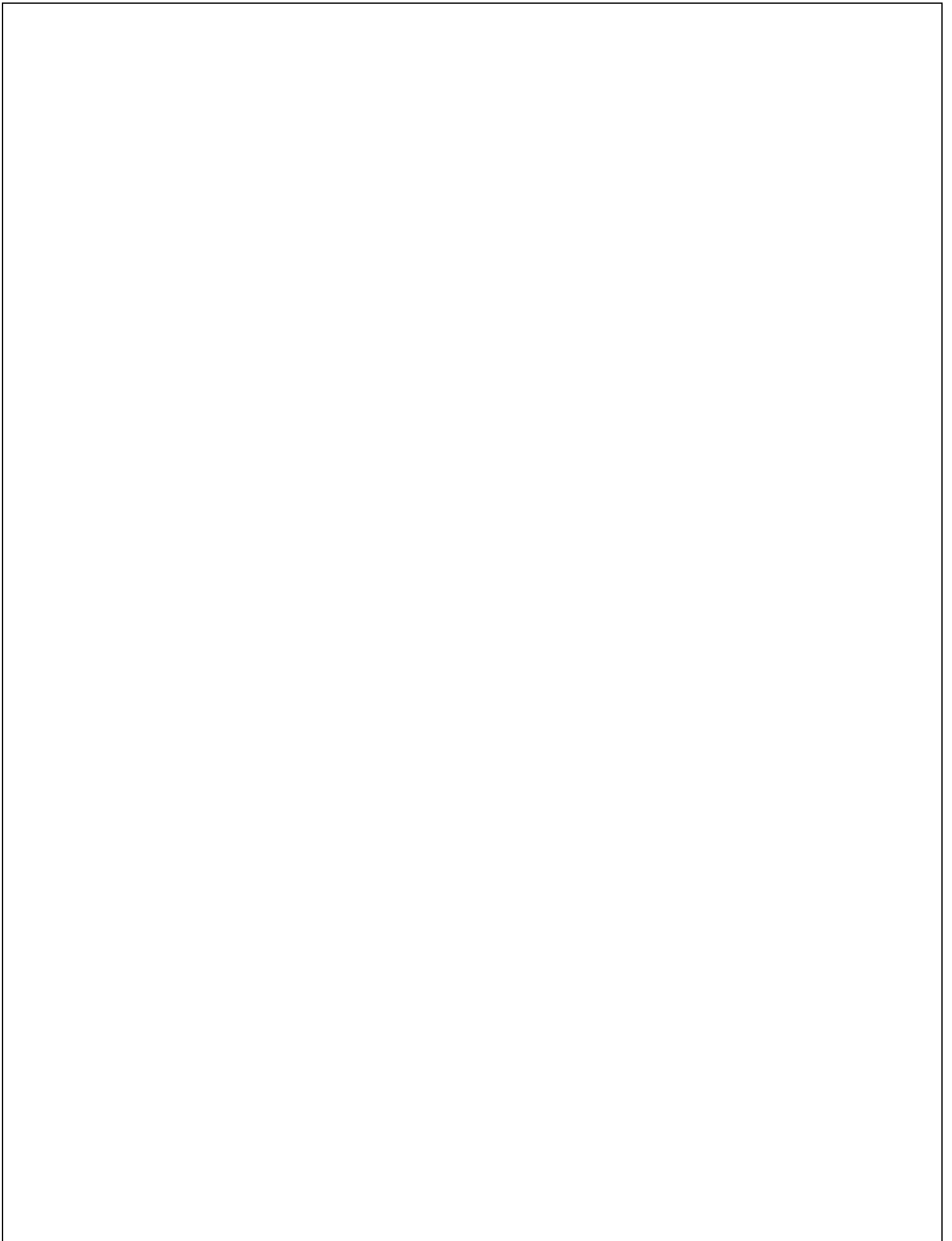


## LENALIDOMIDE

### Material balance:

Material Balance of Lenalidomide Stage-1 Batch Size: 25.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
2-(bromomethyl)-3-nitrobenzoic acid	28.00	Stage-1	30.00
3-aminopiperidine-2,6-dione	14.00	Methanol Recovery	19.00
Hydrochloric acid	4.00	Methanol loss	0.40
Potassium Carbonate	15.00	Dichloromethane recovery	14.25
Methanol	20.00	Dichloromethane loss	0.30
Dichloromethane	15.00	Effluent water (Water-20, Generated water-3.87, Potassium chloride-8.02, Potassium bromide-12.81, Methanol-0.6)	45.30
Water	20.00	Process emission (Carbon dioxide – 4.73)	4.73
		Organic residue (Process residue-1.57, Distillation Residue- (MDC-0.45)	2.02
<b>Total</b>	<b>116.00</b>	<b>Total</b>	<b>116.00</b>

Material Balance of Lenalidomide Stage-2 Batch Size: 25.0Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	30.00	Stage-1	25.00
Activated carbon	0.50	Methanol recovery	19.00
Methanol	20.00	Methanol loss	0.40
Pd/C	0.5	Hexane recovery	28.50
Hexane	30.0	Hexane loss	0.60
Hydrogen	0.25	Spent Pd/C	0.50
		Spent Carbon	0.50
		Process emission (oxygen- 3.32)	3.32
		Organic residue (Process residue-1.93 Distillation Residue-1.5 (Methanol-0.6, Hexane-0.9)	3.43
<b>Total</b>	<b>81.25</b>	<b>Total</b>	<b>81.25</b>



## 16. LINEZOLID

### Process Description:

#### Stage-1

R-3-(3-Fluoro-4-morpholinophenyl)-2-oxooxazolidin-5-yl) methyl methane sulfonate reacts with Potassium phthalide in the presence of TEBAC, MIBK as solvent media to get Stage-1 as product.

#### Stage-2

Stage-1 product reacts with Monomethyl amine in the presence of methanol as solvent media to get stage-2 as product.

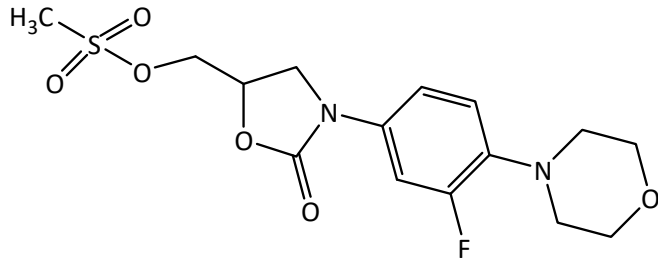
#### Stage-3

Stage-2 product reacts with acetic anhydride by using Ethyl acetate as solvent media to give Linezolid as product.

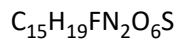
# LINEZOLID

## Route of Synthesis:

### Stage-1:

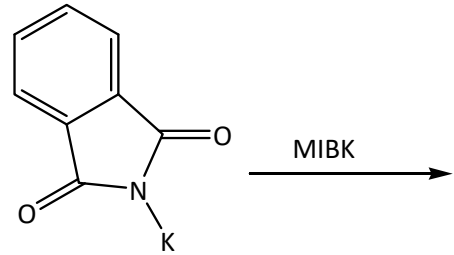


Methanesulfonic acid 3-(3-fluoro-4-morpholin-4-yl-phenyl)-2-oxo-oxazolidin-5-ylmethyl ester

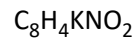


374.38

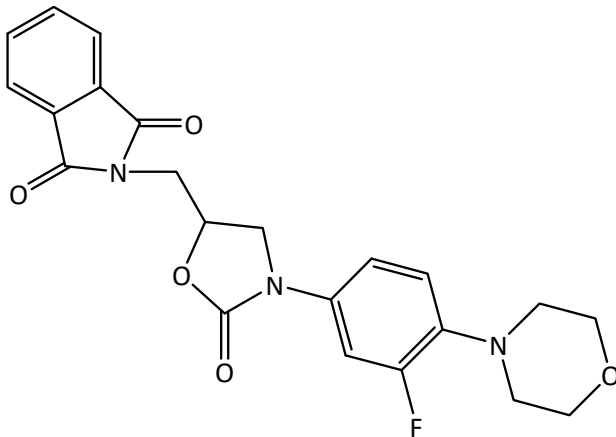
+



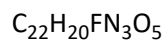
Potassium phthalimide



185.22

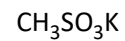


2-[3-(3-Fluoro-4-morpholin-4-yl-phenyl)-2-oxo-oxazolidin-5-ylmethyl]-isoindole-1,3-dione



425.41

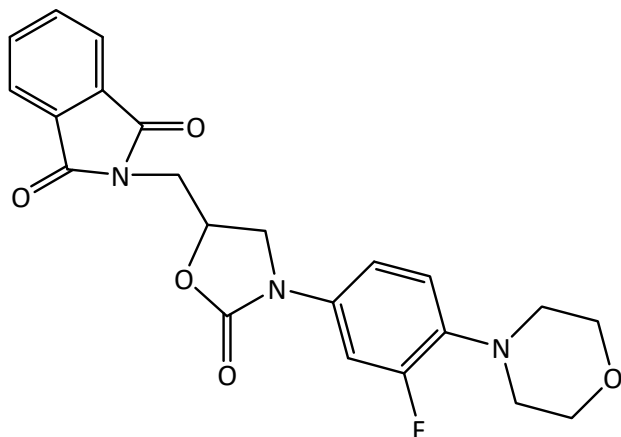
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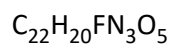
Methane sulfonic acid Potassium salt

134.19

**Stage-2:**



2-[3-(3-Fluoro-4-morpholin-4-yl-phenyl)-2-oxo-oxazolidin-5-ylmethyl]-isoindole-1,3-dione

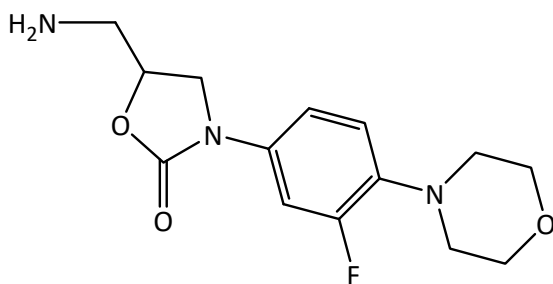


425.41

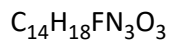


Mono methyl amine

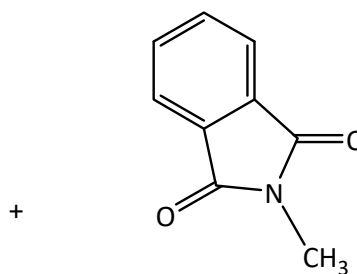
31.06



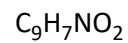
5-Aminomethyl-3-(3-fluoro-4-morpholin-4-yl-phenyl)-oxazolidin-2-one



295.13

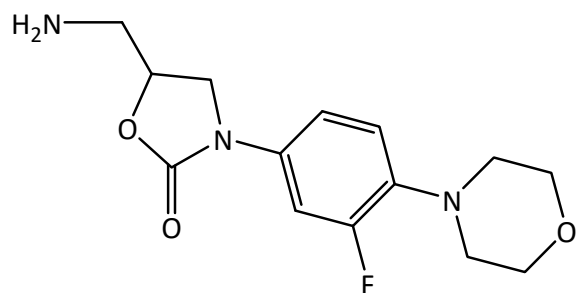


2-Methyl-isoindole-1,3-dione

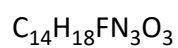


161.15

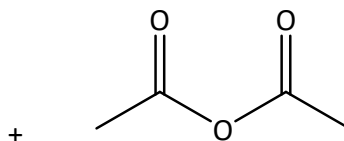
**Stage-3:**



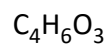
5-Aminomethyl-3-(3-fluoro-4-morpholin-4-yl-phenyl)-oxazolidin-2-one



295.13



Acetic anhydride

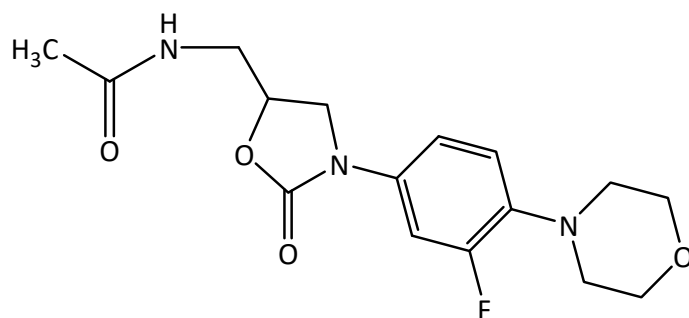


102.09

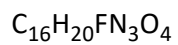


Sodium Hydroxide

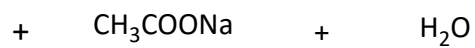
40.0



Linezolid



337.14

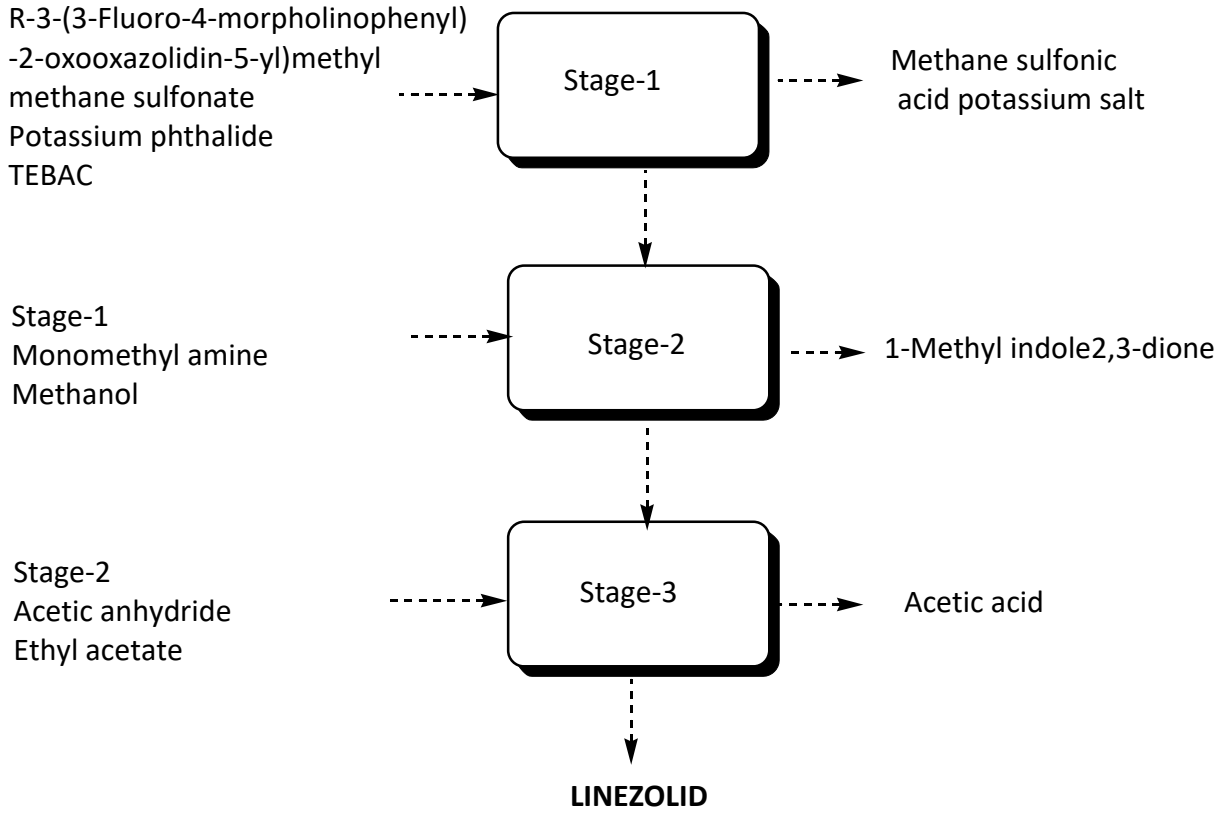


82.03

18.0

# LINEZOLID

## Flow-Chart:



**Material Balance:**

Material Balance of Linezolid Stage-1 Batch Size:100Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
R-3-(3-Fluoro-4-morpholinophenyl)-2-oxooxazolidin-5-yl) methyl methane sulfonate	210.00	Stage-1	180.00
Potassium phthalide	104.00	MIBK Recovery	1145.00
TEBAC	10.00	MIBK Loss	55.00
MIBK	1200.00	MDC Recovery	760.00
MDC	800.00	MDC Loss	40.00
Methanol	800.00	Methanol Recovery	745.00
Water	1500.00	Methanol Loss	40.00
		Effluent water	1600.20
		(Water-1500,Methane sulfonic acid potassium salt -75.2, Methanol-15, TEBAC-10)	
		Organic Residue	58.80
Total	4624.00	Total	4624.00

**Material Balance of Linezolid**

**Stage-2**

Batch Size:100Kg

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	180.00	Stage-2	120.00
Methyl amine (40%)	30.00	Methanol Recovery	428.00
Methanol	450.00	Methanol Loss	22.00
Water	200.00	Effluent Water	223.00
		(Water-200,Methanol-5,Water from monomethyl amine-18)	
		Organic Solid Waste	67.00
<b>Total</b>	<b>860.00</b>	<b>Total</b>	<b>860.00</b>

**Material Balance of Linezolid**

**Stage-3**

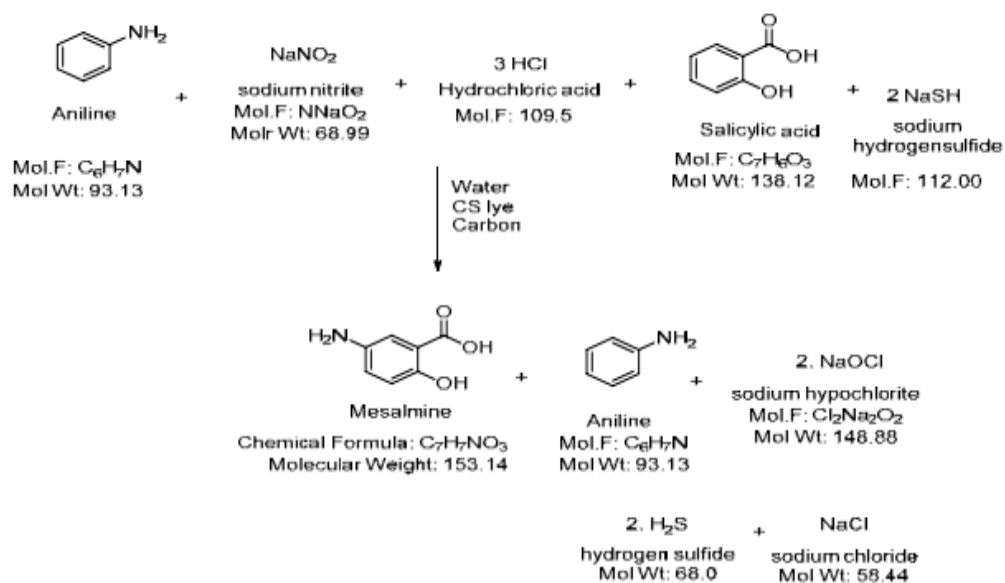
Batch Size:100Kg

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	120.00	Linezolid	100.00
Acetic Anhydride	42.00	MDC Recovery	760.00
MDC	800.00	MDC Loss	40.00
Ethyl acetate	600.00	Ethyl acetate Recovery	570.00
Sodium hydroxide	12.00	Ethyl acetate Loss	30.00
Activated Carbon	10.00	Effluent Water	641.30
Water	600.00	(Water-600,Sodium Acetate-33.7, generated water-7.6)	
		Spent Carbon	10.00
		Organic Residue	32.70
<b>Total</b>	<b>2184.00</b>	<b>Total</b>	<b>2184.00</b>

## 17. MESALAMINE

### 2.1.7 Process Description of Mesalamine

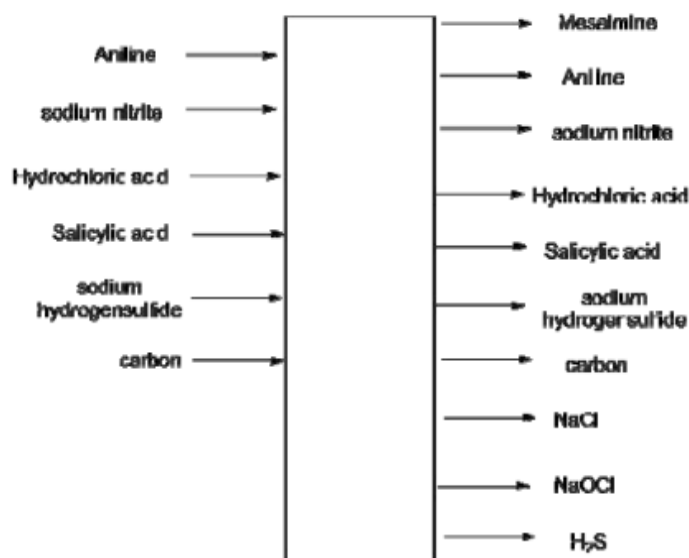
#### Reaction Schemes



#### Process Description:

Aniline reacts with  $NaNO_2$  in the presence of salicylic acid to form 5-Phenylazosalicylic acid.

5-Phenylazosalicylic acid reacts with NaSH to form Mesalamine.



Process Flow Diagram of Mesalamine

Material Balance of Mesalamine

**Stage I**

<b>Input</b>	<b>Quantity (Kg/day)</b>	<b>Output</b>	<b>Quantity (Kg/day)</b>	<b>Remarks</b>
Aniline	26	Mesalamine	33.3	Final product
sodium nitrite	19.3	Aniline	20.3	To Wastewater
Hydrochloric acid	30.6	Sodium hypo chlorite	32.4	Inorganic residue
Salicylic acid	38.5	Sodium chloride	23.5	To Wastewater
sodium hydrosulfide	31.3	Hydrogen sulfide	18.1	To Scrubber
Carbon	5	Aniline	5.7	Organic residue
Water	490	Salicylic acid	8.5	Organic residue
Sodium hydroxide	7.2	Carbon	5	To solid waste
		Sodium nitrite	4.2	To Wastewater
		Sodium hydrosulfide	6.9	Inorganic residue
		Water	490	To Wastewater
<b>Total Input</b>	<b>647.9</b>	<b>Total Output</b>	<b>647.9</b>	

## 18. OLMESARTAN

### Process Description:

#### Stage-1

2-Propyl-1H-imidazole-4, 5-dicarboxylic acid diethyl ester reacts with methyl magnesium bromide in presence of Ammonium chloride and THF to give Stage-1 product.

#### Stage-2

Stage-1 reacts with 5-(4'bromo methyl-biphenyl-2-yl)-1-trityl-5H-tetrazole in presence of TBAB as catalyst and Acetone to give stage-2 product.

#### Stage-3

Stage-2 reacts with Lithium hydroxide in presence of THF to give Stage-3 product.

#### Stage-4

Stage-3 reacts with 4-chloromethyl-5-methyl-[1, 3] dioxolan-2-one in presence of MDC to give stage-4 product.

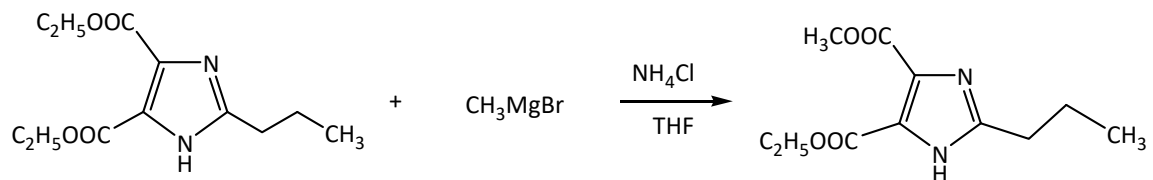
#### Stage-5

Stage-4 reacts with acetic acid in presence of Isopropyl alcohol to give Olmesartan.

## OLMESARTAN

### Route of synthesis:

#### Stage-1:



2-Propyl-1*H*-imidazole  
-4,5-dicarboxylic acid diethyl ester

$\text{C}_{12}\text{H}_{18}\text{N}_2\text{O}_4$   
254.28

Methyl magnesium  
bromide

119.24

2-Propyl-1*H*-imidazole-4,5-dicarboxylic  
acid 5-ethyl ester 4-methyl ester

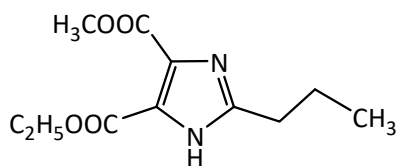
$\text{C}_{11}\text{H}_{16}\text{N}_2\text{O}_4$   
240.25

+  $\text{C}_2\text{H}_5\text{MgBr}$

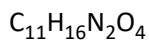
Ethyl magnesium  
bromide

133.27

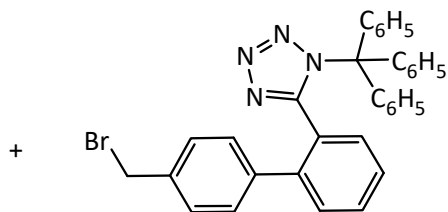
**Stage-2:**



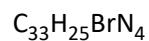
2-Propyl-1*H*-imidazole-4,5-dicarboxylic acid 5-ethyl ester 4-methyl ester



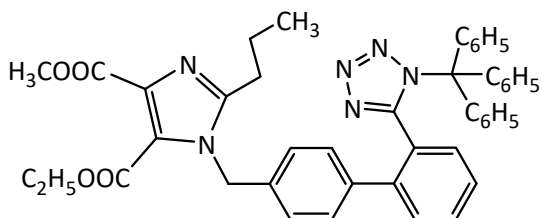
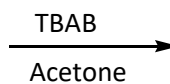
240.25



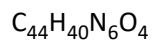
5-(4'-Bromomethyl-biphenyl-2-yl)-1-trityl-5*H*-tetrazole



557.48



2-Propyl-1-[2'-(1-trityl-5*H*-tetrazol-5-yl)-biphenyl-4-ylmethyl]-1*H*-imidazole-4,5-dicarboxylic acid 5-ethyl ester 4-methyl ester



716.82

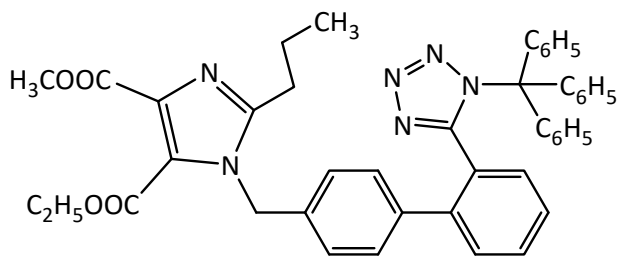
+

HBr

Hydrobromic acid

80.91

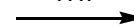
**Stage-3:**



+

LiOH

THF



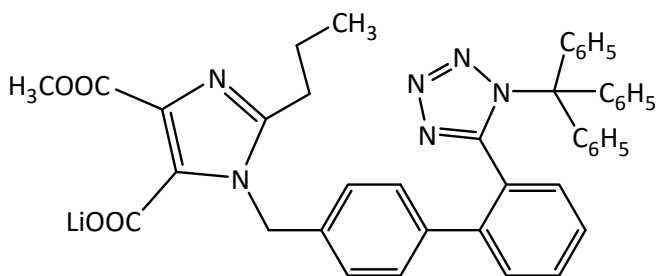
2-Propyl-1-[2'-(1-trityl-5H-tetrazol-5-yl)-biphenyl  
-4-ylmethyl]-1H-imidazole-4,5-dicarboxylic acid  
5-ethyl ester 4-methyl ester

Lithium  
Hydroxide

23.94

$C_{44}H_{40}N_6O_4$

716.82



+

$C_2H_5OH$

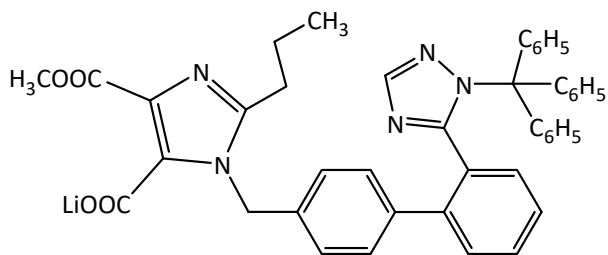
2-Propyl-1-[2'-(1-trityl-5H-tetrazol-5-yl)-biphenyl  
-4-ylmethyl]-1H-imidazole-4,5-dicarboxylic acid  
5-ethyl ester 4-methyl ester

46.06

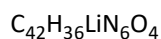
$C_{42}H_{35}LiN_6O_4$

694.70

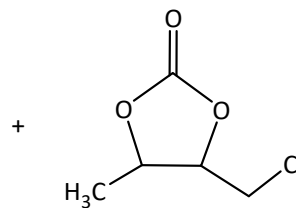
**Stage-4:**



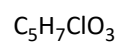
2-Propyl-1-[2'-(1-trityl-5H-tetrazol-5-yl)-biphenyl-4-ylmethyl]-1H-imidazole-4,5-dicarboxylic acid 5-ethyl ester 4-methyl ester



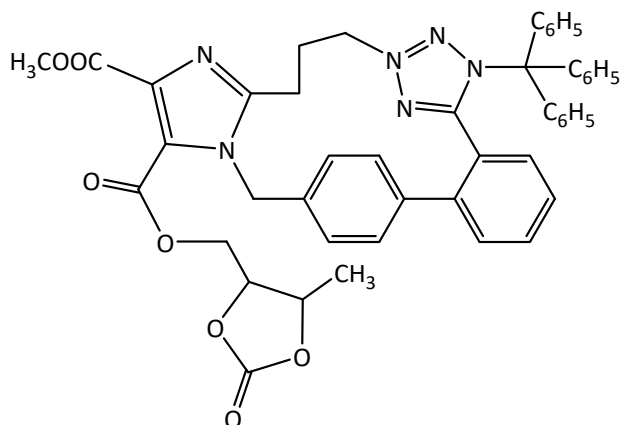
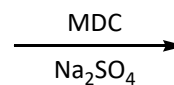
693.71



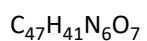
4-Chloromethyl-5-methyl-[1,3]dioxolan-2-one



150.56



2-Propyl-1-[2'-(1-trityl-5H-tetrazol-5-yl)-biphenyl-4-ylmethyl]-1H-imidazole-4,5-dicarboxylic acid 4-methyl ester 5-(5-methyl-2-oxo-[1,3]dioxolan-4-ylmethyl) ester

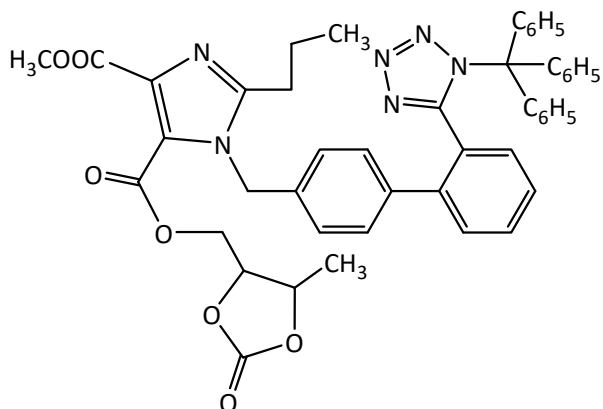


801.86



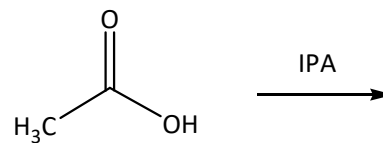
42.39

**Stage-5:**

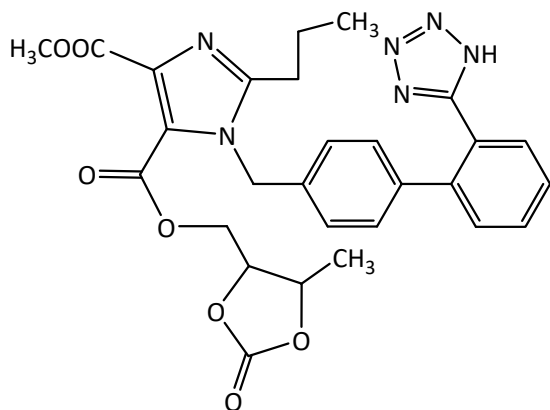


2-Propyl-1-[2'-(1-trityl-5H-tetrazol-5-yl)-biphenyl-4-ylmethyl]  
-1H-imidazole-4,5-dicarboxylic acid 4-methyl ester  
5-(5-methyl-2-oxo-[1,3]dioxolan-4-ylmethyl) ester

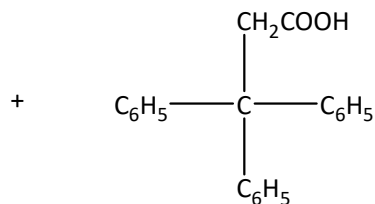
$C_{47}H_{42}N_6O_7$   
802.87



Acetic acid  
 $C_2H_4O_2$   
60.05



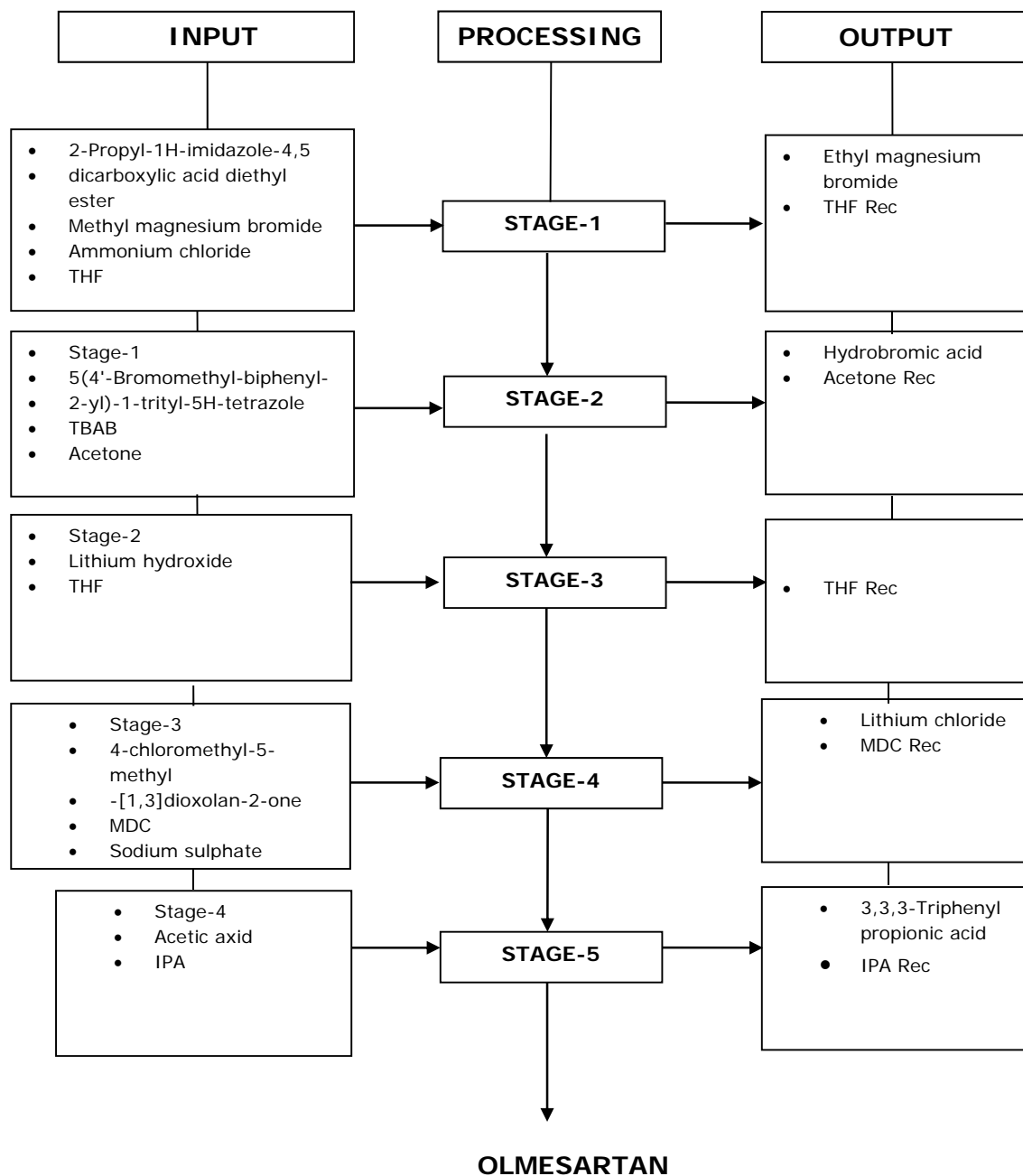
Olmesartan  
 $C_{28}H_{28}N_6O_7$   
560.55



3,3-Triphenyl-propionic acid  
 $C_{21}H_{18}O_2$   
302.37

# OLMESARTAN

## Flow chart:



## OLMESARTAN

### Material Balance:

<b>MATERIAL BALANCE OF OLMESARTAN</b>			
<b>STAGE-1</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
2-Propyl-1H-imidazole-4,5-dicarboxylic acid diethyl ester	68.00	Stage-1	60.00
Methyl magnesium bromide	31.90	THF Recovery	475.00
Tetrahydrofuran	500.00	THF Loss	10.00
Ammonium chloride	10.00	Ethyl acetate Recovery	143.00
Ethyl acetate	150.00	Ethyl acetate Loss	3.00
Sodium sulphate	4.50	Diiso propyl ether Recovery	95.00
Di isopropyl ether	100.00	Diiso propyl ether Loss	5.00
Water	300.00	Effluent water	353.65
		(Water-300, Ethyl magnesium bromide-35.65, Ammonium chloride-10, THF-8)	
		Inorganic solid waste (Sodium sulfate)	4.50
		Organic Residue	15.25
		Process residue - 4.25, Distillation residue - 11 (THF-7, Ethyl acetate -4)	
<b>Total</b>	<b>1164.40</b>	<b>Total</b>	<b>1164.40</b>

<b>MATERIAL BALANCE OF OLMESARTAN</b>			
<b>STAGE-2</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-1	60.00	Stage-2	153.00
TrityltriazoneButylbromide(TTBB)	140.00	Acetone Recovery	470.00
TBAB	10.00	Acetone Loss	10.00
Potassium carbonate	20.00	Effluent water	557.05
Acetone	500.00	(Water-500,Potassium bromide-34.45,Generated water-2.6,TBAB-10, Acetone-10)	
Activated Carbon	10.00	Spent Carbon	10.00
Water	500.00	Process Emission	6.36
		(Carbon dioxide)	
		Organic Residue	33.59
		Process reidue-23.59, Distillation residue -10 (Acetone-10)	
<b>Total</b>	<b>1240.00</b>	<b>Total</b>	<b>1240.00</b>

<b>MATERIAL BALANCE OF OLMESARTAN</b>			
<b>STAGE-3</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-2	153.00	Stage-3	142.00
Lithium hydroxide	6.90	THF Recovery	190.00
Tetrahydrofuran	200.00	THF Loss	4.00
Ethyl acetate	200.00	Ethyl acetate Recovery	190.00
Sodium chloride	28.00	Ethyl acetate Loss	4.00
Sodium sulphate	2.00	Effluent Water	647.60
Water	600.00	(Water-	

		600,Lithium hydroxide-1.8,Ethanol-9.8, Sodium chloride-28, Sodium sulfate-2, ethyl acetate -3, THF-3)	
		Organic Residue	11.30
		Process residue - 6.3, Distillation residue -5 (THF-3, Ethyl acetate -3)	
<b>Total</b>	<b>1189.90</b>	<b>Total</b>	<b>1188.90</b>

<b>MATERIAL BALANCE OF OLMESARTAN STAGE-4 BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-3	142.00	Stage-4	145.00
4-chloromethyl-5-methyl-[1,3]dioxolan-2-one	30.80	MDC Recovery	1140.00
N,N-Di methyl Acetamide	8.30	MDC Loss	24.00
TEA	25.00	Effluent water	341.97
MDC	1200.00	(Water-300,TEA-25, Lithium chloride-8.67,N,N-Dimethyl Acetamide-8.3)	
Sodium sulphate	22.00	Inorganic Solid Waste	22.00
Water	300.00	(Sodium Sulfate)	
		Organic Residue	55.13
		Process residue-19.13, Distillation residue -36 (MDC-36)	

<b>Total</b>	<b>1728.10</b>	<b>Total</b>	<b>1728.10</b>
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<b>MATERIAL BALANCE OF OLMESARTAN STAGE-5 BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-4	145.00	Olmesartan	100.00
Acetic acid	65.00	IPA Recovery	570.00
Isopropyl alcohol	600.00	IPA Loss	20.00
		Acetic Acid Recovery	50.00
		Organic solid waste	70.00
		Process residue - 1.24, (3,3,3- Triphenyl propionic Acid- 54.6, Acetic acid- 4.16) Distillation residue – 10 (IPA- 10)	
<b>Total</b>	<b>810.00</b>	<b>Total</b>	<b>810.00</b>

## 19. PANTOPRAZOLE SODIUM

### Process Description

#### Stage-1

Maltol and Dimethyl sulphate condense in Acetone solvent medium. Excess Dimethyl sulphate is removed by treating the reaction mass with Potassium Carbonate. Reaction takes place as per the below equation.

#### Stage-2

Stage-1 compound on treating with Liquor Ammonia solution stage-2 compound is formed. Reaction proceeds as per the below equation

#### Stage-3

Stage-2 compound on reaction with Phosphorous oxy chloride produces stage-3 compound. Further reaction is stopped by treating the reaction mass with water. Final product is extracted with MDC and after distilling out MDC compound is obtained. Below is the reaction scheme.

#### Stage-4

Stage-3 compound when reacts with Hydrogen peroxide in presence of Acetic acid, stage-4 compound is obtained. Methanol is the solvent employed.

#### Stage-5

Stage-4 compound on reaction with Methanol in sodium methoxide presence produces stage-5 compound. Excess Methanol is used. Below is the reaction

#### Stage-6

Above stage compound on reaction with Acetic anhydride produces an intermediate. MDC used as solvent. Product is precipitated with C.S. Flakes. Below is the reaction scheme.

#### Stage-7

Stage-6 compound when reacts with Sodium hydroxide MDC is used as solvent.

#### Stage-8

Stage-7 compound when reacts with Thionyl chloride an intermediate is formed. MDC is used as solvent. Product is crystallized in Methanol. Finally product is purified with Acetone.

#### Stage-9

When 2-Chloromethyl-3, 4-dimethoxy-pyridine Hydrochloride reacts with 5-diFluoro methoxy-2-mercapto-benzimidazole, in presence of Sodium hydroxide, product is formed. Methylene dichloride is the solvent.

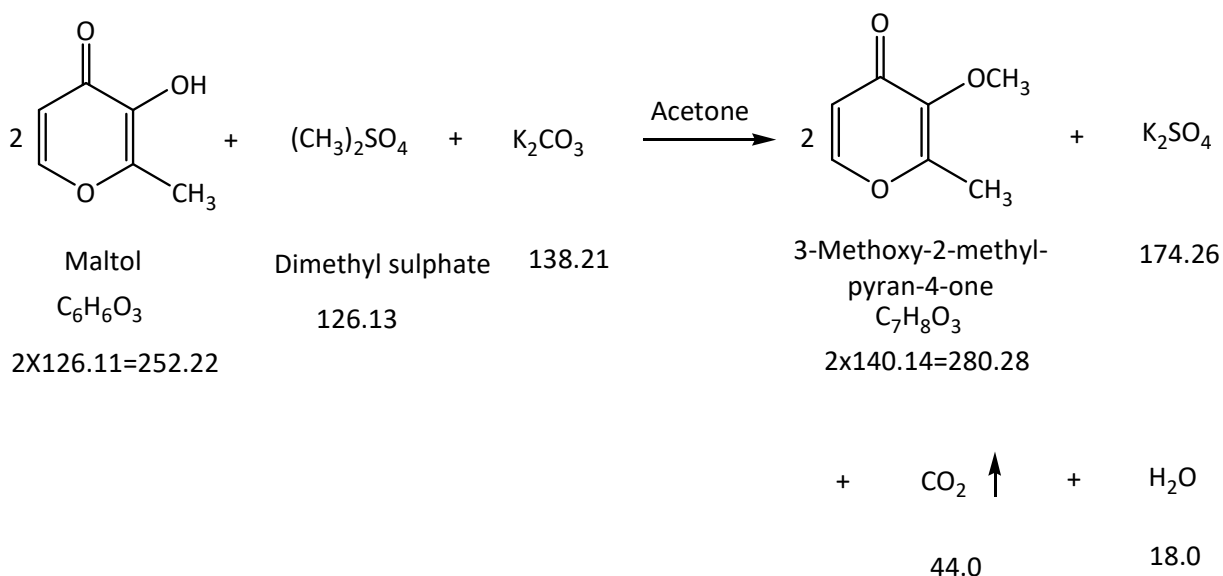
## Stage-10

Stage-9 is treated with Sodium hypochlorite in presence of Sodium hydroxide, to produce the Pantoprazole sodium. This is purified in Acetone. Methylene dichloride is used as solvent.

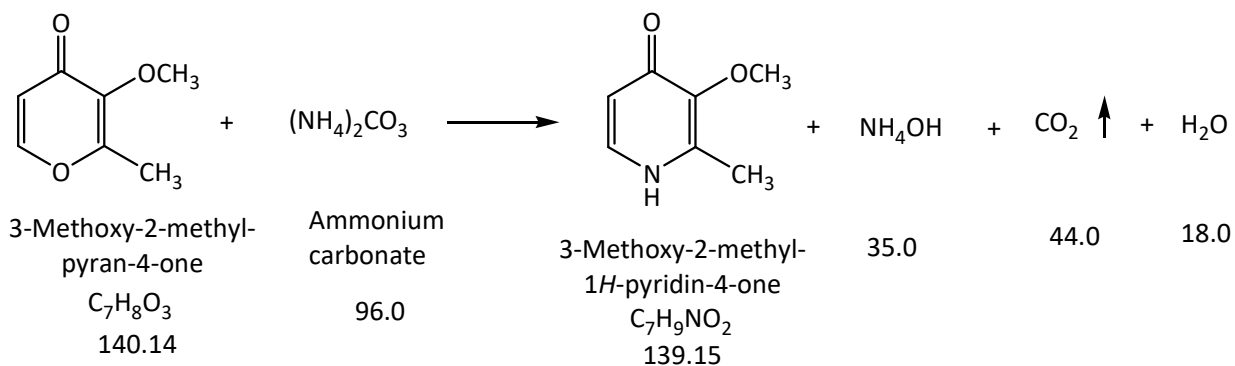
### PANTOPRAZOLE SODIUM

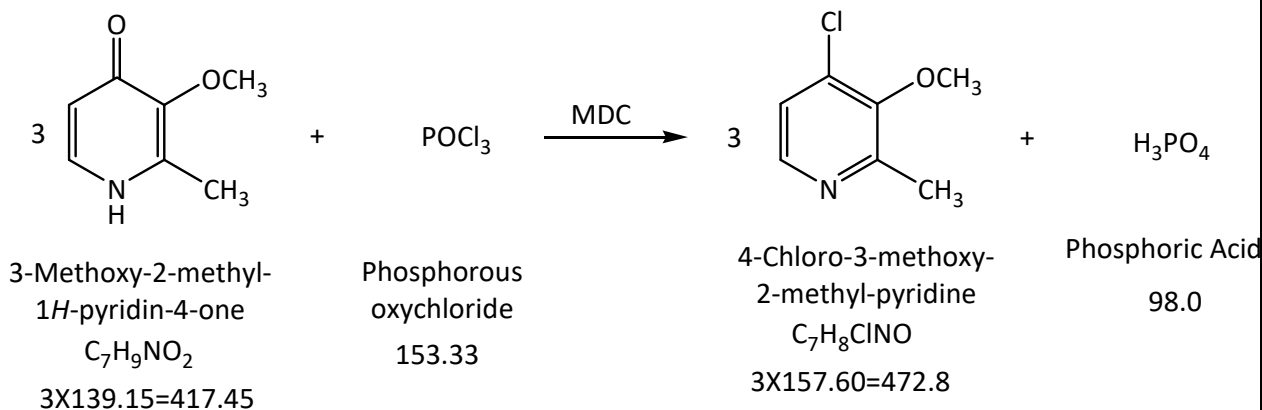
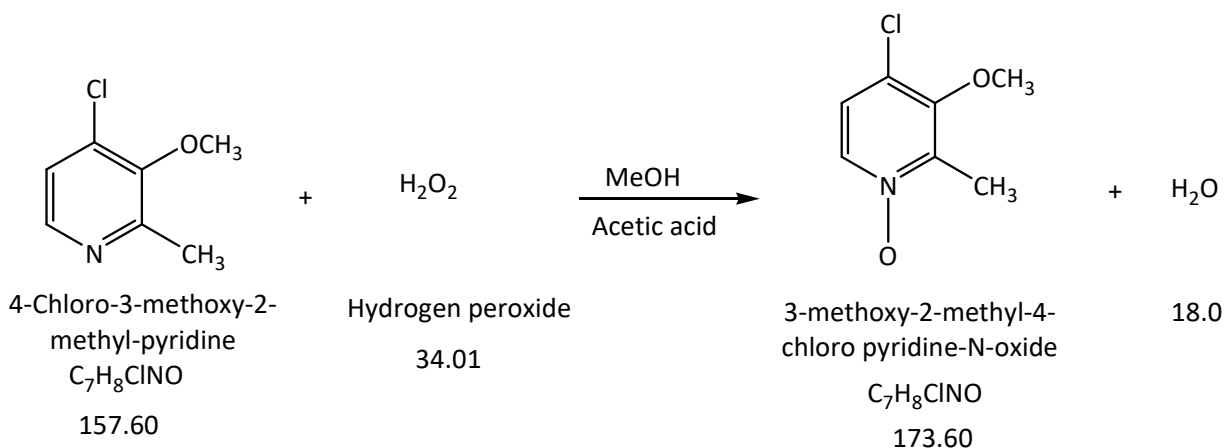
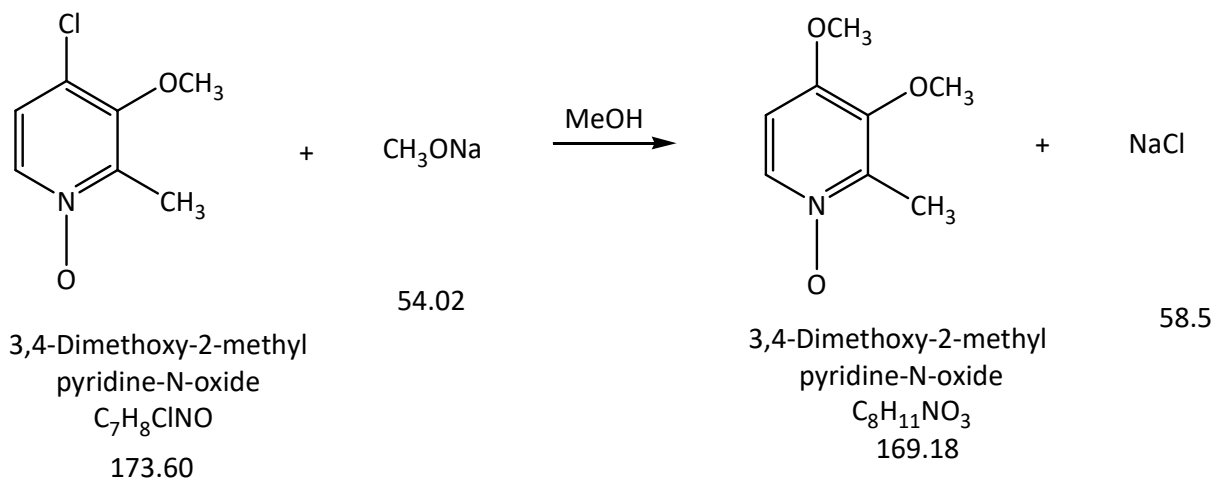
#### Route of Synthesis:

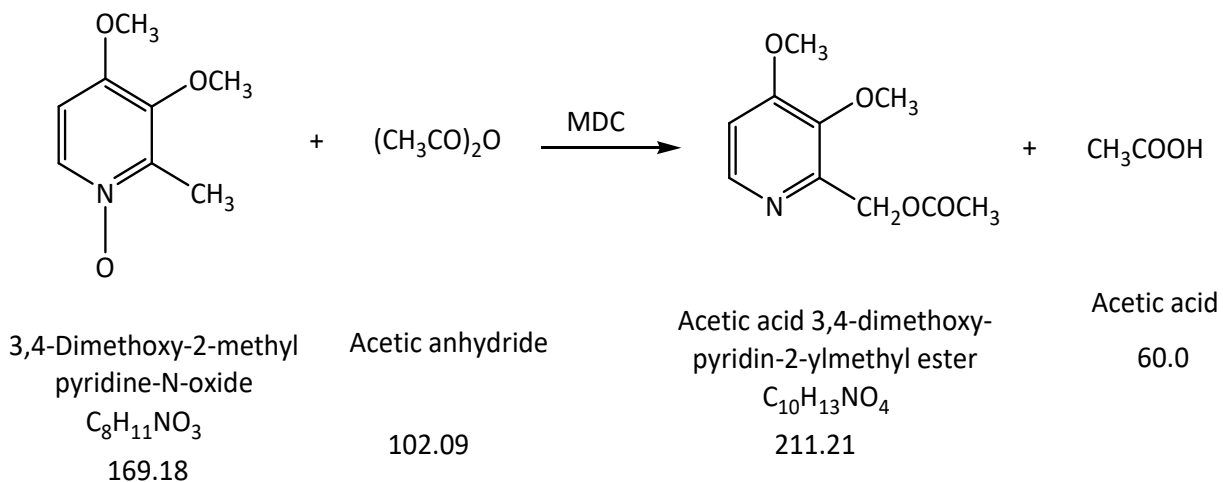
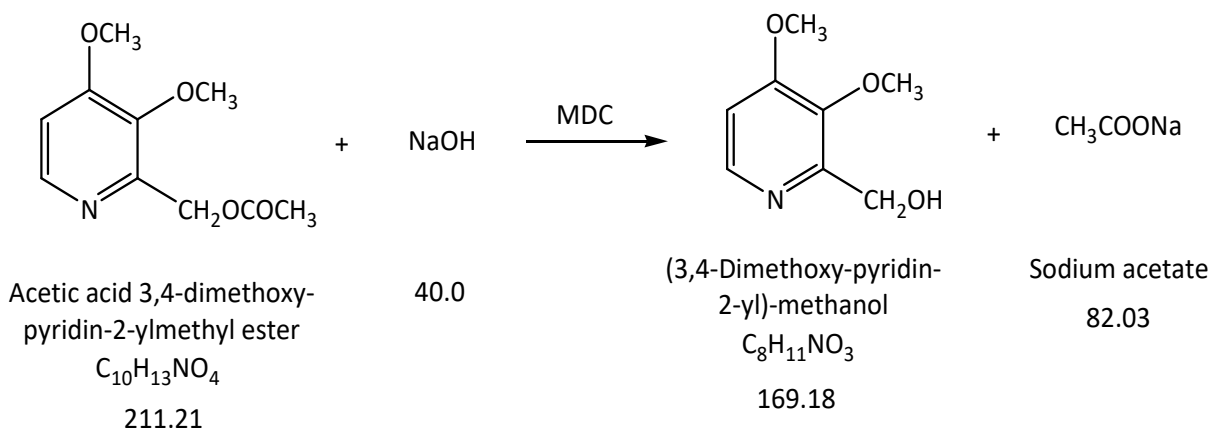
##### Stage-1:



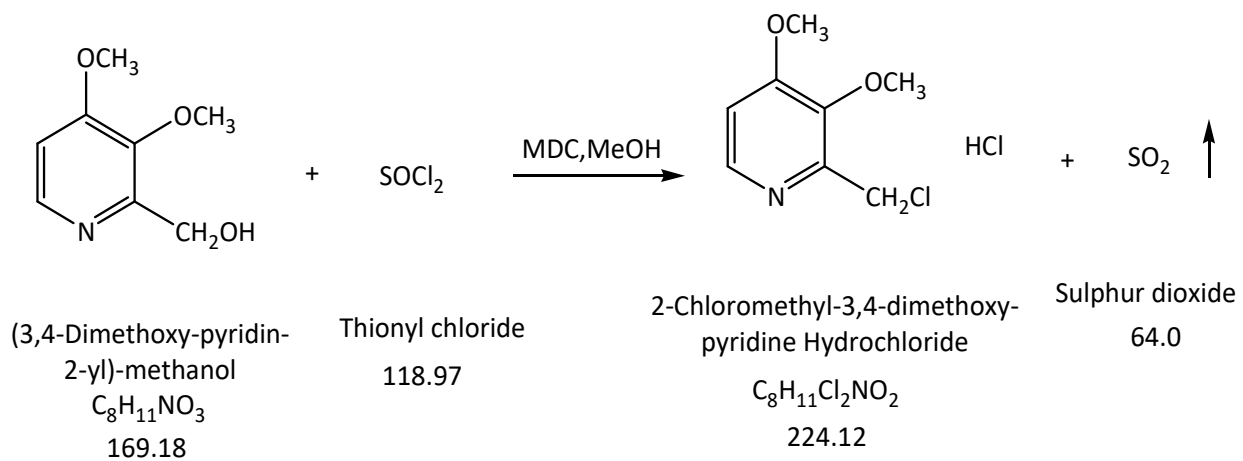
##### Stage-2:



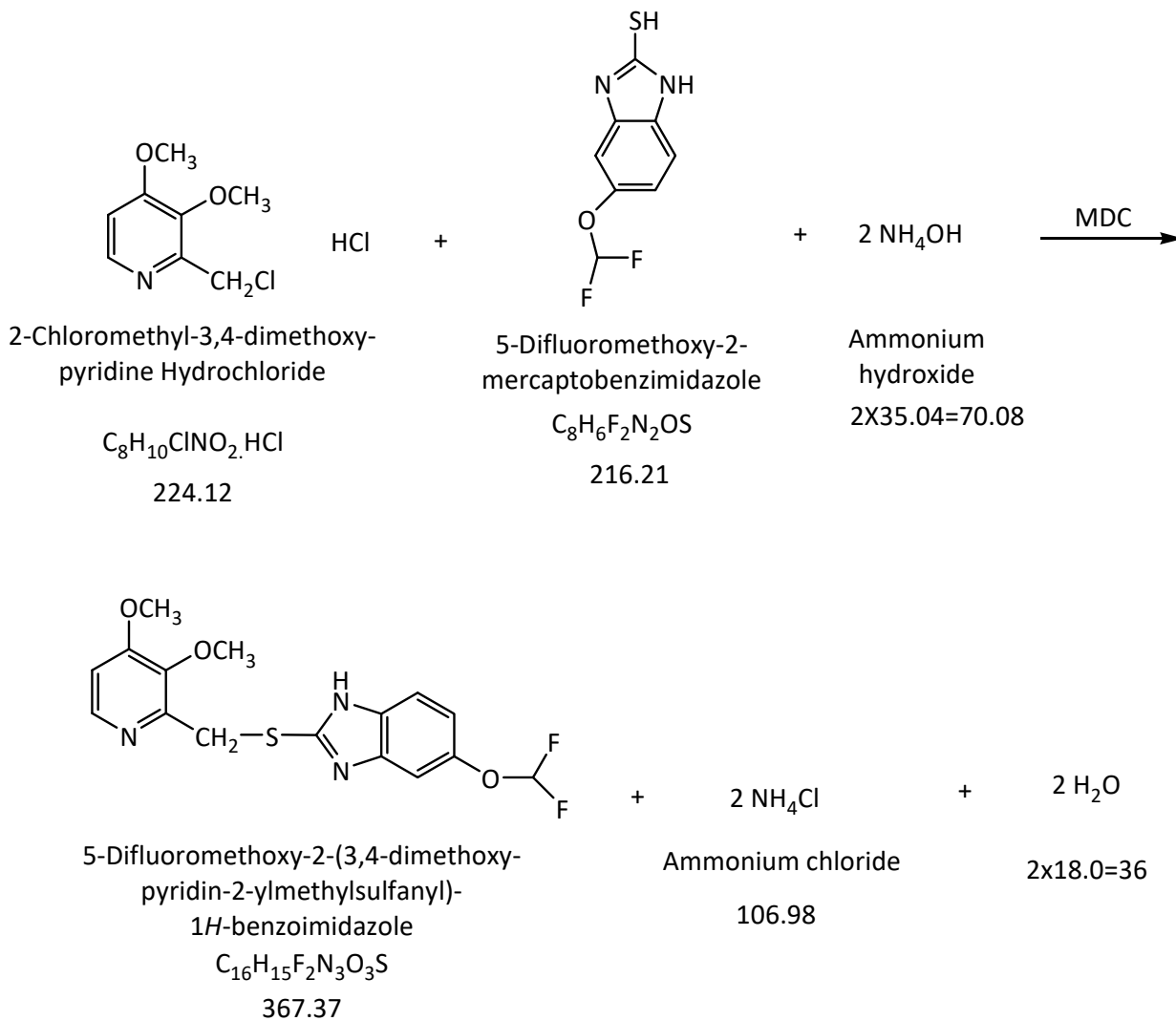
**Stage-3:****Stage-4:****Stage-5:**

**Stage-6:****Stage-7**

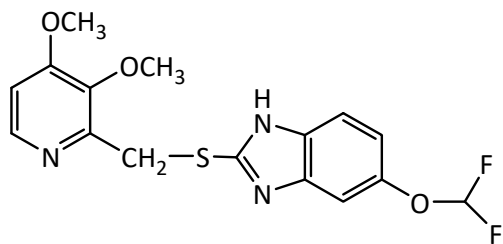
**Stage-8:**



**Stage-9:**



**Stage-10:**



5-Difluoromethoxy-2-(3,4-dimethoxy-pyridin-2-ylmethylsulfanyl)-  
1*H*-benzoimidazole  
 $C_{16}H_{15}F_2N_3O_3S$   
367.37

+ NaOCl

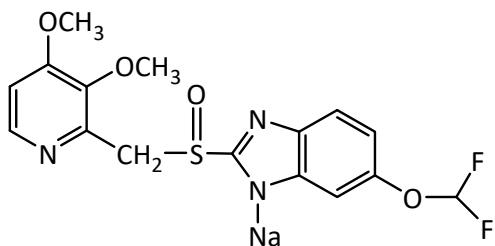
Sodium  
hypochlorite  
74.44

+

NaOH

Sodium  
hydroxide  
40.0

MDC  
→  
Acetone



Pantoprazole sodium  
 $C_{16}H_{14}F_2N_3NaO_4S$   
405.35

+

NaCl

Sodium chloride  
58.5

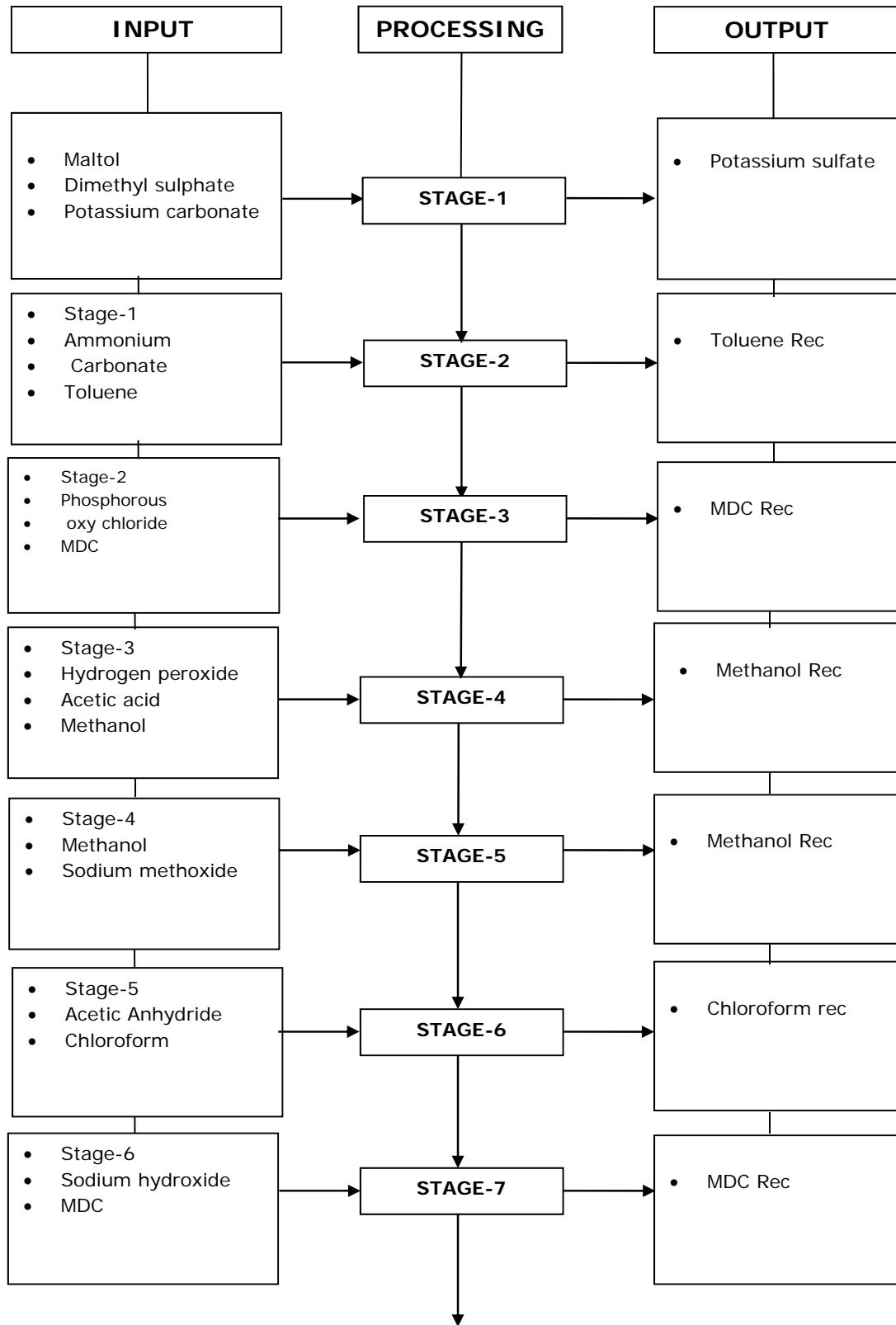
+

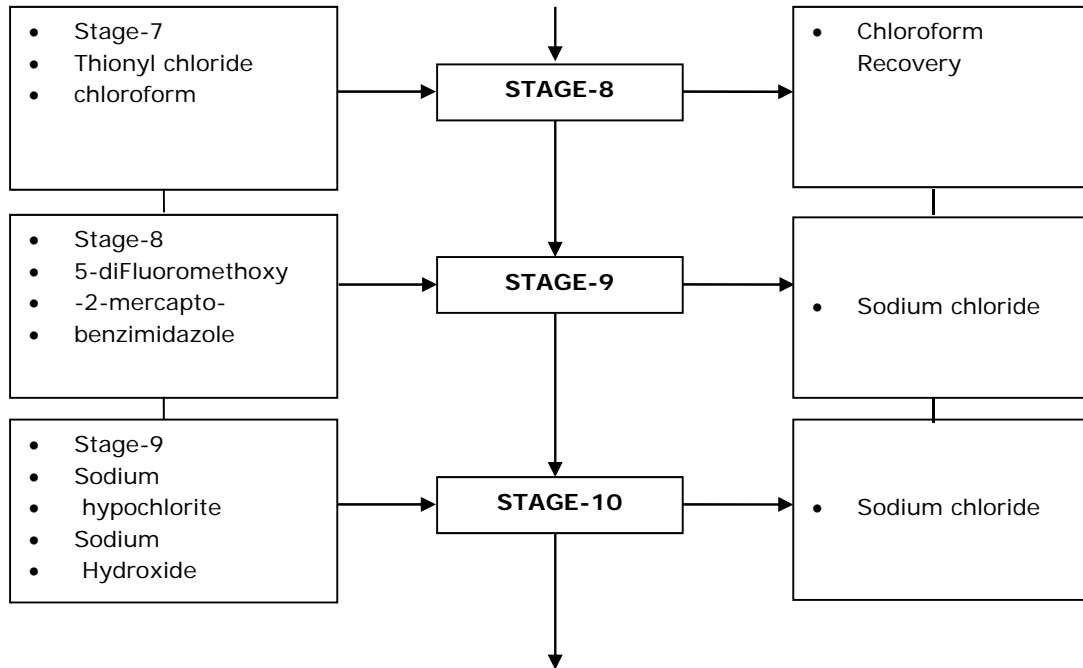
H<sub>2</sub>O

18.0

**PANTOPRAZOLE SODIUM**

**Flow Chart:**





**PANTOPRAZOLE SODIUM**

**Material Balance:**

<b>MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-1 BATCH SIZE: 200.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Maltol	66.00	Stage-1	73.00
Dimethyl sulphate	33.00	Acetone Recovery	378.00
Potassium carbonate	36.00	Acetone Loss	20.00
Acetone	400.00	Generated water	4.70
		Process Emission (Carbon dioxide)	11.46
		By-Product (Potassium Sulphate)	45.60
		Organic Residue (Organic Impurities- 0.24, Acetone-2)	2.24
<b>Total</b>	<b>535.00</b>	<b>Total</b>	<b>535.00</b>

<b>MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-2 BATCH SIZE: 200.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-1	73.00	Stage-2	72.00
Ammonium Carbonate	50.00	Toluene Recovery	280.00
Toluene	300.00	Toluene Loss	15.00
Water	600.00	Effluent Water	629.57
		(Water- 600, Ammonium hydroxide-18.2 , Generated water- 9.37, Toluene-2)	0
		Organic Residue	3.53
		(Organic Impurities- 0.53, Toluene-3)	0
		Process Emission (Carbon dioxide)	22.90
<b>Total</b>	<b>1023.00</b>	<b>Total</b>	<b>1023.00</b>

<b>MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-3 BATCH SIZE: 200.0 KGS</b>			
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INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-2	72.00	Stage-3	79.00
Phosphorous oxy chloride	26.00	MDC Recovery	285.00
Ammonia	9.00	MDC Loss	15.00
Methylenedichloride	300.00	Effluent Water	600.00
Water	600.00	(Water-600)	0
		By-Product	26.30
		(Ammonium phosphate)	0
		Organic Residue	1.70
<b>Total</b>	<b>1007.00</b>	<b>Total</b>	<b>1007.00</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-4 BATCH SIZE: 200.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-3	79.00	Stage-4	87.00
Hydrogen peroxide	17.00	MDC Recovery	668.00
Acetic acid	30.00	MDC Loss	30.00
Methanol	250.00	Methanol Recovery	233.00
Sodium Hydroxide	20.00	Methanol Loss	12.50
MDC	700.00	Effluent Water	419.50
Water	400.00	(Water-400, Generated water-17, Methanol-2.5)	
		By-Product	41.00
		(Sodium acetate)	
		Organic Solid Waste	5.00
		(Organic Impurities- 1,MDC-2,Methanol- 2)	
<b>Total</b>	<b>1496.00</b>	<b>Total</b>	<b>1496.00</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-5 BATCH SIZE: 200.0 KGS	
INPUT	OUTPUT

NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-4	87.00	Stage-5	85.00
Methanol	500.00	Methanol Recovery	460.00
Sodium methoxide	27.00	Methanol Loss	20.00
Acetic Acid	10.00	Effluent Water	642.20
Water	600.00	(Water-600, Sodium Chloride-29.2, Methanol-3, Acetic acid-10)	0
		Organic Residue	16.8
		Process residue-4.8 Methanol-12	
<b>Total</b>	<b>1224.00</b>	<b>Total</b>	<b>1224.00</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-6 BATCH SIZE: 200.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-5	85.00	Stage-6	106.00
Acetic Anhydride	172.00	Chloroform Recovery	190.00
Chloroform	200.00	Chloroform Loss	10.00
Water	400.00	Acetic acid Recovery	101.00
		Effluent Water	400.00
		(Water-400)	0
		Organic Residue	50.00
<b>Total</b>	<b>857.00</b>	<b>Total</b>	<b>857.00</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-7 BATCH SIZE: 200.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-6	106.00	Stage-7	85.00
MDC	200.00	MDC Recovery	190.00
Sodium hydroxide	20.00	MDC Loss	10.00
Water	200.00	Effluent Water	200.00
		(Water-200)	
		By-Product	41.00
		(Sodium acetate)	
<b>Total</b>	<b>526.00</b>	<b>Total</b>	<b>526.00</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-8 BATCH SIZE: 200.0 KGS			
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INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-7	85.00	Stage-8 (Chloro compound)	112.00
Thionyl chloride	60.00	Chloroform Recovery	810.00
Chloroform	850.00	Chloroform Loss	40.00
Methanol	125.00	Methanol Recovery	99.00
Acetone	200.00	Methanol Loss	25.00
		Acetone Recovery	189.00
		Acetone Loss	10.00
		Process Emission	32.00
		(Sulphur Dioxide)	
		Organic Residue	3.00
		(Organic Impurities-1, Methanol-1, Acetone-1)	
<b>Total</b>	<b>1320.00</b>	<b>Total</b>	<b>1320.00</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-9 BATCH SIZE: 200.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-8	112.00	Stage-9	183.00
5-diFluoromethoxy-2-mercapto-Benzimidazole	108.00	Toluene Recovery	472.00
Ammonium hydroxide	35.50	Toluene Loss	25.00
Toluene	500.00	Effluent Water	619.50
Water	600.00	(Water-600, gen.Water-18, Toluene-1.5)	0
		B-Product	54.19
		(Ammonium chloride)	0
		Organic Residue	1.81
		(Organic Impurities-0.31, Toluene-1.5)	
<b>Total</b>	<b>1355.50</b>	<b>Total</b>	<b>1355.50</b>

MATERIAL BALANCE OF PANTOPRAZOLE SODIUM STAGE-10 BATCH SIZE: 200.0 KGS			
--	--	--	--

INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-8	183.00	Pantoprazole Sodium	200.00
Sodium hypochlorite	37.00	MDC Recovery	950.00
Sodium Hydroxide flakes	20.00	MDC Loss	50.00
Ammonium Chloride	25.00	Acetone Recovery	378.00
Methylene dichloride	1000.00	Acetone Loss	20.00
Activated Carbon	10.00	Effluent Water	465.00
Acetone	400.00	(Water-400, gen. water-9, Sodium chloride-29, Aluminum chloride-25, Acetone-2)	0
Water	400.00	Spent carbon	10.00
		Organic Residue	2.00
<b>Total</b>	<b>2075.00</b>	<b>Total</b>	<b>2075.00</b>

## 20. PIRACTONE OLAMINE

### Process Description:

#### Stage-1

3, 3-Dimethyl acrylic acid undergoes Condensation with Methanol to give Stage-1 compound in presence PTSA.

#### Stage-2

Stage-1 compound and 3, 5, 5 tri methyl hexanoyl chloride undergoes friedel craft reaction in presence of anhydride Aluminum tri chloride and EDC at cooling to give Stage-2 compound

#### Stage-3

Stage-2 compound Cyclised with Sodium methoxide in Methanol at cooling to give Stage-3 compound.

#### Stage-4

Stage-3 compound reacts with hydroxylamine hydrochloride and sodium carbonate in presence of Ethyl acetate to give Stage-4 compound

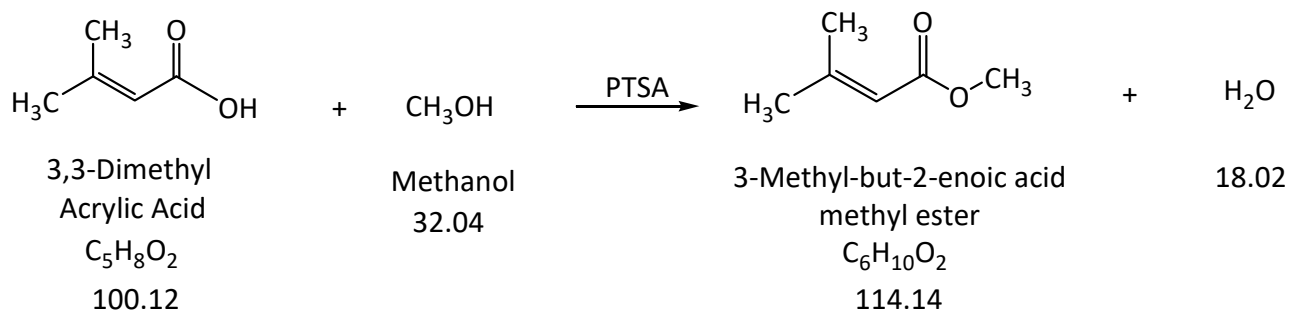
#### Stage-5

Stage-4 compound reacts with mono ethanol amine in presence of Ethyl acetate to give Piroctone Olamine.

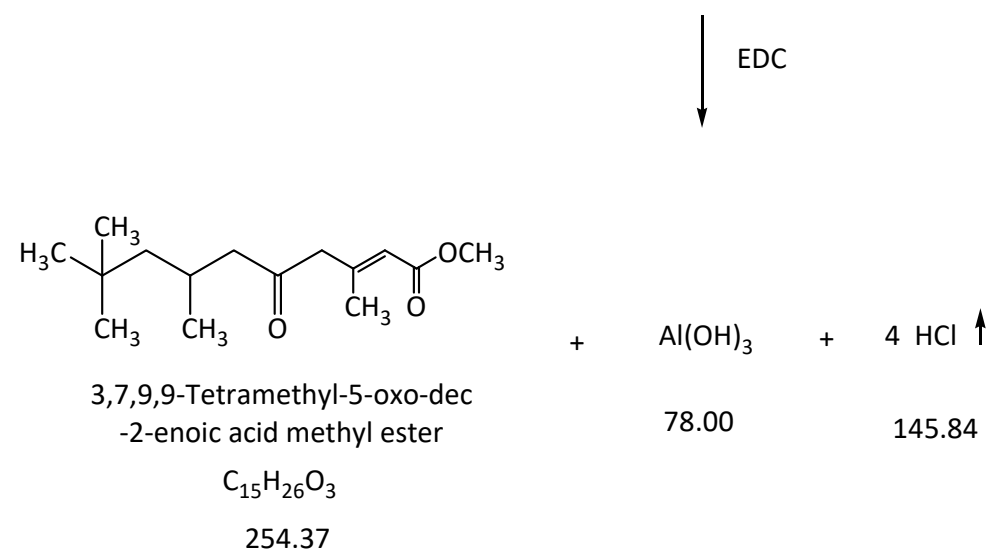
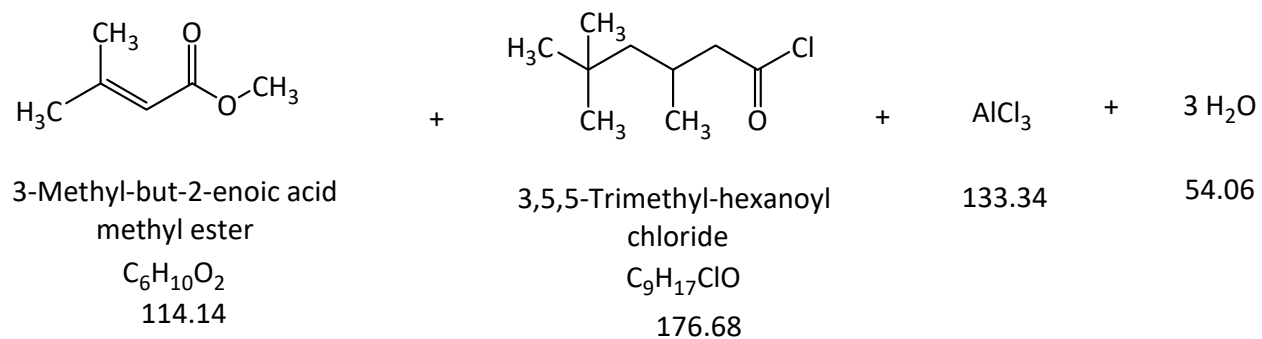
## PIRACTONE OLAMINE

### Route of synthesis:

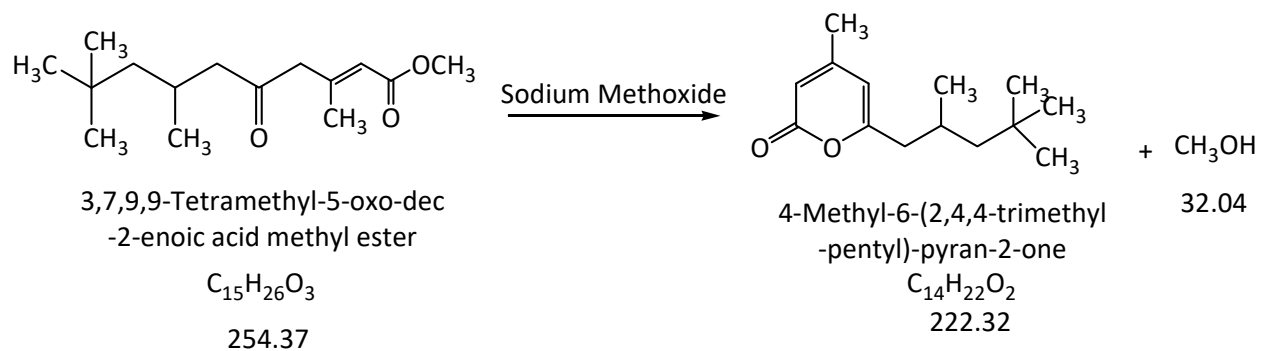
#### Stage-1



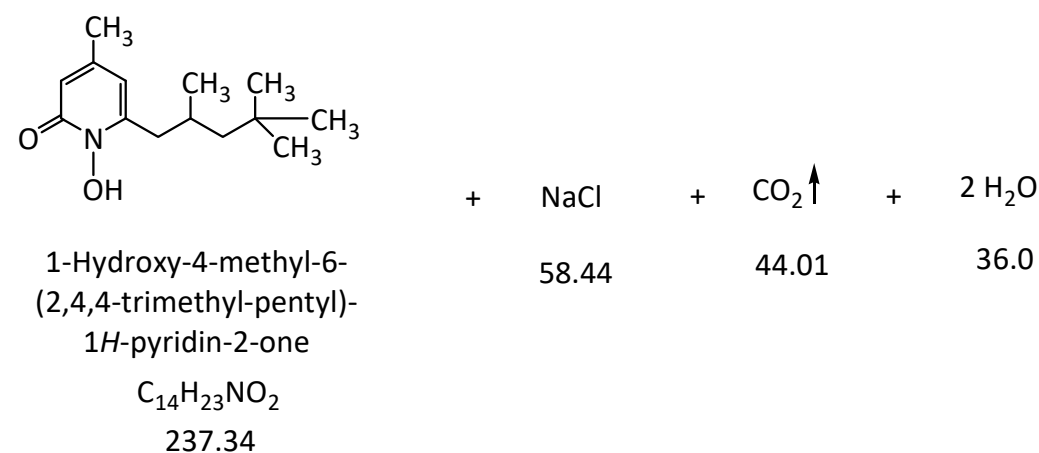
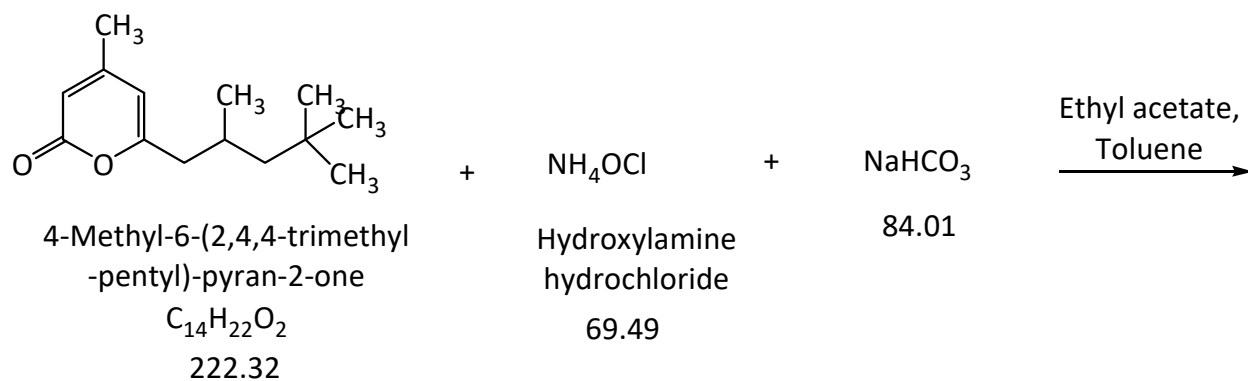
#### Stage-2



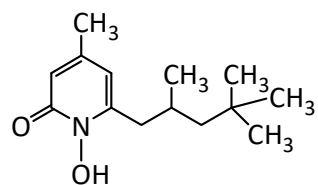
### Stage-3



### Stage-4

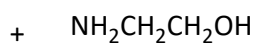


### Stage-5



1-Hydroxy-4-methyl-6-(2,4,4-trimethyl-pentyl)-  
1*H*-pyridin-2-one

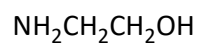
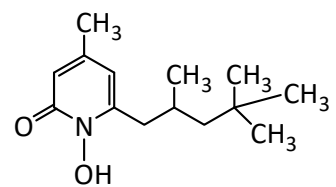
$C_{14}H_{23}NO_2$   
237.34



Ethanolamine

61.08

Ethylacetate

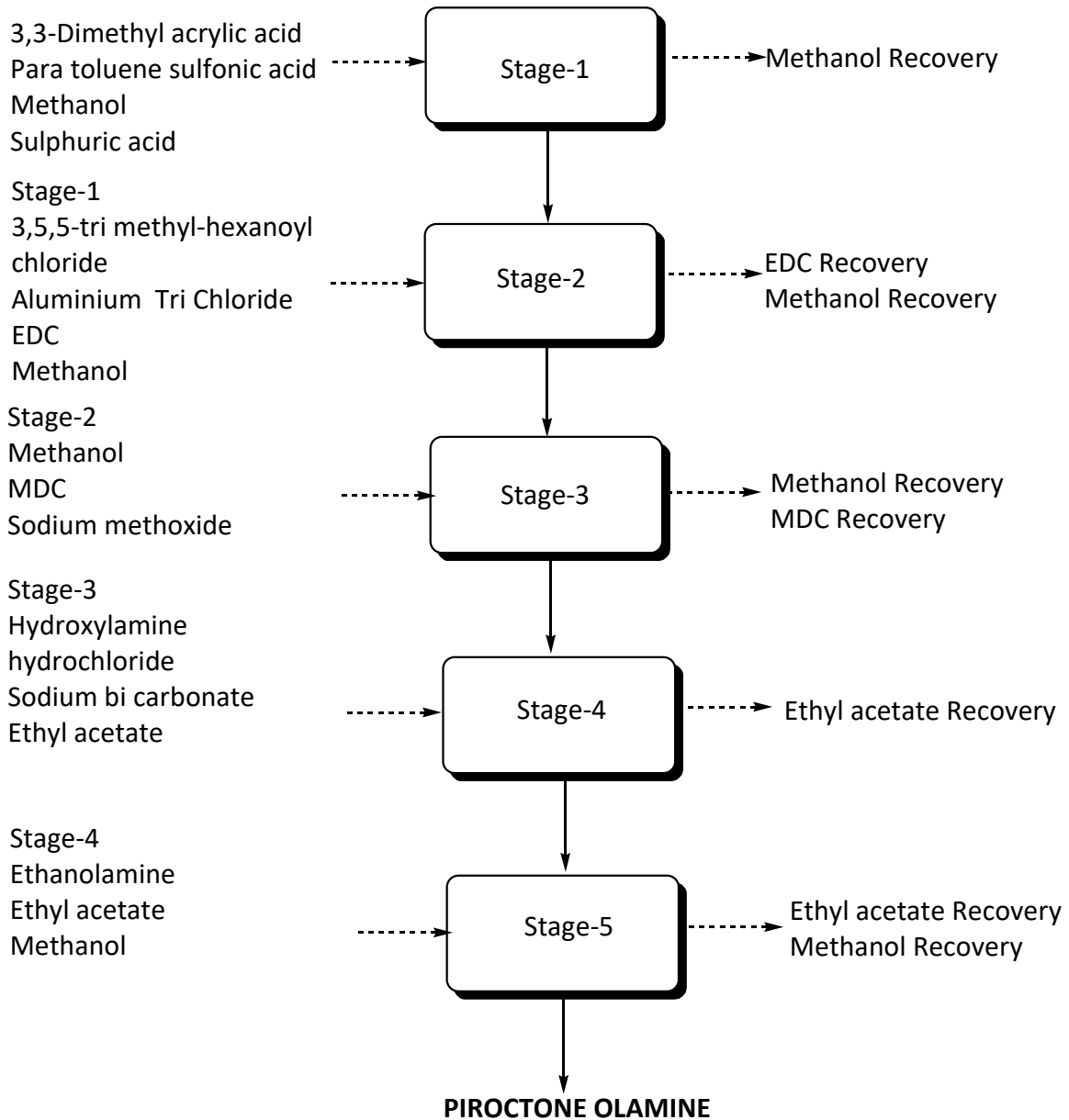


Piractone Olamine

$C_{16}H_{30}N_2O_3$   
298.42

# PIROCTONE OLAMINE

## Flow Chart



## PIROCTONE OLAMINE

### Material Balance

Material Balance of Piroctone Olamine Stage-1 Batch Size: 200.00Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
3,3-Dimethyl acrylic acid	85.00	Stage-1	78.00
Para toluene sulfonic acid	20.00	Methanol Recovery	438.00
Methanol	500.00	Methanol loss	24.00
Sodium sulphate	5.00	Effluent water	540.30
Water	500.00	(water-500,Generated water-15.3, Para toluene sulfonic acid-20,Methanol-5)	
		Inorganic solid waste	5.00
		(Sodium sulphate)	
		Organic Residue	24.70
		(Organic Impurities-19.2, Methanol-5.5)	
<b>Total</b>	<b>1110.00</b>	<b>Total</b>	<b>1110.00</b>

Material Balance of Piroctone Olamine Stage-2 Batch Size: 200.00Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	78.00	Stage-2	172.00
3,5,5-tri methyl-hexanoyl chloride	121.00	EDC Recovery	950.00
Aluminium Tri Chloride	93.00	EDC Loss	50.00
EDC	1000.00	Methanol Recovery	475.00
Methanol	500.00	Methanol Loss	25.00
Sodium sulphate	7.00	By-Product	1750.00
Water	1730.00	(Aluminium hydroxide solution)	
		Process Emissions	100.00
		(Hydrogen chloride-100)	
		Inorganic solid waste	7.00
		(Sodium sulphate)	
<b>Total</b>	<b>3529.00</b>	<b>Total</b>	<b>3529.00</b>

Material Balance of Piroctone Olamine Stage-3 Batch Size: 200.00Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-2	172.00	Stage-3	150.00
Methanol	1000.00	Methanol Recovery	945.00
Sodium methoxide	25.00	Methanol Loss	50.00
Sodium sulphate	2.00	Effluent Water	796.70
Water	750.00	(Water-750,Methanol-21.7, Sodium methoxide-25)	
		Inorganic solid waste	2.00
		(Sodium sulphate)	
		Organic residue	5.30
		(Organic impurities-0.3,Methanol- 5)	
Total	1949.00	Total	1949.00

Material Balance of Piroctone Olamine Stage-4 Batch Size: 200.00Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-3	150.00	Stage-4	160.00
Hydroxylamine hydrochloride	47.00	Ethyl acetate Recovery	470.00
Sodium bi carbonate	57.00	Ethyl acetate Loss	20.00
Ethyl acetate	500.00	Effluent Water	565.80
Sodium sulphate	3.00	(water-500,Generated water- 24.3, Sodium chloride-39.5)	
Water	500.00	Process emission	29.70
		(Carbon dioxide)	
		Inorganic solid waste	3.00
		(Sodium sulphate)	
		Organic Residue	10.50
		(Organic Impurities-0.5,Ethyl acetate-10)	
Total	2057.00	Total	2057.00

Material Balance of Piroctone Olamine

Stage-5

Batch Size: 200.00Kgs

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-4	160.00	Piractone Olamine	200.00
Ethanolamine	45.00	Ethyl acetate Recovery	470.00
Ethyl acetate	500.00	Ethyl acetate loss	25.00
Methanol	1000.00	Methanol Recovery	940.00
Activated carbon	5.00	Methanol loss	50.00
Sodium sulphate	3.00	Effluent water	505.00
Water	500.00	(Water-500,Methanol-5)	
		Spent carbon	5.00
		Inorganic solid waste	3.00
		(Sodium sulphate)	
		Organic Residue	15.00
		(Organic Impurities-5,Ethyl acetate-5,Methanol-5)	
Total	2213.00	Total	2213.00

## 21. RAMIPRIL

### Process description:

#### Stage-1

2-(1-carboxy-ethylamino)-4-phenyl-butyric acid ethyl ester undergoes condensation with (cis, endo)-octahydro-cyclopenta[b]pyrrole-2(s)-carboxylic acid to give Stage-1 compound in presence of Ethyl acetate and Triethylamine.

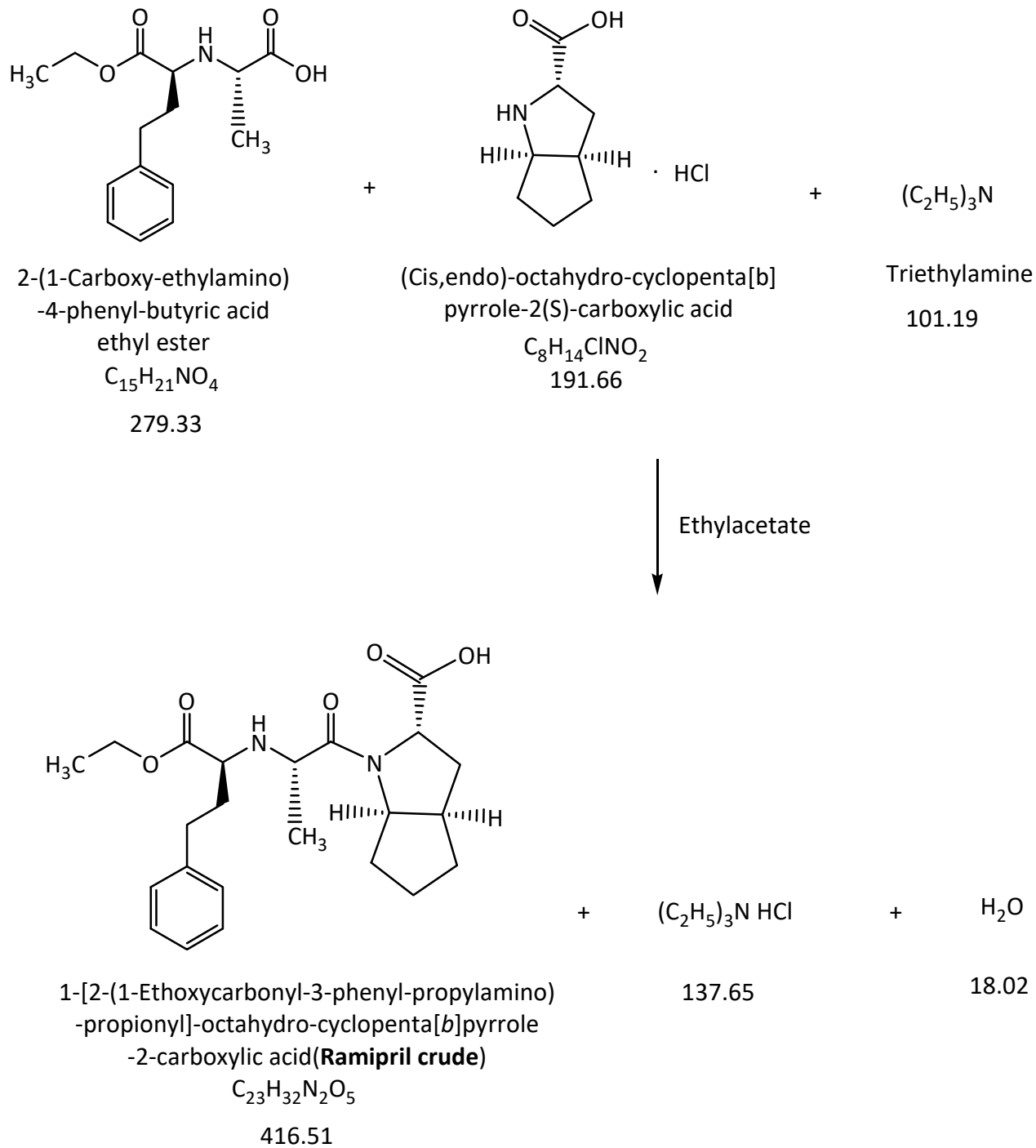
#### Stage-2

Stage-1 compound Purification with Ethanol to give Ramipril

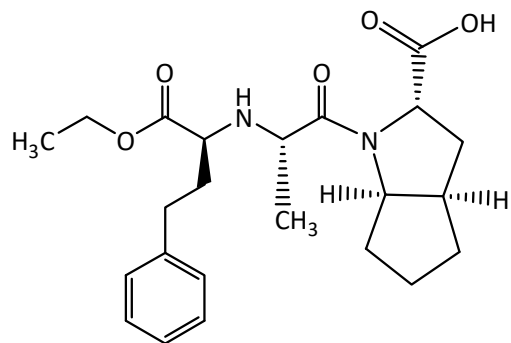
# RAMIPRIL

## Route of synthesis:

### Stage-1



## Stage-2

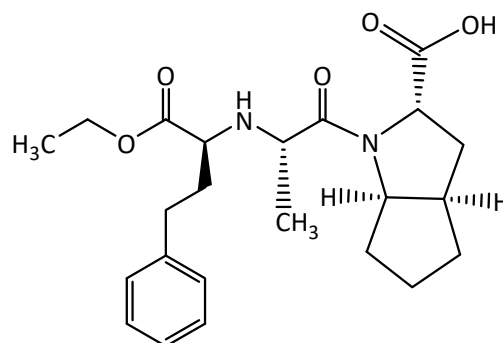


1-[2-(1-Ethoxycarbonyl-3-phenyl-propylamino)-propionyl]-octahydro-cyclopenta[*b*]pyrrole-2-carboxylic acid (**Ramipril crude**)

$C_{23}H_{32}N_2O_5$

416.51

Ethanol



1-[2-(1-Ethoxycarbonyl-3-phenyl-propylamino)-propionyl]-octahydro-cyclopenta[*b*]pyrrole-2-carboxylic acid (**Ramipril pure**)

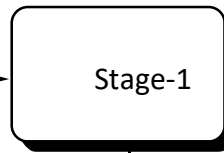
$C_{23}H_{32}N_2O_5$

416.51

# RAMIPRIL

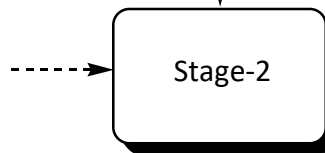
## Flow chart:

2-(1-carboxy-ethylamino)-4-phenyl-butyrlic acid ethylester  
(cis,endo)-octahydro-cyclopenta[b]pyrrole-2(s)-carboxylic acid  
Ethyl acetate  
Triethylamine



Ethyl acetate Recovery  
Triethylamine Recovery

Stage-1  
Ethanol  
5% Pd/Activated carbon



Ethanol recovery

**Ramipril**

## RAMIPRIL

### Material Balance

Material balance of Ramipril Stage-1 Batch Size: 500.00Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity In Kg
2-(1-carboxy-ethylamino)-4-phenyl-butyric acid ethylester	343.00	Stage-1	510.00
(cis,endo)-octahydro-cyclopenta[b]pyrrole-2(s)-carboxylic acid hydrochloride	236.00	By-Product	645.00
Ethyl acetate	600.00	(Triethyl amine Hydrochloride)	
Triethylamine	600.00	Ethyl acetate Recovery	570.00
Water	100.00	Ethyl acetate Loss	30.00
		Effluent water	122.15
		(water-100,Generated water-22.13)	
		Organic residue	1.85
<b>Total</b>	<b>1879.00</b>	<b>Total</b>	<b>1879.00</b>

Material balance of Ramipril Stage-2 Batch Size: 500.00Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity In Kg
Stage-1	510.00	Ramipril (Pure)	500.00
Ethanol	650.00	Ethanol recovery	618.00
5% Pd/Activated carbon	10.00	Ethanol loss	32.00
Water	50.00	Effluent water	50.00
		(Water-50)	
		Spent 5% Pd/Activated carbon	10.00
		Organic residue	10.00
<b>Total</b>	<b>1220.00</b>	<b>Total</b>	<b>1220.00</b>

## 22. RISPERIDONE

### **Process Description:**

#### **Stage-1**

3-(2-chloroethyl)-2-Methyl-6,7,8,9-tetrahydro-4H-pyridol[1,2]pyrimidin-4-one hydrochloride reacts with 6-Fluoro-3-(4-piperidiny)-1,2-benzisoxazole in the presence of Sodium bicarbonate and MIBK as a solvent media to give stage-1 as product.

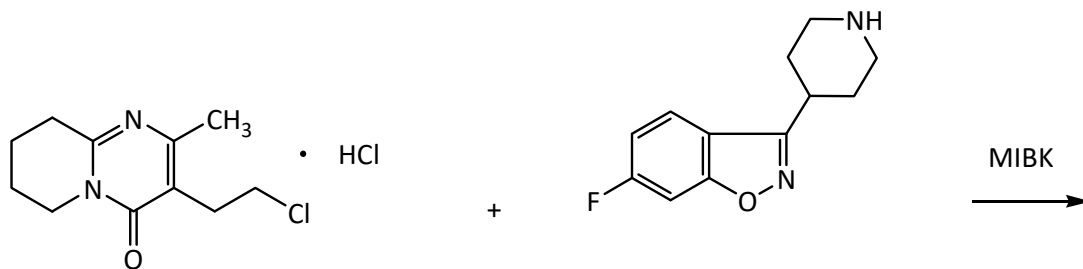
#### **Stage-2**

Stage -1 undergoes purification in the presence of IPA as a solvent media to give Risperidone as product.

# RISPERIDONE

## Route of synthesis:

### Stage-1:



3-(2-chloroethyl)-6,7,8,9-tetrahydro-  
2-methylpyrido[1,2-a]pyrimidin-4-one  
hydrochloride

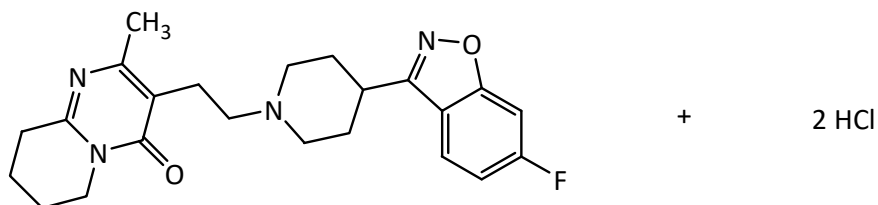
$C_{11}H_{16}Cl_2N_2O$

263.16

6-Fluoro-3-(4-piperidinyl)  
-1,2 benzisoxazole

$C_{12}H_{13}FN_2O$

220.24



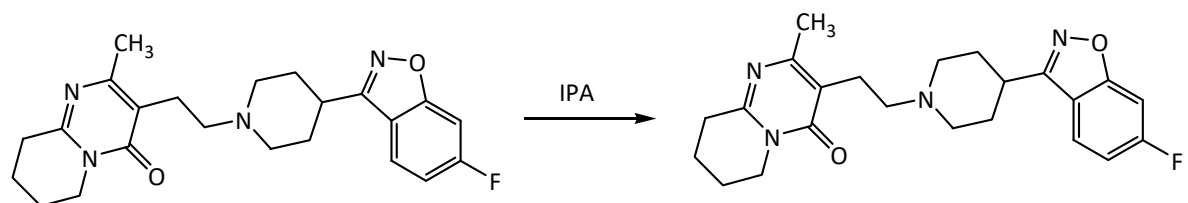
3-[2-[4-(6-fluoro-1,2-benzisoxazol-3-yl)piperidin-1-  
yl]-2-methyl-6,7,8,9-tetrahydro-4H-pyrido-  
[1,2-a]pyrimidin-4-one

$C_{23}H_{27}FN_4O_2$

410.48

2X36.5=73.0

**Stage-2:**



Risperidone crude

$C_{23}H_{27}FN_4O_2$

410.48

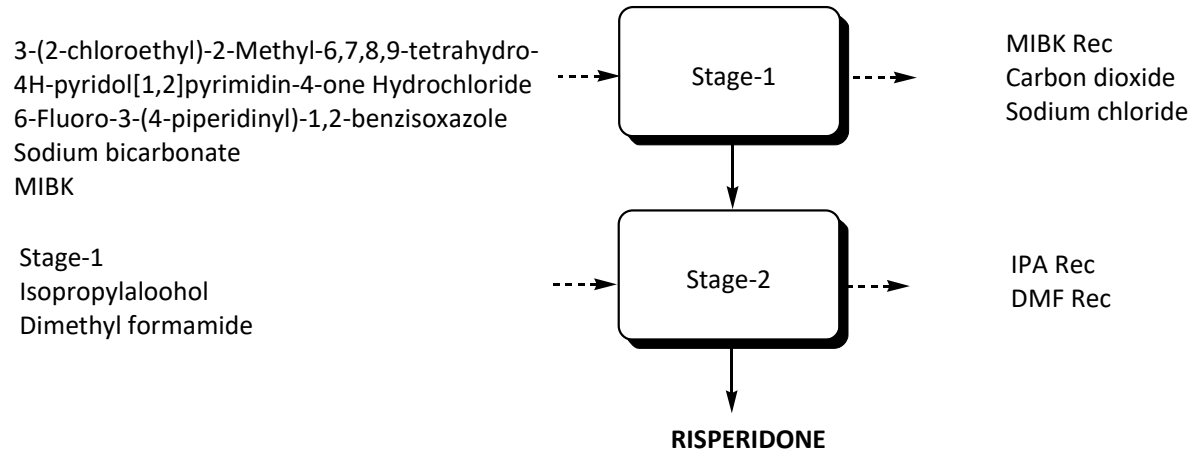
Risperidone Pure

$C_{23}H_{27}FN_4O_2$

410.48

# RISPERIDONE

## Flow Chart:



## RISPERIDONE

### Material Balance:

Material Balance of Risperidone Stage-1 Batch Size: 500Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
6-Fluoro-3-(4-piperidinyl)-1,2-benzisoxazole Hydrochloride	260.00	Stage-1	503.00
3-(2-Chloroethyl)-2-Methyl-6,7,8,9-Tetrahydro-4H-pyrido [1,2- $\alpha$ ]Pyrimidin-4-one HCl	315.12	MIBK Recovery	285.00
Potassium iodide	2.00	MIBK Loss	15.00
Methyl Isobutyl ketone	300.00	Effluent water	111.00
Sodium hydroxide	9.00	(Water-100 Sodium hydroxide-9,Potassium iodide-2)	
Water	100.00	Process Emission	72.12
		(Hydrogen chloride-72.12)	
<b>Total</b>	<b>986.12</b>	<b>Total</b>	<b>986.12</b>

Material Balance of Risperidone Stage-2 Batch Size: 500 Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	503.00	Risperidone (pure)	500.00
Isopropyl alcohol	500.00	IPA Recovery	472.00
DMF	25.00	IPA Loss	25.00
Activated carbon	5.00	DMF Recovery	22.00
Hyflow	5.00	DMF Loss	2.00
		Organic Residue	7.00
		(Organic impurities-3,IPA-3,DMF-1)	
		Spent carbon & hyflow	10.00
<b>Total</b>	<b>1038.00</b>	<b>Total</b>	<b>1038.00</b>

## 23. SACUBITRIL

### Process Description

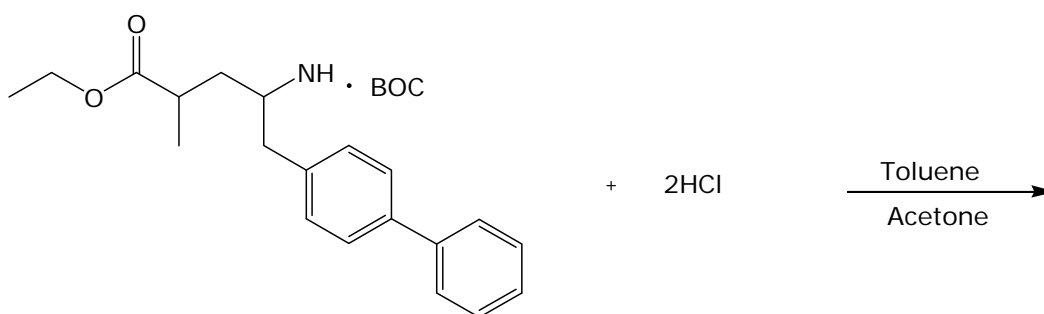
#### Stage-1

Tris(4-methoxyphenyl)borane ammonia complex reacts with Hydrochloric acid in presence of Acetone and Toluene to give Stage-1 products.

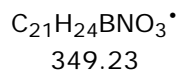
#### Stage-2

Stage-1 products reacts with Furan-2,5-dione in presence of Toluene and Methanol to give Sacubitril.

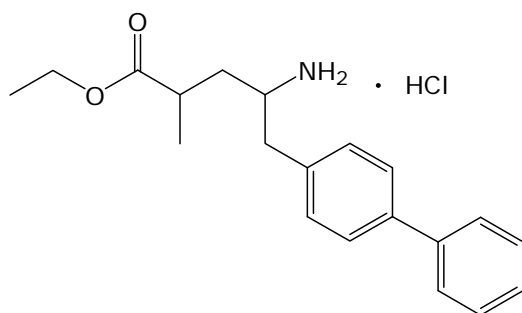
#### Stage-1



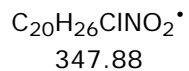
Tris(4-methoxyphenyl)borane ammonia complex



72.92



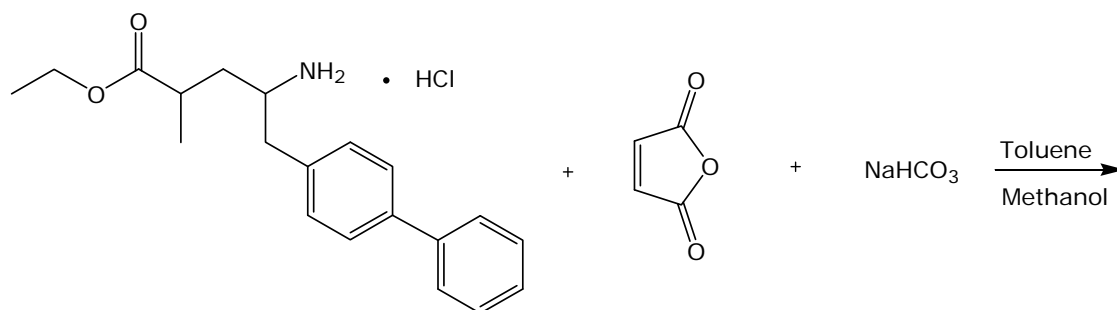
4-Amino-5-biphenyl-4-yl-2-methyl-pentanoic acid ethyl ester



+ BOC . Cl

74.27

## Stage-2



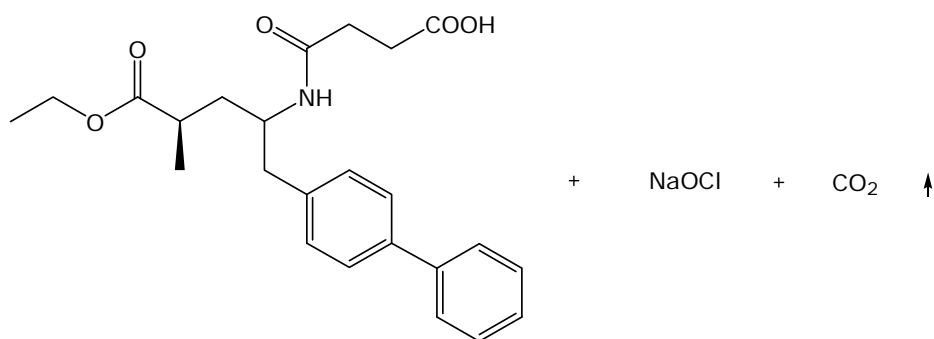
4-Amino-5-biphenyl-4-yl-2-methyl-pentanoic acid ethyl ester

C<sub>20</sub>H<sub>26</sub>ClNO<sub>2</sub>•  
Mol. Wt.: 347.88

Furan-2,5-dione

C<sub>4</sub>H<sub>2</sub>O<sub>3</sub>  
98.06

84.01



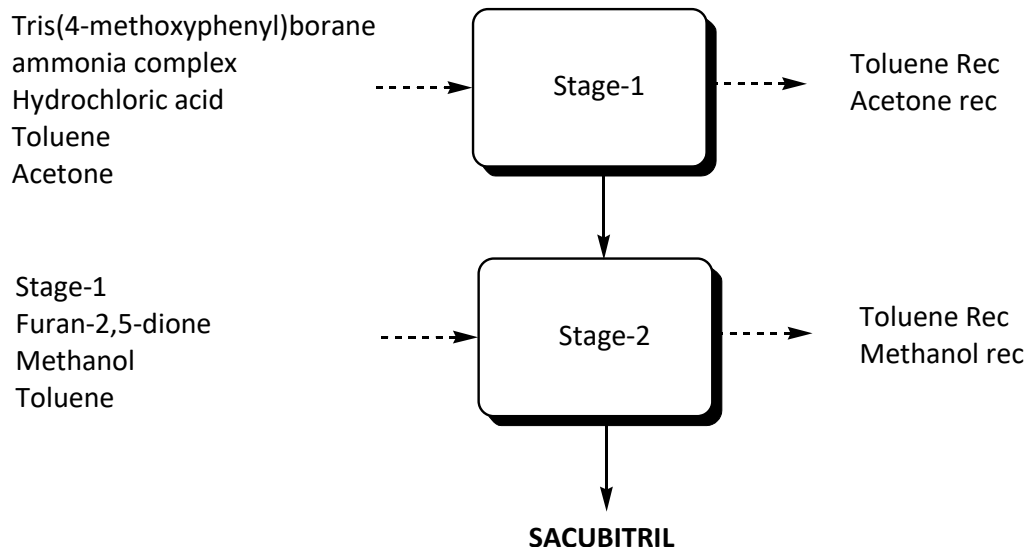
4-(4-decan-2-yloxy-3-nitrophenyl)-3-methylbenzoate

C<sub>24</sub>H<sub>30</sub>NO<sub>5</sub>  
412.50

74.44

44.01

### Flow Chart



### Material Balance:

Material Balance of Sacubitril Stage-1 Batch Size: 100.0 Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Tris(4-methoxyphenyl)borane	98	Stage-1	90
Hydrochloric acid	73	Toluene Recovery	290
Toluene	300	Toluene Loss	5
		Acetone recovery	380
		Acetone loss	10
Acetone	400	Effluent water	300
Water	300	(Water-300)	
		Organic residue	96
		Process residue-60, Toluene-5, Acetone-10, Boc.Cl-21,	
Total	1171	Total	1171

Material Balance of Sacubitril  
 Stage-2  
 Batch Size: 100.0 Kg

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	90	Sacubitril	100
Furan-2,5-dione	26	Toluene Recovery	380
Toluene	400	Toluene Loss	10
Methanol	400	Methanol recovery	380
Sodium bicarbonate	22	Methanol loss	10
Acetone	0	Effluent water	319
Water	300	(Water-300, Sodium hypochlorite-19)	0
		Process emission Carbon dioxide	11
		Organic residue	28
		Process residue-8, Toluene-10, Methanol-10,	
<b>Total</b>	<b>1238</b>	<b>Total</b>	<b>1238</b>

## 24. SPARFLOXACIN

The Pharma is produced in five stages.

### Stage-1

Pentafluorobenzoic acid, Thionylchloride, Diethylmalonate, Sodium Hydroxide and Magnesium react together to produce stage-1 compound. Toluene is the solvent. Inorganic salts are removed by water wash. Finally product is purified with Ethanol.

### Stage-2

Above product on reaction with Triethyloxoformamide, Cyclopropylamine and Potassium caronate produces, stage-2 compound. Ethanol is the solvent used. Inorganic salts are removed by water wash.

### Stage-3

This stage compound is obtained upon reaction between above stage, Benzyl amine and Potassium carbonate in Toluene solvent medium. Product is purified by removing of inorganic salts with water wash.

### Stage-4

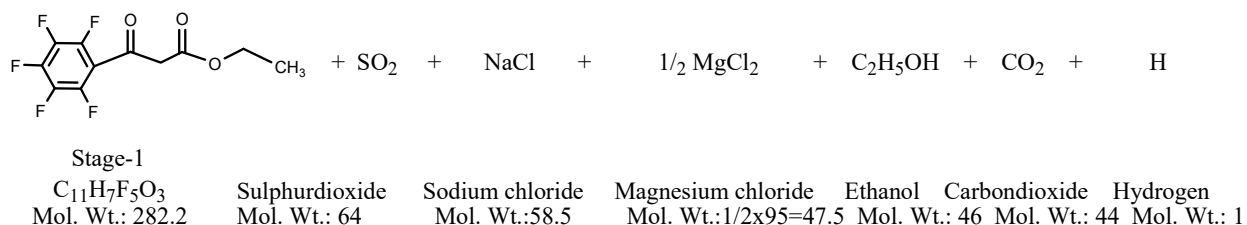
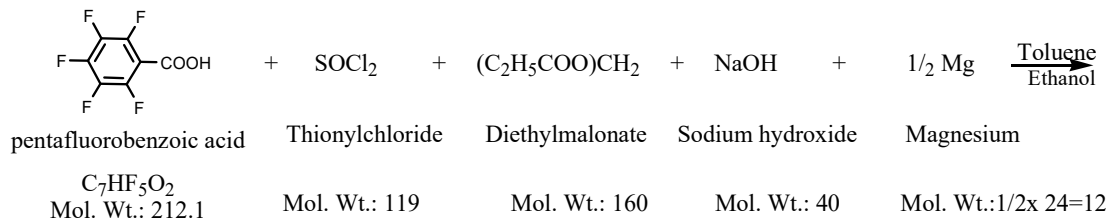
This stage compound is produced by the reaction between above stage and Hydrogen in Ethanol solvent medium.

### Stage-5: Pharma

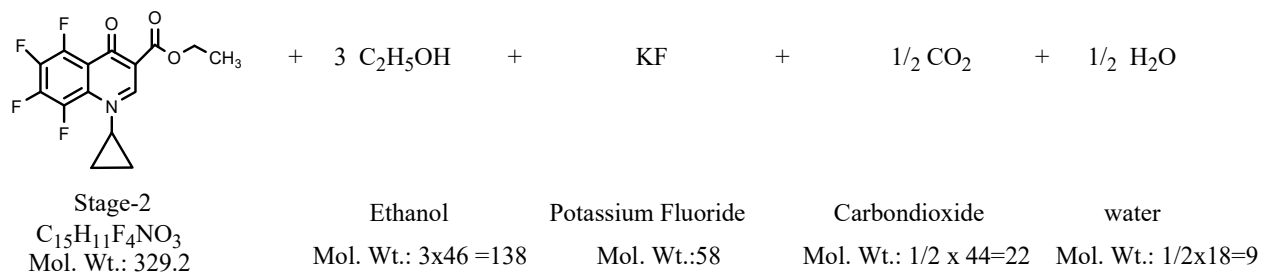
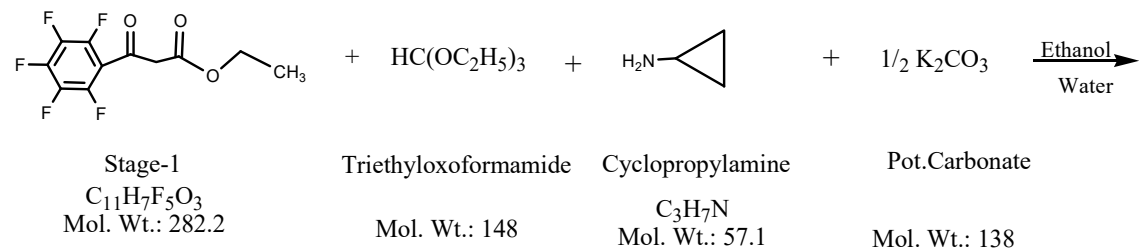
Stage-4 is converted to Pharma by the reaction between above stage and Dimethylpiperazine in presence of Potassium Hydroxide. Ethanol is the solvent used in the process. Pharma is purified with water wash.

## ROUTE OF SYNTHESIS OF SPARFLOXACIN

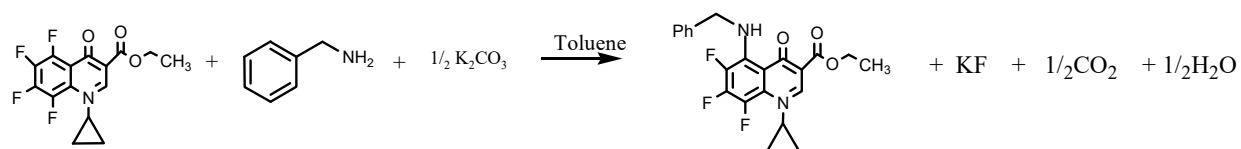
### Stage-1



### Stage-2



### Stage-3



Stage-2  
 $C_{15}H_{11}F_4NO_3$   
 Mol. Wt.: 329.2

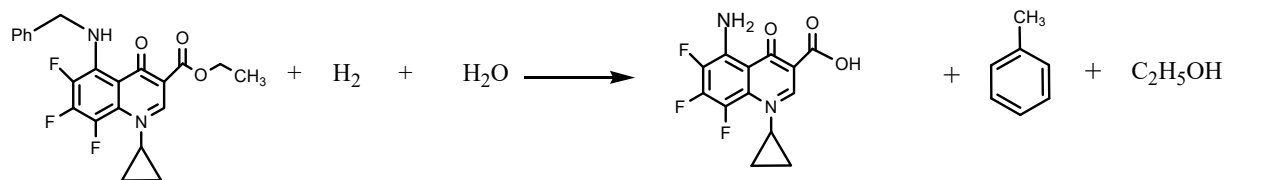
benzylamine  
 $C_7H_9N$   
 Mol. Wt.: 107.2

Potassium carbonate  
 $1/2 K_2CO_3$   
 Mol. Wt.:  $1/2 \times 138 = 69$

Stage-3  
 $C_{22}H_{19}F_3N_2O_3$   
 Mol. Wt.: 416.4

Mol. Wt.: 58    Mol. Wt.: 22    Mol. Wt.: 9

### Stage-4



Stage-3  
 $C_{22}H_{19}F_3N_2O_3$   
 Mol. Wt.: 416.4

Hydrogen  
 $H_2$   
 Mol. Wt.: 2

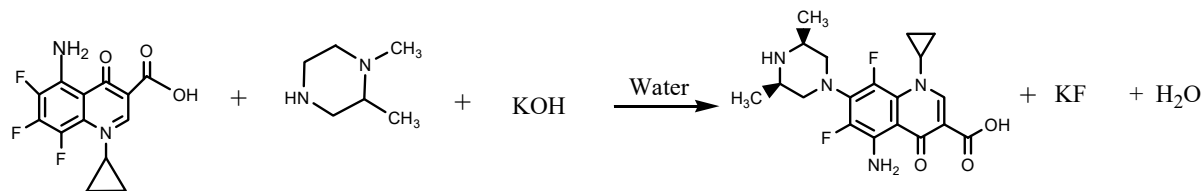
Water  
 $H_2O$   
 Mol. Wt.: 18

Stage-4  
 $C_{13}H_9F_3N_2O_3$   
 Mol. Wt.: 298.4

Toluene  
 $C_7H_8$   
 Mol. Wt.: 92.1

Ethanol  
 $C_2H_5OH$   
 Mol. Wt.: 46

### Stage-5



Stage-4  
 $C_{13}H_9F_3N_2O_3$   
 Mol. Wt.: 298.4

dimethylpiperazine  
 $C_6H_{14}N_2$   
 Mol. Wt.: 114.2

Potassium Hydroxide  
 $KOH$   
 Mol. Wt.: 56

Sparfloxacin  
 $C_{19}H_{22}F_2N_4O_3$   
 Mol. Wt.: 392.4

Pot. Fluoride  
 $KF$   
 Mol. Wt.: 58

Water  
 $H_2O$   
 Mol. Wt.: 18

## Flow chart

pentafluorobenzoic acid

Thionylchloride

Diethylmalonate

Sodium Hydroxide

Magnesium

Toluene

Ethanol

Stage-1

Triethyloxoformamide

Cyclopropylamine

Potassium carbonate

Ethanol

Stage-2

Benzyl amine

Potassium carbonate

Toluene

Stage-3

Hydrogen

Water

Ethanol

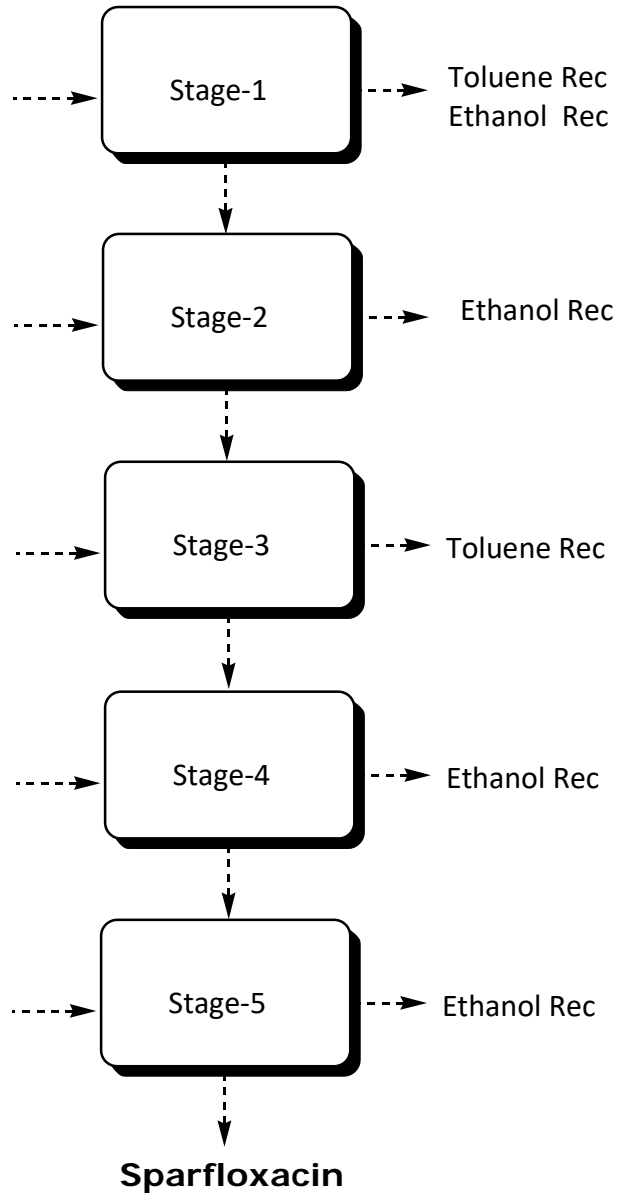
Stage-4

Dimethylpiperazine

Potassium Hydroxide

Ethanol

Activated Carbon



### MATERIAL BALANCE OF SPARFLOXACIN

Material balance of Sparfloxacin Stage-1 Batch Size: 100Kg			
Name of the input	Quantity in Kg		Quantity in Kg
pentafluorobenzoic acid	60.00	Stage-1	75.00
Thionylchloride	33.66	Toluene recovery	570.00
Diethylmalonate	45.26	Toluene loss	30.00
Sodium Hydroxide	11.31	Ethanol recovery	95.00
Magnesium	4.00	Ethanol Loss	5.00
Toluene	600.00	Effluent water	542.94
Ethanol	100.00	(water-500,Sodium chloride-16.54,Magnesium chloride-13.4,Ethanol-13)	
Water	500.00	Process Emissions	30.48
		(Carbon dioxide-12.4,Hydrogen-0.28,Sulphur dioxide-17.8)	
		Organic Residue	5.81
<b>Total</b>	<b>1354.23</b>	<b>Total</b>	<b>1354.23</b>

Material balance of Sparfloxacin Stage-2 Batch Size: 100Kg			
Name of the input	Quantity in Kg		Quantity in Kg
Stage-1	75.00	Stage-2	83.90
Triethyloxoformamide	40.00	Ethanol recovery	713.00
Cyclopropylamine	15.17	Ethanol Loss	37.00
Potassium caronate	18.33	Effluent Water	555.13
Ethanol	750.00	(Water-500,Gen water-2.43,Potassium fluoride-15.4,Ethanol-37.3)	
Water	500.00	Process Emissions	5.84
		(Carbondioxide)	
		Organic Residue	3.63
<b>Total</b>	<b>1398.50</b>	<b>Total</b>	<b>1398.50</b>

Material balance of Sparfloxacin Stage-3 Batch Size: 100Kg			
Name of the input	Quantity in Kg		Quantity in Kg
Stage-2	83.90	Stage-3	106.10
Benzyl amine	27.32	Toluene recovery	750.00
Potassium carbonate	17.60	Toluene loss	40.00
Toluene	800.00	Effluent water	427.09
Water	400.00	(Water-400, Gen water- 2.29, Potassium fluoride- 14.8, Toluene-10)	
		Process Emission	5.63
		(Carbondioxide)	
Total	1328.82		1328.82

Material balance of Sparfloxacin Stage-4 Batch Size: 100Kg			
Name of the input	Quantity in Kg		Quantity in Kg
Stage-3	106.10	Stage-4	76.00
Hydrogen	0.50	Ethanol recovery	190.00
Water	800.00	Ethanol Loss	10.00
Ethanol	200.00	Toluene generation	23.46
		Effluent water	807.14
		(Water-795.42, Ethanol- 11.72)	
Total	1106.60	Total	1106.60

Material balance of Sparfloxacin  
 Stage-5:Pharma  
 Batch Size: 100Kg

Name of the input	Quantity in Kg		Quantity in Kg
Stage-4	76.00	Stage-5:Pharma	100.00
Dimethylpiperazine	29.10	Ethanol recovery	465.00
Potassium Hydroxide	14.30	Ethanol Loss	25.00
Ethanol	500.00	Effluent water	329.40
Water	300.00	(Water-300,Potassium fluoride-14.8,Gen water- 4.6,Ethanol-10)	
Activated Carbon	10.00	Spent Carbon	10.00
Total	929.40	Total	929.40

## 25. TADALAFIL

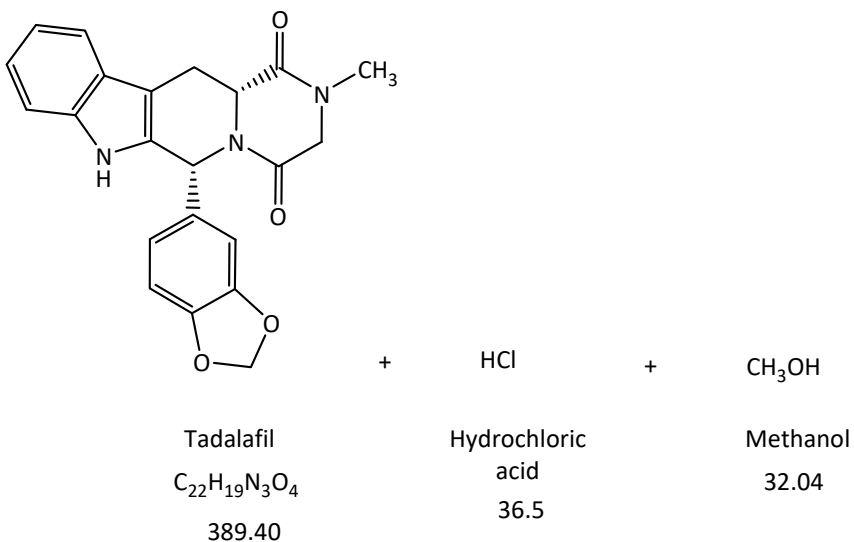
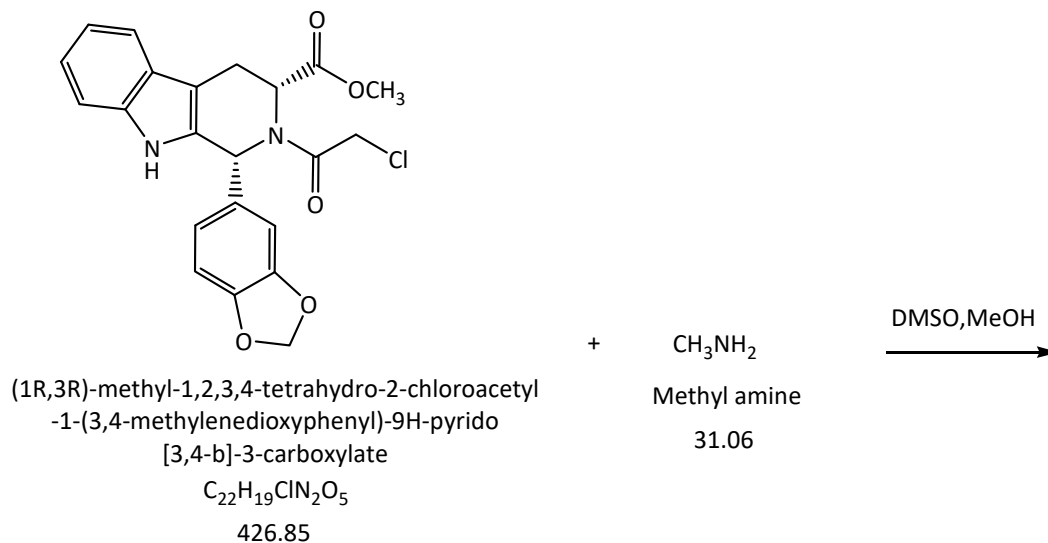
### Process Description

#### Stage-1

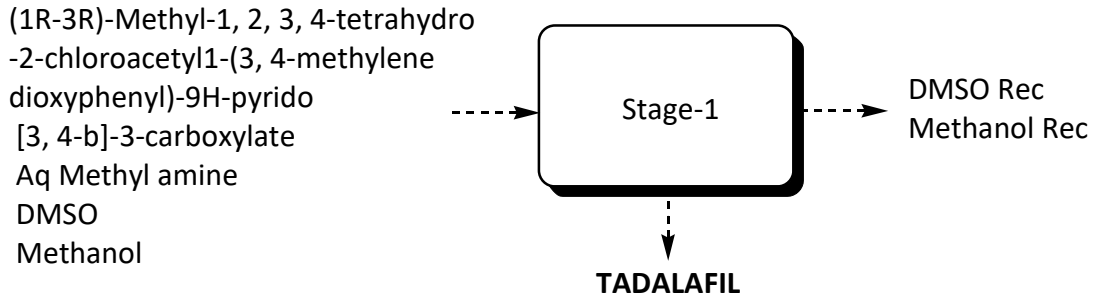
(1R-3R)-Methyl-1, 2, 3, 4-tetrahydro-2-chloroacetyl-1-(3, 4-methylenedioxyphenyl)-9H-pyrido [3, 4-b]-3-carboxylate reacts with Aq methylamine in presence of DMSO and Methanol to give Tadalafil

### Route of Synthesis

#### Stage-1:



**Flow Chart:**



**TADALAFIL**

**Material Balance:**

Material Balance of Tadalafil			
Stage-1			
Batch Size: 100.0Kg			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
(1R-3R)-Methyl-1, 2, 3, 4-tetrahydro-2-chloroacetyl1-(3, 4-methylene dioxypyhenyl)-9H-pyrido [3, 4-b]-3-carboxylate	112.00	Tadalafil	100.00
Aq methyl amine (40%)	10.00	DMSO Recovery	143.00
Dimethyl sulphoxide	150.00	DMSO Loss	4.00
Methanol	150.00	Methanol Recovery	143.00
Water	150.00	Methanol Loss	4.00
		Effluent water - (Water-150,Water from Methyl amine-0.90,Methanol-8.40, DMSO-1.5 )	160.80
		Process emission (Hydrogen Chloride – 9.57)	9.57
		Organic Residue – 7.63	7.63
		Process residue –4.63	
		Distillation residue – 3 (DMSO-1.5, Methanol-1.5)	
<b>Total</b>	<b>572.00</b>	<b>Total</b>	<b>572.00</b>

## 26. TAMSULOSIN HCL

### Process Description

#### Stage-1

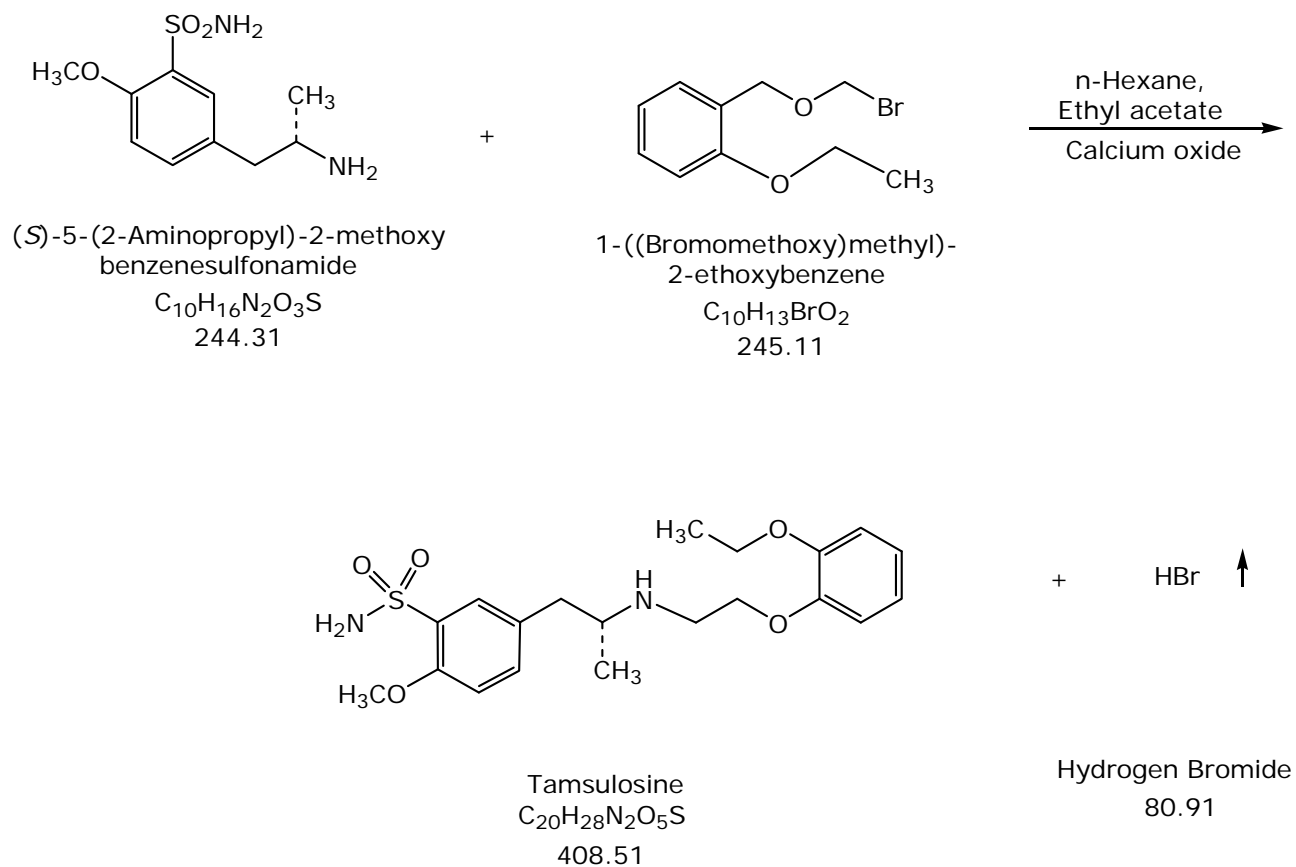
(S)-5-(2-Aminopropyl)-2-methoxybenzenesulfonamide reacts with 2-methoxy benzene sulfonamide in presence of Sodium hydroxide and Ethyl acetate to give Stage-1 compound.

#### Stage-2

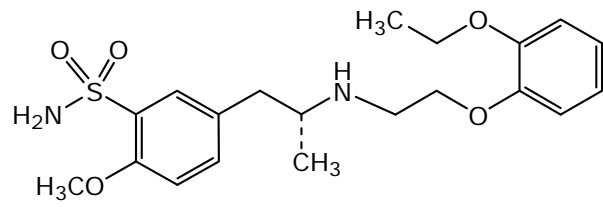
Stage-1 compound undergoes purification in Methanol and Ethanol to give Tamsulosine HCl

### Route of Synthesis

#### Stage-1



## Stage-2



Tamsulosine  
 $C_{20}H_{28}N_2O_5S$   
408.51

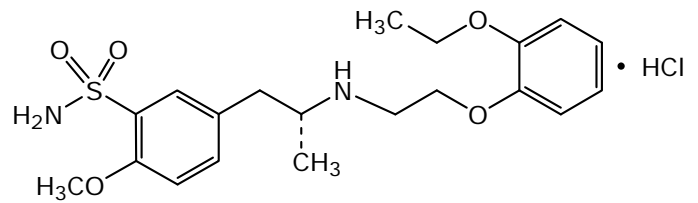
+

HCl

Methanol,  
Ethanol



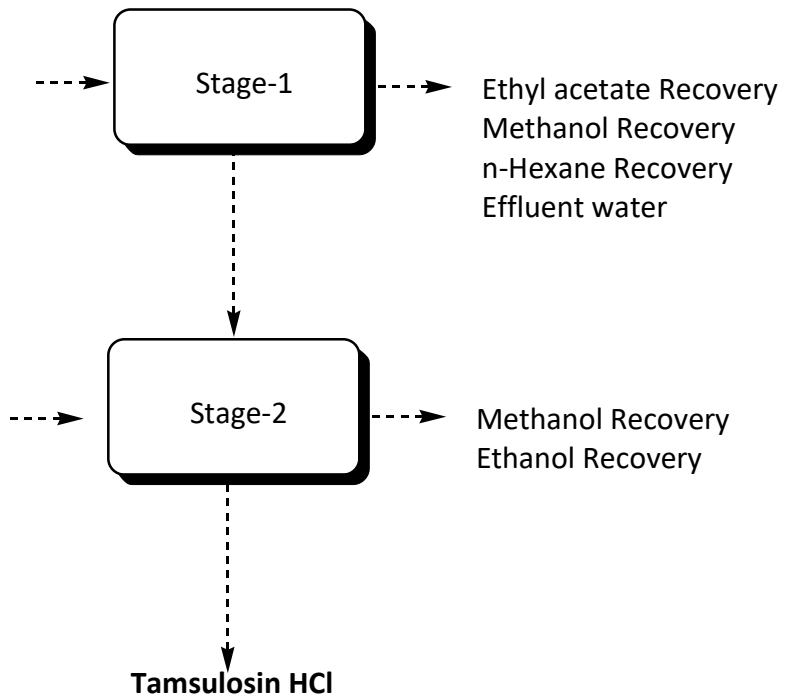
Hydrochloric acid  
36.46



**Tamsulosine HCl**  
 $C_{20}H_{29}ClN_2O_5S$   
444.97

**Flow Chart:**

(S)-5-(2-aminopropyl)-2-methoxy  
benzene sulfonamide  
1-((Bromomethoxy)methyl)-  
2-ethoxybenzene  
Methanol  
n-Hexane  
50% lye solution  
Ethyl acetate  
Ethanol 99%  
Hydrochloric acid



**Material Balance**

<b>Material Balance of Tamsulosin HCl</b>			
<b>Stage-1</b>			
<b>Batch Size:200 Kg</b>			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
(S)-5-(2-aminopropyl)-2-methoxybenzene sulfonamide	129.00	Stage-1	194.00
1-((Bromomethoxy)methyl)-2-ethoxybenzene	130.00	• Methanol Recovery	475.00
Methanol	500.00	• Methanol Loss	20.00
n-Hexane	500.00	• n-Hexane Recovery	475.00
50% lye solution	20.00	• n-Hexane Loss	20.00
Ethyl acetate	500.00	• Ethyl acetate Recovery	475.00
Ethanol 99%	500.00	• Ethyl acetate Loss	15.00
Hydrochloric acid	10.00	• Ethanol Recovery	475.00
Water	1500.00	• Ethanol Loss	20.00
		Effluent Water	1505.00

		<ul style="list-style-type: none"> <li>• Water-1500</li> <li>• Ethyl acetate-5</li> </ul>	0
		Process emission	42.69
		<ul style="list-style-type: none"> <li>• Hydrogen Bromide-42.69</li> </ul>	0
		Organic Residue	72.31
		<ul style="list-style-type: none"> <li>• Process Residue-52.31</li> <li>• Distillation residue-20</li> <li>• Ethyl acetate-5</li> <li>• n-Hexane-5</li> <li>• Methanol-5</li> <li>• Ethanol-5</li> </ul>	
Total	3789.00	Total	3789.00

**Material Balance of Tamsulosin HCl**

**Stage-2**

**Batch Size: 200Kg**

Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Stage-1	194.00	Tamsulosin HCl	200.00
Hydrochloric acid	17.30	<ul style="list-style-type: none"> <li>• Methanol Recovery</li> </ul>	380.00
Methanol	400.00	<ul style="list-style-type: none"> <li>• Methanol Loss</li> </ul>	10.00
Ethanol	400.00	<ul style="list-style-type: none"> <li>• Ethanol Recovery</li> </ul>	380.00
		<ul style="list-style-type: none"> <li>• Ethanol Loss</li> </ul>	10.00
		Organic Residue	31.30
		<ul style="list-style-type: none"> <li>• Process Residue-11.30</li> <li>• Distillation residue -20</li> <li>• Methanol-10</li> <li>• Ethanol-10</li> </ul>	
Total	1011.30	Total	1011.30

## 27. TELMISARTAN

### Process Description

#### Stage-1

##### Step-A

Methyl-4-(butyramido)3-methyl-5-nitrobenzoate undergoes hydrogenation in the presence of Palladium carbon as catalyst by using Methanol as solvent media to give Stage-1A as product.

##### Step-B

Stage-1A product reacts with sodium hydroxide and hydrochloric acid to give Stage-1B as product.

#### Stage-2

Stage-1 B product reacts with N-Methylbenzene-1,2-diamine in the presence of Sodium hydroxide and polyphosphoric acid to give Stage -2 as product.

#### Stage-3

Stage-2 product reacts with 1, 3-dibromo-5, 5-dimethylimidazolidine-2,4-dione in the presence of Chloroform as solvent media to give Stage-3 as product.

#### Stage-4

Stage-2 product reacts with Stage-3 and potassium hydroxide in the presence of acetone as solvent media to give Stage-4 as product.

#### Stage-5

Stage-4 product reacts with potassium hydroxide and hydrochloric acid in the presence of MDC as solvent media to give stage-5 as product.

#### Stage-6

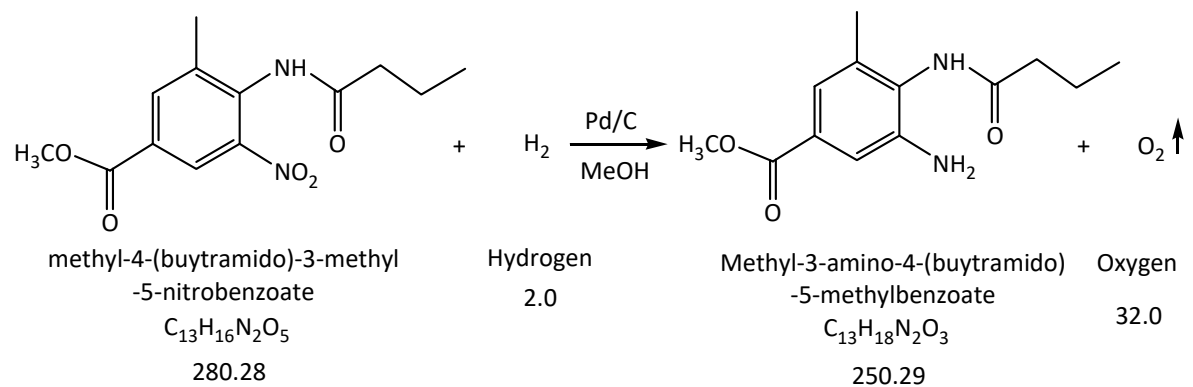
Stage-5 product undergoes purification with Methanolic ammonia, acetic acid and activated carbon in the presence of methanol as solvent media to give Telmisartan as product.

# TELMISARTAN

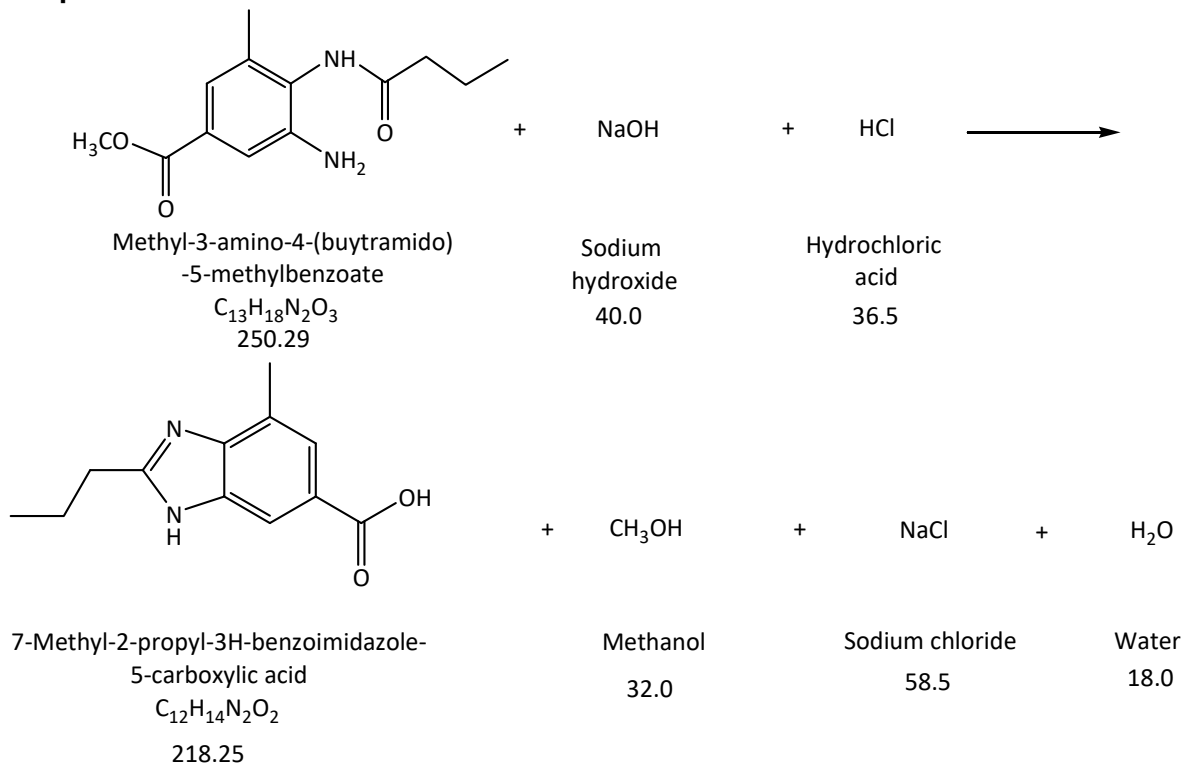
## Route of Synthesis:

### Stage-1

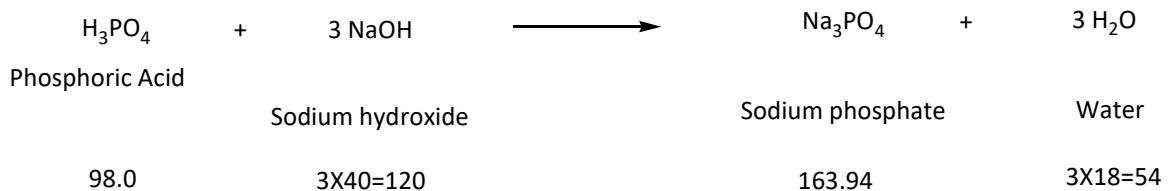
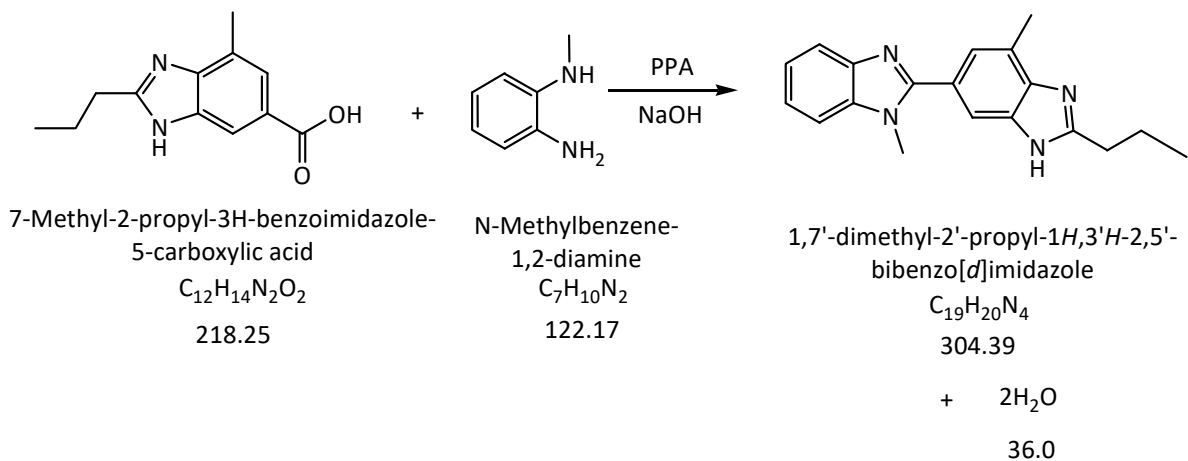
#### Step-A



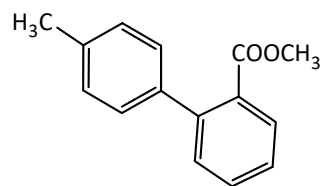
### Step-B



### Stage-2

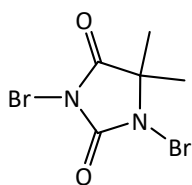


### Stage-3



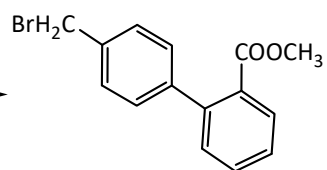
methyl-4-methyl-1,1-biphenyl-  
2-carboxylate  
 $C_{15}H_{14}O_2$   
226.27

+



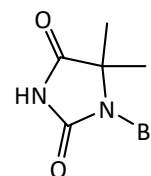
1,3-Dibromo-5,5-dimethyl  
imidazolidine-2,4-dione  
 $C_5H_6N_2O_2$   
285.92

Chloroform  
→



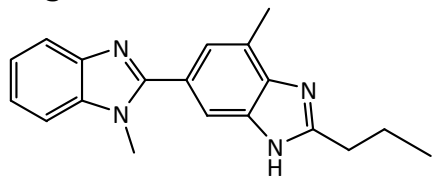
4-(bromomethyl)biphenyl-2-  
carboxylic acid methyl ester  
 $C_{15}H_{13}BrO_2$   
305.17

+



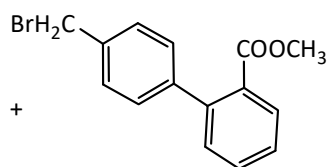
1-Bromo-5,5-dimethyl  
imidazolidine-2,4-dione  
 $C_5H_7BrN_2O_2$   
207.03

### Stage-4



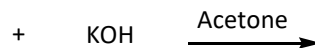
1,7'-dimethyl-2'-propyl-1*H*,3'*H*-2,5'-  
bibenzo[*d*]imidazole

$C_{19}H_{20}N_4$   
304.39

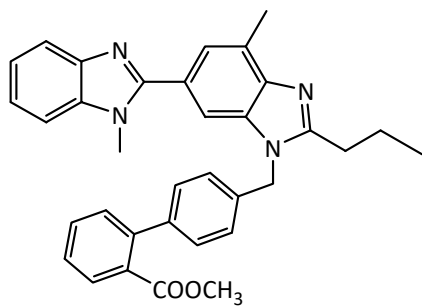


4-(bromomethyl)biphenyl  
-2-carboxylic acid methyl ester

$C_{15}H_{13}BrO_2$   
305.17



Potassium  
hydroxide  
56.11



methyl 4'-((1,7'-dimethyl-2'-propyl-1*H*,3'*H*-[2,5'-  
bibenzo[*d*]imidazol]-3'-yl)methyl)-[1,1'-biphenyl]-2-  
carboxylate

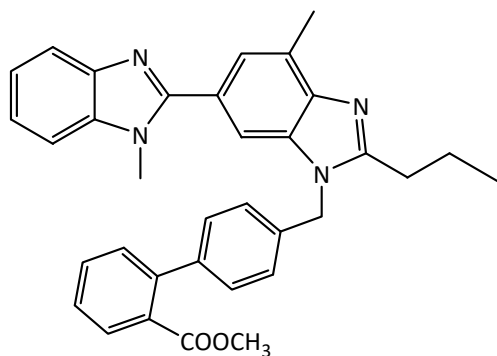
$C_{34}H_{32}N_4O_2$   
528.64



119.0

18.0

## Stage-5

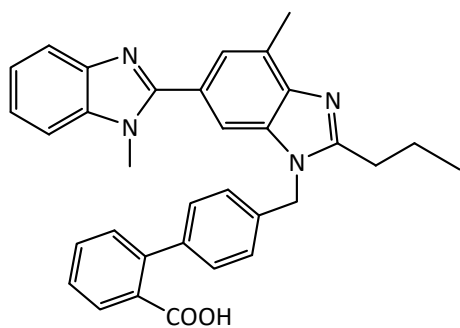


methyl 4'-((1,7'-dimethyl-2'-propyl-1H,3'H-[2,5'-  
bibenzo[d]imidazol]-3'-yl)methyl)-[1,1'-biphenyl]-2-  
carboxylate  
 $C_{34}H_{32}N_4O_2$   
528.64

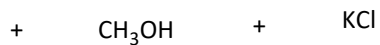


Potassium  
hydroxide  
56.11

Hydrochloric  
acid  
36.5



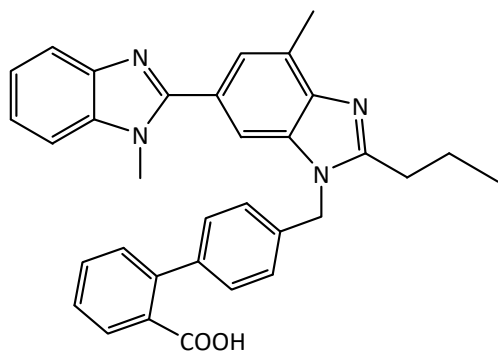
4'-((1,7'-dimethyl-2'-propyl-1H,3'H-[2,5'-  
bibenzo[d]imidazol]-3'-yl)methyl)-[1,1'-biphenyl]-2-  
carboxylic acid  
 $C_{33}H_{30}N_4O_2$   
514.62



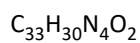
32.0

74.55

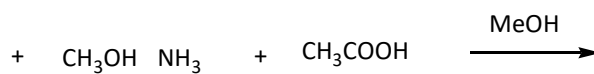
## Stage-6



4'-((1,7'-dimethyl-2'-propyl-1H,3'H-[2,5'-  
bibenzo[d]imidazol]-3'-yl)methyl)-[1,1'-biphenyl]-2-  
carboxylic acid



514.62



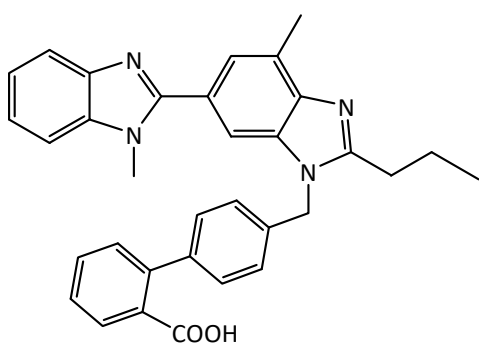
Methanolic  
ammonia



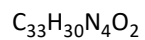
49.07

Acetic acid

60.0



Telmisaratn



514.62



Ammonium acetate

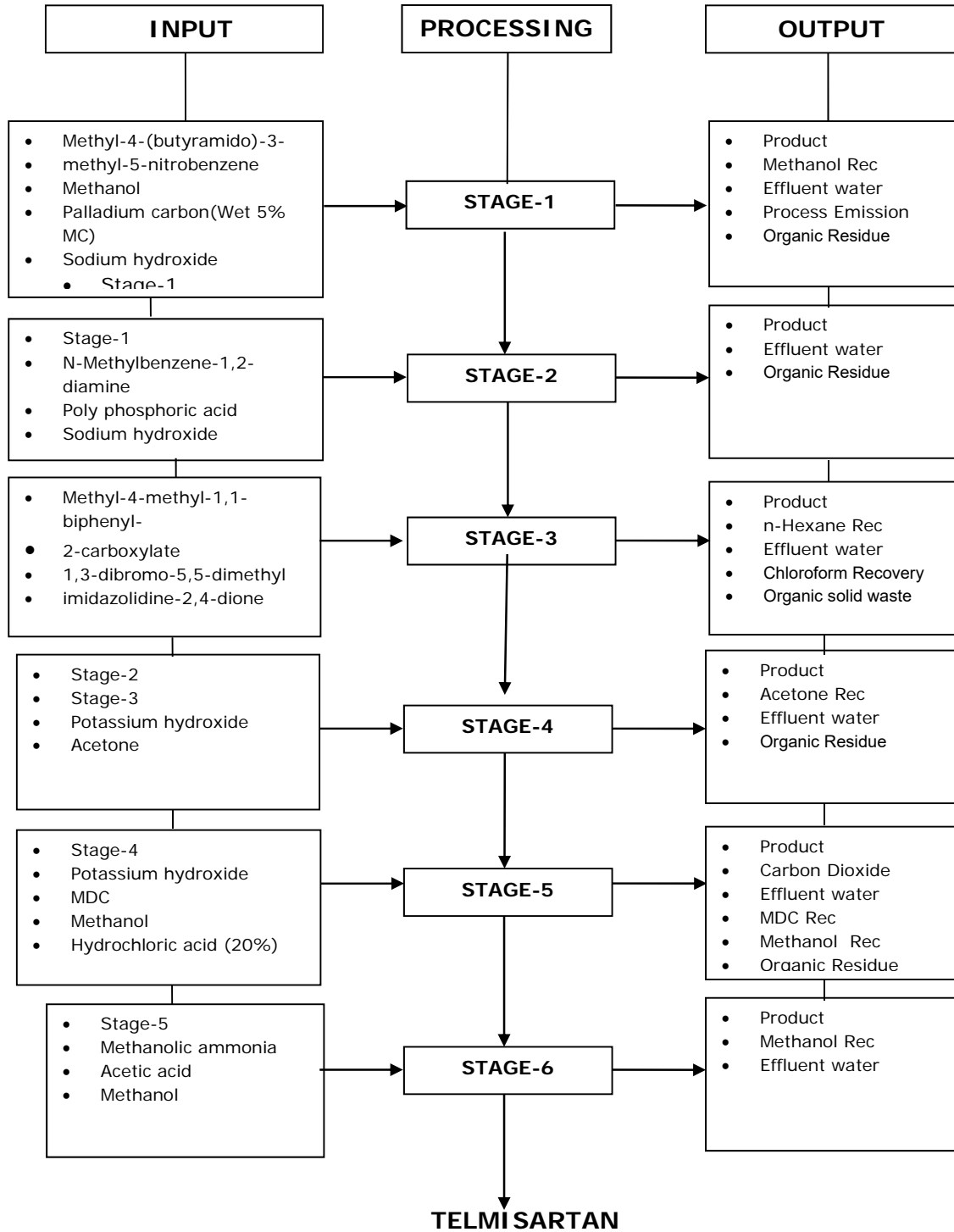
77.08

Methanol

32.0

# TELMISARTAN

## Flow chart:



**Material Balance:**

<b>MATERIAL BALANCE OF TELMISARTAN</b>			
<b>STAGE-1</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Methyl-4-(butyramido)-3-methyl-5-nitrobenzene	73.00	Stage-1	55.00
Methanol	865.00	Methanol Recovery	822.00
Palladium carbon(Wet 5% MC)	3.00	Methanol Loss	43.00
Sodium hydroxide	10.40	Effluent water	550.20
Hydrochloric acid	31.60	(Water-500,generated water-4.6, Sodium chloride-15.2,Hydrochloric acid-22.1, Generated Methanol-8.3)	
Water	500.00	Spent Palladium Carbon	3.00
		Process Emission	8.33
		(Oxygen)	
		Organic Residue	1.47
<b>Total</b>	<b>1483.00</b>	<b>Total</b>	<b>1483.00</b>

<b>MATERIAL BALANCE OF TELMISARTAN</b>			
<b>STAGE-2</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-1	55.00	Stage-2	73.00
N-Methylbenzene-1,2-diamine	32.00	Effluent Water	658.67
Phosphoric acid	90.00	(Water-600,generated water-58.67)	
Sodium hydroxide	110.20	By-Product	150.56
Water	600.00	(Sodium Phosphate)	
		Organic Residue	4.97
<b>Total</b>	<b>887.20</b>	<b>Total</b>	<b>887.20</b>

<b>MATERIAL BALANCE OF TELMISARTAN</b>			
<b>STAGE-3</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Methyl-4-methyl-1,1-biphenyl-2-carboxylate	57.00	Stage-3	73.50
1,3-dibromo-5,5-dimethyl imidazolidine-2,4-dione	72.00	Chloroform Recovery	304.00

Azo bis isobutyronitrile	2.90	Chloroform Loss	16.00
Sodium meta bisulphate	4.30	n-Hexane Recovery	95.00
Chloroform	320.00	n-Hexane Loss	5.00
n-Hexane	100.00	Effluent water	407.20
Water	400.00	(Water-400,Sodium meta bisulphate-4.3,Azobis isobutyronitrile-2.9,)	
		Organic Solid Waste	55.50
		(organic impurities-3.37,1-Bromo-5,5-dimethyl imidazoline-2,4-dione-52.13)	
<b>Total</b>	<b>956.20</b>	<b>Total</b>	<b>956.20</b>

**MATERIAL BALANCE OF TELMISARTAN**

**STAGE-4**

**BATCH SIZE: 100.0 KGS**

<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-2	73.00	Stage-4	123.00
Stage-3	73.50	Acetone Recovery	427.00

Potassium hydroxide	18.00	Acetone Loss	22.00
Acetone	450.00	Effluent water	939.30
Water	900.00	(Water-900,generated water-4.3, Potassium hydroxide-4.5, Acetone-2, Potassium bromide-28.5)	
		Organic Residue	3.20
		(Organic Impurities-2.2, Acetone-1)	
<b>Total</b>	<b>1514.50</b>	<b>Total</b>	<b>1514.50</b>

<b>MATERIAL BALANCE OF TELMISARTAN</b>			
<b>STAGE-5</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-4	123.00	Stage-5	115.00
Potassium hydroxide	15.00	MDC Recovery	1138.00
MDC	1200.00	MDC Loss	60.00
Methanol	1000.00	Methanol Recovery	948.00
Hydrochloric acid (20%)	50.00	Methanol Loss	50.00
Acetic acid	40.00	Effluent water	706.20

Activated carbon	5.00	(Water-600,Potassium chloride-17.3,Methanol-7.4,Acetic acid-40, water from HCl-40,Hydrochloric acid-1.5)	
Water	600.00	Spent Carbon	5.00
		Organic Residue	10.80
		(Organic Impurities-6.8, Methanol-2,MDC-2)	
<b>Total</b>	<b>3033.00</b>	<b>Total</b>	<b>3033.00</b>

<b>MATERIAL BALANCE OF TELMISARTAN</b>			
<b>STAGE-6</b>			
<b>BATCH SIZE: 100.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-5	115.00	Telmisartan	100.00
Methanolic ammonia	50.00	Methanol Recovery	833.00
Acetic acid	20.00	Methanol Loss	40.00
Methanol	830.00	Effluent water	257.10
Activated carbon	5.00	(Water-230,Acetic acid-	

		2.4, Generated Methanol-2, Ammonium acetate-22.7)	
Water	230.00	Spent Carbon	5.00
		Organic Residue	7.90
<b>Total</b>	<b>1243.00</b>	<b>Total</b>	<b>1243.00</b>

## 28. THALIDOMIDE

### Process Description:

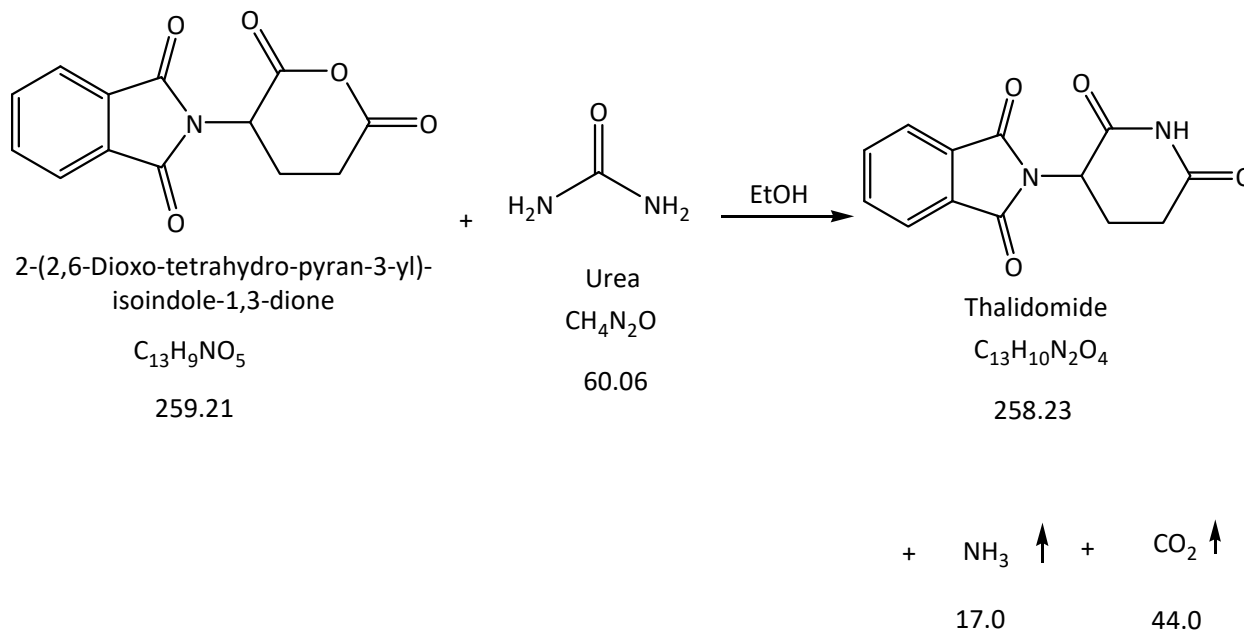
#### Stage-1

2-(2,6-Dihydro tetrahydro pyran-3-yl) isoindole-1,3-dione reacts with urea in the presence of Ethanol as solvent media to give Thalidomide as product.

## THALIDOMIDE

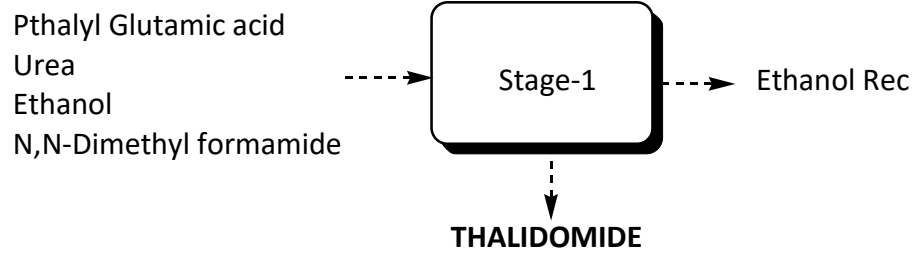
### Route of Synthesis:

#### Stage-1:



# THALIDOMIDE

## Flow Chart:



## THALIDOMIDE

### Material Balance:

Material Balance of Thalidomide Stage-1 Batch Size: 100.00Kgs			
Name of the input	Quantity in Kg	Name of the out put	Quantity in Kg
Pthalyl Glutamic acid	116.00	Thalidomide	100.00
Urea	25.00	N,N-Dimethyl formamide Recovery	87.00
N,N-Dimethyl formamide	100.00	N,N-Dimethyl formamide Loss	10.00
Sodium carbonate	20.00	Effluent water	729.00
Activated carbon	5.00	(Water-700,Ammonia-7,Sodium carbonate-20,DMF-2)	
Water	700.00	Process Emissions	27.30
		(Carbon dioxide-19.7,Ammonia- 7.6)	
		Spent carbon	5.00
		Organic Residue	7.70
		(Organic impurities-6.7,DMF-1)	
<b>Total</b>	<b>966.00</b>	<b>Total</b>	<b>966.00</b>

## 29. TRICLABENDAZOLE

### Process Description:

#### Stage-1:

3, 4, Dichloro aniline undergoes Acetylation with Acetic anhydride in presence of acetic acid to give Acetamide further it reacts with Nitric acid and potassium hydroxide to give stage-1 product

#### Stage-2:

Stage-1 product reacts with 2, 3, Dichloro Phenol in presence of DMSO to give Stage-2 product

#### Stage-3:

Stage-2 product undergoes reduction with Hydrogen in presence of Methanol and Palladium carbon to give Stage-3 product

#### Stage-4:

Stage-3 product reacts with carbon disulfide and sodium hydroxide in presence of Methanol to give Stage- 4 product

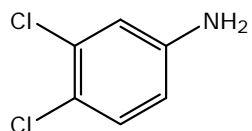
#### Stage-5:

Stage-4 product reacts with Dimethyl sulphate in presence of methanol and Sodium hydroxide to give Triclabendazole.

## Route of Synthesis

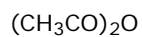
### Stage-1

#### Step-A

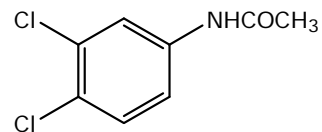


3,4-Dichloro-phenylamine  
 $C_6H_5Cl_2N$   
162.02

+



Acetic anhydride  
102.09

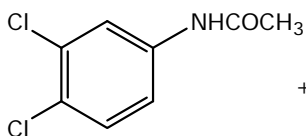


*N*-(3,4-Dichloro-phenyl)-acetamide  
 $C_8H_7Cl_2NO$   
204.05

+  $CH_3COOH$

Acetic acid  
60.05

#### Step-B

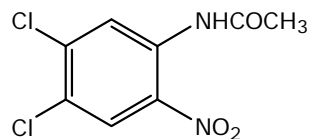


*N*-(3,4-Dichloro-phenyl)-acetamide  
 $C_8H_7Cl_2NO$   
204.05

+



Nitric acid  
63.01



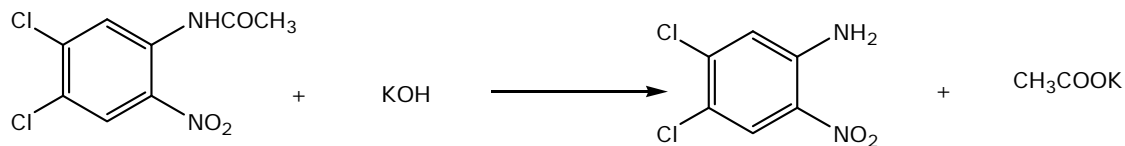
*N*-(4,5-Dichloro-2-nitro-phenyl)-acetamide  
 $C_8H_6Cl_2N_2O_3$   
249.05

+



18.02

### Step-C



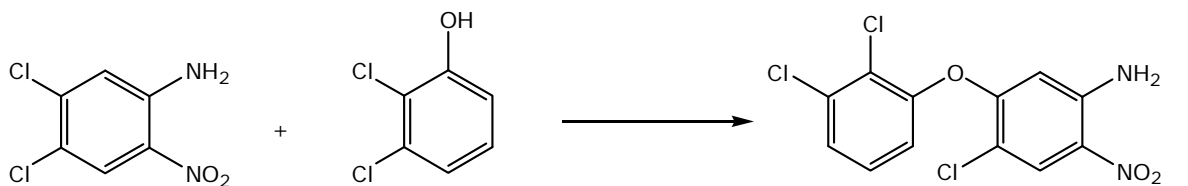
*N*-(4,5-Dichloro-2-nitrophenyl)-acetamide  
 $C_8H_6Cl_2N_2O_3$   
249.05

Potassium Hydroxide  
56.11

4,5-Dichloro-2-nitrophenylamine  
 $C_6H_4Cl_2N_2O_2$   
207.01

Potassium acetate  
98.14

### Stage-2



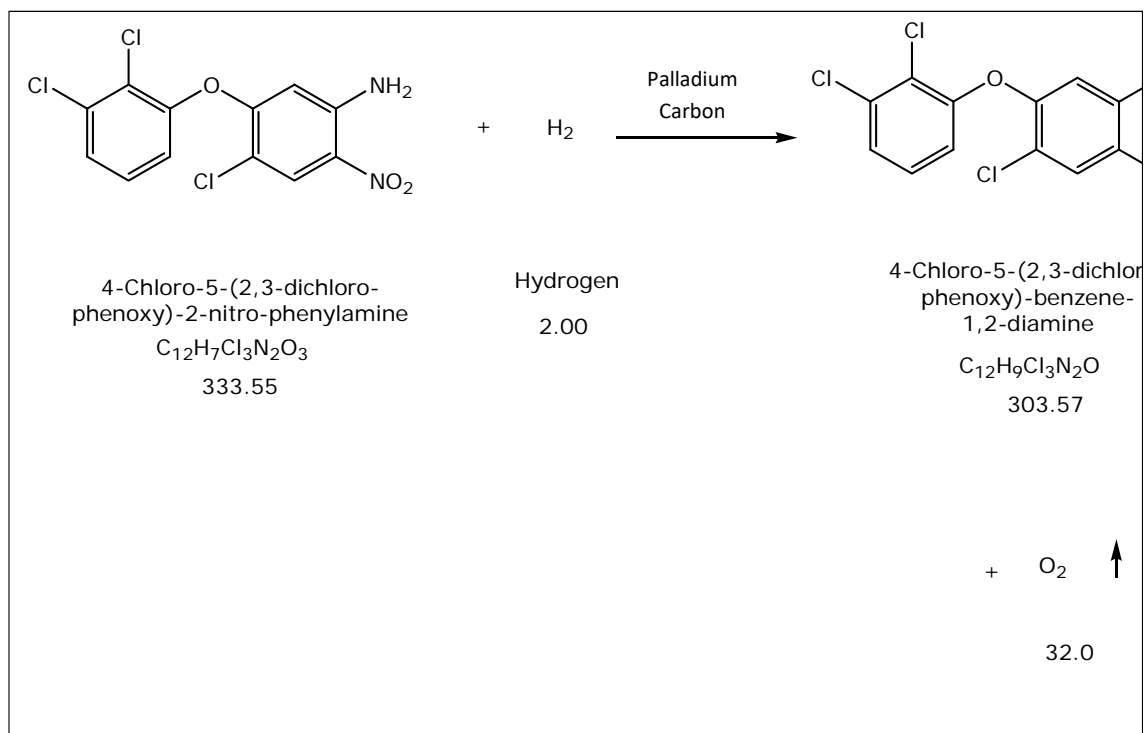
4,5-Dichloro-2-nitrophenylamine  
 $C_6H_4Cl_2N_2O_2$   
207.01

2,3-Dichloro-phenol  
 $C_6H_4Cl_2O$   
163

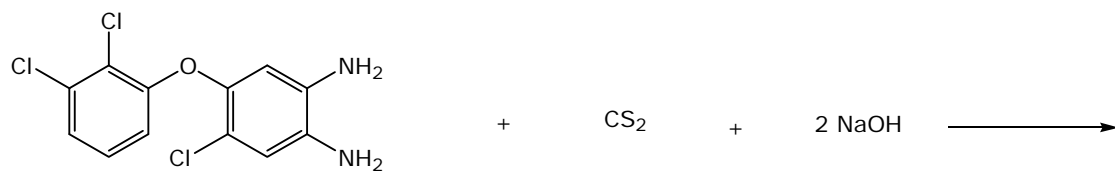
4-Chloro-5-(2,3-dichlorophenoxy)-2-nitrophenylamine  
 $C_{12}H_7Cl_3N_2O_3$   
333.55

+ HCl ↑  
36.5

### Stage-3



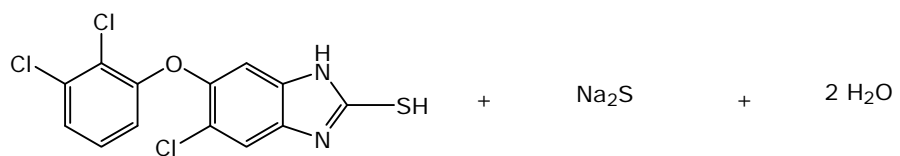
### Stage-4



4-Chloro-5-(2,3-dichloro-  
phenoxy)-benzene-  
1,2-diamine  
C<sub>12</sub>H<sub>9</sub>Cl<sub>3</sub>N<sub>2</sub>O  
303.57

Carbon  
disulfide  
76.14

Sodium Hydroxide  
79.99

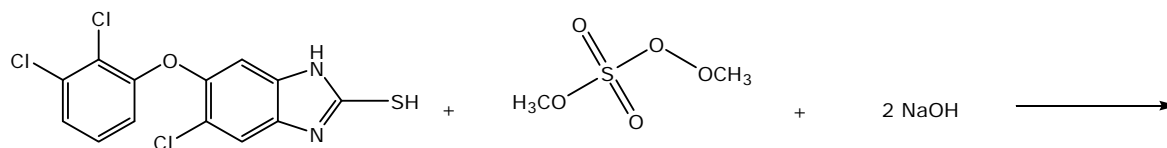


5-Chloro-6-(2,3-dichloro-phenoxy)-  
1H-benzimidazole-2-thiol  
C<sub>13</sub>H<sub>7</sub>Cl<sub>3</sub>N<sub>2</sub>OS  
345.63

Sodium thiosulfate  
78.04

36.03

## Stage-5



5-Chloro-6-(2,3-dichloro-phenoxy)-  
1*H*-benzimidazole-2-thiol

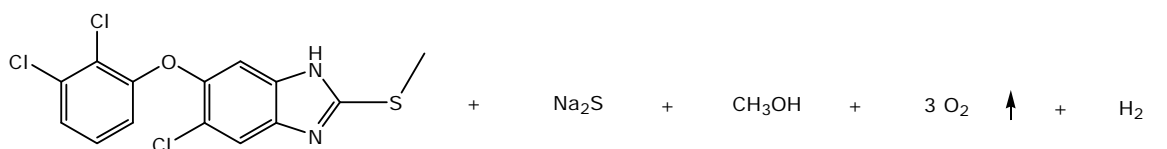
$C_{13}H_7Cl_3N_2OS$   
345.63

Di methyl sulphate

$C_2H_6O_5S$   
142.13

Sodium Hydroxide

80.00



Triclabendazole

$C_{14}H_9Cl_3N_2OS$   
359.66

Sodium thiosulfate

78.04

Methanol

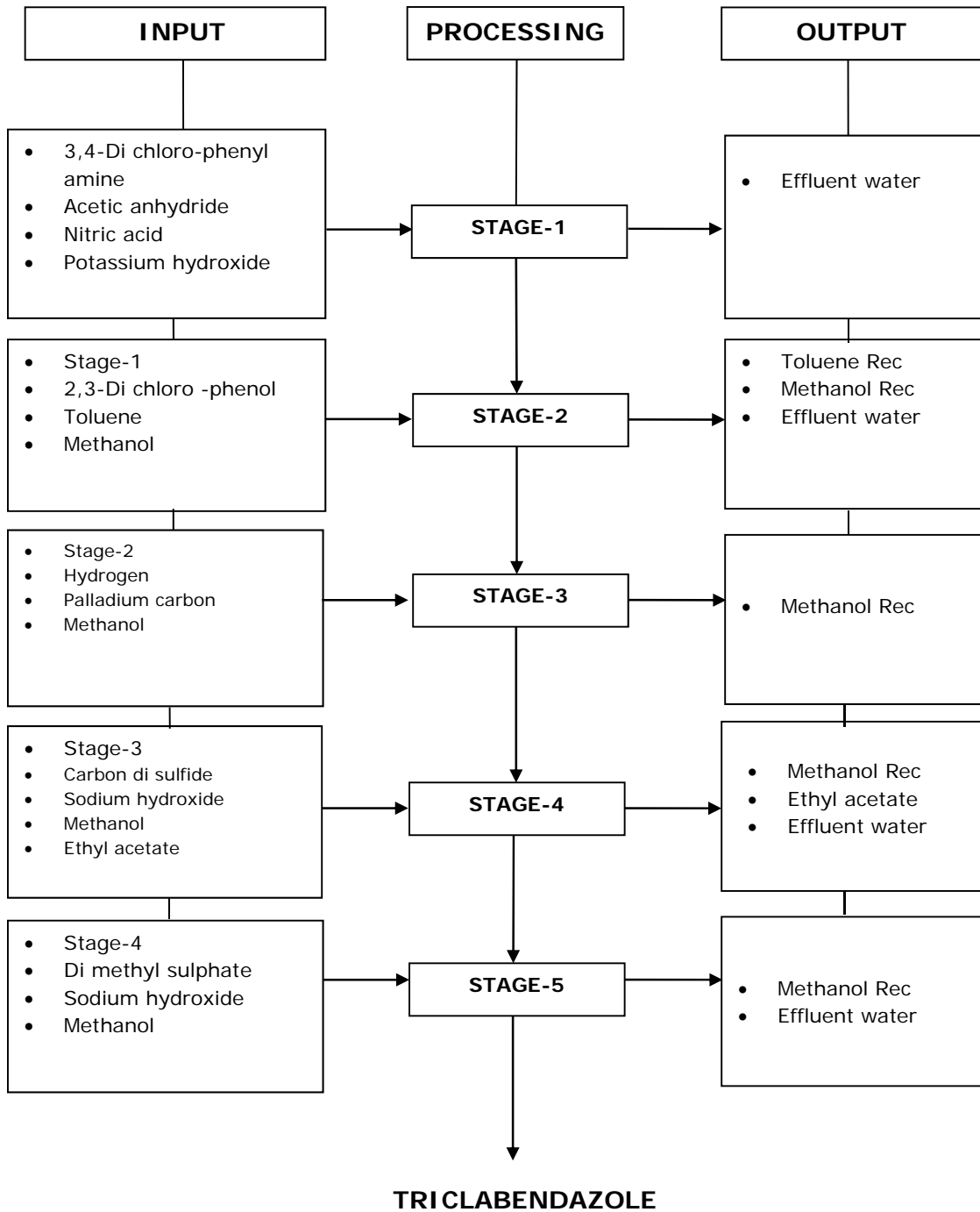
32.04

96.00

2.02

# TRICLABENDAZOLE

## Flow Chart



## TRICLABENDAZOLE

### Material Balance:

<b>MATERIAL BALANCE OF TRICLABENDAZOLE</b>			
<b>STAGE-1</b>			
<b>BATCH SIZE: 500.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
3,4-Di chloro-phenyl amine	283.00	Stage-1	328.00
Acetic anhydride	179.00	Effluent water	1795.33
Nitric acid	107.00	(Water-1500, Acetic acid-104.67, Potassium acetate-160.31, generated water-30.35)	
Potassium hydroxide	92.00	Organic residue	37.67
Water	1500.00	Process Residue-37.67	
<b>Total</b>	<b>2161.00</b>	<b>Total</b>	<b>2161.00</b>

<b>MATERIAL BALANCE OF TRICLABENDAZOLE</b>			
<b>STAGE-2</b>			
<b>BATCH SIZE: 500.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-1	328.00	Stage-2	511.00
2,3-Di chloro -phenol	258.00	Methanol recovery	665.00
Toluene	500.00	Methanol loss	14.00
Methanol	700.00	Toluene recovery	475.00
Water	1500.00	Toluene loss	10.00
		Effluent water	1516
		(Water-1500, Toluene -7, Methanol-9)	
		Process emission	57.64
		(Hydrogen chloride – 57.64)	
		Organic residue	37.36

		Process Residue- 17.36 Distillation bottom Residue-20 (Methanol-12, Toluene-8,)	
<b>Total</b>	<b>3286.00</b>	<b>Total</b>	<b>3286.00</b>

<b>MATERIAL BALANCE OF TRICLABENDAZOLE</b>			
<b>STAGE-3</b>			
<b>BATCH SIZE: 500.0 KGS</b>			
<b>INPUT</b>		<b>OUTPUT</b>	
<b>NAME OF THE INPUT</b>	<b>QUANTITY IN KGS</b>	<b>NAME OF THE OUTPUT</b>	<b>QUANTITY IN KGS</b>
Stage-2	511.00	Stage-3	450.00
Hydrogen	3.05	Methanol Recovery	760.00
Palladium Carbon	10.00	Methanol Loss	16.00
Methanol	800.00	Effluent water	1512.00
Water	1500.00	(Water- 1500,Methanol-12)	
		Spent Palladium Carbon	10.00
		Process emission (Oxygen – 48.90)	48.90
		Organic Residue	27.15
		Process Residue- 15.15, Distillation Residue- 12 (Methanol-12)	
<b>Total</b>	<b>2824.05</b>	<b>Total</b>	<b>2824.05</b>

MATERIAL BALANCE OF TRICLABENDAZOLE			
STAGE-4			
BATCH SIZE: 500.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-3	450.00	Stage-4	496.00
Carbon di sulfide	113.00	Methanol Recovery	760.00
Sodium hydroxide	120.00	Methanol Loss	16.00
Methanol	800.00	Ethyl acetate recovery	475.00
Ethyl acetate	500.00	Ethyl acetate loss	10.00
Water	1500.00	Effluent water	1680.75
		(Water-1500, Methanol-12, Di sodium sulfide-115.45, generated water-53.30)	
		Organic Residue	45.25
		Process Residue-18.25, Distillation residue-27 (Methanol-12, Ethyl acetate-15)	
<b>Total</b>	<b>3483.00</b>	<b>Total</b>	<b>3483.00</b>

MATERIAL BALANCE OF TRICLABENDAZOLE			
STAGE-5			
BATCH SIZE: 500.0 KGS			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-4	496.00	Triclabendazole	500.00
Di methyl sulphate	204.00	Methanol Recovery	760.00
Sodium hydroxide	115.00	Methanol Loss	16.00
Methanol	800.00	Effluent water	1657.80
Water	1500.00	(Water-1500, Methanol-	

		45.95, Di sodium sulfide-111.85)	
		Process emission	140.47
		(Oxygen-137.58, Hydrogen-2.89)	
		Organic Residue	40.73
		Process residue-28.73, Distillation Residue-12 (Methanol-12)	
<b>Total</b>	<b>3115.00</b>	<b>Total</b>	<b>3115.00</b>

## 30. ZOLEDRONIC ACID

### Process Description

#### Stage-1

Imidazole and methyl chloro acetate react in the presence of catalyst and base salt medium. Then the resulting compound hydrolysis with water to form 1H-Imidazole acetic acid.

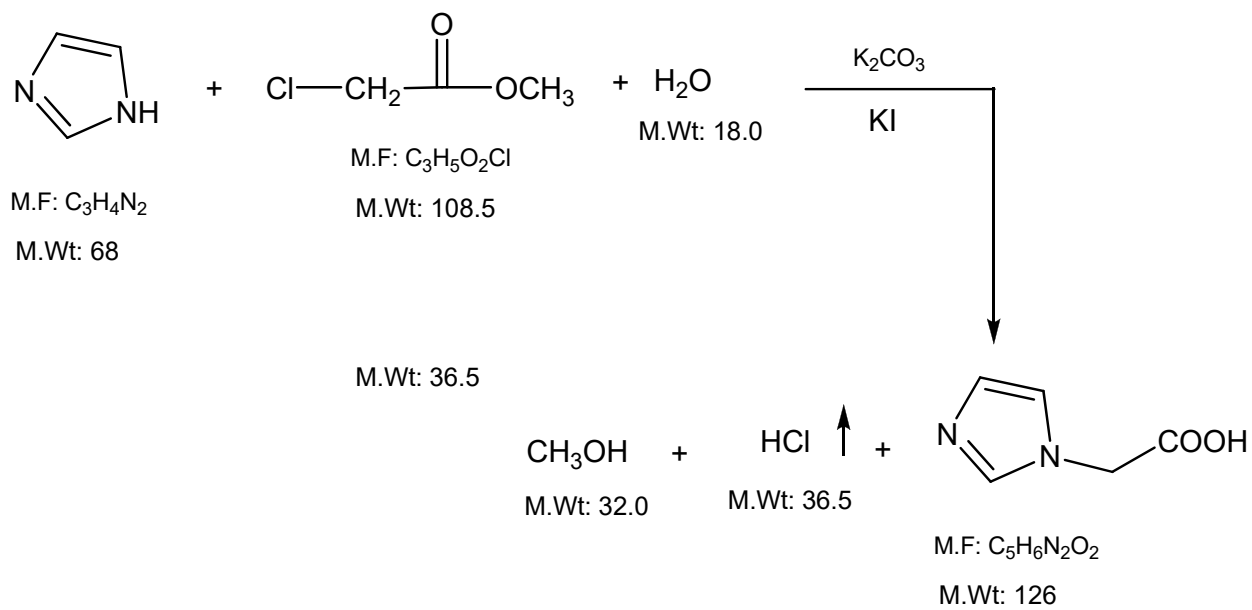
#### Stage-2

1H-Imidazole acetic acid reacts with phosphorous trichloride and ortho phosphoric acid to form acid compound. Then reacts with Hydrochloric acid and hydrolysis water to get zoledronic acid. It is purified with carbon treatment.

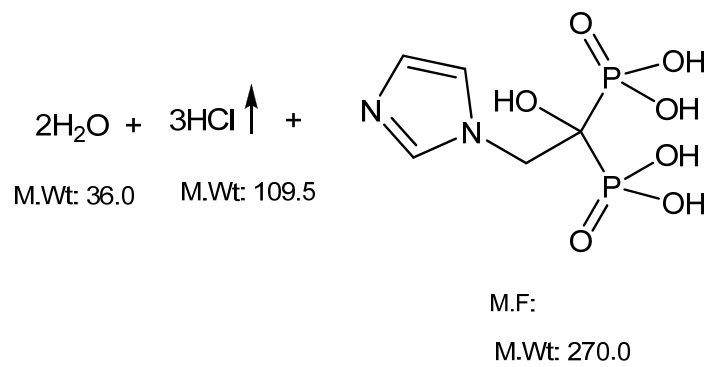
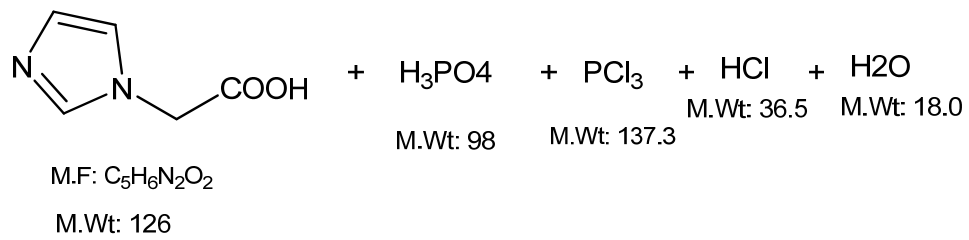
# ZOLEDRONIC ACID

## ROUTE OF SYNTHESIS

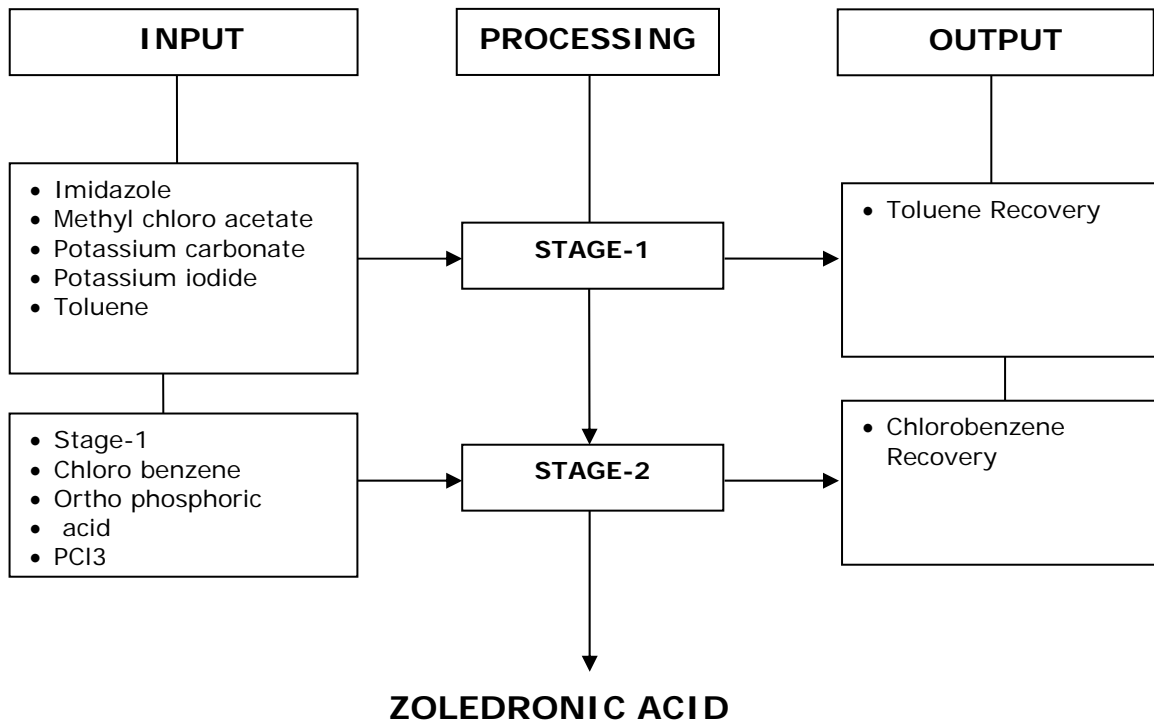
### Stage-1



## Stage-2



**Flow Chart:**



**Material balance:**

Material balance of Zoledronic acid Stage-1 Batch size: 10.0 Kg			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Imidazole	14.30	Stage-1	9.3
Methyl chloro acetate	34.30	• Recovery solvent mixture (Ethyl acetate + Toluene)	130.00
Potassium carbonate	26.00	• Solvent loss	10.00
Potassium iodide	3.00	Effluent water	145.30
Toluene	60.00	• Water-80 • Organic Impurities-14.30 • HCl-25 • K <sub>2</sub> CO <sub>3</sub> -26	
Water	80.00	Organic solid waste	3.00
Ethyl acetate	80.00		
<b>Total</b>	<b>297.6</b>	<b>Total</b>	<b>297.6</b>

Material balance of Zoledronic acid Stage-2 Batch size: 10.0 Kg			
INPUT		OUTPUT	
NAME OF THE INPUT	QUANTITY IN KGS	NAME OF THE OUTPUT	QUANTITY IN KGS
Stage-1	9.30	Zoledronic acid	10.00
Chloro benzene	40.00	• Chloro benzene Recovery	30.00
Ortho phosphoric acid	16.50	• Chloro benzene Loss	10.00
PCl <sub>3</sub>	23.60	Effluent water	66.90
Water	26.00	• Water-26 • Ortho phosphoric Acid-28.60 • Gen.Water-10.8 • HCl-1.5	0
HCl	25.50	Oranic residue	24.00
<b>Total</b>	<b>140.9</b>	<b>Total</b>	<b>140.9</b>

# **ANNEXURE-4**

## **LIST OF RAW MATERIALS**

## LIST OF RAW MATERIALS

### 1. ADEFOVIR

S. No	Raw material used	Quantity per batch in kg	Quantity per day in kg
1	2-(6-Amino-9H-purin9yl)ethanol	10	47.60
2	Ammonium hydroxide	3.62	17.23
3	Diethyl P-Toluene sulfonyloxy methylphosphonate	18	85.68
4	DMF	70	333.20
5	Hydrochloric acid	4	19.04
6	Magnesium tert butoxide	3	14.28
7	Toluene	70	333.20
8	Triethyl benzyl ammoniumchloride	2	9.52

### 2. BORTEZOMIB

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Acetone	15	49.95
2	Di Cyclohexyl Carbodimide	1.4	4.66
3	Di Isopropyl amine	4	13.32
4	Di isopropyl ethylamine	0.45	1.50
5	DIPE	23.85	79.42
6	DMF	15	49.95
7	Ethyl Acetate	20	66.60
8	HMDS	6	19.98
9	Hydrochloric Acid	10.31	34.33
10	IPA	5	16.65
11	Iso Butyl Boronic Acid	7.25	24.14
12	L-Phenyl Alanine	6	19.98
13	MDC	44.5	148.19
14	Methanol	30	99.90
15	N-Heptane	40	133.20
16	N-Hexyl Lithium	4.75	15.82
17	n-Hydroxy Succinamide	3.25	10.82
18	n-Methyl Morpholine	0.35	1.17
19	Pinanediol	6.25	20.81
20	Pyrazine Carboxylic acid	4.5	14.99
21	Sodium bicarbonate	0.39	1.30

22	Sodium Chloride	0.06	0.20
23	Sodium Hydroxide	1.5	5.00
24	Sulphuric acid	4	13.32
25	THF	13	43.29
26	Thionyl Chloride	4.5	14.99
27	Tri Fluoro Acetic Acid	4.25	14.15
29	Zinc Chloride	5.5	18.32

### 3. CAPECITABINE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	5-Deoxy-5-fluorocytidine	19	126.73
2	Chloro pentyl formate	35	233.45
3	Pyridine	6.25	41.69
4	MDC	660	4402.20
5	Ethyl acetate	350	2334.50
6	Hydrochloric acid	8	53.36
7	Sodium hydroxide	3	20.01
8	MDC	350	2334.50
9	Methanol	300	2001.00
10	Capecitabine crude	26	173.42
11	Activated carbon	10	66.70
12	Ethyl acetate	500	3335.00

### 4. CLOPIDOGREL BISULPHATE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Acetone	145	482.85
2	Acetonitrile	50	166.50
3	Activated carbon	13.1	43.62
4	Conc.H2SO4	14	46.62
5	Glycine methyl ester HCl	87.25	290.54
6	IPA.HCl (24%)	85	283.05
7	Isopropyl alcohol	100	333.00
8	Liq.Ammonia solution	19	63.27
9	Methanol	39	129.87
10	Methyl ethyl ketone	145	482.85
11	Methylene Dichloride	300	999.00
12	n-Hexane	250	832.50
13	Paraformaldehyde	21.42	71.33

14	Sodium carbonate	19	63.27
15	Sodium carbonates (20%)	140	466.20
16	Sodium sulfate	21.76	72.46
17	Toluene	685	2281.05
18	Tosylate	90	299.70

### 5. DAPAGLIFLOZIN

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	3,4,5-trihydroxy-6- hydroxymethyl-tetrahydro- pyran-2-one	25	33.25
2	Trimethylsilane Chloride	59	78.47
3	N-Methylmorpholine	55	73.15
4	MDC	300	399.00
5	Toluene	160	212.80
6	Sod.Dihydrogen phosphate	2	2.66
7	Sodium chloride	2	2.66
8	4-Bromo-1-chloro-2-(4- ethoxy benzyl) benzene	43	57.19
9	N-BuLi	10	13.30
10	Methanol	300	399.00
11	Toluene	250	332.50
12	THF	250	332.50
13	n-Hexane	95	126.35
14	Triethyl silane	15	19.95
15	Acetonitrile	300	399.00
16	MDC	300	399.00
17	Sodium bicarbonate	6	7.98
18	Sodium chloride	6	7.98

### 6. DAPOXETINE HYDROCHLORIDE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	(S)-3-Chloro-1-phenyl propan-1-ol	40	33.20
2	1-Naphthol	34	28.22
3	Activated carbon	14	11.62
4	Dimethyl sulfoxide	280	232.40
5	Dimethylamine	10.56	8.76
6	Ethyl acetate	1405	1166.15
7	IsopropanolHCl	22.4	18.59

8	Mesyl chloride	50	41.50
9	Methanol	995	825.85
10	N,N-Dimethyl amino pyridine	0.02	0.02
11	Sodium chloride	34	28.22
12	Triethylamine	126	104.58

#### 7. DARUNAVIR ETHANOLATE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	(3R,3aS,6aR)-Hexahydrofuro [2,3-b]furan-3-yl (4-nitrophenyl) carbonate	83.95	83.95
2	4-Amino-N-((2S,3S)-3-amino-2-hydroxy-4- phenylbutyl)-N-isobutylbenzenesulfonamide	109.44	109.44
3	Ethanol	329.83	329.83
4	Ethyl acetate	1094.45	1094.45
5	N-Methyl-2-Pyrrolidinone	224.88	224.88
6	Sodium Carbonate	29.98	29.98
7	Sodium Chloride	16.49	16.49

#### 8. EMPAGLIFLOZIN

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	2-Chloro-s-iodo-Benzoic acid	72	48.24
2	3,4,5-Tris-trimethylsilanyloxy-6-trimethylsilanyloxymethyl-tetrahydropyran-2-one	109	73.03
3	Acetonitrile	300	201.00
4	Aluminium chloride	10	6.70
5	Fluoro benzene	25	16.75
6	Hydrochloric acid	9	6.03
7	MDC	300	201.00
8	Methanol	600	402.00
9	Sodium borohydride	9.5	6.37
10	Tetra hydro-furan-3-ol	22	14.74
11	THF	600	402.00
12	Toluene	600	402.00

## 9. ETODOLAC

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	7-Ethyl Tryptophol	160	27.20
2	3-Oxo-pentanoic acid methyl ester	110	18.70
3	Methanol	500	85.00
4	Sulphuric acid	24	4.08
5	Sodium hydroxide	100	17.00
6	Lithium hydroxide	6.9	1.17
7	Tetrahydrofuran	200	34.00
8	Ethyl acetate	200	34.00
9	Sodium chloride	28	4.76
10	Sodium sulphate	2	0.34

## 10. ETORICOXIB

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Thioanisole	36	180.00
2	Acetyl chloride	23	115.00
3	Aluminium Chloride	39	195.00
4	Hydrogen peroxide	10.5	52.50
5	EDC	250	1250.00
6	Sulphur	9.1	45.50
7	Sodium hydroxide	11.3	56.50
8	Morpholine	10	50.00
9	Methyl-6-methyl Nicotinate	42.85	214.25
10	THF	1200	6000.00
11	Chloro acetyl chloride	32	160.00
12	Dimethyl formamide	41.2	206.00
13	Phosphorus oxychloride	43.5	217.50
14	Phosphorus Hexafluoride	41	205.00
15	Sodium hydroxide	10	50.00
16	Acetic acid	20	100.00
17	Toluene	500	2500.00
18	Hexane	200	1000.00
19	Activated carbon	2	10.00

## 11. FAMOTIDINE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	1,3-Dichloro acetone	52	52.00
2	Guanyl thiourea	43.48	43.48
3	Potassium Iodide	2.4	2.40
4	Acetone	170	170.00
5	Thiourea	25.13	25.13
6	Sodium hydroxide	40	40.00
7	N-Sulfamyl-3-chloro propionamide HCl	68.64	68.64
8	Ammonia (23%)	17.3	17.30
9	Acetic acid	5	5.00
10	Methanol	39	39.00
11	Activated carbon	3	3.00

## 12. IMATINIB MESYLATE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	3-dimethylamino-1-pyridin-3-yl propenone	15.75	10.55
2	Activated carbon	5	3.35
3	Ammonia	20	13.40
4	Cyanamide	4	2.68
5	Dicyclocarbodiimide	10	6.70
6	Ethyl acetate	120	80.40
7	Hydrogen	0.55	0.37
8	Imatinib	42	28.14
9	Imatinib Intermediate-2 (4-(4-methyl piperazin-1-yl)methyl benzoic acid di hydrochloride)	26.6	17.82
10	IPE	200	134.00
11	Isopropyl alcohol	250	167.50
12	MDC	800	536.00
13	Methane sulfonic acid	10	6.70
14	Methanol	1600	1072.00
15	n-Butanol	1000	670.00
16	Nitric acid	12	8.04
17	Ortho tolylamine	10	6.70
18	Raney nickel	5	3.35
19	Sodium carbonate	10	6.70

20	Sodium hydroxide	6	4.02
21	Sodium sulphate	2	1.34
22	Sulfuric acid	15	10.05

### 13. IRINOTECAN HCL

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	[1,4']Bipiperidiny1-1'- carbonyl chloride Hydrochloride	5	16.65
2	4,11-Diethyl-4,9- dihydroxy-1,12-dihydro-4H-2-oxa-6,12a-diaza-dibenzo[b,h]fluorene-3,13- dione	7	23.31
3	Methylene di chloride	30	99.90
4	N-methyl-2-Pyrrolidine	40	133.20
5	Di isopropyl ether	30	99.90
6	Iso propyl alcohol	50	166.50
7	Hydrochloric acid	0.6	2.00

### 14. IVABRADINE HCL

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	1,3-dihydro-7,8-dimethoxy-2-oxo1H-3-benzazepine	28	37.24
2	1-[(7S)-3,4- dimethoxybicyclo[4.2.0]octa-1,3,5- trien-7-yl]-N-methylmethanamine	24	31.92
3	3-chloro-1-bromo propane	20.5	27.27
4	5%palladium on Carbon	0.5	0.67
5	Acetone	30	39.90
6	Dimethyl sulphoxide	10	13.30
7	Dimethylformamide	20	26.60
8	Hydrochloric acid	5	6.65
9	Hydrochloric acid in IPA	20	26.60
10	Hydrogen	0.25	0.33
11	Hyflow	1	1.33
12	Iso propyl alcohol	10	13.30
13	Methyl iso butyl ketone	15	19.95
14	Methylene dichloride	15	19.95
15	Methylene dichloride	15	19.95
16	Potassium carbonate	17	22.61

17	Potassium Hydroxide	7.16	9.52
18	Sodium Iodide	19	25.27
19	Sodium sulphate anhydrous	0.5	0.67

### 15. LENALIDOMIDE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	[1,4']Bipiperidiny1-1'- carbonyl chloride Hydrochloride	5	6.65
2	4,11-Diethyl-4,9- dihydroxy-1,12-dihydro4H-2-oxa-6,12a-diazadibenzo[b,h]fluorene-3,13- dione	7	9.31
3	Di isopropyl ether	30	39.90
4	Hydrochloric acid	0.6	0.80
5	Iso propyl alcohol	50	66.50
6	Methylene di chloride	30	39.90
7	N-methyl-2-Pyrrolidine	40	53.20

### 16. LINEZOLID

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	R-3-(3-Fluoro-4- morpholinophenyl)-2-oxooxazolidin-5-yl) methyl methane sulfonate	210	350.70
2	Potassium phthalide	104	173.68
3	TEBAC	10	16.70
4	MIBK	1200	2004.00
5	MDC	800	1336.00
6	Methanol	1250	2087.50
7	Methyl amine (40%)	30	50.10
8	Acetic Anhydride	42	70.14
9	MDC	800	1336.00
10	Ethyl acetate	600	1002.00
11	Sodium hydroxide	12	20.04
12	Activated Carbon	10	16.70

### 17. MESALAMINE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Aniline	26	260.26
2	Sodium nitrite	19.3	193.19
3	Hydrochloric Acid	30.6	306.31
4	Salicylic Acid	38.5	385.39
5	Sodium hydrosulfide	31.3	313.31
6	Carbon	5	50.05
7	Sodium hydroxide	7.2	72.07

### 18. OLMESARTAN MEDOXIMIL OTL-III

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	2-Propyl-1H-imidazole-4,5- dicarboxylic acid diethyl ester	68	22.44
2	4-chloromethyl-5-methyl- [1,3]dioxolan-2-one	30.8	10.16
3	Acetic acid	65	21.45
4	Acetone	500	165.00
5	Activated Carbon	10	3.30
6	Ammonium chloride	10	3.30
7	Di isopropyl ether	100	33.00
8	Ethyl acetate	350	115.50
9	Isopropyl alcohol	600	198.00
10	Lithium hydroxide	6.9	2.28
11	MDC	1200	396.00
12	Methyl magnesium bromide	31.9	10.53
13	N,N-Di methyl Acetamide	8.3	2.74
14	Potassium carbonate	20	6.60
15	Sodium chloride	28	9.24
16	Sodium sulphate	28.5	9.41
17	TBAB	10	3.30
18	TEA	25	8.25
19	Tetrahydrofuran	700	231.00
20	TrityltriazoleButylbromide(TTBB)	140	46.20

### 19. PANTOPRAZOLE SODIUM

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	5-diFluoromethoxy-2-mercapto-	108	143.64
2	Acetic acid	40	53.20
3	Acetic Anhydride	172	228.76
4	Acetone	600	798.00
5	Activated Carbon	10	13.30
6	Ammonia	9	11.97
7	Ammonium Carbonate	50	66.50
8	Ammonium Chloride	25	33.25
9	Ammonium hydroxide	35.5	47.22
10	Chloroform	1050	1396.50

### 20. PIROCTONE OLAMINE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	3,3-Dimethyl acrylic acid	85	70.55
2	3,5,5-tri methyl-hexanoyl chloride	121	100.43
3	Activated carbon	5	4.15
4	Aluminium Tri Chloride	93	77.19
5	EDC	1000	830.00
6	Ethanolamine	45	37.35
7	Ethyl acetate	1000	830.00
8	Hydroxylamine hydrochloride	47	39.01
9	Methanol	3000	2490.00
10	Para toluene sulfonic acid	20	16.60
11	Sodium bi carbonate	57	47.31
12	Sodium methoxide	25	20.75
13	Sodium sulphate	20	16.60

### 21. RAMIPRIL

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	(cis,endo)-octahydro- cyclopenta[b]pyrrole- 2(s)-carboxylic acid hydrochloride	236	77.88
2	2-(1-carboxy- ethylamino)-4-phenyl- butyric acid ethylester	343	113.19
3	5% Pd/ Activated carbon	10	3.30

4	Ethanol	650	214.50
5	Ethyl acetate	600	198.00
6	Triethylamine	600	198.00

## 22. RISPERIDONE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	6-Fluoro-3-(4- piperidinyl)-1,2- benzisoxazole Hydrochloride	260	33.80
2	3-(2-Chloroethyl)-2-Methyl-6,7,8,9- Tetrahydro-4H-pyrido[1,2- $\alpha$ ]Pyrimidin-4-one HCl	315.12	40.97
3	Potassium iodide	2	0.26
4	Methyl Isobutyl ketone	300	39.00
5	Sodium hydroxide	9	1.17
6	Isopropyl alcohol	500	65.00
7	DMF	25	3.25
8	Activated carbon	5	0.65
9	Hyflow	5	0.65

## 23. SACUBITRIL

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Tris(4- methoxyphenyl)borane ammonia complex	98	65.66
2	Hydrochloric acid	73	48.91
3	Toluene	700	469.00
4	Acetone	400	268.00
5	Furan-2,5-dione	26	17.42
6	Methanol	400	268.00
7	Sodium bicarbonate	22	14.74

## 24. SPARFLOXACIN

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Pentafluorobenzoic acid	60	100.20
2	Thionylchloride	33.66	56.21
3	Diethylmalonate	45.26	75.58
4	Sodium Hydroxide	11.31	18.89

5	Magnesium	4	6.68
6	Toluene	600	1002.00
7	Ethanol	1050	1753.50
8	Triethylxofomamide	40	66.80
9	Cyclopropylamine	15.17	25.33
10	Potassium caronate	18.33	30.61
11	Benzyl amine	27.32	45.62
12	Potassium carbonate	17.6	29.39
13	Toluene	800	1336.00
14	Hydrogen	0.5	0.84

### 25. TADALAFIL

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	(1R-3R)-Methyl-1, 2, 3, 4- tetrahydro-2-chloroacetyl1-(3, 4- methylene dioxyphenyl)-9H-pyrido [3, 4-b]- 3- carboxylate	112	187.04
2	Aq methyl amine (40%)	10	16.70
3	Dimethyl sulphoxide	150	250.50
4	Hydrogen peroxide	17	28.39
5	MDC	2200	3674.00
6	Methanol	1025	1711.75
7	Phosphorous oxy chloride	26	43.42
8	Sodium Hydroxide	60	100.20
9	Sodium hypochlorite	37	61.79
10	Sodium methoxide	27	45.09
11	Thionyl chloride	60	100.20
12	Toluene	800	1336.00

### 26. TAMSULOSIN HYDROCHLORIDE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	(S)-5-(2-aminopropyl)-2- methoxybenzene sulfonamide	129	21.93
2	1-((Bromomethoxy)methyl)- 2-ethoxybenzene	130	22.10
3	50% lye solution	20	3.40
4	Ethanol	900	153.00
5	Ethyl acetate	500	85.00
6	Hydrochloric acid	27.3	4.64

7	Methanol	900	153.00
8	n-Hexane	500	85.00

### 27. TELMISARTAN

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Methyl-4-(butyramido)-3-methyl-	73	121.91
2	Methanol	865	1444.55
3	Palladium carbon(Wet 5% MC)	3	5.01
4	Sodium hydroxide	10.4	17.37
5	Hydrochloric acid	31.6	52.77
6	N-Methylbenzene-1,2-diamine	32	53.44
7	Phosphoric acid	90	150.30
8	Sodium hydroxide	110.2	184.03
9	Methyl-4-methyl-1,1-biphenyl-2-	57	95.19
10	1,3-dibromo-5,5-dimethyl	72	120.24
11	Azo bis isobutyronitrile	2.9	4.84
12	Sodium meta bisulphate	4.3	7.18
13	Chloroform	320	534.40
14	n-Hexane	100	167.00
15	Potassium hydroxide	18	30.06
16	Acetone	450	751.50

### 28. THALIDOMIDE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Pthalyl Glutamic acid	116	38.28
2	Urea	25	8.25
3	N,N-Dimethyl formamide	100	33.00
4	Sodium carbonate	20	6.60
5	Activated carbon	5	1.65

### 29. TRICLABENDAZOLE

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	2,3-Di chloro -phenol	258	51.60
2	3,4-Di chloro-phenyl amine	283	56.60
3	Acetic anhydride	179	35.80

4	Carbon di sulphide	113	22.60
5	Di methyl sulphate	204	40.80
6	Ethyl acetate	500	100.00
7	Hydrogen	3.05	0.61
8	Methanol	3100	620.00
9	Nitric acid	107	21.40
10	Palladium Carbon	10	2.00
11	Potassium hydroxide	92	18.40
12	Sodium hydroxide	235	47.00
13	Toluene	500	100.00

### 30. ZOLEDRONIC ACID

S. No	Raw material used	Quantity per batch (kg)	Quantity per day in kg
1	Imidazole	14.3	47.62
2	Methyl chloro acetate	34.3	114.22
3	Potassium carbonate	26	86.58
4	Potassium iodide	3	9.99
5	Toluene	60	199.80
6	Ethyl acetate	80	266.40
7	Chloro benzene	40	133.20
8	Ortho phosphoric acid	16.5	54.95
9	PCl <sub>3</sub>	23.6	78.59
10	HCl	25.5	84.92

**ANNEXURE-5**

**TSDF AGREEMENT COPY**

# Laureatz Technochem Pvt Ltd.

Date: 26.06.2021

To,

The Member Secretary, Industry - II,  
Ministry of Environment, Forest & Climate Change,  
Vijaya Vihar, Indira Park, Connaught Place,  
Jor Bagh Road, Jor Bagh, New Delhi - 110003.

Sir,

Sub: Regarding MoU agreement with CETP and TSEF

With reference to the above subject, M/s. Laureatz Technochem Pvt Ltd proposed for JMT manufacturing unit at Kallacher Industrial area, Talagajpet Taluk & District, Karnataka-580021 and accordingly requested KLRDB, to allot 2 acre of land with Application dated 07-10-2020. KLRDB confirmed the land and issued the demand notice to pay initial payment with letter dated 04/08/2020/MSO/Teay-02/11408 /2020-21 dated 22-08-2021. With continuation of the demand notice, M/s. Laureatz Technochem paid the initial payment to KLRDB on 28-08-2021, approached with written letter to KLRDB on 06-09-2021 for allotment of land and parallelly approached M/s. Mother Earth Environ. Tech Pvt. Ltd to have membership for CETP and TSEF facility. KLRDB took time to issue the allotment letter but M/s. Mother Earth Environ. Tech Pvt Ltd processed and issued the CETP and TSEF membership agreement one day earlier than the allotment letter. They with us are submitting the actuals and facts in this regard.

Requesting you to kindly consider the same and issue us the environmental clearance of the unit.

Thanking You,  
Truam Faithfully,

For M/s. Laureatz Technochem Pvt Ltd,



Sri. T. V. Seethal  
Managing Director

Encl: as above



# KARNATAKA INDUSTRIAL AREAS DEVELOPMENT BOARD

(A Government of Karnataka Undertaking)

# 49, 4th & 5th Floors, 'East Wing', Khanija Bhavan, Race Course Road, Bengaluru - 560 001

Phone : 080-22265383 Fax : 080-22267901

Website : www.kiadb.in email: ceoemkiadb@gmail.com

No. IADB/HO/Allot/23147/14198 /2020-21

Date: 20.03.2021.

Prop: T.V.Srihari,  
M/s. Laureatz Technochem Pvt Ltd,  
Plot No.147, Sri Sai Nilayam,  
Near Tennis Park Pragtinagar,  
Kutbullapur, Niza,  
Hyderbad-500 090.

**RPAD**

Sis,

## **ALLOTMENT LETTER**

**Sub:** Allotment of 2.00 acres (8094.00 Smtres) of land in Plot No.62 of Kadechur Industrial Area, Yadgir District - reg.

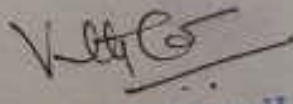
**Ref:** 1. 122<sup>nd</sup> SLSWCC meeting dt: 07.01.2021.  
2. Your letter dt: 16.03.2021.

\*\*\*\*

In pursuance of the approval given by the 122<sup>nd</sup> SLSWCC meeting dt: 07.01.2021 you have been 2.00 acres (8094.00 Smtres) of land in Plot No.62 of Kadechur Industrial Area, Yadgir District for Manufacture of **"APIS & Intermediates"** subject to the terms and conditions indicated in the Annexe-A appended hereto and also the terms and conditions mentioned hereafter.

1. The allotment of land is on lease -cum sale basis for a period of **10** years. The lease is liable to be cancelled automatically in case the land is not utilized within a period of three years in case of MSME, large projects or five years in cases of mega, ultra mega, super mega projects as defined in the industrial policy or the land is not utilized within a specified period approved by DLSWCC/SLSWCC/SHLCC/ Allotment Committee without obtaining valid extensions from the concerned investment approving committees detailed in (c)(iii) of Annexe 'A'.  
The tentative premium payable for allotment of the said land has been fixed at **Rs.37.50/- Lakhs** per Acre.
2. (a) The tentative premium of the said plot is **Rs.75,00,000/-**. and EMD **Rs.10,000/-** per acre  
(b). The tentative premium of the land shall be paid as follows:
  - i. A Sum of **Rs.15,10,000/-** being paid vide Rt. No.0050337 dt:16.03.2021 is adjusted towards 20% land cost & EMD.
  - ii. A sum of **Rs.60,00,000/-** being the balance 80% of the tentative premium of land shall be paid within **150 days** from the date of this letter ie on or before **17.08.2021**.

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Secretary-II  
Karnataka Industrial Areas Development Board  
Bengaluru - 560 001



# MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

(A DIVISION OF CHAITRA GROUP)

**MEEPL**

An Integrated Management System Certified Company | Quality Management System-ISO 9001:2015  
Environmental Management System - ISO 14001:2015 | Occupational Health and Safety Management System- ISO 45001:2018  
Plot No. 158 to 164, KIAOB Kadechur Industrial Estate, Kadechur Village, Tehsil and Yadgiri District, Karnataka - 585221



MEMBERSHIP No. MEEPL/MEM/ 2021 / 2022 / 97

## COMMON HAZARDOUS WASTE TREATMENT STORAGE DISPOSAL FACILITY (CHWTSDF) MANAGING HAZARDOUS WASTE **MEMBERSHIP CERTIFICATE**

This Is To Certify that **KAUREATZ TECHNOCHEM PVT LTD**

Plot No.62, KISADB, Kadechur Industrial Area  
Yadgiri District - 585221 - Karnataka

is a member of Mother Earth Environ Tech Pvt. Ltd.

Date : 13/03/2021

This certificate is valid up to 31/03/2022



*[Signature]*  
Authorised Signatory



Kadachur Industrial Area, Yadgir Taluk & District, Karnataka, having its Registered office at Plot No.147, Sri Sai Nilayam, Pragathi nagar, Kukatpalli, (near JNTU), Hyderabad-500090, Telangana, represented by its Managing Director Mr.T.V. Srihari, S/o Rama Seshagiri Rao aged about 60 hereinafter referred as "GENERATOR/User" which expression shall unless repugnant to the subject or context include its administrators, successors and assigns) as Party No.2

The OPERATOR and GENERATOR hereinafter individually referred as 'Party' and collectively as 'Parties'.

WHEREAS OPERATOR is engaged in the business of Waste Management and presently operating 'Common Hazardous Waste Treatment, Storage and Disposal Facility (TSDF)' Plot No 158 - 164, KIADB Kadachur Industrial Area, Plot No 158-164, KIADB Kadachur I.E, Kadachur, Yadgir Dist., Karnataka State, under its control, as per the guidelines under Hazardous Rules and as per the authorization of CPCB/KSPCB.

WHEREAS the GENERATOR being desirous of availing the services of collection, transport, treatment, storage and disposal of Hazardous Waste generated at their premises approached OPERATOR and the same has been accepted by OPERATOR on the terms and conditions set out in this agreement read with the provisions of Hazardous Waste Rules and supervision of KSPCB.

NOW THEREFORE in consideration of the above, the OPERATOR and GENERATOR have agreed to enter into this agreement under the terms and conditions set forth hereinafter.

**NOW IT IS HEREBY AGREED BY AND BETWEEN THE PARTIES HERETO AS FOLLOWS:**

**I. DEFINITIONS AND INTERPRETATION**

1.1 **Definitions:** In this Agreement, including in the recitals hereof, the following words, expressions and abbreviations shall have the following meanings, unless the context otherwise requires:

"Agreement" means this agreement including all attachments, annexure or Schedules annexed thereto.

"CPCB" means Central Pollution Control Board.

"Hazardous Rules" means Hazardous Waste (Management, Handling & Trans boundary Movement) Rules, 2008 as amended from time to time.

"MoEF" means Ministry of Environment & Forests.

"KSPCB" means Karnataka State Pollution Control Board, Karnataka in the state in which the TSDF operated by OPERATOR is situated.

For LAUREATZ TECHNOCHEM PVT LTD

Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

Director

"TSDF" means the Common Hazardous Waste Treatment, Storage & Disposal Facility by name "MOTHER EARTH ENVIRON TECH PRIVATE LIMITED" (MEEPL) operated by OPERATOR and located at Plot No 158 - 164, KIADB Kadechur Industrial Area, Plot No 158-164, KIADB Kadechur I.E, Kadechur, Yadgir Dist, , Karnataka State, pursuant to the Consent for Operation Storage and Disposal of Hazardous Waste bearing No. AW -319253, dated 24.07.2020 valid up to 30.06.2024 issued by the Competent Authority under Section 25/26 of the Water (Prevention and Control of Pollution) Act, 1974, under Section 21 of Air (Prevention and Control of Pollution) Act, 1981 and Authorization under the Provisions of Hazardous Waste (Management, Handling & Trans boundary Movement) Rules, 2008.

"Waste" means Hazardous waste generated in the premises of the GENERATOR.

- 1.2 **Interpretation:** In this Agreement, unless the subject or context otherwise requires:
- A. Reference to the singular number shall include references to the plural number and vice-versa;
  - B. References to a "person" shall include references to natural persons, partnership firms, companies, bodies corporate and associations, whether incorporated or not or any other organization or entity including any governmental or political subdivision, ministry, department or agency thereof;
  - C. References to recitals, clauses and schedules / annexure are to recitals, clauses and schedules to this Agreement;
  - D. Any reference herein to a statutory provision shall include such provision, as in force for the time being and as from time to time, amended or re-enacted in so far as such amendment or re-enactment is capable of applying to any transactions covered by this Agreement.
  - E. Clause headings used herein are only for ease of reference and shall not affect the interpretation of this Agreement.
- 1.3 The Schedules / Annexure shall form an integral part of this agreement.
- 1.4 All capitalized terms used in this agreement which have not been specifically defined in this Agreement shall, unless inconsistent with the context have the meanings assigned to them under the Authorization Agreement.

## 2 SCOPE OF SERVICES

- 2.1 The scope of services to be provided by OPERATOR under this agreement shall be collection, transportation, treatment, storage and disposal of Hazardous waste generated at the premises of the GENERATOR located at: Plot No.62, KIADB, Kadechur Industrial Area, Yadgir Taluk & District, Karnataka

For LAUREATZ TECHNOCHEM PVT LTD

J. V. Sharma

Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

J. V. Sharma

Director

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- 2.2 It is agreed between the Parties that OPERATOR shall provide the above services to the GENERATOR through Mother Earth Environ Tech Private Limited (MEEPL), a TSDF operated by OPERATOR
- 2.3 OPERATOR shall dispose the Waste as per the mandate of the CPCB guidelines with the provisions of Hazardous Waste Rules.
- 2.4 OPERATOR also agrees to accept even non-hazardous wastes from the GENERATOR provided that the concerned KSPCB issues 'NO OBJECTION' to the GENERATOR.

### 3 GENERAL CONDITIONS

- 3.1 The GENERATOR shall immediately upon execution of this agreement, become registered member of OPERATOR by paying a membership non-refundable fee of **Rs.5000-00. (Excluding GST)**
- 3.2 Security deposit/Advances shall be adjustable against user charges in the event either party decides to terminate this agreement. No financial charges are applicable on such security deposit. The member shall pay (Rs10000) Ten Thousand only a Security Deposit (interest free), equal to the summation of disposal charges and transportation charges of one month or minimum Rs. 50,000/- whichever is higher at the time of membership, which is refundable on termination of agreement.
- 3.3 The GENERATOR shall take the representative of the OPERATOR to collect the sample of the hazardous waste and inform the entire process details which leads to generation of such Waste, for the purpose of determining the Waste characteristics and to decide parameters for comprehensive analysis, as well as its final pathway of treatment, storage and disposal of the Waste.
- 3.4 OPERATOR shall carry on the comprehensive analysis of the Waste in its laboratory or at the collaborative laboratory mutually agreed by the operator at the cost of the GENERATOR, as per the parameters prescribed by CPCB/KSPCB. The comprehensive analysis report shall be used by OPERATOR to determine the disposal pathway based on the waste characteristics & as per MoEF, CPCB and the KSPCB rules and guidelines issued from time to time. The disposal pathway shall be mutually agreed between the GENERATOR & OPERATOR and shall form basis for disposal/ user charges.
- 3.5 The charges for Collection, Transport, Treatment, Storage and Disposal Facility (herein after called as USER CHARGES) will be applicable to GENERATOR as per Annexure – Item No. 01, Item No. 02, Item No. 03 & Item No 04 ( wherever applicable) User Charges quoted in Annexure head wise are the initial basis rates for the GENERATOR which is indicative and all the charges which are defined by MEEPL on a time to time basis shall apply on pro-rata basis common to all MEEPL MEMBERS who have signed similar agreement with MEEPL.
- 3.6 MEEPL, on receipt of information from the GENERATOR, will plan and schedule collection of the Waste from the GENERATOR premises. Safety of community (humans, flora and fauna) during transportation is of prime importance and this safety information

For LAUREATZ TECHCHEM PVT LTD



Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED



Director

will have to be provided by the GENERATOR in (Form 8), Waste Transportation Manifest (Form 10) and TREM Card (Form 9) for every Waste type as per Hazardous Waste (Management and Handling) Rules 1989 and as amended from time to time. In the event of false information to MEEPL of any nature, all associated direct and indirect liabilities are the responsibility of the GENERATOR.

- 3.6 The GENERATOR shall provide the details of Waste to OPERATOR as mentioned below:
- i) Complete details of the Waste and its characteristics regarding presence of explosive / ignitable / corrosive / toxic / odorous compounds in the manifest provided to the transporter for safe transportation and disposal.
  - ii) Safety Information in 'Form 8', 'waste transportation manifest' in Form 10 and 'TREM card' in Form 9 for every Waste type as per Hazardous Rules.
- 3.7 OPERATOR shall analyse the Waste received through finger print analysis as per the parameters prescribed by CPCB/KSPCB.
- 3.8 In the event there are any differences in the analysis results of comprehensive analysis and finger print analysis, the GENERATOR may either accept the results of OPERATOR or send their samples to a mutually agreed third party analysis at their own cost. Any discrepancy in this respect shall be informed to the KSPCB.
- 3.9 The GENERATOR shall provide a fresh comprehensive analysis report when there is a change in the waste characteristics, manufacturing processes, changes in product mix etc.
- 3.10 In the event of any false information or withholding information, all the liabilities, whether directly or indirectly arising therefrom, during transportation, handling, treatment & disposal shall be the responsibility of the GENERATOR.
- 3.11 The GENERATOR shall provide an advance declaration during April every year assuring quantity of Waste they would be sending to OPERATOR during that Financial Year till 31<sup>st</sup> March and declare Waste quantities on annual/monthly basis as per Hazardous Rules as per the declaration format provided in Annexure.
- 3.12 In case of OPERATOR agreeable to provide its containers available at its TSDF to the GENERATOR, the GENERATOR has to pay the container maintenance charges to OPERATOR as per **Annexure Item No. 4**.
- 3.13 The Waste supplied by the GENERATOR shall not contain any kind of nuclear / radioactive or any other prohibited material which is against CPCB/KSPCB/MOEF&CC guidelines as amended from time to time.
- 3.14 OPERATOR shall also supply specially designed containers to help segregate the Waste and arrange the transportation of such containers bearing the waste from the premises of the GENERATOR.

For LAUREATZ TECHNOCHEM PVT LTD

*J.V. Som*

Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

*[Signature]*

Director

Page 5 of 13

- 3.15 In case a waste is classified as explosive in nature, the fact has to be informed to MEEPL. Detailed information on its characteristics and safe handling practices shall be furnished in advance to MEEPL. In case no information is provided, or information is held back and in the event of any explosion or accident during transportation and during handling taking place at MEEPL site, the GENERATOR shall be solely responsible for all such associated direct and indirect liabilities.

#### 4 USER CHARGES & TERMS OF PAYMENT:

- 4.1 The GENERATOR shall pay monthly user charges to OPERATOR for its services as per the slab mentioned in **Annexure Item Nos 1,2& 3**, which is based upon the declaration given by the GENERATOR as per Annexure. In addition the GENERATOR shall also be liable for payment of applicable taxes, levies etc., if any, on the user charges.
- 4.2 The user charges are subject to annual revision on the basis of government of India wholesale price index and also in every event of escalation of fuel costs, power tariff, change in disposal technologies / method, wage hike etc.
- 4.3 OPERATOR shall send the monthly user charges invoice to the GENERATOR on or before 5<sup>th</sup> of every succeeding month and the bill amount shall be payable by the GENERATOR on or before 15<sup>th</sup> of the same month. The GENERATOR shall clear the bills within a period of 15 days from the date of receipt of the invoice.
- 4.4 In case of delayed payments the GENERATOR shall be liable to pay interest at the rate of one and a half per cent (1.5%) per month on the outstanding amount during the default period. In the event of any bill amount along with interest being overdue for more than three months, OPERATOR reserves its right of refusal to extend/provide its services to the GENERATOR and even to terminate this agreement with immediate effect without prejudice to any other steps that it might take against the GENERATOR for recovery of its overdues.
- 4.5 In case, for any reason, if MEEPL vehicle is sent back to MEEPL without providing the waste even after being requisitioned by the GENERATOR, the GENERATOR has to bear and pay the TRANSPORT CHARGE for that trip as mentioned under **Annexure Item 03** for the full capacity load of vehicle.

#### 5 PERIOD OF AGREEMENT

This Agreement shall be valid for a period of 5 years (Five Years) effective from 19/03/2021 subjected to earlier termination by either party in accordance with the provisions of this agreement.

#### 6 FORCE MAJEURE

Notwithstanding anything else contained herein, neither Party hereto shall be liable for damages or to have this agreement terminated for any delay or default in the performance of such Party hereunder if such delay or default in performance derives from conditions beyond the reasonable control of such Party, including but not limited to, acts of god.

For LAUREATZ TECHNOCHEM PVT LTD

J. V. S. M.  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

  
Director

strikes, fires, floods, extreme drought, shortage of supply, riots, work stoppages, embargoes, governmental actions or damage to the plant or facility or any cause unavoidable or beyond the control of either party including any arbitrary ruling by the Government prohibiting the handling of the Waste or continuing domestic or international problems such as wars or insurrections.

## 7 INDEMNITY

The GENERATOR do hereby indemnify, keep indemnified and hold harmless the OPERATOR, its representatives, nominees and officers (including without limitation, reimbursement of any loss suffered by OPERATOR and / or its officers, directors, employees, agents or affiliates and their legal costs), awards, damages, losses and / or expenses, either pecuniary or non-pecuniary in nature, arising directly or indirectly, whether during collection or transportation or treatment or storage or disposal, as a result of:

- a) The Waste supplied by or collected from the GENERATOR in case of any mismatch of waste from TREM Card or finger prints; and any non-disclosure or wrong disclosure of any information as to the characteristic of waste, or
- b) Any civil or criminal proceedings or liability under any law for any unlawful dumping of untreated wastes by the GENERATOR either at the project site of OPERATOR or anywhere else.
- c) Any violation or non-compliance by the GENERATOR of the provisions of Hazardous Rules, Water (Prevention and Control of Pollution) Act, 1974 and Air (Prevention and Control of Pollution) Act, 1981 including any modifications, amendments made thereto and any new acts and rules legislated and promulgated governing the activity under this Agreement during the term of this Agreement or any extension thereof.

## 8. TAKE OVER OF UNIT OF THE GENERATOR

In the event of Change of Management in respect of the GENERATOR by way of takeover of the unit for any reason what-so-ever (including takeover of the assets & liabilities) by a new Management, the old management as well as the new management shall be liable & responsible for payment & settlement of the dues of MEEPL, if any existing on the date of such Management transfer. However, the old Management shall be liable for the amount due, if any only till the date of such Management transfer. Post the effective date of Management transfer, the new Management shall be liable & responsible for all payments, if any & whenever arising under this agreement.

## 9 EVENTS OF DEFAULT

The following shall constitute GENERATOR's events of default:

- a. If the GENERATOR fails / refuses to pay its bills / dues for the user charges payable under this Agreement.

For LAUREATZ TECHNOCHEM PVT LTD

J. V. S. M.

Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

Director

In case of GENERATOR to:

*Attn: T.V. Srihari, Managing Director, M/s. LAUREATZ TECHNOCHEM PVT LTD*

In case of OPERATOR to:

*Attn: Director, Mother Earth Environ Tech Pvt. Ltd.*

And shall be deemed to have been duly given or made by way of presentation as under:

- (a) if personally delivered, upon delivery at the address of the relevant Party;
- (b) if sent by registered post with acknowledgement due, then expiry of seven (7) days after such posting;
- (c) if sent by facsimile, upon receipt of confirmation from the receiver, that the facsimile has been received;
- (d) If sent by courier, four (4) days after the date of such dispatch.

15.2 Either party may notify the other Party of any change in its name, relevant address or contact number for the purposes of Clause 15.1 as provided herein above.

## 16 SURVIVAL

Notwithstanding anything contained in this Agreement, the provisions of clauses 4, 7 and 9 of this Agreement shall continue for a period of 5 years after termination of this agreement or expiry of the period of this agreement whichever is later.

## 17 DISPUTE RESOLUTION

All disputes arising out of this agreement and the contents thereof between the GENERATOR and OPERATOR shall be referred to an Arbitration in accordance with the provisions of the Arbitration and Conciliation Act, 1996. The arbitration proceedings shall be conducted in English and the Arbitration shall take place at Bangalore. The arbitral award shall be final and binding upon both the parties.

**For LAUREATZ TECHNOCHEM PVT LTD**



Managing Director

**For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED**



Director

18 APPLICABLE LAW

OPERATOR and the GENERATOR mutually agree that the courts of law at Bangalore shall have jurisdiction over all the disputes arising out of this Agreement & the decision of such Courts shall be final & binding upon both the parties.

For M/s Laureatz Technochem Pvt Ltd

For LAUREATZ TECHNOCHEM PVT LTD



Name: T.V. Srihari *Managing Director*  
Designation: Managing Director

Witness:

Signature *a. Balakrishna*

Name I. BALAKRISHNA

Designation Engineering Division

Witness:

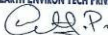
Signature

Name -----

Designation -----

For M/s Mother Earth Environ Tech Pvt Ltd

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED



Name: Hemant Go *Director*  
Designation: Director

Witness:

Signature

Name -----

Designation -----

Witness:

Signature *A. Anand*

Name ABHINANDAN

Designation MARKETING

**ANNEXURE**  
**Common Hazardous Waste Treatment Storage & Disposal Facility**

**1) User Charges:**

The GENERATOR shall pay the following applicable User Charges based on the Waste Types.

Sr. No.	Name Of Waste	Mode of Disposal	Rate Per M.T
1			
2			
3			
4			
5			

**2) Comprehensive Analysis Fee: Rs.15000-00 per waste sample** (Valid for 2 years and if there is any process and raw material change, client will be intimated thereupon and another comprehensive analysis required for that waste shall be conducted at the cost of the GENERATOR)

**3) Transportation Charges:**

**a) Waste Transport Charges: ( To & Fro )**

Minimum Charges shall be Rs. 3000 for 0 to 20 Km, Rs. 5000 for 21 to 50 km and Rs. 6750 for 51 to 100 Km both ways from our facility per trip. For above 100 Km Rs. 6.75 per Km per ton charge will be applicable for both sides. The charges shall be calculated by taking into consideration minimum 90% of the container loading capacity/vehicle capacity. Since the diesel rate is fluctuating frequently the transportation charges/rate is calculated every month based on the average diesel rate during the month. The Distance (D) will be considered on actual basis from the waste generating site of the unit/s to the TSDF site.

**b) Truck Detention Charges:**

Maximum time of Three hours is allowed for the truck to be detained at the premises of the GENERATOR from the time of reporting of the truck to the Security Gate of the premises of the GENERATOR. In the event this three hours period is exceeded, then Rs. 500/- per additional hour shall be charged as detention charges unless it is mutually agreed and accepted beforehand between both the parties in writing about the truck detention beyond the stipulated maximum period of three hours.

**For LAURETZ TECHNOCHEM PVT LTD**

  
Managing Director

**For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED**

Director

#### 4) Container Maintenance Charges:

[Applicable when containerized truck Services are utilized]  
The GENERATOR has to pay the following charges as mentioned below towards the services of the Container, if opted for by the GENERATOR. The cost of such maintenance service shall be decided and mutually agreed upon by both the parties.

Note: Since these containers will be replaced after three years, the applicable container maintenance charges will be valid for **three** years only.

##### a) Container Handling Charges:

The GENERATOR shall pay for Container Handling Charges to MEEPL as follows for utilizing the Material Handling Equipment.

For Hook lift/Crane Operations: Rs. N/A /- per MT  
For Waste transported by GENERATOR, Handling (Unloading) Charges shall be Rs. N/A /- per MT, if not transported by a Dumper/Tipper.

**5) TAXES / LEVIES:** All Government / Municipal / Panchayat Taxes / Duties/ Levies/ Octroi / Tolls etc, as applicable from time to time, shall be payable by the GENERATOR.

#### Other/ Miscellaneous Terms & Conditions:

- This membership is valid as long as the GENERATOR is in good standing with the TSDF and has continued valid authorization from KSPCB regarding the Waste Generation.
- The membership deposit is one time nonrefundable deposit with benefits for full tenure of TSDF. The deposit will not be refunded, when desired to discontinue membership, before the end of life of TSDF.
- This TSDF shall accept all kinds of land fillable hazardous wastes, as classified in Hazardous Waste Rules, as amended from time to time for disposal.
- Acceptance of waste is dependent on the fulfillment of regulatory and statutory guidelines for operations of TSDF issued from time to time.
- Pathway of disposal of wastes and its price shall be decided based on the guidelines issued from time to time by regulatory authorities and shall be at the discretion of TSDF.
- From the date of signing of agreement, the GENERATOR shall submit samples as stipulated in Clause Nos.3.3 and 3.4 of this Agreement for comprehensive analysis within 15 days. The analysis report generated by OPERATOR will form the basis of disposal pathway along with disposal charges as per **Annexure Item No. 02** which will be annexed after analysis of the sample and will form part of this agreement.

For LAUREATZ TECHNOCHEM PVT LTD

  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

  
Director

11/20/20

**DECLARATION**

We M/s. LAUREATZ TECHNOCHEM PVT LTD, hereby declare that based on our industry production and our annual projections we shall be disposing the following Hazardous Waste types to MEEPL. (Additional sheets could be used for multiple waste types)

- The Avg. Yearly generation of Hazardous Waste is expected as follows.
- 1. Avg. \_\_\_\_\_ MT per year of \_\_\_\_\_ type of Hazardous WASTE
- 2. Avg. \_\_\_\_\_ MT per year of \_\_\_\_\_ type of Hazardous WASTE
- 3. Avg. \_\_\_\_\_ MT per year of \_\_\_\_\_ type of Hazardous WASTE
- 4. Avg. \_\_\_\_\_ MT per year of \_\_\_\_\_ type of Hazardous WASTE

FOR ... **For LAUREATZ TECHNOCHEM PVT LTD**

*J. V. Sharma*

Managing Director

Authorized Signatory  
The GENERATOR, the Second Party.

Witness 1: Name: I. Balakrishna

Sign: I. Balakrishna

Company/Occupation: Laureatz Technochem Pvt Ltd.  
Designation: Engineering M.

Witness 2: Name: \_\_\_\_\_

Sign: \_\_\_\_\_

Company/Occupation: \_\_\_\_\_  
Designation: \_\_\_\_\_

For LAUREATZ TECHNOCHEM PVT LTD

**ANNEXURE-6**

**CETP AGREEMENT COPY**



# MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

(A DIVISION OF CHAITRA GROUP)

An Integrated Management System Certified Company | Quality Management System-ISO 9001:2015

Environmental Management System - ISO 14001:2015 | Occupational Health and Safety Management System- ISO 45001:2018

Plot No. 158 to 164, KIADB Kadechur Industrial Estate, Kadechur Village, Tehsil and Yadgiri District, Karnataka - 585221



Reg. No.: R19/1/0468

## COMMON EFFLUENT TREATMENT PLANT (CETP)

## MEMBERSHIP CERTIFICATE

This Is To Certify that **LAUREATA TECHNOCHEM PVT LTD** .....

Plot No. 62, KIADB, Kadechur Industrial Area, .....

Yadgiri District - 585221 - Karnataka .....

is a member of Mother Earth Environ Tech Pvt. Ltd.

Date : 19/03/2021 .....

This certificate is valid up to 31/03/2022 .....



*T. V. Kumar*  
Authorised/Signatory



सत्यमेव जयते

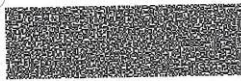
INDIA NON JUDICIAL

**Government of Karnataka**

**e-Stamp**

<b>Certificate No.</b>	: IN-KA78727406909669T
<b>Certificate Issued Date</b>	: 18-Mar-2021 10:36 AM
<b>Account Reference</b>	: NONACC/ kakscsa08/ KENGERI1/ KA-BA
<b>Unique Doc. Reference</b>	: SUBIN-KAKAKSCSA0831847745196846T
<b>Purchased by</b>	: MOTHER EARTH ENVIRONMENT TECH PVT LTD
<b>Description of Document</b>	: Article 12 Bond
<b>Description</b>	: AGREEMENT
<b>Consideration Price (Rs.)</b>	: 0 (Zero)
<b>First Party</b>	: MOTHER EARTH ENVIRONMENT TECH PVT LTD
<b>Second Party</b>	: LAUREATZ TECHNO CHEM PVT LTD
<b>Stamp Duty Paid By</b>	: MOTHER EARTH ENVIRONMENT TECH PVT LTD
<b>Stamp Duty Amount(Rs.)</b>	: 50 (Fifty only)

सत्यमेव जयते



Please write or type below this line

THIS AGREEMENT is made at Bengaluru, Karnataka on this 19<sup>th</sup> Day of March 2021BY  
 AND BETWEEN M/s **MOTHER EARTH ENVIRON TECH PRIVATE LIMITED**, a Company registered under the Companies Act, 1956 and having its registered office at No.13, Challeghatta Village, Kengeri Hobli, Bengaluru South Taluk, Bengaluru - 560074, Karnataka, India, represented by its Director Sri T N Paramesh S/o Ningge Gowda (hereinafter referred as "MEEPL/Operator" which expression shall be unless repugnant to the subject or context include its administrators, successors and assigns) as Party No.1

AND For **MOTHER EARTH ENVIRON TECH PRIVATE LIMITED**  
**For LAUREATZ TECHNOCHEM PVT LTD**  
 M/s. LAUREATZ TECHNOCHEM PVT LTD, having its Factory at Plot No.62, KIADB,

*J.V. Srinivas*  
 Managing Director

*C. N. Jagan*  
 Director

Statutory Alert:  
 1 The authenticity of this Stamp certificate should be verified at 'www.sholestamp.com' or using e-Stamp Mobile App of Stock Holding.  
 Any discrepancy in the details on this Certificate and as available on the website / Mobile App renders it invalid  
 2 The onus of checking the legitimacy is on the users of the certificate

Kadechur Industrial Area, Yadgir Taluk & District, Karnataka and its Registered Office at Plot No.147, Sri Sai Nilayam, Pragathi nagar, Kukatpalli, (near JNTU), Hyderabad-500090, Telangana, represented by its Managing Director T.V. Srihari, S/o Rama Seshagiri Rao aged about 60 Years (Hereinafter referred as "GENERATOR/User" which expression shall unless repugnant to the subject or context include its administrators, successors and assigns) as PartyNo.2

The OPERATOR and GENERATOR hereinafter individually referred as 'Party' and collectively as 'Parties'.

WHEREAS OPERATOR is engaged in the business of Waste Management and presently operating 'Common Effluent Treatment Plant (CETP)' at Plot No. 157 & 158 Kadechur industrial Area Yadgir District - 562112, Karnataka State, under its control, as per the guidelines under Hazardous Rules and as per the authorization of CPCB/KSPCB,

Whereas the OPERATOR offered the facility of CETP to GENERATOR and GENERATOR expressed willingness to availing the services of collection, transport, treatment, storage and disposal of Hazardous Waste generated at their premises, on the terms and conditions set out in this agreement read with the provisions of Hazardous Waste Rules and supervision of KSPCB.

NOW THEREFORE in consideration of the above, the OPERATOR and GENERATOR have agreed to enter into this agreement under the terms and conditions set forth hereinafter.

**NOW IT IS HEREBY AGREED BY AND BETWEEN THE PARTIES HERETO AS FOLLOWS:**

## 1. DEFINITIONS AND INTERPRETATION

- 1.1 **Definitions:** In this Agreement, including in the recitals hereof, the following words, expressions and abbreviations shall have the following meanings, unless the context otherwise requires:

"Agreement" means this agreement including all attachments, annexure or Schedules annexed thereto.

"CPCB" means Central Pollution Control Board.

"Hazardous Rules" means Hazardous Waste (Management, Handling & Trans boundary Movement) Rules, 2008 as amended from time to time.

"MoEF" means Ministry of Environment & Forests.

"KSPCB" means Karnataka State Pollution Control Board, Karnataka in the state in which the TSDF operated by OPERATOR is situated.

"CETP" means the Common Effluent Treatment Plant by name "MOTHER EARTH ENVIRON TECH PRIVATE LIMITED" (MEEPL) operated by OPERATOR and

For LAURETZ TECHNOCHEM PVT LTD

J.V. Srihari

Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED 2 of 14

T.V. Srihari

Director

located at Plot No. 158 to 162 Kadechur industrial Area Yadgir District - 562112, Karnataka State, pursuant to setup the CETP and EC obtained from MoEF &CC F>No.21-8/2014-IA-III dtd: 14-10-2016

"Effluent" means Liquid waste generated in the premises of the GENERATOR.

ZLD means zero Liquid discharge facility

"LOW TDS" means Liquid waste generated in the premises of the GENERATOR as per Annexure- Parameter.

"HIGH TDS" means Liquid waste generated in the premises of the GENERATOR as per Annexure- B parameter.

12. **Interpretation:** In this Agreement, unless the subject or context otherwise requires:

- A. Reference to the singular number shall include references to the plural number and vice-versa;
- B. References to a "person" shall include references to natural persons, partnership firms, companies, bodies corporate and associations, whether incorporated or not or any other organization or entity including any governmental or political subdivision, ministry, department or agency thereof;
- C. References to recitals, clauses and schedules / annexure are to recitals, clauses and schedules to this Agreement;
- D. Any reference herein to a statutory provision shall include such provision, as in force for the time being and as from time to time, amended or re-enacted in so far as such amendment or re-enactment is capable of applying to any transactions covered by this Agreement.
- E. Clause headings used herein are only for ease of reference and shall not affect the interpretation of this Agreement.

13. The Schedules / Annexure shall form an integral part of this agreement.

14. All capitalized terms used in this agreement which have not been specifically defined in this Agreement shall, unless inconsistent with the context have the meanings assigned to them under the Authorization Agreement.

## 2. SCOPE OF SERVICES

The scope of services to be provided by OPERATOR under this agreement shall be collection, transportation, treatment, and disposal (ZLD treatment) of Liquid Effluent as mentioned in Annexure- A & Annexure - B generated at the premises of the GENERATOR located at Plot No.62, KIADB, Kadechur Industrial Area Yadgir District - 562112, Karnataka, India. The GENERATOR agrees to accept the services of OPERATOR on non-exclusive basis in case of CETP is unable to take the effluent only

For LAUREATZ TECHNOCHEM PVT LTD

OTJ TVR For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED Page 3 of 14

  
Director

21. It is agreed between the Parties that OPERATOR shall provide the above services to the GENERATOR through Mother Earth Environ Tech Private Limited (MEEPL), a CETP operated by OPERATOR (Proposed CETP at Kadechur Industrial Area, Yadgir).
22. OPERATOR shall dispose the Waste as per the mandate of the CPCB/KSPCB guidelines with the provisions of Hazardous Waste Rules.
23. OPERATOR agrees to accept liquid Effluent as mentioned in Annexure A & B wastes from the GENERATOR provided that the concerned KSPCB issues 'NO OBJECTION' Authorises to use the CETP of the operator to the GENERATOR.

### 3 GENERAL CONDITIONS

- 3.1 The GENERATOR shall immediately upon execution of this agreement, become registered Life time member of OPERATOR by paying a membership non-refundable fee of **Rs.10000-00. (Rs Ten Thousand Only, Excluding GST)**
- 3.2 Security deposit/Advances shall be adjustable against user charges in the event either party decides to terminate this agreement. No financial charges are applicable on such Security deposit of Rs 1,00,000/ (Rs. One lakh only), if when OPERATORCETP is ready to receive the effluent. The Security deposit which is refundable/adjustable as mentioned above on termination of agreement.
- 3.3 The GENERATOR shall take the representative of the OPERATOR to collect the sample of the Effluent types, for the purpose of determining the Liquid Waste characteristics and to decide parameters for analysis, as well as its final pathway of ZLD treatment.
- 3.4 OPERATOR shall carry on the analysis of the Effluent Waste in its laboratory or at the collaborative laboratory mutually agreed by the Parties operator, as per the parameters Agreed between OPERATOR & GENERATOR. The comprehensive analysis report shall be used by OPERATOR to determine the disposal pathway based on the waste characteristics as per ZLD treatment at CETP.
- 3.5 The charges for Collection, Transport, ZLD Treatment and Disposal (herein after called as USER CHARGES) will be applicable to GENERATOR as per Annexure-C – Item No. 01 for Low TDS(Parameter-A & Parameter-B) & Item No. 02 for High TDS (wherever applicable) User Charges quoted in Annexure-C head wise. Any Changes in the USER CHARGES shall be with mutual consent. Based on mutual consent between OPERATOR and GENERATOR Annexure -C will be revised, However User charges agreed at the time of Agreement signing will be valid for minimum eighteen months from the date of lifting first tanker of Effluent.
- 3.6 MEEPL, on receipt of information from the GENERATOR, will plan and schedule collection of the Effluent Waste from the GENERATOR premises. Safety of community (humans, flora and fauna) during transportation is of prime importance and thus safety information will have to be provided by the GENERATOR in (Form 8), Waste Transportation Manifest (Form 10) and TREM Card (Form 9) for every Waste type as per Hazardous Waste (Management and Handling) Rules 1989 and as amended from time to

For LAUREATZ TECHNOCHEM PVT LTD

  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

  
Director

time. MEEPL has to ensure the quality of effluent being lifted, before leaving the GENERATOR Premises no claims will be accepted once tanker leaves the premises. The GENERATOR shall provide the details of Waste to OPERATOR as mentioned below:

- i. Complete details of the Waste and its characteristics regarding presence of explosive compounds in the manifest provided to the transporter for safe transportation and disposal.
  - ii. Safety Information in 'Form 8', 'waste transportation manifest' in Form 10 and TREM card' in Form 9 for every Waste type as per Hazardous Rules.
- 3.7 OPERATOR shall analyze the Waste received and intimating to the concerned GENERATOR. If there is any discrepancy, this is acceptable provided if the effluent collected from one GENERATOR is not mixed with others.
  - 3.8 In the event there are any differences in the analysis results of comparing to Annexure-A & Annexure-B results, OPERATOR and GENERATOR may approach a mutually agreed third party lab for analysis, in this event whoever is wrong has to bear the cost of analysis. Any discrepancy in this respect shall be mutually solved by GENERATOR & OPERATOR.
  - 3.9 The GENERATOR shall provide a fresh comprehensive analysis report when there is a change in the waste characteristics, manufacturing processes and changes in product mix etc.
  - 3.10 The GENERATOR shall provide an advance declaration during every year quarterly rolling plan of forecast of quantity of Waste they would be sending to OPERATOR during the quarter till that Financial Year till 31<sup>st</sup> March and declare Waste quantities on quarterly/monthly basis.
  - 3.11 The OPERATOR will take full responsibility for 365 days of collection, transportation and treatment as per ZLD method without any trouble to the GENERATOR. During Annual Maintenance period, Collection of effluent from GENERATOR will continue. In case of any unavoidable emergencies it will mutually discussed to manage to treat the Effluent
  - 3.12 The OPERATOR will take full responsibility for legal visits by any legal bodies at CETP behalf of any GENERATOR but prior intimation at least 48 hrs. before need to be intimated.
  - 3.13 If there is **change in the parameters** prescribed in Annexure-A and Annexure-B, The GENERATOR and OPERATOR mutually discussed and if there are any Increase /Decrease of treatment charges applicable for treating that effluent will be mutually discussed and concluded by GENERATOR & OPERATOR

#### 4 USER CHARGES&TERMS OF PAYMENT:

- 4.1 The GENERATOR shall pay monthly user charges to OPERATOR for its services as per in Annexure Item Nos 1&2. This is based upon the declaration given by the

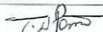
For LAUREATZ TECHNOCHEM PVT LTD

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Page 5 of 14

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

Managing Director

  
Director

GENERATOR as per Annexure. In addition, the GENERATOR shall also be liable for payment of applicable taxes, levies etc., if any, on the user charges. Invoice will be raised on the quantity supplied on Monthly basis

- 42 The user charges are generally fixed, in case of any considerable operating cost variation, OPERATOR may submit the proposal of revision of USER CHARGES, OPERATOR and GENERATOR will have discussion on the same and conclude in mutually acceptable way based on escalation of prices which are consumed in CETP. However, this clause will be applicable after Eighteen Months of starting the effluent lifting from individual GENERATORS.
- 43 OPERATOR shall send the monthly user charges invoice to the GENERATOR on or before 5<sup>th</sup> of every succeeding month and the bill amount shall be payable by the GENERATOR on or before 4<sup>th</sup> of subsequent month. The GENERATOR shall clear the bills within a period of 30 days from the date of receipt of the invoice.
- 44 In case of delayed payments more than two month by the GENERATOR, OPERATOR reserves its right of refusal to extend/provide its services to the GENERATOR and even to terminate this agreement within one month from the default period without prejudice to any other steps that it might take against the GENERATOR for recovery of its overdues.

## 5 PERIOD OF AGREEMENT

This Agreement shall be valid for a period of five (5) years effective from 19/03/2021, subjected to earlier termination by either party in accordance with the provisions of this agreement.

## 5A REPRESENTATION AND WARRANTIES

5A.1 The OPERATOR represents and warrants that the OPERATOR shall be solely responsible to ensure that persons deployed by it for the purpose of this contract are adequately trained for collection; handling, transportation, processing and disposal of the waste are provided with such safety gadgets as required. GENERATOR shall not be liable for any mishap, directly or indirectly.

5A.2 The OPERATOR shall transport the wastes collected from GENERATOR in closed container or will suitably cover the loaded wastes so as to not to litter the areas while transporting the waste.

5A.3 The OPERATOR represents and warrants that the OPERATOR shall comply with all the applicable provisions of labor laws including ESI/Bonus, Provident Fund, Workmen's Compensation and other applicable laws, with regard to the persons deployed by it for providing transportation and treatment of the waste hereunder. Further, the OPERATOR shall obtain and maintain at all times a valid license under Contract Labor (R&A) Act, 1970 whenever it is applicable. The OPERATOR shall be solely responsible for any violation of provisions of the labor laws or any other statutory provisions and shall further keep GENERATOR indemnified from all acts of omissions, faults, breaches and/or

For LAUREATZ TECHNOCHEM PVT LTD

  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED of 14

  
Director

any claim, demand, loss, injury and expenses arising out from the noncompliance of the aforesaid statutory provisions. The OPERATOR's failure to fulfill any of the obligations hereunder and/or under the said Acts, Rules/Regulations and/or any Bye- Laws or rules framed under or any of these, the GENERATOR shall be entitled to recover any of such losses or expenses which it may have to suffer or incur on account of such claims, demands, loss or injury from the OPERATOR.

5A.4 The OPERATOR represents and warrants that the OPERATOR shall comply with all rules and regulations stipulated by the any applicable laws or other applicable government authority and GENERATOR shall not be liable in any manner for improper transportation, processing and disposal of the waste.

5A.5 The OPERATOR represents and warrants that the OPERATOR shall be solely liable for any violation of the Environment (Protection) Act 1986 and the relevant rules made there under.

## **5B COVENANTS OF THE OPERATOR**

5B.1 The OPERATOR shall be responsible for the faithful compliance of the terms and conditions of this Contract. In the event of any breach of the Contract, the remaining work may be performed by another OPERATOR by mutual discussion.

5B.2 The OPERATOR shall be responsible to provide a copy of the valid Consent Letter/Licenses/Registration Certificate or any other relevant document to GENERATOR for the Services upon the signing of this Contract and at any time whenever required by GENERATOR.

5B.3 The OPERATOR shall be responsible to provide a copy of the valid public liability insurance policy to GENERATOR for the purpose of fulfilling their obligation mentioned under this Contract.

5B.4 The OPERATOR shall be responsible for transportation of the waste. Further, the OPERATOR shall be responsible to keep such vehicle road worthy, fit to carry such waste as prescribed by statutory bodies such as, Department of Ecology/Environment, KSPCB, RTO and such other statutory bodies as prescribed from time to time. Such vehicles are used exclusively for the transportation of waste, maintained in good condition and an alternative arrangement made in case of breakdown.

5B.5 The OPERATOR shall be responsible to submit monthly returns to KSPCB or any such applicable government authority of the quantity and nature of the waste received and processed from GENERATOR.

## **6 FORCE MAJEURE**

Notwithstanding anything else contained herein, neither Party hereto shall be liable for damages or to have this agreement terminated for any delay or default in the performance of such Party hereunder if such delay or default in performance derives from conditions beyond the reasonable control of such Party, including but not limited to, acts of god, strikes, fires,

For LAUREATZ TECHNOCHEM PVT LTD

Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

LAUREATZ TECHNOCHEM PVT LTD

Director

floods, extreme drought, shortage of supply, riots, work stoppages, embargoes, governmental actions or damage to the plant or facility or any cause unavoidable or beyond the control of either party including any arbitrary ruling by the Government prohibiting the handling of the Waste or continuing domestic or international problems such as wars or insurrections. If a Party's performance of its obligations hereunder is suspended due to an occurrence of a Force Majeure event the other Party may terminate this Agreement without incurring charges.

#### 7. TAKE OVER OF UNIT OF THE GENERATOR/OPERATOR

In the event of Change of Management in respect of the GENERATOR/OPERATOR by way of takeover of the unit for any reason what-so-ever (including takeover of the assets & liabilities) by a new Management, the old management as well as the new management shall be liable & responsible for payment & settlement of the dues of MEEPL/GENERATOR, if any existing on the date of such Management transfer. However, the old Management shall be liable for the amount due, if any only till the date of such Management transfer. Post the effective date of Management transfer, the new Management shall be liable & responsible for all payments, if any & whenever arising under this agreement. (Change to be informed) in case of change of management of MEEPL/OPERATOR, OPERATOR will ensure that CETP Operations will be continued uninterruptedly.

#### 8. EVENTS OF DEFAULT

The following shall constitute GENERATOR's events of default:

If the GENERATOR fails / refuses to pay its bills / dues for the user charges payable under this Agreement. As defined in Clause 4.3 & 4.4

#### 9. TERMINATION

- 9.1 The Operator shall provide two (2) months prior notice to GENERATOR have the right to terminate this Agreement by giving a proper Notice, immediately upon occurrence of the GENERATOR's event of default as stated in point No. 8 above.
- 9.2 GENERATOR Either party shall have the right to terminate this Agreement by SIX MONTHS prior notice in the event of violation of any of the terms and conditions as agreed upon in this agreement.

#### 10A INDEMNIFICATION

The OPERATOR, apart from providing coverage under the Public Liability Insurance Policy, shall indemnify and hold harmless to GENERATOR, its officers, directors and employees from and against claims, damages, court fees, court awards, losses and expenses arising out of, or resulting from (a) provisions of the service (b) mishandling /omission to handle/process the waste by OPERATOR or its employees or any other person deployed by the OPERATOR (c) non-compliance of applicable laws and rules applicable to this Agreement.

For LAUREATZ TECHNOCHEM PVT LTD

*J. V. Sharma*  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

*C. S. Kumar*  
Director

LAUREATZ TECHNOCHEM PVT LTD

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## 11 ENTIRE AGREEMENT

This Agreement shall be deemed to represent the entire terms and conditions between the parties hereto in respect of the subject matter and shall supersede, cancel and replace any and/or all prior agreements or arrangements, if any, entered into in this behalf, by and between the parties hereto.

## 12 RELATIONSHIP OF THE PARTIES

Nothing contained herein shall be deemed to constitute a partnership, joint venture or agency by and between the parties hereto.

## 13 VARIATIONS

This Agreement may be modified and/or amended only in writing, duly executed by the authorized signatories on behalf of the parties hereto.

## 14 INVALIDITY

In the event that any provisions of this Agreement is held to be illegal, invalid or unenforceable under any present or future laws of the Republic of India, such provisions shall be deemed to terminated forthwith and the remaining parts & provisions of this Agreement shall continue to remain in full force & effect.

## 15 NOTICES

- 15.1 Any notice, request, demand or other communication given or made under or in connection with the matters contemplated by this Agreement shall be in writing and shall be delivered personally or sent by registered post with acknowledgement due or by facsimile or by courier.

In case of GENERATOR to:

Attn: Mr.T.V.Srihari, Managing Director, LAUREATZ TECHNOCHEM PVT LTD

In case of OPERATOR to:

Attn: Mr.T.N.Paramesh, Managing Director/s. Mother Earth Environ Tech Pvt. Ltd.

And shall be deemed to have been duly given or made by way of presentation as under:

- (a) if personally delivered, upon delivery at the address of the relevant Party;
- (b) if sent by registered post with acknowledgement due, then expiry of seven (7) days after such posting;
- (c) if sent by facsimile, upon receipt of confirmation from the receiver, that the facsimile has been received;
- (d) If sent by courier, four (4) days after the date of such dispatch.
- (e) The notice may be sent to e-mail provided by the other party.

- 15.2 Either party may notify the other Party of any change in its name, relevant address or contact number for the purposes of Clause 15.1 as provided hereinabove.

For LAUREATZ TECHNOCHEM PVT LTD

  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

  
Director

**16 DISPUTE RESOLUTION**

All disputes arising out of this agreement and the contents thereof between the GENERATOR and OPERATOR mutually agree that the courts of law at Raichur shall have jurisdiction over all the disputes arising out of this Agreement & the decision of such Courts shall be final & binding upon both the parties.

**17 APPLICABLE LAW**

OPERATOR and the GENERATOR mutually agree that the courts of law at Raichur shall have jurisdiction over all the disputes arising out of this Agreement & the decision of such Courts shall be final & binding upon both the parties.

For LAUREATZ TECHNOCHEM  
PVT LTD.

For LAUREATZ TECHNOCHEM PVT LTD



Name: T.V. Srihari *Managing Director*  
Designation: MANAGING DIRECTOR

**Witness**

Signature *B. Balakrishna*

Name *B. Balakrishna*

Designation: *Engineering division*

**Signature**

Name \_\_\_\_\_

Designation: \_\_\_\_\_

For M/s Mother Earth Environ Tech Private  
Limited. For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED



Director

Name: T.N. Paramesh  
Designation: MANAGING DIRECTOR

**Witness**

**Signature**

Name \_\_\_\_\_

Designation: \_\_\_\_\_

**Signature**

Name \_\_\_\_\_

Designation: \_\_\_\_\_

**ANNEXURE-A**

**Common Effluent Treatment Plant (CETP) & ZLD facility**

**1) Low TDS characteristics:**

**PARAMETER-A (Rs 3000, Three Thousand only per M3)**

Sl.No	Parameters	Value obtained
1	pH @24.80C AMBIENT	5-9
2	Total Dissolved Solids, mg/L	10000-13500
3	Temperature, °C	25.8 AMBIENT
4	TSS (in ppm)	500-1000(200-300)
5	Total Hardness as CaCO3, mg/L	800 to 1000(200-500)
6	Chlorides as Cl, mg/L	3000—5000(500-750)
7	Total Alkalinity as CaCO3, mg/L	800 to 1000
8	Oil & Greece, mg/L	50—60
9	Organic Solvents, mg/L	1000-1500(200-400)
10	Chemical Oxygen Demand, mg/L	10000—20000 (1500-2500)
11	Biochemical Oxygen Demand (3Days at 270C), mg/L	8000-12000(3000-4000)

**PARAMETER-B (Rs 2100, Twenty One Hundred Only per M3)**

Sl. No	Parameters	Value obtained
1	pH @24.80C AMBIENT	5-9
2	Total Dissolved Solids, mg/L	10000-13500
3	Temperature, °C	25.8 AMBIENT
4	TSS (in ppm)	200-300
5	Total Hardness as CaCO3, mg/L	200 to 500
6	Chlorides as Cl, mg/L	500—750
7	Total Alkalinity as CaCO3, mg/L	800 to 1000
8	Oil & Greece, mg/L	50—60
9	Organic Solvents, mg/L	200-400
10	Chemical Oxygen Demand, mg/L	1500—2500
11	Biochemical Oxygen Demand (3Days at 270C), mg/L	3000-4000

2) **Comprehensive Analysis Fee:** Rs 5000 per waste sample plus applicable Taxes (Valid for 2 years and if there is any process and raw material change, client will be intimated thereupon and another comprehensive analysis required for that waste shall be conducted at the cost of the GENERATOR)

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

For LAUREATZ TECHNOCHEM PVT LTD

*D.V. Somani*

Managing Director

*T. J. Bhat*  
Director

ANNEXURE -B

Common Effluent Treatment Plant (CETP) & ZLD facility

1. High TDS characteristics:

**PARAMETER-A (Rs 4000,Four Thousand only per M3)**

<u>Sl. No</u>	<u>Parameters</u>	<u>Value obtained</u>
1	pH @24.80C	5-9
2	Total Dissolved Solids, mg/L	50000 to 100000
3	Temperature, °C	25.8 AMBIENT
4	TSS (inppm)	2000-8000
5	Total Hardness as CaCO3, mg/L	2500 to 5000
6	Chlorides as Cl, mg/L	10000- 20000
7	Total Alkalinity as CaCO3, mg/L	1000 to3000
8	Oil & Greece, mg/L	50—100
9	Organic Solvents, mg/L	2000-4000
10	Chemical Oxygen Demand, mg/L	50000-100000
11	Biochemical Oxygen Demand (3Days at 270C), mg/L	10000-20000

2) **Comprehensive Analysis Fee:** Rs 6000 per waste sample plus applicable taxes (Valid for 2 years and if there is any process and raw material change, client will be intimated thereupon and another comprehensive analysis required for that waste shall be conducted at the cost of the GENERATOR)

For LAUREATZ TECHNOCHEM PVT LTD

  
Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED

  
Director

### ANNEXURE -C

The GENERATOR shall pay the following applicable User Charges (Inclusive of transportation) based on the Waste Types.

Item. No.	Name Of Waste	Mode of Disposal	Rate, Rs Per m3
1	Low TDS (parameter-A)	ZLD	3000
2	Low TDS (Parameter-B)	ZLD	2100

Item. No.	Name of Waste	Mode of Disposal	Rate Per m3
2	High TDS	ZLD	4000/-

Note: The Above-mentioned prices are exclusive of Taxes, Taxes needs to be paid extra as applicable.

For LAUREATZ TECHNOCHEM PVT LTD



Managing Director

For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED



Director

For LAUREATZ TECHNOCHEM PVT LTD


**Annexure-F**

**5) TAXES / LEVIES:** All Government / Municipal / Panchayat Taxes / Duties/ Levies/Octroi / Tolls etc., as applicable from time to time, shall be payable by the GENERATOR.

❖ **Other/ Miscellaneous Terms & Conditions:**

- This membership is valid as long as the GENERATOR is in good standing with the CETP and has continued valid authorization from KSPCB regarding the Waste Generation.
- The membership Fees is one-time nonrefundable deposit with benefits for full tenure of CETP. The deposit will not be refunded, when desired to discontinue membership.
- Acceptance of waste is dependent on the fulfillment of regulatory and statutory guidelines for operations of CETP issued from time to time.
- Pathway of disposal of wastes shall be decided based on the guidelines issued from time to time by regulatory authorities
- From the date of signing of agreement, the GENERATOR shall submit samples once CETP is starts its Operation as stipulated in Clause Nos.3.3 and 3.4of this Agreement for comprehensive analysis within 15 days. The analysis report generated by OPERATOR will form the basis of disposal of ZLD method pathway along with disposal charges as per **Annexure-A & B Item No. 02** which will be annexed after analysis of the sample and will form part of this agreement.

**For LAUREATZ TECHNOCHEM PVT LTD**

  
Managing Director

**For MOTHER EARTH ENVIRON TECH PRIVATE LIMITED**

  
Director

# **ANNEXURE-7**

## **RISK ASSESSMENT REPORT**

## **RISK ASSESSMENT REPORT**

**The proposed green field project is for the manufacturing of Active Pharmaceutical Ingredients (API's).**

### **1. INTRODUCTION TO RISK ASSESSMENT**

M/s. Laureatz Technochem Pvt. Ltd has proposed to establish API manufacturing unit in an area of 8089.8 Sqm (2.0 Acres) at Plot No. 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka-585221. M/s. Laureatz Technochem Pvt. Ltd handles various chemicals, some of which are hazardous in nature by virtue of their intrinsic chemical properties or their operating temperatures or pressures or a combination of them. Fire, explosion, toxic release or combinations of them are the hazards associated with industrial plants using hazardous chemicals. More comprehensive, systematic and sophisticated methods of Safety Engineering, such as, Hazard Identification and Risk Assessment is essential to improve upon the integrity, reliability and safety of industrial plants, the same has been discussed in detail under their respective headings.

### **2. OBJECTIVES OF RISK ASSESSMENT**

As per CIMAH Rules under Factories Act and Rules, 10 to 13 under Manufacture, Storage and Import of Hazardous Chemicals Rules, 1989 as amended in 2000, under Environment (Protection) Act, 1986 the occupier of the industry using hazardous chemicals in its manufacturing activity is obliged to submit report on Hazard Identification and Risk Assessment to the authorities towards an objective evaluation of safety related to industrial activity and measures taken and to identify what further measures are required to operate the plant in a safe manner.

Hazard Identification and Risk Assessment involves collection of all relevant information on a object, quantifying as much of it as is reasonably practicable in terms of its benefits and deficiencies and making this information available to the decision-maker. It includes the identification and quantification of the various hazards (unsafe conditions) that exist in the factory. On the other hand, risk analysis deals with the identification and quantification of risks; the plant equipment and personnel are exposed to, due to accidents resulting from the hazard present in the factory. Objective of the risk assessment as follows,

- Understand and analyze the maximum credible accident scenarios.
- Design the system for controlling and containing the frequency and consequences of significant effects of emergencies and to prepare disaster management plan.

### **3. METHODOLOGY FOR RISK ASSESSMENT**

- Collection of information with respect to facility, process and hazardous chemicals.
- Collection and analysis of meteorological data of the region
- Identification of the hazardous chemicals as per MSIHC amendment rules.
- Identification of the hazard associated with each chemical, process and operations
- Identification of release type and determine release rate.
- Consequence analysis using ALOHA (Area Locations of Hazardous Atmospheres)

### **4. IDENTIFICATION OF HAZARDS**

- Hazard identification is the most critical step in the risk assessment. This is because to identify the hazards, experience, detailed process knowledge, engineering codes, checklist, HAZOPs etc is required.
- Hazard identification is carried out to ascertain the controls required and available in order to mitigate the risk of exposure to the hazards. This would substantially help in overcoming costly errors and prolonged delays that may be caused due to the design changes that may be required on a later date.
- Hazard assessment is carried out at the equipment design stage and the control / mitigation measures are put in place overcome them to avoid costly errors at a later stage.
- Hazard assessment in our plant is carried out examining the, material storage, type of operations, locations to find out the facilities in place to overcome the risks of exposure to the hazards.
- After a critical analysis of the chemicals used, stored, defined safe operating procedures and the different manufacturing processes, the following table lists the safety measures / installations in place and mitigation measures to overcome the hazards.

Following are the Hazards identified in proposed project activities:

- Fire Hazards

- Spillage of Hazardous chemicals which leads to Air pollution
- Explosion Hazards
- Toxic gas release
- Noise

**TABLE: 1 AREA WISE IDENTIFIED HAZARDS, PRECAUTIONS TAKEN WITH MITIGATION MEASURES.**

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
1]	RM Storage area	Spillage of chemicals	Low to medium 2 persons	<ol style="list-style-type: none"> <li>1. Approved layout as per legal requirements.</li> <li>2. Flame proof electrical fittings installed</li> <li>3. Chemicals stored in safe Containers with secondary containment to prevent spillages.</li> <li>4. Storage quantity is limited</li> <li>5. Storage area is well ventilated by a forced air ventilation system.</li> <li>6. Material accessed only by authorized personnel using mechanized systems</li> <li>7. Double door entry to ensure a clean atmosphere.</li> <li>8. Body showers provided for decontamination.</li> </ol>	<ol style="list-style-type: none"> <li>1. Area will be cordoned off.</li> <li>2. Information will be passed to Emergency control center is informed.</li> <li>3. Information will be given to the declarer of emergency on the scale of Leakage.</li> <li>4. Emergency Response teams will be kept on alert for swift response.</li> <li>5. All hot works being carried out in the surrounding areas will be stopped</li> <li>6. Personnel working in the area will be evacuated.</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
				<p>9. Personnel are provided with full body protection suits and nose masks to prevent exposure to chemicals.</p> <p>10. Fire hydrant system with hydrant points with hose reels and nozzles installed to mitigate fire hazards</p> <p>11. Fire extinguishers deployed adequately</p> <p>12. Fully fledged medical center / arrangements</p> <p>13. Periodical occupational health checks to personnel working in the area to assess health effects, if any.</p>	<p>7. Spilled powders will be collected in vacuum cleaners.</p> <p>8. The spillage will be cleared and the area is made fit work</p>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
2]	Chemical Tanks Storage area	Fire & Explosion	Medium to Low 2 persons	<ol style="list-style-type: none"> <li>1. Storage facility located in isolated area</li> <li>2. Natural ventilation for supply of fresh air</li> <li>3. No electrical fittings in the area to prevent any fire hazard.</li> <li>4. No electrical gadgets or items capable of generating static electric charges permitted inside the area.</li> <li>5. Personnel are trained about Do's &amp; Don'ts during emergency. authorized personnel only</li> <li>6. No heat sources are permitted near the facility.</li> <li>7. Hot work is controlled through a work permit system</li> <li>8. Room kept under lock and key with access to authorized personnel only.</li> </ol>	<ol style="list-style-type: none"> <li>1. Area will be cordoned off.</li> <li>2. Hot work being carried out in the vicinity will be stopped to prevent accidental spread of fire.</li> <li>3. Personnel working in the area will be evacuated</li> <li>4. Emergency control center will be informed</li> <li>5. Information will be given to the declarer of emergency on the scale of Fire &amp; Explosion.</li> <li>6. Emergency Response teams will be kept on alert for swift response.</li> <li>7. The spillage will be cleared and the area is made fit work</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
				<p>9. Storage quantity is limited and material is handled by trained and authorized personnel.</p> <p>10. Mechanical foam type fire is provided to mitigate fires</p> <p>11. Fire hydrant system with hose reels are provided in the vicinity</p>	

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
3]	Production Block	Spillages / Fire /Explosion	Low to medium 15 persons	<ol style="list-style-type: none"> <li>1.Flame proof electrical fittings installed</li> <li>2. Freight lift installed for movement of material</li> <li>3. Material stored at production blocks in safe containers for batch charging with secondary containment to prevent Spillages.</li> <li>4. Earthing and bonding carried out for all reactor vessels and pipelines</li> <li>5.Nitrogen lines are provided to reaction vessel to create inert atmosphere inside the reactor to avoid fire and explosion</li> <li>6. Work permit system implemented for hazard assessment in case of any hot work / height work</li> <li>7. Work permit system implemented for hazard assessment in case of any hot work / height work.</li> </ol>	<ol style="list-style-type: none"> <li>1. Area will be cordoned off.</li> <li>2. Power supply will be cut off to the area to prevent accidental fire.</li> <li>3. All hot work carried out in the vicinity will be stopped.</li> <li>4. Emergency control center will be informed.</li> <li>5. Information will be given to the declarer of emergency on the scale of Leakage / Accident.</li> <li>6. Emergency Response teams will be kept on alert for swift response.</li> <li>7. Personnel working in the area will be evacuated.</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
				<p>8. Manufacturing area is ventilated by a forced air ventilation system.</p> <p>9. Fire hydrant system with hydrant points with hose reels and nozzles installed to mitigate fire hazards</p> <p>10. Fire extinguishers deployed adequately</p> <p>11. Emergency exit glass door with glass breaking hammer provided for safe escape in case of any emergencies.</p> <p>12. Eye wash fountain / Body shower provided for decontamination.</p>	

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
4]	Boiler House	Fire / Explosion	Low to medium Approx. 2	<ol style="list-style-type: none"> <li>1. All requirements specified under Boiler Act and Boiler licensed is adhered to.</li> <li>2. All electrical fittings are of flameproof type.</li> <li>3. Entry restricted only to trained and authorized personnel to work in the area.</li> <li>4. Fire extinguishers are positioned at different locations in case of any emergencies.</li> <li>5. No material storage is permitted in the area.</li> </ol>	<ol style="list-style-type: none"> <li>1. Shutting down the plant, declaring the emergency.</li> <li>2. Electrical supply will be isolated.</li> <li>3. Type of emergency will be informed to the emergency declarer/ central authority.</li> <li>4. Emergency response teams will be kept on alert for swift action.</li> <li>5. Movement of personnel and vehicles will prohibited.</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
				<p>6. Area is well ventilated and illuminated for safe working.</p> <p>7. 24 x 7 manning of the area for monitoring the operation.</p> <p>8. All maintenance /repair works are carried out after issuing work permits and under constant supervision of experts.</p> <p>9. Periodical cleaning of soot in furnace to prevent formation of explosive mixtures.</p> <p>10. Monitoring the boiler operational parameters and periodical cleaning</p> <p>11. Checking of boiler internals to prevent accidents.</p> <p>12. Sign boards are displayed to inform personnel about the hazards present in the area</p>	<p>6. Area is well ventilated and illuminated for safe working.</p> <p>7. 24 x 7 manning of the area for monitoring the operation.</p>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
5]	Diesel Generator	Noise & Fire	Two	<ol style="list-style-type: none"> <li>1. Noise abatement thru' modular acoustic paneling of D.G sets</li> <li>2. Secondary containment to prevent Diesel leakage from day tanks.</li> <li>3. Adequate no. of fire extinguishers is kept to handle emergency</li> <li>4. Entry access to the area controlled</li> </ol>	<ol style="list-style-type: none"> <li>1. Information will be given to Emergency control center.</li> <li>2. Power supply will be cut off to the storage area to prevent accidental fire.</li> <li>3. All hot work around the area will be stopped and the area will be cordoned off</li> <li>4. The concerned maintenance personnel will be carried repairs to mitigate the leakages.</li> <li>5. Emergency Response Team will be kept on alert for swift response.</li> <li>6. Periodical occupational health checks to personnel working in the area to assess exposure to noise.</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
6]	Electrical sub stations	Electric shock / fire	2 persons	<ol style="list-style-type: none"> <li>1. Layout confirm to legal requirements specified under Indian Electrical Rules.</li> <li>2. Entry restricted to licensed and authorized personnel only.</li> <li>3. Earthing provided for leakage of stray currents.</li> <li>4. Electronic mimic panels installed for fault indication at the entry of the sub-station.</li> <li>5. Insulating rubber mats conforming to IS 15652:2006 provided in front of all electrical switchgear.</li> <li>6. Periodical inspection and maintenance carried out to ensure good health of the equipment.</li> <li>7. CO2 / DCP fire extinguishers deployed to handle emergency fires</li> </ol>	<ol style="list-style-type: none"> <li>1. Information will be given to Emergency control center.</li> <li>2. Power supply will be cut off from incoming source.</li> <li>3. Electricity supply company is alerted for cut off power supply in case of major risks</li> <li>4. All hot work around the area will be stopped and the area is cordoned off.</li> <li>5. The concerned maintenance personnel will be carried repairs to restore normalcy.</li> <li>6. Emergency Response Team will be kept on alert for swift response</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
7]	Hazardous waste storage room	Fire	Low to medium 2 persons / Unmanned	<ol style="list-style-type: none"> <li>1. Storage shed in an isolated location.</li> <li>2. Conditions specified in hazardous waste authorization issued by SPCB implemented.</li> <li>3. Compatible wastes are stored in separate enclosures.</li> <li>4. Layout provides adequate ventilation and illumination</li> <li>5. Secondary containment provided to prevent leakages / spillages.</li> <li>6. Storage quantity is limited.</li> <li>7. Periodical disposal of accumulated waste to Authorized landfills.</li> <li>8. Flame proof electrical fittings installed to prevent fire / explosion hazards</li> </ol>	<ol style="list-style-type: none"> <li>1. Information will be given to Emergency control center.</li> <li>2. Power supply will be cut off from incoming source.</li> <li>3. All hot work around the area is stopped and the area is cordoned off.</li> <li>4. The concerned maintenance personnel will be carried repairs to restore normalcy</li> </ol>

S.NO	AREA	IDENTIFIED HAZARD	SEVERITY & NO. OF PERSONS EXPOSED	PRECAUTIONS TAKEN	MITIGATION MEASURES
				<p>9. Eye wash / body shower is provided for decontamination in case of spillage on body parts.</p> <p>10. PPE box is equipped with gum boots, splash proof safety goggles, aprons for use during handling of chemicals.</p> <p>11. Access to the area restricted to authorize personnel only.</p> <p>12. Fire hydrant point with hose reels provided for fire mitigation</p>	<p>5. Emergency Response Team will be kept on alert for swift response.</p> <p>6. Support of external agencies will be sought in case situation poses major risks and is not controllable by in-house infrastructure</p>

**TABLE:2 LIST OF SOLVENTS**

<b>S.N O</b>	<b>NAME OF THE SOLVENT</b>	<b>PHYSICAL STATE</b>	<b>MODE OF STORAGE</b>	<b>MAX. INVENTORY IN KL.</b>	<b>NATURE OF HAZARD</b>	<b>NFPA RATING</b>
1.	Methanol	Liquid	Tank	25	Flammable	H: 1 F: 3 R: 0
2.	MDC	Liquid	Tank	25	Harmful	H: 2 F: 1 R: 0
3.	Ethyl Acetate	Liquid	Tank	25	Flammable	H: 1 F: 3 R: 0
4.	Toluene	Liquid	Tank	20	Flammable	H: 2 F: 3 R: 0
5.	THF	Liquid	Tank	20	Flammable	H: 2 F: 3 R: 1
6.	Ethanol	Liquid	Tank	20	Flammable	H: 3 F: 2 R: 0
7.	Acetone	Liquid	Drums	15	Flammable	H: 1 F: 3 R: 0
8.	Hexane	Liquid	Drums	15	Flammable	H: 2 F: 3 R: 0

#### **a. HANDLING PRECAUTIONS**

- Use in a closed system under argon or nitrogen.
- Do not get in eyes, on skin or clothing.
- Do not breathe vapors or mist.
- Store in a cool place. Keep container closed.
- Keep away from sources of ignition, water, air, acids and oxidizing agents
- In case of fire, do not use water or carbon dioxide

#### **5. EMERGENCY PREPAREDNESS**

- On Site Emergency Plan
- Training & Awareness

#### **6. SAFE PRACTICES [HANDLING, STORAGE, TRANSPORTATION AND UNLOADING OF CHEMICALS]**

##### **Drums**

Liquid Raw materials will be transferred from the drums to the day tank situated at the production block with the help of leak proof drum pumps / pumps / Vacuum through pipe lines from day tank to reaction vessel unloading by gravity.

##### **6.1 Storage Tanks**

Solvent will be transferred to the day tank situated at the production block with the help of mechanical seal pump through pipe lines from the tank, from day tank to reaction vessel unloading by gravity.

Tank is connected to chilled water circulated condenser with reflux system.

##### **6.2 Measures to Avoid Evaporation**

- Keep containers tightly closed.
- Keep away from heat, spark & flame
- Keep away from sources of ignition
- Store in a cool, dry, well-ventilated area away from incompatible substances.

##### **6.3 Safety Systems**

- Designated areas with proper indication & safety signs.
- Double earthing systems

- Flame arrestor to the vent
- Flame proof transferring pumps
- Handling precautions/SOP protocol
- Pressure Gauges
- Level indicators
- Flame proof lighting to storage yard

#### **6.4 TRANSPORTATION / UNLOADING**

Highly inflammable chemicals will be transported by road. Therefore, adequate safety precautions for transportation are followed. During transportation of hazardous chemicals, MSDS & TREM card will be provided to driver. As per Motor Vehicle Rules, PESO rules and Factory Rules all safety precautions will be followed during transportation of hazardous chemicals.

The following safety precautions are suggested during transportation of toxic, inflammable and corrosive chemicals in tankers, while loading and unloading, transportation and meeting the emergencies arising out of leakages and spillages of hazardous materials:

- Park the vehicle at designated place.
- Stop the engine.
- Check-up spark arrester.
- Provide earthing to tanker securely.
- Ensure that fireman is available near the place with proper equipment's.
- Connect the piping properly
- Before start unloading, check that, there should not be any leakage.
- In case of leakage, immediately attend the leakages & rectify it.
- After unloading is over, close the lid properly.
- Vehicle to be started only after removal of all pipelines connected with tanker.

#### **6.5 SAFETY INSTRUCTIONS FOR TRANSPORTATION OF HAZARDOUS MATERIALS**

- The name of the chemical along with pictorial sign denoting the dangerous goods should be marked on the vehicle and the packing material.
- The name of the transporter, his address and telephone number should be clearly written on the road tanker and on the vehicle.
- The tanker or vehicle should not be used to transport any material other than what is

written on it.

- Only trained drivers and cleaners should transport hazardous chemicals.
- The transporter and the manufacturer must ensure the safe transportation of the material.
- The Tanker / Vehicle should be checked for its fitness and safe condition before loading.
- During loading and unloading, the tanker/vehicle should be braked and isolated against any movement, while loading/unloading, use safety appliances.
- The tanker / vehicle should not be overloaded beyond the weight permitted by R.T.O.
- Check for leakages from the line connections / containers before starting and Stopping the filling operations.
- Drive the vehicles carefully, especially in crowded localities and on Bumpy roads.
- Do not apply sudden break.
- The tanker / vehicle should not be parked for long time on the way and especially in crowded places. Park the vehicle away from residential areas

## **6.6 SPILL CONTROL**

- For all plants spill control procedures will be displayed. Spillage shall be controlled as per concerned spill control procedure.
- Unprotected personnel up wind will be kept upwind.
- Like any spilled materials to contain. Absorb spilled liquid by dry absorbent clay or vermiculite.
- Collect most of the contaminated absorbent with shovel for further disposal/incineration.
- If spill of material directly on the ground, dig up and remove saturated soil for disposal/incineration.
- Inactivate poisonous chemical with suitable method.

## **7. EFFECT AND CONSEQUENCE ANALYSIS**

- In a plant handling hazardous chemicals, the main hard due to storage, handling and use of these chemicals. If these chemicals are released into the atmosphere, they may cause damage due to resulting fires or vapor clouds last over pressures depend upon the reactivity class of material between two explosive limits.

### **7.1 OPERATING PARAMETERS**

- Potential vapor release for the same material depends significantly on the operating conditions especially for any liquefied gas, operating conditions are very critical to assess the damage potential.
- If we take up an example of ammonia, if it is stored at ambient temperature say 30°C, and then the vapor release potential of the inventory is much higher as compared to the case if it is stored at 0°C.

## 7.2 INVENTORY

- Inventory analysis is commonly used in understanding the relative hazards and short listing of release scenarios.
- Inventory plays an important role in regard to the potential hazard.
- Larger the inventory of a vessel or a system, larger the quantity of potential release.
- The potential vapor release [source strength] depends upon the quantity of liquid release, the properties of the materials and the operating conditions [pressure, temperature].
- If all these influencing parameters are combined into a matrix and vapor source strength estimated for each release case, a ranking should become a credible exercise.

## 7.3 LOSS OF CONTAINMENT

- Plant inventory can get discharged to environment due to Loss of Containment.
- Certain features of materials to be handled at the plant need to be clearly understood to firstly list out all significant release cases and then to short list release scenarios for a detailed examination.
- Liquid release can be either instantaneous or continuous.
- Failure of a vessel leading to an instantaneous outflow assumes the sudden appearance of such a major crack that practically all of the contents above the crack shall be released in a very short time.
- The more likely event is the case of liquid release from a hole in a pipe connected to the vessel. The flow rate will depend on the size of the hole as well as on the pressure, which was present, in front of the hole, prior to the accident. Such pressure is basically dependent on the pressure in the vessel.
- The vaporization of released liquid depends on the vapor pressure and weather conditions. Such consideration and others have been kept in mind both during the initial listing as well as during the short listing procedure.

In the study, Maximum credible loss accident methodology is to be used, therefore, the largest potential hazard inventories have been considered for consequence estimation.

#### **7.4 Damage Criteria**

In consequence analysis, use is made of a number of calculation models to estimate the physical effects of an accident [spill of hazardous material] and to predict the damage [lethality, injury, material destruction] of the effects. The calculations can roughly be divided in three major groups.

- Determination of the source strength parameters;
- Determination of the consequential effects;
- Determination of the damage or damage distances.

The basic physical effect models consist of the following.

#### **7.5 Source strength parameters**

- Calculation of the outflow of liquid, vapor or gas out of a vessel or a pipe, in case of rupture. Also two-phase outflow can be calculated.
- Calculation, in case of liquid outflow, of the instantaneous flash evaporation and of the dimensions of the remaining liquid pool.
- Calculation of the evaporation rate, as a function of volatility of the material, pool dimensions and wind velocity.
- Source strength equals pump capacities, etc. in some cases.

#### **7.6 Consequential effects**

- Dispersion of gaseous material in the atmosphere as a function of source strength, relative density of the gas, weather conditions and topographical situation of the surrounding area.
- Intensity of heat radiation [in KW / m<sup>2</sup>] due to a fire or a BLEVE, as a function of the distance to the source.
- Energy of vapor cloud explosions [in KW / m<sup>2</sup>], as a function of the distance to the distance of the exploding cloud.
- Concentration of gaseous material in the atmosphere, due to the dispersion of evaporated chemical. The latter can be either explosive or toxic.
- It may be obvious, that the types of models that must be used in a specific risk study strongly depend upon the type of material involved:
- Gas, vapor, liquid, solid

- Inflammable, explosive, toxic, toxic combustion products
- Stored at high/low temperatures or pressure
- Controlled outflow (pump capacity) or catastrophic failure?

### 7.7 Selection of Damage Criteria

- The damage criteria give the relation between extent of the physical effects (exposure) and the percentage of the people that will be killed or injured due to those effects
- The knowledge about these relations depends strongly on the exposure. For instance, much more is known about the damage caused by host radiation, than about the damage due to toxic exposure, and for these toxic effects, the knowledge differs strongly between different materials.

In consequence analysis studies, in principle three types of exposure to hazardous effects are distinguished:

- Heat radiation, from a jet, pool fire, a flash fire or a BLEVE.
- Explosion
- Toxic effect, from toxic materials or toxic combustion products.

### 7.8 Heat Radiation

The consequence caused by exposure to heat radiation is a function of:

- The radiation energy onto the human body [KW /M<sup>2</sup>]
- The exposure duration[sec]
- The protection of the skin tissue [clothed or naked body]

The limits for 1% of the exposed people to be killed due to heat radiation, and for second-degree burns are given in below:

**TABLE:3 DAMAGES TO HUMAN LIFE DUE TO HEAT RADIATION**

EXPOSURE DURATION	RADIATION FOR 1% LETHALITY (KW/M <sup>2</sup> )	RADIATION FOR 2 <sup>ND</sup> DEGREE BURNS (KW/M <sup>2</sup> )	RADIATION FOR FIRST DEGREE BURNS, (KW/M <sup>2</sup> )
10 sec	21.2	16	12.5
30 sec	9.3	7.0	4.0

Since in practical situations, only the own employees will be exposed to heat radiation in case of a fire, it is reasonable to assume the protection by clothing. It can be assumed that people would be able to find a cover or a shield against thermal radiation in 10 sec. time.

Furthermore, 100% lethality may be assumed for all people suffering from direct contact with flames, such as the pool fire, a flash fire or a jet flame. The effects due to relatively lesser incident radiation intensity are given in below.

**TABLE:4 EFFECTS DUE TO INCIDENT RADIATION INTENSITY**

INCIDENT RADIATION KW/M <sup>2</sup>	TYPE OF DAMAGE
0.7	Equivalent to solar radiation
1.6	No discomfort for long exposure
4.0	Sufficient to cause pain within 20 sec. blistering of skin (first degree burns are likely)
9.5	Pain threshold reached after 8 sec. second degree burns after 20 sec.
12.5	Minimum energy required for piloted ignition of wood, melting plastic tubing etc.

### 7.8 Explosion

In case of vapor cloud explosion, two physical effects may occur:

- A flash fire over the whole length of the explosive gas cloud;
- A blast wave, with typical peak overpressures circular around ignition source.

As explained above, 100% lethality is assumed for all people who are present within the cloud proper.

For the blast wave, the lethality criterion is based on:

- A peak over pressure of 0.1 bars will cause serious damage to 10% of the housing/structures.
- Falling fragments will kill one of each eight persons in the destroyed buildings.

The following damage criteria may be distinguished with respect to the peak overpressures resulting from a blast wave:

**TABLE:5 DAMAGE DUE TO OVERPRESSURES**

<b>PEAK OVERPRESSURE</b>	<b>DAMAGE TYPE</b>
0.83 bar	Total destruction
0.30 bar	Heavy damage
0.10 bar	Moderate damage
0.03 bar	Significant damage
0.01 bar	Minor damage

From this it may be concluded that  $p=0.17 \text{ E}+5 \text{ pa}$  corresponds approximately with 1% lethality. Furthermore it is assumed that everyone inside an area in which the peak overpressure is greater than  $0.17 \text{ E}+ 5 \text{ pas}$  will be wounded by mechanical damage. For the gas cloud explosion this will be inside a circle with the ignition source as its center.

## **8. INCIDENTS IMPACT**

The identified failure scenarios in plant have been analyzed for the impact zones considering damage due to thermal, explosive and toxic impacts. Each incident will have Impact on the surrounding environment which in extreme case may cross plant boundary.

### **8.1 MAXIMUM CREDIBLE LOSS ACCIDENT SCENARIOS**

A Maximum Credible Accident (MCA) can be characterized as the worst credible accident. In other words: an accident in an activity, resulting in the maximum consequence distance that is still believed to be possible. A MCA-analysis does not include a quantification of the probability of occurrence of the accident. Another aspect, in which the pessimistic approach of MCA studies appears, is the atmospheric condition that is used for dispersion calculations. The Maximum Credible Loss (MCL) scenarios have been developed for the Facility. The MCL cases considered, attempt to include the worst "Credible" incidents-what constitutes a credible incident is always subjective. Nevertheless, guidelines have evolved over the years and based on basic engineering judgment, the cases have been found to be credible and modeling for assessing vulnerability zones is prepared accordingly.

The objective of the study is Emergency planning, hence only holistic & conservative assumptions are used for obvious reasons. Hence, though the outcomes may look pessimistic, the planning for emergency concept should be borne in mind whilst interpreting the results.

In Consequence analysis, geographical location of the source of potential release plays an

important role. Consideration of a large number of scenarios in the same geographical location serves little purpose if the dominant scenario has been identified and duly considered.

The Consequence Analysis has been done for selected scenarios by ALOHA [version 5.4.1.] of EPA. The details of software used for MCA analysis are described below.

- A computer based version ALOHA 5.4.1.2 is used to calculate toxic and explosive effect of the accidental release of liquid chemicals within the plant area.
- ALOHA (Areal Locations of Hazardous Atmosphere) is a computer program designed especially for use by people responding to chemical release as well as for emergency planning and training.
- ALOHA was jointly developed by the National Oceanic and Atmospheric Administration (NOAA) and the Environment Protection Agency[EPA]
- The mathematical model is based on the Emergency Response Planning Guidelines (ERPGs) which gives Toxic Levels of Concern (LOCs) to predict the area where a toxic liquid concentration might be high enough to harm people.
- ALOHA models key hazards-toxicity, flammability, thermal radiation (Heat), and over pressure (expansion blast force)-related to chemical releases that result in toxic gas dispersion, fire and/or explosion
- 

## 8.2 CONSEQUENCE ANALYSIS

From the list mentioned below, all the Solvents are considered and have been taken for the consequences analysis considering their hazardous nature, Storage conditions and threshold values, other properties.

**TABLE:6 LIST OF SOLVENTS WITH STORAGE CAPACITY**

Sl. No.	Solvent Name	Maximum storage (KL)	Physical status	Storage	Storage pressure & temp
1	Methanol	25	Liquid	Tanks	Ambient
2	MDC	25	Liquid	Tanks	Ambient
3	Ethyl Acetate	25	Liquid	Tanks	Ambient
4	Toluene	20	Liquid	Tanks	Ambient
5	THF	20	Liquid	Tanks	Ambient
6	Ethanol	20	Liquid	Tanks	Ambient
7	Acetone	15	Liquid	Drums	Ambient
8	Hexane	15	Liquid	Drums	Ambient

## **SITE DATA**

Location: **KADECHUR**

## **CHEMICAL DATA:**

- Chemical Name: METHANOL
- CAS Number: 67-56-1
- Molecular Weight: 32.04 g/mol
- AEGL-1 (60 min): 530 ppm
- AEGL-2 (60 min): 2100 ppm
- AEGL-3 (60 min): 7200 ppm
- IDLH: 6000 ppm
- LEL: 71800 ppm
- UEL: 365000 ppm
- Ambient Boiling Point: 63.4° C
- Vapor Pressure at Ambient Temperature: 0.23 atm
- Ambient Saturation Concentration: 235,756 ppm or 23.6%

## **ATMOSPHERIC DATA: (MANUAL INPUT OF DATA)**

- Wind: 4.5 meters/second from SW at 3 meters
- Ground Roughness: open country
- Cloud Cover: 5 tenths
- Air Temperature: 31° C
- Stability Class: D
- No Inversion Height
- Relative Humidity: 50%

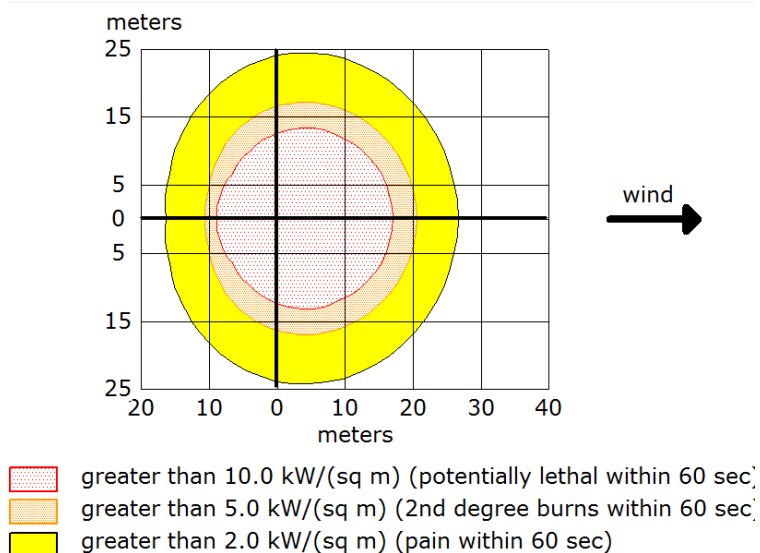
## **SOURCE STRENGTH**

- Leak from hole in horizontal cylindrical tank
- Flammable chemical is burning as it escapes from tank
- Tank Diameter: 3 meters      Tank Length: 5 meters
- Tank Volume: 35.3 cubic meters
- Tank contains liquid      Internal Temperature: 31° C
- Chemical Mass in Tank: 20000 kilograms

- Tank is 72% full
- Circular Opening Diameter: 3 inches
- Opening is 0.3 meters from tank bottom
- Max Flame Length: 8 meters
- Burn Duration: ALOHA limited the duration to 1 hour
- Max Burn Rate: 210 kilograms/min
- Total Amount Burned: 11,838 kilograms
- Note: The chemical escaped as a liquid and formed a burning puddle.
- The puddle spread to a diameter of 16.3 meters.

### THREAT ZONE:

- Threat Modeled: Thermal radiation from pool fire
- Red : 17 meters --- (10.0 kW/(sq m) = potentially lethal within 60 sec)
- Orange: 21 meters --- (5.0 kW/(sq m) = 2nd degree burns within 60 sec)
- Yellow: 27 meters --- (2.0 kW/(sq m) = pain within 60 sec)



### Common Hazards

- Physical such as ventilation, poor illumination, noise, extreme temperature, humidity and radiation.
- Biological such as variety of pathogenic bacteria and parasites.
- Chemical due to hazardous gases and dusts.
- Ergonomic.

## 9. Industrial Hygiene Monitoring

- Industrial hygiene monitoring is to be located and identify source of exposure in the workplace so that they can be corrected and to quantify the exposure of employees to chemicals in the air.

## 10. Occupational Health Monitoring System

### Air samples

Locations of samples – air samples are generally collected in one or three locations:

- At the breathing zone of the worker [Personal sample]
- In the general room air [Areas ample]
- At the operation which is generating the hazardous substance [Area sample]

Lengths of samples – Air samples are generally collected for two lengths of time.

- Grab samples [instantaneous] measure conditions at one moment in time and can be likened to a still photograph. They give only a picture of conditions at one place at one instant in time.
- Continuous Samples [range from twenty minutes to 8 – 10 Hours].These is used to evaluate all day exposure by a series of continuous samples. Continuous samples may be thought of as like a motion picture since they record activity taking place in various places over a period of time. They provide an average of conditions over a period samples.

### Other sampling methods

#### Bulk samples

Bulk samples will be collected from settled dust in the work place or from drums or bags of chemicals. Their purpose is to analyze and identify the substances present. For example, bulk samples are used to analyze the percent of asbestos in insulation or dust. Usually, a substance which is greater than one percent of bulk sample is considered a concern.

#### Wipe Samples

Wipe samples will be used when skin absorption or ingestion is a suspected rote of exposure. The purpose is to show whether skin, respirators, clothing, lunch rooms, lockers, etc. are contaminated.

It can show which surfaces are clean and which are contaminated. It can also show if some

surfaces are more contaminated than others.

### **Sampling Devices**

The general principle of sampling is to collect an amount of a contaminant onto a medium from a known quantity of air.

Air samples will be collected using small pumps to suck air from the workroom. The pump is attached by tubing to a sampling device which contains the sampling medium; for example a glass tube containing charcoal.

The sampling method will be used depends on the physical form of the substance:

- **DUSTS** -The sampling device is a filter of plastic or paper in sholder:
- **VAPORS** -The sampling device is a glass tube containing activated charcoal as a medium.
- **GASES** -The sampling device is a bubbler containing a fluid medium to dissolved or react with the gas

The collected samples will be sent to a laboratory where the amount of the substance on the sampling medium [filter, tube, etc.] is measured.

In some cases air monitoring will be conducted by using direct reading instrument such as a monitoring for carbon monoxide these instruments can measure the amount of a contaminant in the air immediately without being sent to a laboratory.

- **PELs** [Permissible Exposure Limits] - these are legal limits which have been established by OSHA.
- Recommended PELs - also reference to as **RELs** [Recommended Exposure Limits] often these values are based on more recent scientific information than the legal PELs enforced by OSHA.
- **TLVs** [Threshold Limit Values] - These are exposure limits put out by a nongovernmental group, the **ACGIH** [American Conference of Governmental Industrial Hygienists]. Many of these were adopted as legal requirements.
- Revised **TLVs** are often based on the most recent and accurate scientific information.
- Permissible Exposure Limits by **OSHA** [Occupational Safety and Health Administration] when it started back in 1970.
- **IDLH** [Immediate Dangerous to Life or Health] limits are prescribed by **NIOSH** [National Institute of Occupational Safety and Health]

**11. CHEMICAL EXPOSURE LIMITS & EMP FOR THE OCCUPATIONAL SAFETY & HEALTH HAZARDS**

**TABLE:6 CHEMICAL EXPOSURE LIMITS**

S. No	SOLVENT NAME	Exposure Standards		
		ACGIH [TLV]	OSHA [PEL]	NIOSH [IDLH]
1	Acetone	500	750	2500
2	Tetrahydrofuran	50	200	2000
3	Ethanol	1000	1000	1000
4	Methylene Dichloride	500	500	500
5	Ethyl Acetate	250	250	2000
6	Methanol	200	200	6000
7	Hexane	50	50	5000
8	Toluene	50	100	500

**Notes:**

- All the above Values are in **ppm**
- PPE Means Personal Protective Equipment like Helmets, Safety Goggles, Breathing apparatus, Nose Masks, Gloves, Gum Shoes etc.,

**NOTE:** Medical testing reports of the Employees will be available at the time of industry in operation

**EMP for the Occupational Safety & Health Hazards** so that such exposure can be kept within permissible exposure level (PEL) / Threshold Level value (TLV) so as to protect health of workers.

1. It is proposed to formulate and implement an EMP for Occupational Safety and Health with following aim
  - To keep air-borne concentration of toxic (if available) and hazardous chemicals below PEL and TLV.
  - Protect general health of workers likely to be exposed to such chemicals
  - Providing training, guidelines, resources and facilities to concerned department for occupational health hazards
  - Permanent changes to workplace procedures or work location to be done if it is found necessary on the basis of findings from workplace Monitoring Plan.
2. It is proposed that this EMP be formulated on the guidelines issued by Bureau of Indian

Standards on OH&S Management Systems: IS 18001:2000 Occupational Health and Safety Management Systems.

3. Proposed EMP will be incorporated in Standard Operating Procedure also
4. The proposed EMP will also include measure to keep air-borne concentration of toxic and hazardous chemicals below its PEL and TLV, like...
  - Leak Surveys
  - Separate storage for toxic chemicals
  - Exhaust Ventilation
  - Proper illumination
  - On-line detectors toxic chemical like Anhydrous Ammonia
  - Close processes to avoid spills and exposures
  - Atomization of process operations to hazards of manual handling of chemicals
  - Supply of proper PPEs like Air mask, Berating canisters, SCBA sets, On-line breathing apparatus at the places where there is possibility of presence of toxic chemicals
  - Decontamination procedure for empty drums and carboys.
  - Regular maintenance program for pumps, equipment, instruments handling toxic and corrosive chemicals
  - Display of warning boards
  - Training to persons handling toxic and corrosive chemicals

#### **Workplace Monitoring Plan**

- It is proposed that a Workplace Monitoring Plan to be prepared & implemented accordingly.
- Each workplace must be evaluated to identify potential hazards from toxic substances or harmful physical agents. Air-borne concentration of toxic chemicals will be measured and records will be kept.
- The current state-of-the-art exposure measurement model is as follows: For purposes of measuring worker exposure across a single shift it is sufficient to place a reasonably accurate exposure measuring device near the worker's area, within the worker's breathing zone, and have it operate for nearly the full shift. Client has been proposed to study the exposure data when the plant is operative.

## **Health Evaluation of Workers**

- It is proposed that management will devise a plan to check and evaluate the exposure specific health status evaluation of workers.
- Workers will be checked for physical fitness with special reference to the possible health hazards likely to be present, where he/she is being expected to work before being employed for that purpose. Basic examinations like
  1. Liver Function tests,
  2. Chest X-ray,
  3. Audiometry,
  4. Spirometer Vision testing (Far & Near vision, color vision and Any other ocular defect)
  5. ECG, etc. will be carried out.

However, the parameters and frequency of such examination will be decided in consultation with Factory Medical Officer.

- While in work, all the workers will be periodically examined for the health with specific reference to the hazards which they are likely to be exposed to during work. Health evaluation will be carried out considering the bodily functions likely to be affected during work. The parameters and frequency of such examination will be decided in consultation with Factory Medical Officer. Plan of monthly and yearly report of the health status of workers with special reference to Occupational Health and Safety, will be maintained.

## **12. TREATMENT OF WORKERS AFFECTED BY ACCIDENTAL SPILLAGE OF CHEMICALS**

Interim First Aid is essential in many injuries while injured waits for trained personnel to arrive.

### **12.1 BLEEDING**

- Apply direct pressure on the wound with a clean dressing.
- If bleeding continues and you do not suspect a fracture, elevate the wound above the victim's heart and continue to apply direct pressure.
- If bleeding continues, apply pressure at a pressure point.
- Maintain body temperature.
- Do not use a tourniquet unless this is a serious amputation.

## **12.2 BREATHING PROBLEMS**

- Move victim to fresh air if smoke or dangerous gases are present.
- Otherwise, do not move victim.
- If victim loses consciousness, call doctor
- Never enter into a room with toxic gases released -call without protection

## **12.3 UNCONSCIOUS VICTIM**

- Move victim to fresh air if smoke or dangerous gases exist.
- Begin rescue breathing- is First Aid trained ahead of time! Instead.
- Never enter into a room with toxic gases released- call without protection

## **12.4 CHEMICAL BURNS**

- Have victim remain under a safety shower or flush skin with an available water source for 15-30 minutes.
- Remove all contaminated clothing and jewelry.
- Cover burns with dry, loose dressings.
- Wash all clothing thoroughly before wearing it again.

## **12.5 ACID BURNS**

- In case of acid burn, the operator should with all possible speed get under a safety shower and use the full flow of water - the more water the better. A small amount of water will incase severity of the burn Water should be used until all traces of acid have been washed from the burn. Alkaline solutions are not needed; if used at all they should be used only after all acid has been washed from the burn, it may to treat in the same manner as a heat burn.

## **12.6 CHEMICAL INGESTIONS**

- Never enter into a room with toxic gases released without protection
- Do not give victim any food or liquids without specific advice from physician.

## **12.7 EYE INJURIES FROM CHEMICALS**

- Get victim to a safety shower or eye wash immediately.
- Never enter into a room with toxic gases released- call without protection
- Flush eye for 15-30 minutes with both lids held open. Keep the injured eye lower than

the uninjured eye.

- Keep the eyelids open hold fingers at top and bottom of the eyeball. Wrap a bandage loosely around both eyes.

### **13. SAFE OPERATING PROCEDURES**

- Safe operating procedures will be available for all materials, operations and equipment.
- The workers will be informed of consequences of failure to observe the safe operating procedures.
- Safe operating procedures will be formulated and updated, specific to process & equipment and distributed to concerned plant personnel.
- Safety procedures will be prepared and displayed meticulously in Kannada and English languages.

#### **13.1 FIRE PROTECTION**

- Well-designed pressured hydrant system comprising with jockey pump, electrical & diesel pumps, hydrant, monitor etc. will be installed at the plant.
- The firefighting system and equipment will be tested and maintained as per relevant standards.
- Heat and smoke detectors will be provided at the plant and calibrated and maintained properly.

#### **13.2 STATIC ELECTRICITY**

- All equipment and Storage tanks / Containers of flammable chemicals are will be bounded and earthed properly.
- Electrical pits will be maintained clean and covered.
- Electrical continuity for earthing circuits shall be maintained.
- Periodic inspections shall be done for earth pits and record will be maintained.

#### **13.3 COMMUNICATION SYSTEM**

Communication facilities will be checked periodically for its proper functioning.

### **14. SAFETY INSPECTIONS**

The system will be initiated for checklist based routine safety inspection and internal

audit of the plant. Safety inspection team will be formed from various disciplines and departments.

**15. PREDICTIVE AND PREVENTIVE MAINTENANCE**

Predictive and preventive maintenance schedule will be followed in religious manner.

**16. ELECTRICAL SAFETY**

- Insulation pad at HT panels will be replaced at regular interval.
- Housekeeping in MCC room will be kept proper for safe working conditions.

**17. COLOUR CODING SYSTEM**

Color coding for piping and utility lines are will be followed in accordance with IS: 2379:1990.

**ANNEXURE-8**

**ALLOTMENT LETTER**



# KARNATAKA INDUSTRIAL AREAS DEVELOPMENT BOARD

(A Government of Karnataka Undertaking)

# 49, 4th & 5th Floors, 'East Wing', Khanija Bhavan, Race Course Road, Bengaluru - 560 001

Phone : 080-22265383 Fax : 080-22267901

Website : www.kiadb.in email: ceoemkiadb@gmail.com

No. IADB/HO/Allot/23147/14148 /2020-21

Date: 20.03.2021.

Prop: T.V.Srihari,  
M/s. Laureatz Technochem Pvt Ltd,  
Plot No.147, Sri Sai Nilayam,  
Near Tennis Park Pragtinagar,  
Kutbullapur, Niza,  
Hyderbad-500 090.

RPAD

Sis,

## ALLOTMENT LETTER

**Sub:** Allotment of 2.00 acres (8094.00 Smtrs) of land in Plot No.62 of Kadachur Industrial Area, Yadgir District - reg.

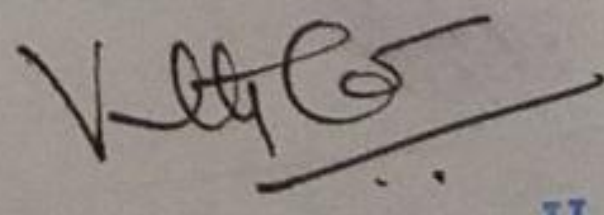
**Ref :** 1. 122<sup>th</sup> SLSWCC meeting dt: 07.01.2021.  
2. Your letter dt: 16.03.2021.

\*\*\*\*

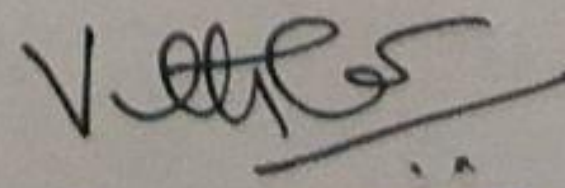
In pursuance of the approval given by the 122<sup>th</sup> SLSWCC meeting dt: 07.01.2021 you have been 2.00 acres (8094.00 Smtrs) of land in Plot No.62 of Kadachur Industrial Area, Yadgir District for Manufacture of **"APIS & Intermediates"** subject to the terms and conditions indicated in the Annexe-A appended hereto and also the terms and conditions mentioned hereafter.

1. The allotment of land is on lease -cum sale basis for a period of **10** years. The lease is liable to be cancelled automatically in case the land is not utilized within a period of three years in case of MSME, large projects or five years in cases of mega, ultra mega, super mega projects as defined in the industrial policy or the land is not utilized within a specified period approved by DLSWCC/SLSWCC/SHLCC/ Allotment Committee without obtaining valid extensions from the concerned investment approving committees detailed in (c)(iii) of Annexe 'A'.  
The tentative premium payable for allotment of the said land has been fixed at **Rs.37.50/- Lakhs** per Acre.
2. (a) The tentative premium of the said plot is **Rs.75,00,000/-**. and EMD **Rs.10,000/-** per acre  
(b). The tentative premium of the land shall be paid as follows:
  - i. A Sum of **Rs.15,10,000/-** being paid vide Rt. No.0050337 dt:16.03.2021 is adjusted towards 20% land cost & EMD.
  - ii. A sum of **Rs.60,00,000/-** being the balance 80% of the tentative premium of land shall be paid within **150 days** from the date of this letter ie on or before **17.08.2021**.

Page 1 of 4

  
Secretary-II  
Karnataka Industrial Areas Development Board  
Bengaluru - 560 001.

- (c) In the event of your furnishing letter of commitment from KSFC/KSIIDC/ Reserve Bank of India approved Financial Institutions/ Corporations/ Companies agreeing to pay the premium indicated at 2(b)(ii) directly to the Board (applicable only to Medium, Small and Micro Enterprises) the allotment will be confirmed and documentation will be permitted subject to payment of **interest @10.50% per annum** on amount due from the date of handing over possession of land to the date of payment which should be made within 180 days from the date of execution of Lease Agreement.
- (d) You should pay lease rent of Rs.1000/- per acre/per annum.
- (e) You should pay maintenance charges as may be fixed by the Board from time to time.
- (f) Interest at 10.95% per annum shall be levied in case the lease rents are not paid within one month from the date on which the lease rents fall due every year.
3. (a) In case of your failure to pay the amount mentioned at Para 2(b)(ii) before the expiry of the time stipulated therein, this offer of allotment stands automatically cancelled and the Earnest Money Deposit and **20%** of the amount paid by you towards premium stands automatically forfeited.
- (b) If the balance premium is not paid within 180 days from the date of execution of lease agreement in respect of cases mentioned at Para 2(c), the plot would be resumed on expiry of the time stipulated without issuing any fresh notice.
4. Soon after receipt of 100% premium of land as at para 3(a)(i) & (ii) and on your acceptance of all the terms and conditions indicated herein before and also those mentioned hereinafter, the possession of land will be handed over within 30 days from the date of payment. At the time of taking over possession, you should produce the original receipts, issued for the payments made, to the Engineer in charge of the area.
5. On taking possession of land, you shall adhere to the time schedule indicated in the Annexure-A.
6. Your failure to take possession of land within 30 days from the date of payment of the premium shall result in cancellation of allotment and **20%** of the amount paid towards premium and E.M.D shall stand forfeited.
7. The Board may accept voluntary surrender of plot subject to levy of penalty at **15%** of the allotment cost paid by you.
8. All taxes in respect of the lease including service tax shall be payable by you to the Board.
9. Any deposits made by you towards allotment consideration will not carry any interest.



Secretary-II

Karnataka Industrial Areas Development Board  
Bengaluru - 560 001.



# KARNATAKA INDUSTRIAL AREAS DEVELOPMENT BOARD

(A Government of Karnataka Undertaking)

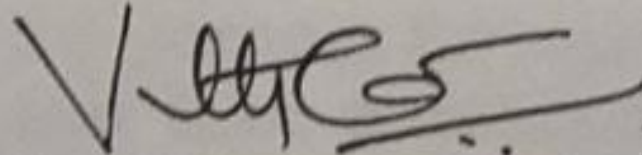
# 49, 4th & 5th Floors, 'East Wing', Khanija Bhavan, Race Course Road, Bengaluru - 560 001

Phone : 080-22265383 Fax : 080-22267901

Website : www.kiadb.in email: ceoemkiadb@gmail.com

10. You are also requested to remit **Rs.20,240/-** towards slum improvement Cess as per Govt. Order No. HUD/180/MIB/94/dt: 29.03.1984 together with balance premium.
11. It shall be mandatory for you to obtain all statutory clearances from the Karnataka State Pollution Control Board and other statutory competent authorities before commencement of the approved project.
12. Any deposit made by you towards allotment consideration will not carry any interest.
13. Only jurisdictional courts shall have Jurisdiction.
14. You are required to inform any change in address of the Registered Office or Administrative Office, to the Board immediately.
15. This allotment is subject the other terms and conditions of the lease cum sale agreement the sale deed will be executed after completion of 10 years from the date of execution of lease-cum-sale agreement, even though the project is implemented and 50% or more than of the area allotted has been utilized. You have to clear all the dues before execution of absolute sale deed. After execution of sale deed, the land/shed shall be utilized only for industrial purpose.
16. This letter is issued with the approval of Chief Executive Officer & Executive Member.

Yours faithfully,

  
20/3/21  
AUTHORISED SIGNATORY  
Secretary-II

Karnataka Industrial Areas Development Board  
Bengaluru - 560 001.



# KARNATAKA INDUSTRIAL AREAS DEVELOPMENT BOARD

(A Government of Karnataka Undertaking)  
# 49, 4th & 5th Floors, 'East Wing', Khanija Bhavan, Race Course Road, Bengaluru - 560 001  
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Annexe-A

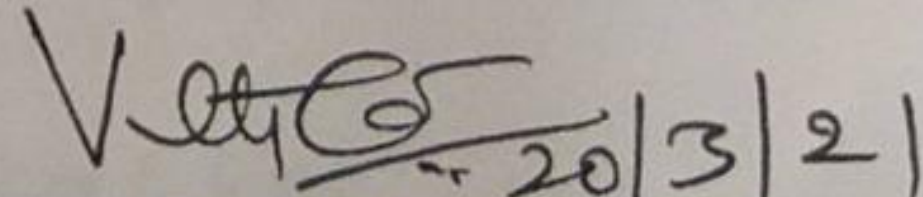
## CONDITIONS OF ALLOTMENT

The time schedule prescribed for various activities subsequent to payment of premium.

1.(a) For taking over possession of land.	30 days from the date of payment of entire premium.
(b) For execution of Lease Agreement	30 days from the date of receipt of Possession Certificate.
(c) For commencement of construction and completion of project by commencing production.	Construction should be commenced within nine months from the date of taking over possession and production should be commenced :- i) within a period of three years after taking over possession in case of MSME and large industries ii) within a period of five years after taking over possession in cases of mega, ultra mega and super mega projects. iii) Promoters to seek extension of time in writing by giving valid reasons to be concerned investment approving committees viz., DLSWCC / SLSWCC / SHLCC/Allotment Committee prior to the above mentioned periods.

2. On being satisfied that the land is not put to use for the purpose for which it was allotted, the Board will be free to re-enter upon and take possession of the whole or any part of the land which has not been put to proper use.

3. If necessary, the interest in this plot of land may be offered as security in order to obtain financial assistance from the Govt. or Corporate bodies like Life Insurance Corporation of India, Karnataka State Financial Corporation, Karnataka State Industrial Investment & Development Corporation, Trustees for Debenture Stock or Banks. However, prior permission of the Board shall be obtained for creating second and subsequent charges on the land.

  
20/3/21  
AUTHORISED SIGNATORY

Karnataka Industrial Areas Development Board  
Bengaluru - 560 001.

**ANNEXURE-9**

**KIADB GAZETTE**  
**NOTIFICATION COPY**

## *Land Notification*





# ಕರ್ನಾಟಕ ರಾಜ್ಯಪತ್ರ

ಅಧಿಕೃತವಾಗಿ ಪ್ರಕಟಿಸಲಾದುದು  
ವಿಶೇಷ ಪತ್ರಿಕೆ

ಭಾಗ - III	ಬೆಂಗಳೂರು, ಶುಕ್ರವಾರ, ಡಿಸೆಂಬರ್ 20, 2011 (ಸಂಖ್ಯೆ F, ಪಕ ವರ್ಷ ೧೯೩೩)	ಸಂ. ೧೦೪೮
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ವಾಣಿಜ್ಯ ಮತ್ತು ಕೈಗಾರಿಕಾ ಸಚಿವಾಲಯ

ಕರ್ನಾಟಕ ಕೈಗಾರಿಕಾ ಪ್ರದೇಶಾಭಿವೃದ್ಧಿ ಮಂಡಳಿ ಕಾಯ್ದೆ 1966 ರ ಕಲಂ 28(4) ರನ್ವಯ ಅಧಿಸೂಚನೆ  
ಸಂಖ್ಯೆ : 18 455 ಎಸ್‌ಪಿ.ಸಿ. 2011, ಬೆಂಗಳೂರು, ದಿನಾಂಕ : 30ನೇ ಡಿಸೆಂಬರ್, 2011

ಕರ್ನಾಟಕ ಕೈಗಾರಿಕಾ ಪ್ರದೇಶಾಭಿವೃದ್ಧಿ ಕಾಯ್ದೆ 1966 (ಕರ್ನಾಟಕ ಕಾಯ್ದೆ 1966) (ಈ ಮುಂದೆ ಪ್ರಸ್ತುತ ಕಾಯ್ದೆ ಎಂದು ಹೇಳಲಾಗಿದೆ) ಕಲಂ 28(1) ರನ್ವಯ ವಿಷಯವಾಗಿರುವ ಅಧಿಕಾರದಡಿ ಸಂಖ್ಯೆ:ಪಿ.ಎಸ್.ಪಿ.2010:ಬೆಂಗಳೂರು ದಿನಾಂಕ: 15-7-2010 (ಈ ಮುಂದೆ ಅಧಿಸೂಚನೆ ಎಂದು ಹೇಳಲಾಗಿದೆ) ರಂದು ಹೊರಡಿಸಿ ದಿನಾಂಕ: 19-7-2010 ರಂದು ಪ್ರಕಟವಾದ ರಾಜ್ಯ ಪತ್ರದ ಪುಟ (1) ರಿಂದ (92) ರ ವರೆಗೆ (ಭಾಗ-3) ರಲ್ಲಿ ಕರ್ನಾಟಕ ಸರ್ಕಾರವು ಪ್ರಸ್ತುತ ಅಧಿಸೂಚನೆಯಲ್ಲಿ ಕಾಣಿಸಿರುವ ಕೈಗಾರಿಕಾ ಅಭಿವೃದ್ಧಿಗೋಷ್ಠಿ ರ ಅಂದರೆ ಕೈಗಾರಿಕಾ ಪ್ರದೇಶಕ್ಕಾಗಿ ಪ್ರಸ್ತುತ ಅಧಿಸೂಚನೆಯಲ್ಲಿ ಕಾಣಿಸಿರುವ ಜಮೀನುಗಳನ್ನು ಸ್ವಾಧೀನಪಡಿಸಿಕೊಳ್ಳಲು ತನ್ನ ಉದ್ದೇಶವನ್ನು ಪ್ರಕಟಿಸಿತ್ತು.

ಅದರಂತೆ ಪ್ರಸ್ತುತ ಕಾಯ್ದೆಯನ್ವಯ 28 ರ ಉಪ ಕಲಂ (3) ರನ್ವಯ ಅದೇಶವನ್ನು ಹೊರಡಿಸಲಾಗಿದೆ. ಮತ್ತು ಈ ಕೆಳಗೆ ಅನುಸೂಚಿಯಲ್ಲಿ ಕಾಣಿಸಿರುವ ಜಮೀನುಗಳು ಪ್ರಸ್ತುತ ಅಧಿಸೂಚನೆಯಲ್ಲಿಯೂ ಕಾಣಿಸಲ್ಪಟ್ಟವೆ ಹಾಗೂ ಪ್ರಸ್ತುತ ಅಧಿಸೂಚನೆಯಲ್ಲಿ ಕಾಣಿಸಿರುವ ಉದ್ದೇಶಕ್ಕಾಗಿ ಸ್ವಾಧೀನಪಡಿಸಿ ಕೊಳ್ಳಬೇಕೆಂದು, ಕರ್ನಾಟಕ ಸರ್ಕಾರಕ್ಕೆ ಮನವರಿಕೆಯಾಗಿದೆ.

ಅದುದರಿಂದ ಕರ್ನಾಟಕ ಕೈಗಾರಿಕಾ ಪ್ರದೇಶಾಭಿವೃದ್ಧಿ ಕಾಯ್ದೆ 1966-(ಕರ್ನಾಟಕ ಕಾಯ್ದೆ 18:1966) ರ ಕಲಂ 28 ರ ಉಪ ಕಲಂ (4) ರನ್ವಯ ವಿಷಯವಾಗಿರುವ ಅಧಿಕಾರದ ಮೇರೆಗೆ ಅಧಿಸೂಚನೆಯಲ್ಲಿ ಕಾಣಿಸಿರುವ ಉದ್ದೇಶಕ್ಕಾಗಿ ಈ ಕೆಳಗೆ ಅನುಸೂಚಿಯಲ್ಲಿ ಕಾಣಿಸಿರುವ ಜಮೀನುಗಳನ್ನು ಸ್ವಾಧೀನಪಡಿಸಿಕೊಳ್ಳಬೇಕೆಂದು ಈ ಮೂಲಕ ಕರ್ನಾಟಕ ಸರ್ಕಾರವು ಘೋಷಿಸಿದೆ.

ಅನುಸೂಚಿ

ಬೆಂಗಳೂರು

ತಾ. ಯಾದಗಿರಿ

ಮೋಟಾರ್ ವ್ಯವಹಾರ

ಗ್ರಾಮ: ಕೋಟಕೋಟ

ಅ. ಸಂ.	ಸಾರಾಂಶ ಕಾರ್ಯ	ಅರ್ಜಿ ಸಲ್ಲಿಸಿದ ದಿನಾಂಕ	ರ.ವ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಅನುಮತಿ ದಿನಾಂಕ ೨-೨೦	ಅವಧಿ ದಿನ-೨೨	ಮಾನ್ಯತೆ ಪಡೆದ	ಬಿಲ್ಲು (ಬಿಲ್ಲು)				ಇತರೆ	
							ಮಾನ್ಯತೆ	ಬಿಲ್ಲು	ಲಾಭ	ಬಿಲ್ಲು		
1	2	3	4	5	6	7	8	9	10	11		
1	1) ಪಂಚಾಯತನ ಕೆ/ ಮಾರ್ಗದರ್ಶಿ ಬಿಲ್ಲು (2-04) 2) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 3) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 4) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 5) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 6) ಪಂಚಾಯತನ ಕೆ/ ಮಾರ್ಗದರ್ಶಿ ಬಿಲ್ಲು (0-34)	02-26	೪೫೬	430/1.2.3	05-24	2-44 3-07	ಮಾನ್ಯತೆ	428	431	352	429	
2	1) ಪಂಚಾಯತನ ಕೆ/ ಮಾರ್ಗದರ್ಶಿ ಬಿಲ್ಲು (02-14) 2) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (0-38) 3) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (2-05) 4) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (02-21)		೪೫೬	431	00-36 0-05(ಎ) 10-33	4-23 1-00 2-24 2-68	ಮಾನ್ಯತೆ	430	432	352	458	
3	1) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-32) 2) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-32) 3) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-32) 4) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-33) 5) ಮಾರ್ಗದರ್ಶಿ ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 6) ಮಾರ್ಗದರ್ಶಿ ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 7) ಮಾರ್ಗದರ್ಶಿ ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 8) ಮಾರ್ಗದರ್ಶಿ ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್	(2-00)	೪೫೬	432/೫೫೬	17-09 05-12(ಎ) 11-37	10-05	ಮಾನ್ಯತೆ	431	435	433	456	
4	1) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-25) 2) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-29) 3) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (04-07)		೪೫೬	433/೫೫೬	11-21 0-02(ಎ) 11-19	5-76 4-06 4-50	ಮಾನ್ಯತೆ	431	434	312	432	
5	1) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (00-13) 2) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (3-11) 3) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 4) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ 5) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (1-11) 6) ಮಾರ್ಗದರ್ಶಿ ಕೆ/ ಮೆಟ್ರಿಕ್ (2-28)	(1-14)	೪೫೬	434 ಆ 00೮ ಉ ಬ ಮೆಟ್ರಿಕ್	18-16	3-07 3-67	ಮಾನ್ಯತೆ	433	437	309	435	

ಕ್ರ. ಸಂ.	ಪಾವತಿಯ ವಿವರ	ಅಂದಾಜಿತ ಲಾಭ ವಿವರ	ಒ.ಸ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಲಾಭಾಂಶ Dy/MSR 0-100	ಅಂದಾಜಿತ ಲಾಭ-ಶೇ.ಕೆ	ಅಂದಾಜಿತ ಮೊತ್ತ	ಅಂದಾಜಿತ (ಅಂದಾಜಿತ)				ಮೊ.
							ಮೊತ್ತ	ಶೇ.ಕೆ	ಅಂದಾಜಿತ	ಶೇ.ಕೆ	
1	2	3	4	5	6	7	8	9	10	11	
	7) ಖರೀದಿ ಅಥವಾ ತೆರಿಗೆ ಪಾವತಿಯು (02-30) 8) ಉದ್ಯೋಗ ತೆರಿಗೆ/ ಸಂಯೋಜನೆ ಅನುದಾನ (3-11) 9) ಅಡ್ಡ ತೆರಿಗೆ/ ಬಾಡಿಗೆ ಪಡೆ (2-05) 10) ಹಿಡ್ಡ ತೆರಿಗೆ/ ಬಾಡಿಗೆ (1-23)										
6	1) ಸಂಯೋಜನೆ ತೆರಿಗೆ/ ಲಾಭಾಂಶ } 6-17 2) ಲಾಭಾಂಶ ತೆರಿಗೆ/ ಲಾಭಾಂಶ } 3) ಶೇ.ಕೆ ಸಿಬ್ಬಂದಿ ತೆರಿಗೆ/ ಲಾಭಾಂಶ } 4) ಸಿಬ್ಬಂದಿ ತೆರಿಗೆ/ ಲಾಭಾಂಶ } 6-18 5) ಹಿಡ್ಡ ತೆರಿಗೆ/ ಬಾಡಿಗೆ (6-18) 6) ಹಿಡ್ಡ ತೆರಿಗೆ/ ನಿರೀಕ್ಷಿತ ಅಭಿವೃದ್ಧಿಗೋಲ (4-13) 7) ಲಾಭಾಂಶ ತೆರಿಗೆ/ ಸಂಯೋಜನೆ ಅನುದಾನ (2-05)	ಶೇ.ಕೆ	435,436	32-08	-	ಶೇ.ಕೆ	432	437	434	436	
7	1) ಪಾವತಿ ತೆರಿಗೆ/ ಪಾವತಿಗಾಗಿ U/G ಪಾವತಿಗಾಗಿ ಗಿ/ಪಾವತಿಗಾಗಿ (9-15) 2) ಪಾವತಿ ತೆರಿಗೆ/ ಪಾವತಿಗಾಗಿ U/G ಪಾವತಿಗಾಗಿ ಗಿ/ಪಾವತಿಗಾಗಿ (5-16)	ಶೇ.ಕೆ	437/90.0	14-31	10-22 5-87	ಶೇ.ಕೆ	435	438	700	ಪೆಟ್ಟ	
8	1) ಅಡ್ಡ ತೆರಿಗೆ/ ಪಾವತಿ (2-16) 2) ಶೇ.ಕೆ ಪಾವತಿಗಾಗಿ ತೆರಿಗೆ/ ಶೇ.ಕೆ ಪಾವತಿಯು (4-04) 3) ಸಂಯೋಜನೆ ತೆರಿಗೆ/ ಸಂಯೋಜನೆ ನಿಲುವು (2-17) 4) ಲಾಭಾಂಶ ತೆರಿಗೆ/ ಪಾವತಿಗಾಗಿ (4-35) ಶೇ.ಕೆ ಪಾವತಿಗಾಗಿ ತೆರಿಗೆ/ ಪಾವತಿಯು (2-50)	ಶೇ.ಕೆ	438/1,2,3	16-22	10-00 6-00 2-54	ಶೇ.ಕೆ	437	445	700	ಪೆಟ್ಟ	
9	1) ಸಂಯೋಜನೆ ತೆರಿಗೆ/ ಲಾಭಾಂಶ ಅಡ್ಡ (4-26) 2) ಪಾವತಿಗಾಗಿ ತೆರಿಗೆ/ ಅಡ್ಡ ತೆರಿಗೆ ಅನುದಾನ (4-12) 3) ಸಂಯೋಜನೆ ತೆರಿಗೆ/ ಅಡ್ಡ (2-28) 4) ಪಾವತಿಗಾಗಿ ತೆರಿಗೆ/ ಅಡ್ಡ (1-31)	ಶೇ.ಕೆ	439/1,2,3,4	13-17	5-20 4-82 3-03 1-31	ಶೇ.ಕೆ	438	440	700	445	
10	1) ಉದ್ಯೋಗ ತೆರಿಗೆ/ ಸಿಬ್ಬಂದಿ ಪಾವತಿ (4-39) 2) ಹಿಡ್ಡ ತೆರಿಗೆ/ ಸಿಬ್ಬಂದಿ ಪಾವತಿ (5-13) 3) ಸಿಬ್ಬಂದಿ ತೆರಿಗೆ/ ಸಿಬ್ಬಂದಿ ಪಾವತಿ (3-30) 4) ಉದ್ಯೋಗ ತೆರಿಗೆ/ ಸಿಬ್ಬಂದಿ (4-03)	ಶೇ.ಕೆ	440/1,2,3	18-05 0-14(ಎ) 17-31	5-49 5-92 8-57	ಶೇ.ಕೆ	439	442	700	444	

ಕ್ರ. ಸಂ.	ಪರಿಷತ್ತಿನ ವಿವರ	ಅ. ಸಂ.	ಒ.ಸ.ಸಂ.	ಉದ್ದೇಶಪಟ್ಟಿ ಸಂಖ್ಯೆ	ಅಂದಾಜು ಮೊತ್ತ	ಉದ್ದೇಶ ಪದ	ಒಟ್ಟು (ಒಟ್ಟು)				ಒಟ್ಟು	
							ಪ್ರಾರಂಭ	ಪೂರ್ಣ	ಉಳಿದ	ಒಟ್ಟು		
1	2	3	4	5	6	7	8	9	10	11	12	
11	1) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ ಯೋಜನೆ 2) ನರಸೀಪುರ ತಂ/ ಉಪಯುಕ್ತ 3) ಜನಶಿಕ್ಷಣ ತಂ/ ಮುಂಚೂಣಿ 4) ಯೋಜನೆ ತಂ/ ಕಾರ್ಯಕ್ರಮ 5) ಜನಜನನ ತಂ/ ನಿರೀಕ್ಷೆ (2-25) 6) ಮದರಾಸು ತಂ. ನಿರೀಕ್ಷೆ (2-00) 7) ಮದರಾಸು ನರಸೀಪುರ ತಂ/ ನಿರೀಕ್ಷೆ (4-34) 8) ಕೆ.ಆರ್.ಎ. ತಂ/ ಜನಜನನ ಸಾ.ಸಂ. (4-02) 9) ನರಸೀಪುರ ತಂ/ ಮದರಾಸು ಜನಜನನ (1-39) 10) ಜನಜನನ ತಂ/ ಜನಜನನ ಜನಜನನ (2-00) 11) ಕೆ.ಆರ್.ಎ. ತಂ/ ಜನಜನನ ಜನಜನನ (2-17) 12) ಜನಜನನ ತಂ/ ಮದರಾಸು ಜನಜನನ ತಂ (2-19) 13) ನರಸೀಪುರ ತಂ/ ಉಪಯುಕ್ತ ಯೋಜನೆ (4-00) 14) ಜನಜನನ ತಂ/ ನರಸೀಪುರ ಜನಜನನ (5-00) 15) ಮದರಾಸು ತಂ/ ಜನಜನನ ನಿರೀಕ್ಷೆ (4-15) 16) ನರಸೀಪುರ ತಂ/ ನರಸೀಪುರ ಯೋಜನೆ (4-15)	13-06	ಭೂಮಿ	441,442,443	53-12 6-09(ಎ) 53-03	-	ಮಿಷನ್	440	ಗಿರಿ	ಗಿರಿ	442	
12	1) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ (4-20) 2) ಮದರಾಸು ತಂ/ ಮದರಾಸು ಜನಜನನ (4-20) 3) ಮದರಾಸು ತಂ/ ಮದರಾಸು (5-00) 4) ಜನಜನನ ತಂ/ ಜನಜನನ ಜನಜನನ (3-39)		ಭೂಮಿ	444/ಅ.ಸಂ.	17-39	10-07 10-07	ಮಿಷನ್	445	443	440	447	
13	1) ಅಧ್ಯಯನ ಯೋಜನೆ ತಂ/ ಮದರಾಸು (1-21) 2) ಕೆ.ಆರ್.ಎ. ಜನಜನನ ತಂ/ ಮದರಾಸು (2-00) 3) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ (3-35) 4) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ (2-08) 5) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ (0-04) 6) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ (2-09)		ಭೂಮಿ	445/1,2,3,4	11-39 0-09(ಎ) 11-30	3-84 4-17 2-37 2-43	ಮಿಷನ್	438	444	439	446	
14	1) ಅಧ್ಯಯನ ಯೋಜನೆ ತಂ/ ಮದರಾಸು (0-17) 2) ಮದರಾಸು ತಂ/ ಮದರಾಸು ತಂ (2-11) 3) ಮದರಾಸು ತಂ/ ಮದರಾಸು ತಂ (2-22) 4) ಮದರಾಸು ತಂ/ ಅಧ್ಯಯನ (2-01)		ಭೂಮಿ	446/1,2,3,4	9-23 0-07(ಎ) 9-16	2-75 2-77 2-22 2-57	ಮಿಷನ್	438	447	445	447	

ಕ್ರ. ಸಂ.	ಪ್ರಾಜೆಕ್ಟ್ ವಿವರ	ಅಂದಾಜಿತ ವಾರ್ಷಿಕ ವೆಚ್ಚ	ಒ.ಸ.ಸಂ.	ಸ್ಥಳೀಯವರಿಗೆ ಅನುಬಂಧಿಸಿದ ಡ್ರಿಗ್ಗಿಂಗ್ & ಸಿಂ.	ಅಂದಾಜಿತ ಧನ-ಸೃಷ್ಟಿ	ಅನುಬಂಧಿತ ವೆಚ್ಚ	ಫಲಾನುಭವಿ (ಸರ್ಕಾರದ)				ಮೊ.
							ಪ್ರಾಥಮಿಕ	ಮಧ್ಯಮ	ಅಧ್ಯಯನ	ತಜ್ಞರು	
1	2	3	4	5	6	7	8	9	10	11	
	5) ಮನೇಶ್ವರ ತಂ/ ಅಶ್ವತ್ಥ (0-11) 6) ದೇವೇಂದ್ರಶ್ವರ ತಂ/ ಯಂಕಪ್ಪ (2-01)										
15	1) ಸೋಮಪ್ಪ ತಂ/ ಮಾಳವ್ವ (5-19) 2) ವಾಳೇಶ್ವರ ತಂ/ ಸತ್ಯ ನರಸಿಂಹ (5-00)	ಸ್ಥಳ	447	10-19 0-09(ಎ) 10-10	9-95	ಮಿಕ್ಕಿ	446	443	444	ಹಳ್ಳಿ	
16	1) ಚಂದ್ರಶ್ವರ ತಂ/ ನರಸಿಂಹ (1-24) 2) ಚಂದ್ರಶ್ವರ ತಂ/ ನರಸಿಂಹ (1-10)	ಸ್ಥಳ	448/44.8	2-34	1-69 1-32	ಮಿಕ್ಕಿ	449	448	447	ಹಳ್ಳಿ	
17	ಪಾನೀಯ ಪಾನಾ ಸೇವಾ (0-29)	-	449	0-29	0-77	ಮಿಕ್ಕಿ	ಹಳ್ಳಿ	448	447	450	
18	1) ಮಂಜುನಾಥ ತಂ/ ಸಾಯಬ್ಬ (6-00) 2) ಅಬ್ದುಲ್ ಕರೀಂ ತಂ/ ದೇವೇಂದ್ರ (8-08)	ಸ್ಥಳ	450/1.2	14-08	6-66 8-29	ಮಿಕ್ಕಿ	451	449	449	ಊರಿ	
19	1) ಸಿದ್ದಪ್ಪ ತಂ/ ನರಸಿಂಹ (5-00) 2) ಅಮೀನಾಬೇಗಂ ಗಂ/ ನಿಜಾಮಾಬಾದ್ ಪಿಂಚಣಿ (2-20) 3) ಶೇಖರೇಡು ಗಾಂ ತಂ/ ಶೇಖರೇಡು (2-20) 4) ಸೇವೇಂದ್ರ ವೇಣು ಗಂ. ಶೇಖರೇಡು (3-13) 5) ಅಮೀನಾಬೇಗಂ ಗಂ/ ನಿಜಾಮಾಬಾದ್ ಲಡಾಖ್ (1-20)	ಸ್ಥಳ	451	14-33	14-98	ಮಿಕ್ಕಿ	452	450	450	ಹಳ್ಳಿ	ಊರಿ
20	ಶಿವಪ್ಪ ತಂ/ ಶರಣಪ್ಪ ಪಾಟೀಲ	ಸ್ಥಳ	452	10-39	10-83	ಮಿಕ್ಕಿ	453	451	454	ಊರಿ	
21	1) ನಿಜಾಮಾಬಾದ್ ತಂ/ ಮನೇಶ್ವರೇಡು ಲಡಾಖ್ (1-18) 2) ಅಬ್ದುಲ್ ಅಲಿ ತಂ/ ಮನೇಶ್ವರೇಡು ಲಡಾಖ್ (1-18) 3) ಅಬ್ದುಲ್ ಅಲಿ ತಂ/ ಅಕ್ಬರ ಅಲಿ 4) ಮಂಜುನಾಥ ತಂ/ ಅಕ್ಬರ ಅಲಿ 5) ನಿಜಾಮಾಬಾದ್ ಗಂ/ ಸುಬ್ಬರಾಯ ಲಡಾಖ್ 6) ನಿಜಾಮಾಬಾದ್ ತಂ/ ಮನೇಶ್ವರೇಡು ಲಡಾಖ್ (1-22) 7) ಅಬ್ದುಲ್ ಅಲಿ ತಂ. ಮನೇಶ್ವರೇಡು ಲಡಾಖ್ (1-01) 8) ಅಬ್ದುಲ್ ಅಲಿ ತಂ/ ಅಕ್ಬರ ಅಲಿ 9) ಮಂಜುನಾಥ ತಂ/ ಅಕ್ಬರ ಅಲಿ 10) ವಾಳೇಶ್ವರ ಗಂ/ ಸುಬ್ಬರಾಯ ಲಡಾಖ್	ಸ್ಥಳ	453/1.2	10-38	5-63 5-00	ಮಿಕ್ಕಿ	462	452	454	ಊರಿ	
22	1) ಚಂದ್ರನಾಥ ತಂ/ ನಿಜಾಮಾಬಾದ್ ಪಿಂಚಣಿ (4-28) 2) ನಿಜಾಮಾಬಾದ್ ತಂ/ ಮನೇಶ್ವರೇಡು ಪಿಂಚಣಿ (3-28) 3) ನರಸಿಂಹ ತಂ/ ಭವಾನಿ ಕುಮಾರಿ (4-36) 4) ದೇವೇಂದ್ರ ಚಂದ್ರನಾಥ ತಂ/ ಮುಕ್ತೇಶ್ವರೇಡು ಪಿಂಚಣಿ (3-20)	ಸ್ಥಳ	454/1.2	16-32	9-16 9-16	ಮಿಕ್ಕಿ	461	437	455	453	

ಅ. ಸಂ.	ಸಾಹಿತ್ಯಕ ಕೃತಿ	ಅವಧಿ ಕಾಲ ಮಾಸ	ಒ.ಸ.ನಂ.	ಪ್ರಕಟಣೆಯ ವರ್ಷ ೧೯೫೦-೫೧	ಅವಧಿ ದಿನ-ಶುಕ್ರ	ಮಾಸ	ಪುಟ (ಪುಟಗಳು)				ನೋಟ
							ಮೊತ್ತ	ಶುಭ್ರ	ಅಕ್ಷರ	ಪುಟ	
1	2	3	4	5	6	7	8	9	10	11	
23	1) ಪಾಪಾ ಹುಣಿಸೆ ತಂ/ ಲಾಕ್ಷ್ಮೀನಾಥ ಚೋದರಗಿ (7-00) 2) ಮುಕ್ತಕ ಹುಣಿಸೆ ತಂ/ ಹನುನಾಥ 3) ಮೌಲಿಕಿ ತಂ/ ಹನುನಾಥ 4) ಮಗನುಮ ಅರಿ ತಂ/ ಹನುನಾಥ	4-05	455/೮,೮	11-05	7-07 4-18	ಮಾಸಿ	456	436	436	454	
24	1) ಅನುಭವ ತಂ/ ಹನುನಾಥ (4-00) 2) ಮುಕ್ತಕ ಹುಣಿಸೆ ತಂ/ ಮುಕ್ತಕ ಅಕ್ಷರಲೇಖಕ ಹವನಾಥ 3) ಮೌಲಿಕಿ ಹುಣಿಸೆ ತಂ, ಮುಕ್ತಕ ಅಕ್ಷರ ಲೇಖಕ ಹವನಾಥ	3-14	456	09-14	10-48	ಮಾಸಿ	457	455	432	461	
25	1) ಮಹಿಮಾ ಹುಣಿಸೆ ತಂ/ ಕೇವಲಾಂದನಾಥ (4-35) 2) ಬಸವರಾಜ ತಂ/ ಅಯ್ಯಪ್ಪ ಕುಮಾರ (4-12) 3) ಕುಮಾರಿ ಅಂತರಾಂಗ ತಂ/ ಅಕ್ಷರ ಹುಣಿಸೆ (4-21) 4) ಅಕ್ಷರ ಹುಣಿಸೆ ತಂ/ ಹುಣಿಸೆನಾಥ (1-39) 5) ಅಕ್ಷರ ಹುಣಿಸೆ ತಂ/ ಹುಣಿಸೆನಾಥ (1-39)		457/ ೮ ೦೦೮ ಉಪ ಪರಿಷೆ	17-07	5-64 5-31 5-31 2-30 2-30	ಮಾಸಿ	458	456	456	460	
26	1) ಹುಣಿಸೆ ನಾಥ (0-04) 2) ಅನುಭವ (0-05) 3) ನನ್ನನಾಥ ತಂ/ ಲಾಕ್ಷ್ಮೀನಾಥ (0-25) 4) ಮಹಿಮಾ ಹುಣಿಸೆ ತಂ/ ಮೌಲಿಕಿ (1-20) 5) ಲಾಕ್ಷ್ಮೀನಾಥ (1-21) 6) ಪಾಪಾ ಹುಣಿಸೆ ತಂ/ ಕೇವಲಾಂದನಾಥ (1-30) 7) ನನ್ನನಾಥ (3-06) 8) ಅನುಭವ ತಂ/ ಮೌಲಿಕಿ 9) ಪಾಪಾ ಹುಣಿಸೆ ತಂ/ ಮೌಲಿಕಿ 10) ಹುಣಿಸೆನಾಥ ತಂ/ ಹುಣಿಸೆನಾಥ (1-01) 11) ನನ್ನನಾಥ ತಂ/ ಹನುನಾಥ 12) ಮಹಿಮಾ ಹುಣಿಸೆ ತಂ/ ಹನುನಾಥ	0-38 1-15	458/೮ ೦೦೮ ೮೮ ಪರಿಷೆ	11-09	0-26 0-71 1-72 1-39 3-51 1-6 1-16 1-84	ಮಾಸಿ	429	457	431	465	
27	1) ಪಾಪಾ ಹುಣಿಸೆ ತಂ/ ಮೌಲಿಕಿ 2) ಅನುಭವ ತಂ/ ಮೌಲಿಕಿ 3) ಪಾಪಾ ಹುಣಿಸೆ ತಂ/ ಕೇವಲಾಂದನಾಥ (3-17)	3-17	459/೮,೮	6-35	3-99 3-99	ಮಾಸಿ	458	460	457	465	
28	1) ಮಹಿಮಾ ಹುಣಿಸೆ ತಂ/ ಮಹಿಮಾ ಅರಿ (4-05) 2) ಗುಣಾಧಾರ ತಂ/ ಹುಣಿಸೆನಾಥ ಕುಮಾರೇಂದ್ರ (1-33)		460/೮,2,3,4	11-37	4-57 4-07	ಮಾಸಿ	459	461	457	464	

ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಪುಸ್ತಕ ವಿವರ	ಅನುಷ್ಠಾನ ಉದ್ದೇಶ ಪರಿಷ್ಕರಣೆ	ಒ.ಸ.ಸಂ.	ಸ್ವೀಕೃತವಿಷಯ ಉಪನಾಮ ಸಂಖ್ಯೆ ೨-೧೦	ಅಂದಾಜಿತ ದೇ-ಶೈ	ನಿರೀಕ್ಷಿತ ಸಂಖ್ಯೆ	ಶಿಕ್ಷಣ (ಶಿಕ್ಷಣ)				ಮಾ
							ಕಾರ್ಯ	ಪ್ರತಿಭ	ಉದ್ದ	ವಿಷಯ	
1.	2	3	4	5	6	7	8	9	10	11	
	3) ಅಂತರರಾಜ್ಯ ತಂ/ ನಿಜಾಯುಕ್ತ (1-32) 4) ಕೆಲವುಕೋಶ ತಂ/ನಿಜಾಯುಕ್ತ ಪರಿಷ್ಕರಣೆ (1-28) 5) ಕೆಲವುಕೋಶ ತಂ/ನಿಜಾಯುಕ್ತ ಪರಿಷ್ಕರಣೆ (1-30) 6) ಕೆಲವು ಅಂತರರಾಜ್ಯ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-11)										
29	1) ಕಾಲೇಜು ತಂ/ ಪರಿಷ್ಕರಣೆ ಪರಿಷ್ಕರಣೆ (4-22) 2) ಅಂತರರಾಜ್ಯ ತಂ/ ನಿಜಾಯುಕ್ತ ಪರಿಷ್ಕರಣೆ (2-03) 3) ನಿಜಾಯುಕ್ತ ತಂ/ ಪರಿಷ್ಕರಣೆ ಪರಿಷ್ಕರಣೆ (2-03) 4) ಕೆಲವುಕೋಶ ತಂ/ನಿಜಾಯುಕ್ತ ಪರಿಷ್ಕರಣೆ (1-26) 5) ಕೆಲವುಕೋಶ ತಂ/ನಿಜಾಯುಕ್ತ ಪರಿಷ್ಕರಣೆ (1-23) 6) ಅನುಷ್ಠಾನ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-26)	ಭೂ	461/1,2	11-23	3-87	ಪಂಕ್ತಿ	460	454	456	462	
30	1) ಅನುಷ್ಠಾನ ತಂ/ ಫಲಾನುಭವಿ (2-07) 2) ಪರಿಷ್ಕರಣೆ ತಂ/ಪರಿಷ್ಕರಣೆ (1-04) 3) ಪರಿಷ್ಕರಣೆ ತಂ/ಪರಿಷ್ಕರಣೆ (1-04) 4) ಅನುಷ್ಠಾನ ತಂ/ ಪರಿಷ್ಕರಣೆ (4-29) 5) ಪರಿಷ್ಕರಣೆ ತಂ/ಪರಿಷ್ಕರಣೆ (3-38) 6) ಫಲಾನುಭವಿ ತಂ/ ಪರಿಷ್ಕರಣೆ (5-07)	ಭೂ	462/1,2,3,4	18-09	4-90 5-29 4-13 5-80	ಪಂಕ್ತಿ	464	453	461	೧೦೦	
31	1) ಶಿಕ್ಷಣ ಅನುಷ್ಠಾನ ತಂ/ ನಿಜಾಯುಕ್ತ (2-24) 2) ಪರಿಷ್ಕರಣೆ ತಂ/ ಅನುಷ್ಠಾನ (2-01)	ಭೂ	463/1,2	4-25 0-05(A) 4-20	0-90 0-65	ಪಂಕ್ತಿ	465	462	464	೧೦೦	
32	1) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (7-22) 2) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-20) 3) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ } 2-21 4) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ } 5) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-20) 6) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (2-21) 7) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ } 0-38 8) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ } 9) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-22) 10) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ U/G ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-20)	ಭೂ	464/165	28-24 0-02, ೩ 28-22	9-85 16-69	ಪಂಕ್ತಿ	465	462	460	463	

ಕ್ರ. ಸಂ.	ಸಂಕೇತ ಕೆ.ಸಿ.	ಪ್ರಾರಂಭ ತಾರೀಖು	ಒ.ಸ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಉಪಗ್ರಹಗಳ ಸಂಖ್ಯೆ a-b	ಉಪಗ್ರಹಗಳ ಸಂಖ್ಯೆ	ಪರಿಶೀಲನೆ ತಾರೀಖು	ಒಟ್ಟು (ಒಟ್ಟು)				ಮಾ.
							ಮಾ.	ಸಂಖ್ಯೆ	ಉದ್ದ	ವಿಸ್ತೀರ್ಣ	
1	2	3	4	5	6	7	8	9	10	11	
	11) ಉಪಗ್ರಹ ತಂ./ ಸಂಕೇತಗಳು(1-20) 12) ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹ ಚೋದನೆ(0-17) 13) ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹ ಚೋದನೆ(0-17) 14) ಅಧಿಗ್ರಹ ತಂ./ ಪರಿಶೀಲನೆ (0-17) 15) ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹ ಚೋದನೆ (0-17) 16) ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹ ಚೋದನೆ (0-16) 17) ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹ ಚೋದನೆ (0-16)										
33	ಸಂಕೇತ ತಂ./ ಪರಿಶೀಲನೆ (14-05)	ಪೂರ್ವ	466	14-05 0-01(ಸ) 14-04	12-35	ಮಾಂ.	532	465	429	100	
34	1) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ (0-18) 2) ಸಂಕೇತ ತಂ./ ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ (02-08)	ಪೂರ್ವ	500	02-26 0-18(ಸ) 02-08	01-87	ಮಾಂ.	499	507	501	-	
35	1) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ (0-23) 2) ಪರಿಶೀಲನೆ ತಂ./ ಉಪಗ್ರಹಗಳು (01-30)	ಪೂರ್ವ	501/ಉ.	02-13 0-05 ಸ 02-08	1-91	ಮಾಂ.	485	506	502	507 500	
36	1) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಪರಿಶೀಲನೆ ಮಾಡಿದ (01-25) 2) ಅಧಿಗ್ರಹ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹಗಳು (01-10)	ಪೂರ್ವ	502/1,2	02-35 00-07(ಸ) 02-28	2-30	ಮಾಂ.	488	505	503	501	
37	1) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಪರಿಶೀಲನೆ (01-11) 2) ಅಧಿಗ್ರಹ ತಂ./ ಪರಿಶೀಲನೆ 3) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಪರಿಶೀಲನೆ 4) ಅಧಿಗ್ರಹ ತಂ./ ಪರಿಶೀಲನೆ } (01-12)	ಪೂರ್ವ	503/1,2	2-23 00-07(ಸ) 02-16	02-04	ಮಾಂ.	481	505	476 477	502	
38	1) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಪರಿಶೀಲನೆ 2) ಕೇಂದ್ರೀಕರಣ ಮಾಡಿದ ತಂ./ ಉಪಗ್ರಹಗಳು 3) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಉಪಗ್ರಹಗಳು (00-16) 4) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಉಪಗ್ರಹಗಳು (00-11) 5) ಕೇಂದ್ರೀಕರಣ ತಂ./ ಉಪಗ್ರಹಗಳು (0-11) } 01-16	ಪೂರ್ವ	504/ಉ.	02-14 00-05(ಸ) 02-09	01-40 00-40 00-28 00-42	ಮಾಂ.	503	523	476	505	

ಕ್ರ. ಸಂ.	ಪ್ರಾಜೆಕ್ಟ್ ಹೆಸರು	ಅಧಿಕಾರ ವ್ಯಾಪ್ತಿ	ಒ.ಕ.ನಂ.	ಸ್ಥಾಪನಾಕಾಲ ಆರಂಭ - ಸಂಪೂರ್ಣ	ಅಂತಿಮ ದಿನ-ತ್ಥಿ	ಅಧಿಕಾರ ಪಡೆ	ಸಮಯ (ಸಂವತ್ಸರ)				ಇತರೆ
							ಮಾರ್ಚ್	ಏಪ್ರಿಲ್	ಮೇ	ಜೂನ್	
1	2	3	4	5	6	7	8	9	10	11	12
39	1) ಕುನೀಕೋಟಾ ತಂ/ ಲಾಡ್ಜ್‌ಗಳು (00-24) 2) ಕೇವಲಕುನೀಕೋಟಾ ತಂ/ ಬಾವುಟಗಳು ತಂಜಾವು (00-06)	ಸ್ವಂತ	505	00-31 00-03(ಒ) 00-28	00-20 00-11	ಮಿಕ್ಕಿ	502	506	504	506	
40	1) ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ ತಂ/ ಬಾಡಿಗೆಯ ಯೋಜನೆ ಅಧೀನ (00-06) 2) ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ ತಂ/ ಬಾಡಿಗೆಯ ಯೋಜನೆ ಅಧೀನ (00-06) 3) ಕುನೀಕೋಟಾ ತಂ/ ಲಾಡ್ಜ್‌ಗಳು (01-26)	ಸ್ವಂತ	506	01-38 00-04(ಒ) 01-34	02-02	ಮಿಕ್ಕಿ	507	510	505	508	
41	1) ಕೆ.ಎಂ.ಎಸ್.ಎಸ್. ತಂ/ ಸೀನಿಯರಿಟಿಯಲ್ಲಿ (00-19) 2) ಆರೋಗ್ಯ ತಂ/ ಸೀನಿಯರಿಟಿಯಲ್ಲಿ (01-10)	ಸ್ವಂತ	507	01-29 00-04(ಒ) 01-25	01-89	ಮಿಕ್ಕಿ	500	508	501	500	
42	ಕುನೀಕೋಟಾ ತಂ/ ಲಾಡ್ಜ್‌ಗಳು	ಸ್ವಂತ	508	01-19	00-92	ಮಿಕ್ಕಿ	507	510	506	509	
43	1) ಮೆಟ್ರೋ ತಂ/ ಬಸ್‌ಗಳು 2) ಕುನೀಕೋಟಾ ತಂ/ ಬಸ್‌ಗಳು 3) ಪೂಜಾರಿ ತಂ/ ಬಸ್‌ಗಳು 4) ಸೀನಿಯರಿಟಿಯಲ್ಲಿ ತಂ/ ಮೆಟ್ರೋ ಆಗರದ 5) ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ ತಂ/ ಬಾವುಟಗಳು ಆಗರದ (00-28) 6) ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ ತಂ/ ಬಾವುಟಗಳು ಆಗರದ (00-28) 7) ಕೆ.ಎಂ.ಎಸ್.ಎಸ್. ತಂ/ ಸೀನಿಯರಿಟಿಯಲ್ಲಿ (02-31)	ಸ್ವಂತ	509/ಆ ದಿಂದ 64 ಪದೇಗೆ	05-22	01-88 0059 00-19 02-36	ಮಿಕ್ಕಿ	-	512	510	500	
44	1) ಕೇವಲಕುನೀಕೋಟಾ ಆರೆ ತಂ/ ಮೆಟ್ರೋದ ಕೆಲಸಗಾರರು (00-28) 2) ಕೇವಲಕುನೀಕೋಟಾ ಆರೆ ತಂ/ ಮೆಟ್ರೋದ ಕೆಲಸಗಾರರು (01-16)	ಸ್ವಂತ	510/ಸಿ	02-04 00-04(ಒ) 02-00	01-00 02-00	ಮಿಕ್ಕಿ	508	511	522	509	
45	ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ/ ಕಾರ್ಯಾಲಯ ಆರೋಗ್ಯ (00-30)	ಸ್ವಂತ	511	00-30 00-02(ಒ) 00-28	00-60	ಮಿಕ್ಕಿ	512	512	516	512	
46	1) ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ/ ಕಾರ್ಯಾಲಯ ಆರೋಗ್ಯ (00-27) 2) ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ/ ಬಾವುಟ ತಂ/ ಬಾವುಟ (01-22)	ಸ್ವಂತ	512	02-09 00-05(ಒ) 02-04	0-79	ಮಿಕ್ಕಿ	509	514	511	500	
47	ಮುಖ್ಯಮಂತ್ರಿಗಳ ಕಛೇರಿ/ ಕಾರ್ಯಾಲಯ ಆರೋಗ್ಯ	ಸ್ವಂತ	513	00-32	00-50	ಮಿಕ್ಕಿ	512	514	515	512	

ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಕ್ರಮ ವಿವರ	ಅಧ್ಯಯನ ಕಾಲ	ಕ್ರ.ಸಂ.	ಪ್ರಾಥಮಿಕ ಹಂತದ ಪಾಠ್ಯಕ್ರಮ	ಅಧ್ಯಯನ ಕಾಲ	ಪಾಠ್ಯಕ್ರಮ	ಪರೀಕ್ಷೆ (ಮಾಹಿತಿ)				ಮಾ.
							ಕ್ರ.ಸಂ.	ಕ್ರ.ಸಂ.	ಕ್ರ.ಸಂ.	ಕ್ರ.ಸಂ.	
1	2	3	4	5	6	7	8	9	10	11	
48	ಪಾಠ್ಯಕ್ರಮ (02-27)	-	514/1	02-27 00-23(ಎ) 02-04	00-86	ಮಾಹಿತಿ	515	514/2	527	530	
49	1) ಪಾಠ್ಯಕ್ರಮ (00-20) 2) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ (01-00)	ಪೂರ್ಣ	514/2	01-20 00-03(ಎ) 01-17	01-22	ಮಾಹಿತಿ	514/1	-	530	530	
50	1) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ 2) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ 3) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ 4) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ	00-11	515	00-11	00-27	ಮಾಹಿತಿ	516	514/1	514/1	513	
51	1) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ (00-27) 2) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ (01-10) 3) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ (00-25)	ಪೂರ್ಣ	516	02-22 00-10(ಎ) 02-12	3-24	ಮಾಹಿತಿ	521	515	517	511	
52	ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ	ಪೂರ್ಣ	517	0-14	00-42	ಮಾಹಿತಿ	519	514	518	516	
53	ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ	ಪೂರ್ಣ	518	00-18 00-01(ಎ) 00-17	0047	ಮಾಹಿತಿ	520	514/1	524	517	
54	ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ	ಪೂರ್ಣ	519	00-06	00-09	ಮಾಹಿತಿ	520	517	520	516	
55	ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ	ಪೂರ್ಣ	520	01-12 00-03(ಎ) 01-09	0-05	ಮಾಹಿತಿ	523	518	524	519	
56	1) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ(0-22) 2) ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ(1-04)	ಪೂರ್ಣ	521/ಎ	01-26 00-04(ಎ) 01-22	0-66 01-30	ಮಾಹಿತಿ	522	516	520	510	
57	ಪಾಠ್ಯಕ್ರಮ ಸುಸಜ್ಜಿತ ಪಾಠ್ಯಕ್ರಮ	ಪೂರ್ಣ	522	00-30 0-01(ಎ) 00-29	00-62	ಮಾಹಿತಿ	506	521	523	510	

ಕ್ರ. ಸಂ.	ಪರಿಷತ್ತಿನ ಹೆಸರು	ಉಪ-ಪರಿಷತ್ತಿನ ಹೆಸರು	ಒ.ಸ.ನಂ.	ಪ್ರಾರಂಭಿಸಿದ ದಿನಾಂಕ ೨-೧೦	ಉಪ-ದಿನಾಂಕ	ಪರಿಷತ್ತಿನ ಹೆಸರು	ಸಭಾಸದ (ಸದಸ್ಯರು)				ಮತ
							ಮಾನ್ಯ	ವಿಜ್ಞಾನ	ಉಪ	ವಿಜ್ಞಾನ	
1	2	3	4	5	6	7	8	9	10	11	12
58	ಬುಲೆಟ್ ತಂ/ ಬುಲೆಟ್ ಹರಿಹರ	ಸ್ವಂತ	523	01-17 00-04(ಎ) 01-13	01-49	ಪಿಂಚಿ	504	520	524	522	
59	ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ	ಸ್ವಂತ	524	03-15 00-25(ಎ) 02-30	02-78	ಪಿಂಚಿ	475	527	525	520	
60	1) ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ (01-33) 2) ಬುಲೆಟ್ ತಂ/ ಬುಲೆಟ್ (00-21)	ಸ್ವಂತ	525	02-14 00-04(ಎ) 02-10	00-19	ಪಿಂಚಿ	475	527	525	520	
61	1) ಬುಲೆಟ್ ತಂ/ ಬುಲೆಟ್ ಲೇಔಟ್ 2) ಮಾರಿಟೈಮ್ ಗೆಂ/ ಹೆಲ್ಪ್ ಲೇಔಟ್ (01-07) 3) ಪಾರಿಜಾತ ತಂ/ ಬುಲೆಟ್ ಹರಿಹರ (01-07)	ಸ್ವಂತ	526	02-14	00-84	ಪಿಂಚಿ	525	-	468	527	
62	ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ	-	527	02-06 00-04(ಎ) 02-02	01-91	ಪಿಂಚಿ	524	528	526	514/1	
63	ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ	-	528	0-36 00-09(ಎ) 00-15	0-32	ಪಿಂಚಿ	527	529	526	527	
64	ಸರಕಾರಿ ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ	-	529	00-28 00-06(ಎ) 00-22	00-28	ಪಿಂಚಿ	528	530	-	530	
65	ಸರಕಾರಿ ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ	-	530	00-32 00-02(ಎ) 00-30	00-64	ಪಿಂಚಿ	527	-	529	514/2	
66	ಸರಕಾರಿ ಪಾರಿಜಾತ ಪಾಠಶಾಲೆ	-	531	01-21 0-06(ಎ) 01-15	01-12	ಪಿಂಚಿ	530	532	-	530	
67	ಬುಲೆಟ್ ಲೇಔಟ್ ತಂ/ ಬುಲೆಟ್ ಹರಿಹರ	ಸ್ವಂತ	532	06-27 0-15(ಎ) 06-12	01-96	ಪಿಂಚಿ	530	466	466	533	

ಕ್ರ. ಸಂ.	ಪದವಿಪೂರ್ವ ಪಾಠ	ಪದವಿ ಪೂರ್ವ ಪಾಠ	ಒ.ಸ.ಸಂ.	ಸ್ವೀಕೃತವಿಷಯಗಳ ಸಂಖ್ಯೆ	ಉಪ-ದಿ-ಕ್ರ.	ಪದವಿಪೂರ್ವ ಪಾಠ	ವಿಷಯ (ಸೆಮಿಸ್ಟರ್)				ಒಟ್ಟು
							ಪ್ರಥಮ	ದ್ವಿತೀಯ	ತೃತೀಯ	ಚತುರ್ಥ	
1	2	3	4	5	6	7	8	9	10	11	
68	ಪದವಿಪೂರ್ವ ಪಾಠ	-	533	01-02 01-02(ಸಿ) 00		ಪಂಕ್ತಿ	532	466	466	೮೬೪	
69	ದೊಡ್ಡಮೂವು ಪಂ/ ಪದವಿಪೂರ್ವ (1-17)	ಸ್ವಂತ	534/1	10-03 02-33(ಸಿ) 07-20	1-36	ಪಂಕ್ತಿ	537	546	೮೬೪	536	
70	ಎನ್.ಸಿ. ಜಾಗರಣಾ ತಂ/ಎಂ.ಆರ್.ಆರ್. ಎನ್ ಪದವಿಪೂರ್ವ 2-20	ಸ್ವಂತ	534/2		2-21	ಪಂಕ್ತಿ	537	546	೮೬೪	536	
71	ಎನ್.ಸಿ. ಜಾಗರಣಾ ತಂ/ಎಂ.ಆರ್.ಆರ್. ಎನ್ ಪದವಿಪೂರ್ವ 1-37	ಸ್ವಂತ	534/3		1-80	ಪಂಕ್ತಿ	537	546	೮೬೪	536	
72	ಬಿ.ಎಸ್ಸಿ.ಪದವಿಪೂರ್ವ ಪಂ/ ಪದವಿಪೂರ್ವ 3-14	ಸ್ವಂತ	534/535/ಆ		1-10	ಪಂಕ್ತಿ	537	546	೮೬೪	536	
73	ಪದವಿಪೂರ್ವ ಪಂ/ ಪದವಿಪೂರ್ವ 0-35	ಸ್ವಂತ	534/535/ಇ		0-75	ಪಂಕ್ತಿ	537	546	೮೬೪	536	
74	ಎನ್.ಸಿ. ಜಾಗರಣಾ ತಂ/ಎಂ.ಆರ್.ಆರ್. ಎನ್ ಪದವಿಪೂರ್ವ 2-20	ಸ್ವಂತ	534/535/2		2-20	ಪಂಕ್ತಿ	537	546	೮೬೪	536	
75	ಎನ್.ಸಿ. ಜಾಗರಣಾ ತಂ/ ಎಂ.ಆರ್.ಎನ್. ಪದವಿಪೂರ್ವ	ಸ್ವಂತ	536	14-38 0-16(ಸಿ) 14-22	10-77	ಪಂಕ್ತಿ	537	545	535	542	
76	ಪದವಿಪೂರ್ವ ಪಂ/ ಪದವಿಪೂರ್ವ ಪಾಠ	ಸ್ವಂತ	537	09-34 0-04(ಸಿ) 09-30	08-29	ಪಂಕ್ತಿ	538	536	535	541	
77	1) ಬಡಗಾಲು ತಂ/ ಪದವಿಪೂರ್ವ ಪದವಿಪೂರ್ವ } 01-09 2) ಪಾಠ್ಯಪುಸ್ತಕಗಳ ತಂ/ ಅಭ್ಯಾಸ ಪಾಠ್ಯ ಪುಸ್ತಕಗಳು 3) ದೊಡ್ಡ ಮೂವು ಪಂ/ ಬಡಗಾಲು 01-05 4) ದೊಡ್ಡ ಮೂವು ಪಂ/ ಬಡಗಾಲು 01-14 5) ಪದವಿ ಪಾಠ್ಯ ಪುಸ್ತಕಗಳು 01-14 6) ಪದವಿಪೂರ್ವ ಪಂ/ ಬಡಗಾಲು 00-13 7) ಅಭ್ಯಾಸ ಪದವಿಪೂರ್ವ ಪಂ/ ಬಡಗಾಲು 4-30 8) ಪದವಿಪೂರ್ವ ಪಂ/ ಪದವಿಪೂರ್ವ ಪಾಠ್ಯ ಪುಸ್ತಕಗಳು 02-07 9) ಬಡಗಾಲು ತಂ/ ಪದವಿಪೂರ್ವ ಪಾಠ್ಯ ಪುಸ್ತಕಗಳು 00-29 10) ಪದವಿಪೂರ್ವ ಪಂ/ ಪದವಿಪೂರ್ವ ಪಾಠ್ಯ ಪುಸ್ತಕಗಳು 00-15	ಸ್ವಂತ	538/ಉ. ಕೂಡ ಆಂ ಪದವಿ	16-18 0-03(ಸಿ) 16-15	0-59 00-92 01-15 01-15 00-27 03-80 01-76 00-89 00-31 00-29	ಪಂಕ್ತಿ	೮೬೪	537	೮೬೪	539	

ನ. ಸಂ.	ಪಾಠ್ಯಕ್ರಮ ವಿವರ	ಪುಸ್ತಕ ವಿವರ	೦.ಕೆ.ನಂ.	ಪುಸ್ತಕದ ಉಪಯುಕ್ತ ಪುಟಗಳ ಸಂಖ್ಯೆ	ಪುಸ್ತಕದ ದಿನಾಂಕ	ಪುಸ್ತಕದ ವಿವರ	ಪರಿಷತ್ (ಪರಿಷತ್)				ಒಟ್ಟು
							ಮಾಹಿತಿ	ಪರಿಷತ್	ಪರಿಷತ್	ಪರಿಷತ್	
1	2	3	4	5	6	7	8	9	10	11	12
	1) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ 00-14 2) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ 00-37 3) ಬಾಲಕರ ಸಂ/ ಬಾಲಕರ ಸಂ 00-33 4) ಕನ್ನಡ ಭಾಷಾ ಸಂ/ ಅರಿವು ಸಂ 0-35										
78	1) ಬಾಲಕರ ಸಂ/ ಬಾಲಕರ ಸಂ 00-37 2) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ 00-11 3) ಬಾಲಕರ ಸಂ/ ಬಾಲಕರ ಸಂ 01-03 4) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ 00-26 5) ಬಾಲಕರ ಸಂ/ ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 00-37 6) ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 00-14 7) ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 00-14 8) ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 0-16 9) ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 0-16 11 10) ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 0-16 11 11) ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ ಕೋಶದಲ್ಲಿ 0-16 11 12) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (00-05) 13) ಬಾಲಕರ ಸಂ/ ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ (00-05) 14) ಬಾಲಕರ ಸಂ/ ಅಲ್ಲಾ ಪಾಠ್ಯಕ್ರಮ 00-14 15) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ 00-25 16) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (00-08) 17) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (00-08) 18) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (00-08) 19) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (00-08)	ಸ್ತಂಭ	539/2	5-02 00-01(ಎ) 05-01		ಮಂತ್ರಿ	538	540	538	೮೦೦	
79	1) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ/ ಬಾಲಕರ ಸಂ 02-29 2) ಮಹಿಳಾ ಅರಿ ಸಂ/ ಮಹಿಳಾ ಸಂ 3) ಮಹಿಳಾ ಅರಿ ಸಂ/ ಮಹಿಳಾ ಸಂ 4) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ	ಸ್ತಂಭ	540/1,2	06-01 00-06(ಎ) 05-35	02-42 01-18	ಮಂತ್ರಿ	539	541	538	೮೦೦	
80	1) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ/ ಬಾಲಕರ ಸಂ (04-02) 2) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (07-08) 3) ಬಾಲಕರ ಸಂ/ ಮಹಿಳಾ ಸಂ (04-00)	ಸ್ತಂಭ	541/2	15-02 00-10(ಎ) 14-32	13-27	ಮಂತ್ರಿ	540	542	537	೮೦೦	

ಕ್ರ. ಸಂ.	ಪ್ರಾಜೆಕ್ಟ್ ಹೆಸರು	ಆರಂಭಿಸಿದ ತಾರೀಖು	ಒಳಸಂ.	ಸ್ವರೂಪಿಸಿದ ಉಪಸಂಖ್ಯೆ ೦-೧೦	ಉಪ ಸಂ-೨	ಮಾಹಿತಿ ಸಹಿ	ಸೇವೆ (ಸೇವೆಗಳು)				ಇತರೆ
							ಸಂಖ್ಯೆ	ಮೊತ್ತ	ವ್ಯಯ	ಸೇವೆ	
1	2	3	4	5	6	7	8	9	10	11	12
81	1) ಕೆ.ಎಂ.ಪುರ ತಂ/ಪುನರ್ನಿರ್ಮಾಣ 01-12	ಪೂರ್ಣ	542/1000 II ರ ಪದವಿ	11-01 0-01a 11-06	00-85 00-59 00-57	ಮಂತ್ರಿ	541	545	536	631	
	2) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಅಪ್ಪುಲಾಪುರ 01-27										
	3) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಅಪ್ಪುಲಾಪುರ 01-04										
	4) ಅಪ್ಪುಲಾಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ 01-02										
	5) ಪುನರ್ನಿರ್ಮಾಣ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ 01-15										
	6) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಅಪ್ಪುಲಾಪುರ ಕೋಶಕ್ಕೆ 01-15										
	7) ಪುನರ್ನಿರ್ಮಾಣ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ 01-03										
	8) ಅಪ್ಪುಲಾಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ (00-24)										
	9) ಮಾಣಿಕ್ಯಪುರ ತಂ/ಮಾಣಿಕ್ಯಪುರ (00-24)										
	10) ಮಾಣಿಕ್ಯಪುರ ತಂ/ಪುನರ್ನಿರ್ಮಾಣ 01-06										
	11) ಪುನರ್ನಿರ್ಮಾಣ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ 01-00										
	12) ಪುನರ್ನಿರ್ಮಾಣ ತಂ/ಪುನರ್ನಿರ್ಮಾಣ 00-28										
	13) ಅಪ್ಪುಲಾಪುರ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ 00-12										
	14) ಅಪ್ಪುಲಾಪುರ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ ಕೋಶಕ್ಕೆ 0-36										
	15) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ ಕೋಶಕ್ಕೆ 0-36										
82	1) ಕೆ.ಎಂ.ಪುರ ತಂ/ ಕೆ.ಎಂ.ಪುರ ತಂ (04-39)	ಪೂರ್ಣ	543	10-21 00-24(ಎ) 09-37	06-60	ಮಂತ್ರಿ	542	544	536	630	
	2) ಕೆ.ಎಂ.ಪುರ ತಂ/ ಕೆ.ಎಂ.ಪುರ ತಂ (04-38)										
83	ಅಪ್ಪುಲಾಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ ಅಪ್ಪುಲಾಪುರ	ಪೂರ್ಣ	544	07-36	08-36	ಮಂತ್ರಿ	543	550	545	629	
84	1) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ ಅಪ್ಪುಲಾಪುರ (02-05)	ಪೂರ್ಣ	545/೧೯	14-10 00-08(ಎ) 14-02	05-97	ಮಂತ್ರಿ	539	548	547	544	
	2) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ (04-00)										
	3) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ (04-03)										
	4) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ (04-02)										
85	ಪುನರ್ನಿರ್ಮಾಣ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ, ಕೆ.ಎಂ.ಪುರ	ಪೂರ್ಣ	546	04-26 00-03(ಎ) 04-23	04-28	ಮಂತ್ರಿ	535	547	೮೦೦	545	
86	1) ಪುನರ್ನಿರ್ಮಾಣ ತಂ/ ಪುನರ್ನಿರ್ಮಾಣ, ಕೆ.ಎಂ.ಪುರ 04-16	ಪೂರ್ಣ	547/12	09-06 00-01(ಎ) 19-05	03-74 12-80	ಮಂತ್ರಿ	535	547	೮೦೦	545	
	2) ಮಾಣಿಕ್ಯಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ ತಂ (06-14)										
	3) ಅಪ್ಪುಲಾಪುರ ತಂ/ ಮಾಣಿಕ್ಯಪುರ ತಂ (09-15)										

ಅ. ಸಂ.	ಸಂಪನ್ಮೂಲ ವಿವರ	ಅನುದಾನ ವಿವರ	ಒ.ಸಂ.	ಸುಪ್ರಸಂಗದ ವರ್ಷ	ಅನುದಾನ ಮೊತ್ತ	ಅನುದಾನದ ವಿವರ	ಸಂಪನ್ಮೂಲ (ಸಂಪನ್ಮೂಲ)				ಮೊ.
							ಮೊ.	ಸಂಪನ್ಮೂಲ	ಅನುದಾನ	ಒಟ್ಟು	
1	2	3	4	5	6	7	8	9	10	11	12
87	1) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 05-30 2) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 06-15 3) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 06-15	ಸ್ವಂತ	548/1.2	12-05	06-27 03-06	ಮಂಜೂ	545	549	547	544	
88	1) ಸಾಕಾಣಿಕೆ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 01-22 2) ಸಾಕಾಣಿಕೆ ಕೆ/ ಅನುದಾನ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 01-24 3) ಸಾಕಾಣಿಕೆ ಕೆ/ ಅನುದಾನ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 01-22 4) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ (00-19) 5) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ ಯಾವುದೇ ಅನುದಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ (01-01) 6) ಸಾಕಾಣಿಕೆ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 00-20 7) ಸಾಕಾಣಿಕೆ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 00-22 8) ಅನುದಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 9) ಬಜೆಟ್ ಸಹ ಕೆ/ ಬಜೆಟ್ ಸಹ } 00-20 10) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 01-24 11) ಬಜೆಟ್ ಸಹ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 03-00	ಸ್ವಂತ	549/1 ರಿಂದ 9 ರ ಪರಿಷ್ಕರಣೆ	12-14	01-57 01-61 01-57 01-52 00-51 00-56 00-51 01-61 03-02	ಮಂಜೂ	548	552	547	550	
89	1) ಸಾಕಾಣಿಕೆ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 2) ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 3) ಅನುದಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 4) ಸಾಕಾಣಿಕೆ ಕೆ/ ಬಜೆಟ್ ಸಹ } 08-04	ಸ್ವಂತ	550	08-04	08-19	ಮಂಜೂ	548	551	549	562	
90	1) ಸಾಕಾಣಿಕೆ ಕೆ/ ಅನುದಾನ 03-38 2) ಸಾಕಾಣಿಕೆ ಕೆ/ ಮಹಿಳಾ ಸಂವಿಧಾನ 04-08 3) ಅನುದಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 04-02 4) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ 04-02	ಸ್ವಂತ	551/1 ರಿಂದ 4 ರ ಪರಿಷ್ಕರಣೆ	16-10	04-43 04-70 04-57 04-54	ಮಂಜೂ	549	559	552	561	
90	08 ರಿಂದ 10/ ಬಜೆಟ್ ಸಹ	ಸ್ವಂತ	552	15-38	17-39	ಮಂಜೂ	547	553	540	551	
91	1) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ (03-35) 2) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ (03-35) 3) ಬಜೆಟ್ ಸಹ ಕೆ/ ಬಜೆಟ್ ಸಹ (02-00) 4) ಮಹಿಳಾ ಸಂವಿಧಾನ ಕೆ/ ಬಜೆಟ್ ಸಹ (02-00)	ಸ್ವಂತ	553/1.2	15-27	07-90 07-90	ಮಂಜೂ	552	54	540	559	

ಕ್ರ. ಸಂ.	ಸಾರಾಂಶ ವರ್ಗ	ಅನುಷ್ಠಾನದ ಸ್ಥಾನ	ಒ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಉಪಾಧಿ ವಿಧಾನ ಅ-ಸಂ	ಆರಂಭದ ದಿನ-ವೃ	ಅಂತಿಮದ ದಿನ	ಪರೀಕ್ಷೆ (ಘಂಟೆಗಳು)				ಮಾ
							ಪ್ರಾಥಮಿಕ	ಮಧ್ಯಮ	ಉನ್ನತ	ಒಟ್ಟು	
1	2	3	4	5	6	7	8	9	10	11	
	5) ಯಂತ್ರಣ ತಂ/ ಛಾತುಣ್ಣ ಗುಣ್ಣ ಶೈಕ್ಷಣಿ (02-00) 6) ಛಾತುಣ್ಣ ತಂ/ ಛಾತುಣ್ಣ ಗುಣ್ಣ (01-37)										
92	1) ಛಾತುಣ್ಣ ತಂ/ಛಾತುಣ್ಣ ಗುಣ್ಣ (02-28) 2) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ಶೈಕ್ಷಣಿ (02-32) 3) ಯಂತ್ರಣ ತಂ/ ಛಾತುಣ್ಣ ಶೈಕ್ಷಣಿ (01-30) 4) ಛಾತುಣ್ಣ ತಂ/ ಯಂತ್ರಣ ತಂ (07-32)	ಸ್ವಂತ	554/L2	17-02	10-08 08-51	ಮಾ	553	555	ಮಾ	558	ಸರ್ಕಾರಿ ಸರ್ಕಾರಿ ಸಂಸ್ಥೆಗಳಲ್ಲಿ ಒಳಗಡೆ ವಿಶ್ವವಿದ್ಯಾನಿಲಯಗಳಲ್ಲಿ 00-18 ಗುಣ್ಣ ಹಾಗೂ ಯಂತ್ರಣ ತಂ/ಛಾತುಣ್ಣ ಶೈಕ್ಷಣಿಗಳಲ್ಲಿ.
93	1) ಗುಣ್ಣ ತಂ/ ಯಂತ್ರಣ ತಂ (00-05) 2) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ (07-37) 3) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ (07-36)	ಸ್ವಂತ	555	15-38 00-05(ಎ) 15-33	17-39	ಮಾ	554	ಗುಣ್ಣ	ಮಾ	556	ಸರ್ಕಾರಿ ಸರ್ಕಾರಿ ಸಂಸ್ಥೆಗಳಲ್ಲಿ ಒಳಗಡೆ ವಿಶ್ವವಿದ್ಯಾನಿಲಯಗಳಲ್ಲಿ 1-20 ಎರಡು ಹಾಗೂ ಯಂತ್ರಣ ತಂ/ಛಾತುಣ್ಣ ಶೈಕ್ಷಣಿಗಳಲ್ಲಿ.
94	1) ಯಂತ್ರಣ 2) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } 10-39 3) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } 4) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } 03-37 5) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } 02-38 6) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } (02-12) 7) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } (02-12) 8) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } 02-16 9) ಯಂತ್ರಣ ತಂ/ ಯಂತ್ರಣ ತಂ } 02-30	ಸ್ವಂತ	556/ 1 ರಿಂದ 5 ರ ವರೆಗೆ	16-25	11-99 04-28 03-22 05-01 02-62 03-00	ಮಾ	557	ಗುಣ್ಣ	555	573	

ಕ್ರ. ಸಂ.	ಪರಿಷತ್ತಿನ ವಿವರ	ಅಧ್ಯಯನ ವರ್ಷ	ಒ.ಸಿ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಪಾಠ್ಯಕ್ರಮದ ಸಂಖ್ಯೆ	ಅಧ್ಯಯನದ ಸಂಖ್ಯೆ	ಅಧ್ಯಯನದ ವರ್ಷ	ವಿಷಯ (ಅಧ್ಯಯನ)				ಮಾ. ಸಂ.
							ಮೊದಲ	ಮಧ್ಯಮ	ಅಂತಿಮ	ಒಟ್ಟು	
1	2	3	4	5	6	7	8	9	10	11	12
95	1) ಹುಣಸೀದಿ ಗಂ/ ಪಾಠ್ಯಕ್ರಮ ಅಂಶ (1-20) 2) ಸಣ್ಣ ಕುಟುಂಬ ತಂ/ ಅಧ್ಯಯನ ಚೀಲದೊಡನೆ (1-12) 3) ಕೇವಲವೇದನಾ ತಂ/ ಪಾಠ್ಯಕ್ರಮ ಚೀಲದೊಡನೆ (0-20) 4) ಕೇವಲವೇದನಾ ತಂ/ ಪಾಠ್ಯಕ್ರಮ ಚೀಲದೊಡನೆ (02-24) 5) ಪಾಠ್ಯಕ್ರಮ ತಂ/ ವೇದವೇದನಾ (0-10) 6) ಶ್ರೀಮತಿ ಅಲಾಪನೆ ಗಂ/ ವಿಷಯವೇದನಾ ಚೀಲದೊಡನೆ (0-06) 7) ಕೇವಲ ಕುಟುಂಬ ತಂ/ ಪಾಠ್ಯಕ್ರಮ (01-22) 8) ಮೈಟಿಂಗ್‌ನಲ್ಲಿ ಹಾಜರಿ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ 9) ವಿದ್ಯಾರ್ಥಿಗಳ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ } (02-06) 10) ವಿದ್ಯಾರ್ಥಿಗಳ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ } 11) ವಿದ್ಯಾರ್ಥಿಗಳ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ (01-00) 12) ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಅಧ್ಯಯನ (03-02)	ಸ್ವಂತ	557/1 ರಿಂದ 10	14-02	01-02	ಮಾ.ಸಂ.	560	556	558	557	
96	1) ಸಜ್ಜಿದ ತಂ/ ಪಾಠ್ಯಕ್ರಮ ಕುಟುಂಬ (03-27) 2) ಸಾಧನ ತಂ/ ಪಾಠ್ಯಕ್ರಮ ಕುಟುಂಬ (03-26) 3) ಪಾಠ್ಯಕ್ರಮ ಹಾಜರಿ ತಂ/ ಪಾಠ್ಯಕ್ರಮ (03-26) 4) ಮೈಟಿಂಗ್ ಗಂ/ ಪಾಠ್ಯಕ್ರಮ ಚೀಲದೊಡನೆ (03-26)	ಸ್ವಂತ	558/1,2	14-25	08-21 08-18	ಮಾ.ಸಂ.	559	556	554	557	ಇದು ಸರ್ಕಾರದ ಅಧೀನದಲ್ಲಿರುವ 1-15 ಎಂಬ ವಿಷಯವನ್ನು ಈಗಾಗಲೇ ಸಂಪೂರ್ಣವಾಗಿ ಪರಿಶೀಲಿಸಲಾಗಿದೆ.
97	1) ಮಹಿಳಾಸಂಘ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ (03-05) 2) ಮಹಿಳಾಸಂಘ ಗಂ/ ಮಹಿಳಾಸಂಘ ವಿಷಯ (03-35) 3) ಪಾಠ್ಯಕ್ರಮವೇದನಾ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ 08-24	ಸ್ವಂತ	559/ಅ,ಆ	15-24	07-63 09-38	ಮಾ.ಸಂ.	551	558	563	560	
	1) ಮಹಿಳಾಸಂಘ ಹಾಜರಿ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ } 00-25 2) ಸಮೀಕ್ಷಣೆ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ } 3) ಅಧ್ಯಯನ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ } 4) ವಿದ್ಯಾರ್ಥಿಗಳ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ 0-11 5) ಪಾಠ್ಯಕ್ರಮವೇದನಾ ತಂ/ ಅಧ್ಯಯನ 01-24 6) ಪಾಠ್ಯಕ್ರಮವೇದನಾ ಗಂ/ ಪಾಠ್ಯಕ್ರಮ ಅಧ್ಯಯನ 01-24 7) ವಿದ್ಯಾರ್ಥಿಗಳ ತಂ/ ಪಾಠ್ಯಕ್ರಮವೇದನಾ } 03-28 8) ಪಾಠ್ಯಕ್ರಮವೇದನಾ ಗಂ/ ಕೇವಲ ವೇದನಾ 04-16	ಸ್ವಂತ	560/1 ರಿಂದ 6 ರ ವರೆಗೆ	19-12	00-95 01-68 03-81 04-62 04-93	ಮಾ.ಸಂ.	561	557	559	570	ಇದು ಸರ್ಕಾರದ ಅಧೀನದಲ್ಲಿರುವ 2-28 ಎಂಬ ವಿಷಯವನ್ನು ಈಗಾಗಲೇ ಸಂಪೂರ್ಣವಾಗಿ ಪರಿಶೀಲಿಸಲಾಗಿದೆ.

ಕ್ರ. ಸಂ.	ಇಂದಿವಾರ್ಥ ಪರಿಚ	ಇವೆ ದಾರಂ ಪರಿಚ	D.X.ಸಂ.	ಪ್ರಾರಂಭದ ತಾರೀಖು	ಅಂತ್ಯ ದಿನ	ಪಾಠ್ಯಕ್ರಮ (ಪುಸ್ತಕಗಳು)					ಪರಿಶೀಲನೆ
						ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	
1	2	3	4	5	6	7	8	9	10	11	12
98	9) ಆರಾಧನಾ ಗೀತೆ/ ಪಾಠ್ಯಕ್ರಮ ಪುಸ್ತಕ 04-28 10) ಆರಾಧನಾ ಗೀತೆ/ ಪಾಠ್ಯಕ್ರಮ ಪುಸ್ತಕ 04-00 1) ಸದ್ಗುಣಗಳ ತಂ/ ರೀತಿಯ ಪಾಠ್ಯಕ್ರಮ 08-03 2) ಸದ್ಗುಣಗಳ ತಂ/ ರೀತಿಯ ಪುಸ್ತಕ 00-08 3) ಆರಾಧನಾ ಪಾಠ್ಯಕ್ರಮ/ ಆರಾಧನಾ ಪುಸ್ತಕ 08-12	ಪೂರ್ಣ	561/2	16-25	08-25 00-12 08-32	ಪುಸ್ತಕ	562	560	551	565	ಪರಿಶೀಲನೆ
99	1) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (04-16) 2) ಸದ್ಗುಣಗಳ ಗೀತೆ/ ಪಾಠ್ಯಕ್ರಮ (03-30) 3) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ 4) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ 5) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (03-20)	ಪೂರ್ಣ	562/1,2,3	11-26 00-01(ಪ) 11-25	04-95 03-789 03-51	ಪುಸ್ತಕ	563	561	550	564	
100	1) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ 2) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (03-33) 3) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ 4) ಸದ್ಗುಣಗಳ ಗೀತೆ/ ಪಾಠ್ಯಕ್ರಮ (03-30) 5) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (03-13)	ಪೂರ್ಣ	563/1,2,3	10-16	04-18 03-55 03-61	ಪುಸ್ತಕ	629	562	550	554	
101	1) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (05-20) 2) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ 05-29	ಪೂರ್ಣ	564/1,2	11-09	06-25 06-00	ಪುಸ್ತಕ	628	565	563	619	
102	1) ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (6-31) 2) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (05-20) 3) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ 02-18	ಪೂರ್ಣ	565/1,2	14-29	13-75 02-75	ಪುಸ್ತಕ	564	566	561	567	ಪರಿಶೀಲನೆ ಪಾಠ್ಯಕ್ರಮ 03-33 ಗೀತೆ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ಪಾಠ್ಯಕ್ರಮ ಪಾಠ್ಯಕ್ರಮ ಪಾಠ್ಯಕ್ರಮ
103	1) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (05-06) 2) ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ ತಂ/ ಮಹಾದ್ ಪಾಠ್ಯಕ್ರಮ (05-33)	ಪೂರ್ಣ	566/1-570	8-38	11-99	ಪುಸ್ತಕ	565	520	561	567	ಪರಿಶೀಲನೆ ಪಾಠ್ಯಕ್ರಮ 03-33 ಗೀತೆ ಪಾಠ್ಯಕ್ರಮ 567 02-1-23 02-1-23

ಕ್ರ. ಸಂ.	ಪಾವತಿಸಿದ ಹೆಸರು	ಅಧಿಕಾರ ಪಡೆದ ಹೆಸರು	D.ಕ.ಸಂ.	ಸ್ವೀಕರಿಸಿದಂತಹ ಆಯಾ ವಿಭಾಗದ ಅಂಕ	ಆರಂಭ ದಿನ-ಶುಕ್ರ	ಮುಕ್ತಾಯ ದಿನ	ಅಂಕಗಳು (ಸಾಮಾನ್ಯ)				ಇತರ	
							ಪ್ರಾರಂಭ	ಪೂರ್ಣ	ಅಂತಿಮ	ಒಟ್ಟು		
1	2	3	4	5	6	7	8	9	10	11		
104	ಮೌಲಾಲಿ ತಂ/ ಪಾವತಿಸಿದವರು ಗೋದಾಂಜಲಿ 01-29	ಸ್ವಂತ	566/೮ 570		02-29	ಮುಕ್ತಿ						ಸು 568 ರಲ್ಲಿ 0-32 ರಂತೆ, ಅವಶ್ಯಕವಾಗಿ ಅದೇ ಅಂಕ ಪಡೆಯುವಂತೆ ಮಾಡಬಹುದು.
105	ಶಿವಮೊಗ್ಗಿನ ತಂ/ಮೆಚಿದಿ ಹಳಸ ಕೋಶಂಪಲ್ಲಿ 03-31	ಸ್ವಂತ	566/೮ 570		03-50	ಮುಕ್ತಿ						
106	1) ಶಿವಮೊಗ್ಗಿನ ಅರೆ ತಂ/ಶಿವಮೊಗ್ಗಿನ ಕೋಶಂಪಲ್ಲಿ 1-01 2) ಶಿವಮೊಗ್ಗಿನ ಅರೆ ತಂ/ಹಳಸವಾಡು ಕೋಶಂಪಲ್ಲಿ 4-19	ಸ್ವಂತ	566/8-570		05-79	ಮುಕ್ತಿ						
107	1) ಶಿವಮೊಗ್ಗಿನ ತಂ/ಗೋದಾಂಜಲಿ ಕುರುಕೂಲಾಚ್ಚಿ(04-38) 2) ಸಿಕ್ಕಿ ಕೋಶಂಪಲ್ಲಿ ತಂ/ ಮುಕ್ಕುಳುಕುಲು (00-28) 3) ಮುಕ್ಕುಳು ತಂ/ಅನ್ನಮುಕ್ಕುಳು ಕೋಶಂಪಲ್ಲಿ ಕುರುಕೂಲಾಚ್ಚಿ (08-35) 4) ಮೌಲಾಲಿ ಗಂ/ಗೋದಾಂಜಲಿ (03-27)	ಸ್ವಂತ	567/1,2	19-28	07-80 13-68	ಮುಕ್ತಿ	564	569	565	568		
108	1) ಸಾಂಪುಟ ತಂ/ ಹಳಸವಾಡು ಕೋಶಂಪಲ್ಲಿ (07-32) 2) ಅಮೀರಲಿ ತಂ/ಹಳಸವಾಡು ಕೋಶಂಪಲ್ಲಿ(07-32)	ಸ್ವಂತ	568/1,2	15-24 0-10(ಎ) 15-14	08-06 08-06	ಮುಕ್ತಿ ಮುಕ್ತಿ	619	569	567	617		
109	1) ಸಾಂಪುಟ ತಂ/ ಸರಸವಳ್ಳಿ ಕೋಶಂಪಲ್ಲಿ (07-29) 2) ಸರಸವಳ್ಳಿ ತಂ/ ಸರಸವಳ್ಳಿ ಕೋಶಂಪಲ್ಲಿ (08-00)	ಸ್ವಂತ	569	15-29 0-30(ಎ) 14-39	13-33	ಮುಕ್ತಿ	558	577	570	-		
110	1) ಶಿವಮೊಗ್ಗಿನ ಸುಬ ತಂ/ ಹಳಸವಾಡು 05-22 2) ಶಿವಮೊಗ್ಗಿನ ತಂ/ ಸಾಂಪುಟ ಕೋಶಂಪಲ್ಲಿ 04-06 3) ಶಿವಮೊಗ್ಗಿನ ತಂ/ ಅಮೀರಲಿ ಕೋಶಂಪಲ್ಲಿ 03-13	ಸ್ವಂತ	570/1,2,೩	13-01	6-05 03-63	ಮುಕ್ತಿ ಮುಕ್ತಿ	566	571	560	569		
111	1) ಸಾಂಪುಟ ಕೋಶಂಪಲ್ಲಿ ತಂ/ಅಮೀರಲಿ 01-26 2) ಸಾಂಪುಟ ತಂ/ ಹಳಸವಾಡು 01-24 3) ಸಿಕ್ಕಿ ತಂ/ ಹಳಸವಾಡು 00-20 4) ಅನ್ನಮುಕ್ಕುಳು ತಂ/ ಗೋದಾಂಜಲಿ ಕೋಶಂಪಲ್ಲಿ 02-03 5) ಸಾಂಪುಟ ತಂ/ ಹಳಸವಾಡು (02-15)	ಸ್ವಂತ	571/ 1 00೯ 6	10-23	01-80 01-75 00-55 02-26	ಮುಕ್ತಿ	570	573	572	577		



ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಕ್ರಮ ವಿವರ	ಪರಿಷ್ಕರಣೆ ಮಾಡಿದ ವರ್ಷ	ಒ.ಕ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಯುಜಿಸಿ ವಿಧಾನ ಅ-ಸಂ	ಆರಂಭ ದಿನ-ವೃ	ಏರ್ಪಡಿಸಿದ ವರ್ಷ	ಪಠ್ಯಕ್ರಮ (ಪುಸ್ತಕಗಳು)				ಪುಸ್ತಕ ಸಂಖ್ಯೆ
							ಪುಸ್ತಕ ಸಂಖ್ಯೆ	ಪುಸ್ತಕ ಸಂಖ್ಯೆ	ಪುಸ್ತಕ ಸಂಖ್ಯೆ	ಪುಸ್ತಕ ಸಂಖ್ಯೆ	
1	2	3	4	5	6	7	8	9	10	11	12
	6) ಅರಿವು-ಮನೋನಿರೀಕ್ಷಣೆ ತಂ/ಆಧುನಿಕತೆಗಳು 7) ಅನುಭವಾತ್ಮಕ ತಂ/ಆಧುನಿಕತೆಗಳು } 00-04 8) ನವ್ಯತೆ ಗ್ರಂಥ ಅಭಿವೃದ್ಧಿ ಹಾಗೂ ಕೊಡುಗೆಯನ್ನು 9) ಮನೋನಿರೀಕ್ಷಣೆ ಗ್ರಂಥ/ಸಂಪನ್ಮೂಲಗಳು } 02-00 10) ಮಕ್ಕಳ ಅರಿವು ತಂ/ ಮನೋನಿರೀಕ್ಷಣೆ 02-26 11) ಪಾಠ್ಯಕ್ರಮದ ತಂ/ಆಧುನಿಕತೆಗಳ ಕೊಡುಗೆಯನ್ನು 04-38 12) ನವ್ಯತೆ ತಂ/ ಮನೋನಿರೀಕ್ಷಣೆ 06-03										
114	1) ಭೂಮಿಶಾಸ್ತ್ರ ತಂ/ ಯಂತ್ರ ಸಾ/ ಸೈದ್ಧಾಂತಿಕ 05-28 2) ಭೂಮಿಶಾಸ್ತ್ರ ತಂ/ ಯಂತ್ರ ಸೈದ್ಧಾಂತಿಕ 02-33	ಸ್ವಂತ	574/1,2	08-21	05-07 02-52	ಮಾಹಿತಿ	573	ಶಿಕ್ಷಣದ ಗ್ರಂಥ	ಶಿಕ್ಷಣದ ಗ್ರಂಥ	575	
115	1) ಭೂಮಿಶಾಸ್ತ್ರ ತಂ/ ಯಂತ್ರ ಸೈದ್ಧಾಂತಿಕ (05-28) 2) ಭೂಮಿಶಾಸ್ತ್ರ ತಂ/ ಯಂತ್ರ ಸೈದ್ಧಾಂತಿಕ (08-37)	ಸ್ವಂತ	575/1,2	12-25 00-15(ಎ) 12-10	02-21 06-36	ಮಾಹಿತಿ	573	ಮಾಹಿತಿ ಯಂತ್ರ ಗ್ರಂಥದ ಗ್ರಂಥ	574	576	
116	ಸರಕಾರಿ ಸೈದ್ಧಾಂತ (20-19)	-	576	20-19 00-17(ಎ) 20-02	14-84	ಮಾಹಿತಿ	577	ಮಾಹಿತಿ ಯಂತ್ರ ಗ್ರಂಥದ ಗ್ರಂಥ	573	579	
117	1) ಅನುಭವಾತ್ಮಕ ಗ್ರಂಥ ಅರಿವು (03-29) 2) ಮನೋನಿರೀಕ್ಷಣೆ ತಂ/ ಅರಿವು (02-11) 3) ಅನುಭವಾತ್ಮಕ ತಂ/ ಗ್ರಂಥ 08-27	ಸ್ವಂತ	577/1,2	14-27	05-00 07-48	ಮಾಹಿತಿ	569	576	571	578	
118	1) ಅನುಭವ ತಂ/ ಸಾಮಾನ್ಯ ಮಾರ್ಗದರ್ಶಿ (03-04) 2) ಅನುಭವ ತಂ/ ಮನೋನಿರೀಕ್ಷಣೆ (06-06) 3) ಮಕ್ಕಳ ಶಿಕ್ಷಣದ ತಂ/ ಸೈದ್ಧಾಂತಿಕ ಬದಲಿ (03-03)	ಸ್ವಂತ	578	12-13 00-31(ಎ) 13-22	09-36	ಮಾಹಿತಿ	569	579	577	580	
119	ಅಭಿವೃದ್ಧಿ ತಂ/ ತಂತ್ರ	ಸ್ವಂತ	579 580-581- 582	42-27 04-19(ಎ) 38-08	28-06	ಮಾಹಿತಿ	578	580	576	580	
120	1) ಅರಿವು ತಂ/ ವಿಶ್ವವಿದ್ಯಾ ಪಾಠ್ಯಕ್ರಮ (04-19) 2) ವಿಶ್ವವಿದ್ಯಾ ತಂ/ ವಿಶ್ವವಿದ್ಯಾ (06-20) 3) ಮಕ್ಕಳ ಶಿಕ್ಷಣದ ತಂ/ ವಿಶ್ವವಿದ್ಯಾ (06-20)	ಸ್ವಂತ	583	17-19 0-09(ಎ) 17-30	17-43	ಮಾಹಿತಿ	584	ಮಾಹಿತಿ ಯಂತ್ರ ಗ್ರಂಥದ ಗ್ರಂಥ	582	591	

ಅ. ಸಂ.	ಪಾಠಶಾಲೆ ಹೆಸರು	ಅಧ್ಯಯನ ಕಾಲದ ಹೆಸರು	ಓ.ಸ.ನಂ.	ಸ್ಥಳೀಯವಿಷಯದ ಪಾಠಶಾಲೆಗಳಿಗೆ 0-100	ಅವಧಿ ದಿನ-ಸಂ.	ವಿಧಾನ ಸಭೆಯ ಸಂಖ್ಯೆ	ಒಟ್ಟು (ಸಂಖ್ಯೆ)				ಮಾ
							ಪ್ರತಿ	ಒಟ್ಟು	ಒಟ್ಟು	ಒಟ್ಟು	
1	2	3	4	5	6	7	8	9	10	11	
121	1) ರಂಗಪ್ಪ ತಂ/ ರಂಗಪ್ಪ ಪಾಠಶಾಲೆ (07-05) 2) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ರಂಗಪ್ಪ ಪಾಠಶಾಲೆ(7-06)	ಸ್ವಂತ	584	14-11 00-03(ಎ) 14-08	14-91	ಎಂ.ಸಿ.	590	583	ಎಂ.ಸಿ.	591	
122	1) ಬಸವಯ್ಯ ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ (07-10) 2) ಕೆ.ಎಸ್.ಎಂ. ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ (07-31)	ಸ್ವಂತ	585	15-21 01-04(ಎ) 14-17	12-00	ಎಂ.ಸಿ.	587	582	ಎಂ.ಸಿ.	588	
123	ಸಂಗಪ್ಪ ತಂ/ ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ	ಸ್ವಂತ	586	0-13	0-28	ಎಂ.ಸಿ.	587	582	ಎಂ.ಸಿ.	588	
124	1) ಸಂಗಪ್ಪ ತಂ/ ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ (02-20) 2) ಕೆ.ಎಸ್.ಎಂ. ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ (07-30)	ಸ್ವಂತ	587	10-10 0-29(ಎ) 09-21	07-43	ಎಂ.ಸಿ.	588	585	586	ಎಂ.ಸಿ.	
125	1) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ರಂಗಪ್ಪ / ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (12-00) 2) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಬಿ. ಕೆ.ಎಸ್.ಎಂ. (03-00) 3) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. (03-34)	ಸ್ವಂತ	588	18-34 0-34(ಎ) 18-00	14-04	ಎಂ.ಸಿ.	616	587	ಎಂ.ಸಿ.	588	
126	1) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (06-09) 2) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (06-09) 3) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (03-05) 4) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (03-04)	ಸ್ವಂತ	589	18-27 0-27(ಎ) 18-00	-	ಎಂ.ಸಿ.	614	590	ಎಂ.ಸಿ.	597	
127	1) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ (07-27) 2) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಸಂಗಪ್ಪ ಪಾಠಶಾಲೆ (07-28)	ಸ್ವಂತ	590	15-15	14-92	ಎಂ.ಸಿ.	589	584	ಎಂ.ಸಿ.	591	
128	1) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (06-10) 2) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (06-29) 3) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (03-15) 4) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (03-15)	ಸ್ವಂತ	591	20-08 0-04(ಎ) 20-04	20-21	ಎಂ.ಸಿ.	596	590	590	592	
129	1) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (11-33) 2) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (04-00) 3) ಕೆ.ಎಸ್.ಎಂ. ತಂ/ ಕೆ.ಎಸ್.ಎಂ. ಪಾಠಶಾಲೆ (04-00)	ಸ್ವಂತ	592, L2, 3	19-33 0-05(ಎ) 19-28	17-54	ಎಂ.ಸಿ.	596	590	591	593	

ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಪುಸ್ತಕ ವಿವರ	ಅಧ್ಯಯನ ಕಾಲ	ಒ.ಕೆ.ಸಂ.	ಸ್ವೀಕೃತವಿಷಯದ ಸಂಖ್ಯೆ	ಅಧ್ಯಯನ ಕಾಲ	ಪರಿಷರಣೆ	ಪಾಠ್ಯಪುಸ್ತಕ (ಪುಟಗಳು)				ಮಾ
							ಪುಟ	ಪುಟ	ಪುಟ	ಪುಟ	
1	2	3	4	5	6	7	8	9	10	11	-
130	1) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಸ್ವೀಕೃತವಿಷಯ ಕೊಡುವುದು (2-21)	ಸ್ವಂತ	593	15-07 0-03(ಪು) 15-02	13-40	ಪುಸ್ತಕ	594	758	592	758	
	2) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಸ್ವೀಕೃತವಿಷಯ ಕೊಡುವುದು (2-21)										
	3) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-21)										
	4) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಸ್ವೀಕೃತವಿಷಯ ಕೊಡುವುದು (2-21)										
	5) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-21)										
	6) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಸ್ವೀಕೃತವಿಷಯ ಕೊಡುವುದು (2-22)										
131	1) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-28)	ಸ್ವಂತ	594/1.2	16-08 0-15(ಪು) 15-33	15-36	ಪುಸ್ತಕ	595	593	596	758	
	2) ಸ್ವೀಕೃತವಿಷಯ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-28)										
	3) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-22)										
	4) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-22)										
	5) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಸ್ವೀಕೃತವಿಷಯ ಕೊಡುವುದು (2-28)										
	6) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (2-25)										
132	1) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಸ್ವೀಕೃತವಿಷಯ ಕೊಡುವುದು (07-21)	ಸ್ವಂತ	595/ಪು.ಆ	15-01	14-88	ಪುಸ್ತಕ	600	594	597	758	
	2) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (07-20)										
133	1) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (03-06)	ಸ್ವಂತ	596/1 ಪುಟ 6	18-14 0-15(ಪು) 17-39	16-91	ಪುಸ್ತಕ	597	591	589	594	
	2) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (02-20)										
	3) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (02-30)										
	4) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (02-10)										
	5) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (05-06)										
	6) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (05-06)										
	7) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (02-31)										
134	1) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (7-10)	ಸ್ವಂತ	597	20-30 0-29(ಪು) 19-21	8-18 8-52	ಪುಸ್ತಕ	598	596	589	595	
	2) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (3-00)										
	3) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (10-00)										
	4) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (10-00)										
135	1) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (07-04)	ಸ್ವಂತ	598	14-08	7-18 7-17	ಪುಸ್ತಕ	611	597	612	599	
	2) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (07-04)										
	3) ಪಾಠ್ಯಪುಸ್ತಕ ತಂ/ ಪಾಠ್ಯಪುಸ್ತಕ ಕೊಡುವುದು (07-04)										

ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಪುಸ್ತಕ ವಿವರ	ಆವೃತ್ತಿ	ಪುಸ್ತಕ ಸಂ. (1-3)	ಪುಸ್ತಕ ಸಂ. (4-6)	ಪುಸ್ತಕ ಸಂ. (7-9)	ಪುಸ್ತಕ ಸಂ. (10-12)	ಪುಸ್ತಕ (ಪುಸ್ತಕ)				ಮೊ.
							ಪುಸ್ತಕ	ಪುಸ್ತಕ	ಪುಸ್ತಕ	ಪುಸ್ತಕ	
136	1) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ (5-18) 2) ಹಣಕಾಸು ತಂ/ ಆಕರಣೆ (5-18) 3) ಹಣಕಾಸು ತಂ/ ಆಕರಣೆ (3-12) 4) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ (1-12) 5) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ (2-08)	ಪುಸ್ತಕ	599	13-08	11-87 4-15 1-42 2-40	ಮಿಕ್ಕಿ	605	597	598	600	
137	1) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ (04-34) 2) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 3) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 4) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 5) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (0-30) 6) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 7) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 8) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (01-27) 9) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (1-27) 10) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (02-20) 11) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 12) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 13) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ	ಪುಸ್ತಕ	600	19-32	20-59	ಮಿಕ್ಕಿ	601	595	599	ಗಿರಿ	
138	1) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 2) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 3) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 4) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (05-06)	ಪುಸ್ತಕ	601	10-11	10-80	ಮಿಕ್ಕಿ	602	600	599	ಗಿರಿ	
139	1) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (4-35) 2) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (2-30) 3) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (5-14) 4) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ (2-10) 5) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ 6) ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ	ಪುಸ್ತಕ	602	19-29	5-00 16-50	ಮಿಕ್ಕಿ	603	601	604	ಗಿರಿ	
140	ಹಣಕಾಸು ತಂ/ ಪರಿಷ್ಕರಣೆ ಕೋಶ	ಪುಸ್ತಕ	603	06-05 0-05(20) 06-00	5-34	ಮಿಕ್ಕಿ	657	602	607	ಗಿರಿ	

ಕ್ರ. ಸಂ.	ಸಾಹಿತ್ಯಕ ಕೃತಿ	ಅವಧಿ ವಾರ ಪುಟ	ಒ.ಪ.ಸಂ.	ಸ್ವೀಕೃತವಾಗಿದ ಕಾರಣ ಮೃತ್ತರ ೨-೨೦	ಅವಧಿ ದಿನ-ಶುಕ್ರ	ಪರಿಷದ್ ಪುಟ	ಅಧಿಕಾರ (ಅಧಿಕಾರಿ)				ಪುಟ
							ಮಂಡ	ಪ್ರಕಾಶ	ಅಧಿಕಾರ	ಪ್ರಕಾಶ	
1	2	3	4	5	6	7	8	9	10	11	
141	ಪಾಪವಿವೇಕ ಕಂ/ ಮಾರ್ಗದರ್ಶಿ ಬೋಧನೆ	ಪುಸ್ತಕ	604	9-26	08-54	ಪುಸ್ತಕ	603	601	605	602	
142	1) ಸ್ವಯಂಚರಿತ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು } 2-00 2) ಸ್ವಯಂಚರಿತ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು } 3) ಸ್ವಯಂಚರಿತ ಮಹಿಳಾ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (2-00) 4) ಸ್ವಯಂಚರಿತ ಅಪರಾಧವಿವೇಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (2-00) 5) ಸ್ವಯಂಚರಿತ ವಾಚನವಿವೇಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (2-00) 6) ಪಾಪವಿವೇಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (2-00) 7) ಸ್ವಯಂಚರಿತ ಅಪರಾಧ ವಿವೇಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (2-00) 8) ಸ್ವಯಂಚರಿತ ನಾಟಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (3-18) 9) ಅಪರಾಧ ವಿವೇಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (2-00)	ಪುಸ್ತಕ	605	17-18	18-33	ಪುಸ್ತಕ	607	599	606	604	
143	ಪಾಪವಿವೇಕ ಕಂ/ ಮಾರ್ಗದರ್ಶಿ ಕಾರ್ಯಗಳು	ಪುಸ್ತಕ	606	14-26	14-30	ಪುಸ್ತಕ	607	599	611	605	
144	1) ಸ್ವಯಂಚರಿತ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (08-22) 2) ಪಾಪವಿವೇಕ ನಾಟಕ ಕಂ/ ಸ್ವಯಂಚರಿತ ಅಧಿಕಾರಿಗಳು (08-22)	ಪುಸ್ತಕ	607	17-04 9-08(೪) 16-36	17-75	ಪುಸ್ತಕ	608	605	610	603	
145	ಪಾಪವಿವೇಕ ಕಂ/ ಸ್ವಯಂಚರಿತ	ಪುಸ್ತಕ	608	15-22 1-07(೨) 14-15	14-13	ಪುಸ್ತಕ	654	607	609	607	ಇದು ಸರ್ಕಾರಿ ಪುಸ್ತಕದ ಅಧಿಕಾರಿಗಳು 1-17 ಎಕೆ ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು
146	ಪಾಪವಿವೇಕ ಕಂ/ ಪಾಪವಿವೇಕ ಬೋಧನೆ	ಪುಸ್ತಕ	609	10-24	9-44	ಪುಸ್ತಕ	649	610	648	608	ಇದು ಸರ್ಕಾರಿ ಪುಸ್ತಕದ ಅಧಿಕಾರಿಗಳು 0-15 ಏಕೆ ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು ಅಧಿಕಾರಿಗಳು

ಅ. ಸಂ.	ಪಾಠ್ಯಕ್ರಮ ವಿವರ	ಅಧ್ಯಯನ ಕಾಲಾವಧಿ	ಒ.ಸ.ಸಂ.	ಪ್ರಯೋಗಗಳ ಸಂಖ್ಯೆ ಒ-ಸಂ	ಅವಧಿ ದಿನ-ರಾತ್ರಿ	ಅಧ್ಯಯನ ಪದ್ಧತಿ	ಛೇದನ (ಛೇದನ)				ಮಾ
							ಸಂಖ್ಯೆ	ಪ್ರಮಾಣ	ಅವಧಿ	ಮಾ	
1	2	3	4	5	6	7	8	9	10	11	
147	ಪಂಚರಸ ತಂ/ಸೋಲರೈ ಯು/ಪಿ ಸೋಲರೈ ತಂ/ ಸಿಕ್ಲೋರೈ	ಸ್ವಂತ	610	12-27 6-39(ಎ) 11-28	10-89	ಮಿಕ್ಕಿ	609	611	610	607	ಸಂಖ್ಯೆ ಛೇದನ ಒ.ಸಂ ಮಾಂಸ 0-39 ಸಂಖ್ಯೆ ಅಧ್ಯಯನ ಮಾಂಸ ಛೇದನ
148	1) ಭುವನಗಿ ತಂ/ ಸಾಬಣ್ಣ (06-00) 2) ಸೋಲರೈ ತಂ/ ಸಿಕ್ಲೋರೈ (06-00) 3) ಭುವನಗಿ ತಂ/ ಸೋಲರೈ (06-01)	ಸ್ವಂತ	611	18-02	17-51	ಮಿಕ್ಕಿ	610	612	615	606	ಸಂಖ್ಯೆ ಛೇದನ ಒ.ಸಂ ಮಾಂಸ 1-20 ಸಂಖ್ಯೆ ಅಧ್ಯಯನ ಮಾಂಸ ಛೇದನ
149	1)ಸಾಯಬಣ್ಣ ತಂ/ ಸಾಯಬಣ್ಣ ಕುರುಕುರು (05-05) 2)ಸಾಯಬಣ್ಣ ತಂ/ಸಾಯಬಣ್ಣ ಕಾವುಕುರುಕುರು (04-26)	ಸ್ವಂತ	612	09-31	0-09	ಮಿಕ್ಕಿ	611	613	615	698	ಸಂಖ್ಯೆ ಛೇದನ ಒ.ಸಂ ಮಾಂಸ 1-24 ಸಂಖ್ಯೆ ಅಧ್ಯಯನ ಮಾಂಸ ಛೇದನ
150	ಸಾಯಬಣ್ಣ ತಂ/ ಬಂಜೆ ಯು/ಪಿ ಬಂಜೆ ಸಾಯಬಣ್ಣ	ಸ್ವಂತ	613	10-02	11-26	ಮಿಕ್ಕಿ	612	597	614	598	ಸಂಖ್ಯೆ ಛೇದನ ಒ.ಸಂ ಮಾಂಸ 0-23 ಸಂಖ್ಯೆ ಅಧ್ಯಯನ ಮಾಂಸ ಛೇದನ

ಕ್ರ. ಸಂ.	ಸಂಕೇತದ ವಿವರ	ಅಧಿಕಾರ ಮಂಡನೆ	ಕ್ರ.ಸಂ.	ಸ್ವೀಕರಣದ ತಾರೀಖು	ಅವಧಿ	ಅಧಿಕಾರ ವಿಸ್ತಾರ	ಅಧಿಕಾರ (ಸಂಖ್ಯೆ)				ಮಾ.
							ಮಾ.	ಸಂಖ್ಯೆ	ಅಧಿಕಾರ	ಮಾ.	
1	2	3	4	5	6	7	8	9	10	11	
151	1) ಪಬ್ಲಿಕ್ ಅಂಡ್ ಪ್ರೈವೇಟ್ ಸಂಸ್ಥೆಗಳ ಅಧಿಕಾರ 2) ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ	ಸ್ವಂತ	614	08-01	08-12	ಪ್ರಾ.ಸಂ.	615	589	616	613	
152	ಪ್ರಾ.ಸಂ. ಸಂಸ್ಥೆಗಳ ಅಧಿಕಾರ	ಸ್ವಂತ	615	13-36 0-17(2) 13-19	12-54	ಪ್ರಾ.ಸಂ.	623	616	617	612	
153	ಸರ್ಕಾರ	-	616	16-23 0-20(2) 16-04	13-69	ಪ್ರಾ.ಸಂ.	615	588	617	614	ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ 1-36 ಎಂಬ ಸಂಖ್ಯೆಯಲ್ಲಿ ಪ್ರಾ.ಸಂ. ಸಂಸ್ಥೆಗಳಿಗೆ ವಿಸ್ತರಿಸಲಾಗಿದೆ.
154	ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ	ಸ್ವಂತ	617	15-27 02-07(2) 13-20	07-29	ಪ್ರಾ.ಸಂ.	623	688	619	615	ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ 0-30 ಎಂಬ ಸಂಖ್ಯೆಯಲ್ಲಿ ಪ್ರಾ.ಸಂ. ಸಂಸ್ಥೆಗಳಿಗೆ ವಿಸ್ತರಿಸಲಾಗಿದೆ.
155	ಸರ್ಕಾರ	-	618	6-22	-	ಪ್ರಾ.ಸಂ.	619	619	619	617	
156	1) ಅಧಿಕಾರ ವಿಸ್ತಾರ 2) ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ	ಸ್ವಂತ	619	15-34 0-34(2) 15-20	12-09	ಪ್ರಾ.ಸಂ.	620	568	564	618	ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ 1-00 ಎಂಬ ಸಂಖ್ಯೆಯಲ್ಲಿ ಪ್ರಾ.ಸಂ. ಸಂಸ್ಥೆಗಳಿಗೆ ವಿಸ್ತರಿಸಲಾಗಿದೆ.
157	1) ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ (00-22) 2) ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ (01-02) 3) ಸರ್ಕಾರದ ಅಧಿಕಾರಗಳ ಅಧಿಕಾರ (00-32)	ಸ್ವಂತ	621, 2, 3	02-16	2-03	ಪ್ರಾ.ಸಂ.	626	620	627	620	



ಕ್ರ. ಸಂ.	ಸಂಕೇತದ ವಿವರ	ಅಧಿಕಾರದ ವಿವರ	ಒ.ಸ.ಸಂ.	ಉದ್ಘಾಟನೆಯ ದಿನಾಂಕ	ಉದ್ದೇಶ	ಒಟ್ಟು ವೆಚ್ಚ	ಸಂಖ್ಯೆ (ಸಂಖ್ಯೆ)				ಮೊ.
							ಮೂಲ	ಪರಿಷ್ಕರಣೆ	ಉಪ	ಉಪ	
167	1) ಕೆಲಸ ಮಾಡಿದ ತಂ/ ಪರಿಷ್ಕರಣೆ (01-16)	ಪ್ರೌಢ	631	19-15 0-04(ಸಿ) 19-11	ಮಕ್ಕಳ	ಮೂ	630	542	632		
	2) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಅಭ್ಯಾಸದಾಯಕ (5-19)										
	3) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಅಭ್ಯಾಸದಾಯಕ (01-32)										
	4) ಅಭ್ಯಾಸದಾಯಕ ತಂ/ ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಕೊಡುಗೆ (01-18)										
	5) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (00-12)										
	6) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ 0-27										
	7) ಅಭ್ಯಾಸ ತಂ/ ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಪರಿಷ್ಕರಣೆ (00-12)										
	8) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಉಪ (00-12)										
	9) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಪರಿಷ್ಕರಣೆ (01-22)										
	10) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-04)										
	11) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-22)										
	12) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-11)										
	13) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-06)										
	14) ಪರಿಷ್ಕರಣೆ ತಂ/ ಅಭ್ಯಾಸದಾಯಕ (0-08)										
	15) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಅಭ್ಯಾಸದಾಯಕ (0-12)										
	16) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-04)										
	17) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-16)										
	18) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-08)										
	19) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-12)										
	20) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (1-02)										
	21) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-20)										
	22) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-12)										
	23) ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-16)										
	24) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-06)										
	25) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ (0-22)										
	168										1) ಅಭ್ಯಾಸದಾಯಕ ತಂ/ ಸಾಂಪ್ರದಾಯಿಕ ತಂ/ ಪರಿಷ್ಕರಣೆ 0-22
2) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ 0-24											
3) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ 0-16											
4) ಪರಿಷ್ಕರಣೆ ತಂ/ ಪರಿಷ್ಕರಣೆ 0-05											

ಅ. ಸಂ.	ಪಾಠ್ಯಪುಸ್ತಕ ಕೃತಿ	ಅಧ್ಯಯನ ಕಾಲದ ವರ್ಷ	ಒ.ಕೆ.ಸಿ.	ಸ್ವಯಂಸೇವಕ ಅಥವಾ ಪ್ರಾಚಾರ್ಯ ಅ-ಸಂ	ಅಧ್ಯಯನ ಕಾಲದ ದಿನ-ರಾತ್ರಿ	ಪರಿಶೀಲನೆ ಕಾಲದ	ಅಳವಡು (ಸಂಖ್ಯೆಗಳು)					ಮಾ
							ಮೇಲೆ	ಕೆಳಗೆ	ಅಧ್ಯಯನ	ಅಧ್ಯಯನ	ಅಧ್ಯಯನ	
1	2	3	4	5	6	7	8	9	10	11		
169	1) ಕೆಲವುಪುಸ್ತಕ ತಂ/ ಮೂಲಕವನ (01-02) 2) ಪಾಂಡುಪಾಠ ತಂ/ ಮುಖ್ಯ ಅಂ (01-02)	ಸ್ವಂತ	633	02-04 0-05(ಅ) 1-39	3-42	ಮಧ್ಯ	635	635	638	635		
170	1) ಕೆಲವುಪುಸ್ತಕ ತಂ/ ಮೂಲಕ ವನ (0-18) 2) ಪಾಂಡುಪಾಠ ತಂ/ ಮುಖ್ಯ ಅಂ (0-17)	ಸ್ವಂತ	634	0-15 0-03(ಅ) 0-32	01-18	ಮಧ್ಯ	635	620	626	620		
171	1) ಕೆಲವುಪುಸ್ತಕ ತಂ/ ಮೂಲಕ ವನ (04-25) 2) ಪಾಂಡುಪಾಠ ತಂ/ ಮುಖ್ಯ ಅಂ (04-25)	ಸ್ವಂತ	635	09-26 0-10(ಅ) 09-00	08-37	ಮಧ್ಯ	643	638	636	646		
172	1) ಕೆಲವುಪುಸ್ತಕ ತಂ/ ಮೂಲಕ ವನ (0-32) 2) ಪಾಂಡುಪಾಠ ತಂ/ ಮುಖ್ಯ ಅಂ (0-31)	ಸ್ವಂತ	636	01-23	02-57	ಮಧ್ಯ	637	635	630	635		
173	1) ಮೌಲ್ಯ ತಂ/ ಪುಸ್ತಕಗಳು } (0-26) 2) ಪಾಂಡುಪುಸ್ತಕ ತಂ/ ಪುಸ್ತಕಗಳು ಗೊಂದಲ 3) ಮೌಲ್ಯ ತಂ/ ಪುಸ್ತಕಗಳು ಗೊಂದಲದ (0-04) 4) ಪಾಂಡು ಪುಸ್ತಕ (0-05) 5) ಮೌಲ್ಯ ತಂ/ ಪುಸ್ತಕಗಳು ಗೊಂದಲದ (0-08) 6) ಕೆಲವು ಅಧ್ಯಯನ ಅಂ ತಂ/ ಪಾಂಡುಪುಸ್ತಕ (0-13)	ಸ್ವಂತ	637	1-36 0-04(ಅ) 01-12	0-36 0-07 0-02 0-13 0-20	ಮಧ್ಯ	638	637	630	643		
174	1) ಮೌಲ್ಯ ತಂ/ ಪುಸ್ತಕಗಳು ಗೊಂದಲದ 01-05 2) ಕೆಲವು ಅಧ್ಯಯನ ಅಂ ತಂ/ ಪಾಂಡುಪುಸ್ತಕ ಗೊಂದಲದ 0-18 3) ಪಾಂಡು ತಂ/ ಪಾಂಡುಪುಸ್ತಕ ಅಂ 01-20 4) ಪಾಂಡುಪುಸ್ತಕ ತಂ/ ಪಾಂಡುಪುಸ್ತಕ ಅಂ 01-08 5) ಪಾಂಡುಪುಸ್ತಕ ತಂ/ ಪಾಂಡುಪುಸ್ತಕ ಅಂ 02-17 6) ಮೌಲ್ಯ ತಂ/ ಪುಸ್ತಕಗಳು } 7) ಪಾಂಡುಪುಸ್ತಕ ತಂ/ ಪುಸ್ತಕಗಳು } 1-37	ಸ್ವಂತ	638	09-05	0-74 0-63 0-98 0-80 1-61 1-27	ಮಧ್ಯ	639	637	630	643		
175	1) ಸೂಚಕ ತಂ/ ರಂಗದ ಪಾಠ (01-13) 2) ಪಾಂಡು ತಂ/ ರಂಗದ ಪಾಠ (03-13) 3) ರಂಗದ ತಂ/ ಸೂಚಕ (03-12) 4) ಸೂಚಕ ತಂ/ ಪಾಂಡು ಪಾಠ (03-12) 5) ಪಾಂಡು ತಂ/ ರಂಗದ ಪಾಠ 1-33	ಸ್ವಂತ	639	17-03 0-04(ಅ) 16-39	5-39 5-15	ಮಧ್ಯ	-	638	630	643		

ಕ್ರ. ಸಂ.	ಸಾಮಗ್ರಿಯ ವಿವರ	ಅನುಮತಿಸಿದ ದಿನಾಂಕ	ಒ.ಎ.ಸಂ.	ಪ್ರಸ್ತಾವಿಸಿದ ಮೊತ್ತವನ್ನು ಒಟ್ಟಾರೆ ಎ-ರೂ	ಅಂದಾಜು ದಿನಾಂಕ	ಅನುಮತಿಸಿದ ದಿನಾಂಕ	ಮೊಂಡು (ಮೊಂಡು)				ಮೊ
							ಜುಲೈ	ಆಗಸ್ಟ್	ಸೆಪ್ಟೆಂಬರ್	ಅಕ್ಟೋಬರ್	
1	2	3	4	5	6	7	8	9	10	11	
176	ಸರಕು ಪರಿವೇಷಣೆ	-	640	0-10 0-10(ಎ) 0-00	-	ಮುಕ್ತಿ	-	643	639	641	
177	ಸಣ್ಣ ಪೇಪರಿಂಗ್ ಮತ್ತು ಪೇಪರಿಂಗ್	ಸ್ವಂತ	641	2-01 2-29	1-26	ಮುಕ್ತಿ	-	640	643	630	
178	ಸರಕು	-	642	0-05(ಎ) 2-24	1-23	ಮುಕ್ತಿ	641	643	643	643	
179	ಸರಕು	-	643	00-11(ಎ) 14-36	8-93	ಮುಕ್ತಿ	642	635	638	645	
180	1) ಪೇಪರಿಂಗ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ 4-16 2) ಪೇಪರಿಂಗ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ 4-06 3) ಪೇಪರಿಂಗ್ ಮತ್ತು ಪೇಪರಿಂಗ್ (04-16) 4) ಪೇಪರಿಂಗ್ ಮತ್ತು ಪೇಪರಿಂಗ್ (07-29)	ಸ್ವಂತ	644/ 12.3	20-31	4-80 4-52 12-79	ಮುಕ್ತಿ	673	645	643	678	
181	ಪೇಪರಿಂಗ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ	ಸ್ವಂತ	645	08-12 0-13(ಎ) 07-39	07-10	ಮುಕ್ತಿ	644	646	643	650	
182	ಪೇಪರಿಂಗ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ (13-38)	ಸ್ವಂತ	646	13-38 0-12(ಎ) 13-26	9-36	ಮುಕ್ತಿ	645	647	635	650	
183	ಪೇಪರಿಂಗ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ	ಸ್ವಂತ	647	07-04 0-27(ಎ) 6-17	3-99	ಮುಕ್ತಿ	646	648	ಮಾಂ	650/2	
184	ಪೇಪರಿಂಗ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ (16-14)	ಸ್ವಂತ	648	0-10(ಎ) 16-04	13-05	ಮುಕ್ತಿ	647	ಹೆಚ್	ಹೆಚ್	609	
185	ಎನ್.ಪಿ. ಪೇಪರಿಂಗ್ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ ಮತ್ತು ಎಕ್ಸಪೆಂಜ್ ರಚನಾತ್ಮಕ	ಸ್ವಂತ	649	09-09 0-08(ಎ) 09-01	05-96	ಮುಕ್ತಿ	651	609	650/2	ಹೆಚ್	

ಕ್ರ. ಸಂ.	ಪ್ರಾಜೆಕ್ಟ್ ನಾಮ	ಪ್ರಾ. ಉ. ಸಂ.	ಒ.ಸ.ಸಂ.	ಪ್ರಾರಂಭದ ಉಪಗ್ರಹ ದಿನಾಂಕ ೦-೧೦	ಉಪಗ್ರಹದ ದಿನಾಂಕ ೦-೧೦	ಉಪಗ್ರಹದ ವರ್ಷ	ಪ್ರಯೋಗ (ಕೆ.ಎಚ್.ಎಸ್.)				ಇತರೆ
							ಪ್ರಯೋಗ	ಪ್ರಯೋಗ	ಪ್ರಯೋಗ	ಪ್ರಯೋಗ	
1	2	3	4	5	6	7	8	9	10	11	
186	ಎನ್.ಪಿ. ನಾಗರಾಯ ಪಂ/ಎಚ್.ಆರ್. ಎನ್ ಪಾಠಶಾಲೆ	ಸ್ವಂತ	650/1	5-39 0-01(ಎ) 05-38	5-54	ಮಿಕ್ಕಿ	678	648	646	651	
187	ಗೈರಾ	-	650/2	10-17	4-90	ಮಿಕ್ಕಿ	678	648	646	651	
188	ನೀಲಗಿರಿ ಪಂ/ ನೀಲಗಿರಿ ಕೋಶ ಕುಟುಂಬ (04-33)	ಸ್ವಂತ	651/ 652/೮	38-27 0-02(ಬಿ) 38-25	04-50	ಮಿಕ್ಕಿ	677	649	650/1	652	ಪರಿಶಿಷ್ಟ ಜಾತಿಗಳ ಸಂರಕ್ಷಣೆ ಮತ್ತು ವಿಸ್ತರಣೆ ಕಾರ್ಯಕ್ರಮದಡಿ 0-68 ರೂರದ ಜನಜನನಕ್ಕೆ ಯಜ್ಞ ಪದ್ಧತಿ ಕಾರ್ಯಕ್ರಮದಡಿ 6.88ರೂರದ
189	ನಾಯಕಾಂಗು ಪಂ/ ಶಿವಪ್ಪ ಪಾಠಶಾಲೆ (04-33)	ಸ್ವಂತ	651/ 652/೮		04-50	ಮಿಕ್ಕಿ	677	649	650/1	652	
190	ಶರಣಮ್ಮ ಗಂ/ ಮಾದೇಪ್ಪ ಪಾಠಶಾಲೆ (03-34)	ಸ್ವಂತ	651/ 652/೮		04-50	ಮಿಕ್ಕಿ	677	649	650/1	652	
191	ಮಾಳವ್ವ ಪಂ/ ಮಾಳವ್ವ ಯಾಣಿ ಯಜ್ಞಮ್ಮ ಗಂ/ ಮಾಳವ್ವ ಪಾಠಶಾಲೆ (04-33)	ಸ್ವಂತ	651/ 652/೮		04-50	ಮಿಕ್ಕಿ	677	649	650/1	652	
192	ಮಲ್ಲಪ್ಪ ಪಂ/ ಪಾಠಶಾಲೆ (04-34)	ಸ್ವಂತ	651/ 652/೮		04-50	ಮಿಕ್ಕಿ	677	649	650/1	652	
193	ಬೆಂಗಳೂರು ಪಂ/ ರಾಮಪ್ಪ ಕವರಿ (03-13)	ಸ್ವಂತ	651/ 652/೮		03-39	ಮಿಕ್ಕಿ	677	649	650/1	652	
194	ಮಲ್ಲಪ್ಪ ಪಂ/ ಪಾಠಶಾಲೆ ಕಾರ್ಯಕ್ರಮ (03-05)	ಸ್ವಂತ	651/ 652/೮		03-00	ಮಿಕ್ಕಿ	677	649	650/1	652	
195	1) ಸುಬ್ಬಪ್ಪ ಪಂ/ ನರಸಪ್ಪ 2) ಸೋಮಪ್ಪ ಪಂ/ ನರಸಪ್ಪ 3) ಯಜ್ಞಪ್ಪ ಪಂ/ ನರಸಪ್ಪ	ಸ್ವಂತ	651/ 652/೮		06-39	ಮಿಕ್ಕಿ	677	649	650/1	652	(06-18)
196	ಭೀಮಪ್ಪ ಗಂ/ ನರಸಪ್ಪ ಪಾಠಶಾಲೆ (06-17)	ಸ್ವಂತ	651/ 652/೮		06-38	ಮಿಕ್ಕಿ	677	649	650/1	652	

೧. ಸಂ.	ಖಾತಾಂಶ ವಿವರ	ಅಂಚೆ ಸಾರ್ವಜನಿಕ ಸಂಖ್ಯೆ	೦.ಸಂ.	ಸುರಕ್ಷಿತವಾಗಿಟ್ಟುಕೊಳ್ಳುವ ಸಂಖ್ಯೆ	ಅಂಚೆ ದಿನ-ಶೈ	ಅಂಚೆ ಸಂಖ್ಯೆ	ಅಂಚೆ (ಸಂಖ್ಯೆ)				ಮಾ.
							ಸಂಖ್ಯೆ	ಸಂಖ್ಯೆ	ಸಂಖ್ಯೆ	ಸಂಖ್ಯೆ	
1	2	3	4	5	6	7	8	9	10	11	
197	ಸಂಯೋಜನೆ ತಂ/ ಕೆಲವು ವಿಭಾಗ (04-35) ನವದೆಹಲಿ ತಂ/ ಮಾರಾಟ ವಿಭಾಗ (03-14)	ಪ್ರಂತ	652		04-30 04-50	ಮಿಕ್ಕಿ	662	661	649	653	
198	1) ಬಲಾಚಲ ವಿಭಾಗ (12-27) 2) ಹಣಕಾಸು ತಂ/ ಸಾಂಸ್ಕೃತಿಕ ವಿಭಾಗ (01-07)	ಪ್ರಂತ	653/1	15-34 0-17(20) 15-17	14-57	ಮಿಕ್ಕಿ	661	660	652	654	ಕೆಲವು ಸರ್ಕಾರಿ ಸಂಸ್ಥೆಗಳಿಗೆ ಸಂಬಂಧಿಸಿದಂತೆ 2-25 ಎಂಬ ವಿಭಾಗವನ್ನು ಹೊಂದಿಸಿ ಕೊಡಲಾಗುತ್ತದೆ.
199	ಮಾರಾಟ ತಂ/ ಹಣಕಾಸು ವಿಭಾಗ (11-32)	ಪ್ರಂತ	654-655- 656-657/೮		09-07	ಮಿಕ್ಕಿ	654	653	648	655	
200	ಹಣಕಾಸು ತಂ/ ಮತ್ತಿತರ ವಿಭಾಗ (11-32)	ಪ್ರಂತ	654-655- 656-657/೮		09-06	ಮಿಕ್ಕಿ	654	653	648	655	
201	ಕುಟುಂಬ ತಂ/ ರಾಜಕೀಯ (04-28)	ಪ್ರಂತ	654-655- 656-657/೮		03-63	ಮಿಕ್ಕಿ	654	653	648	655	
202	ಶೇಖರಿಕರಣನಾಟಕ ತಂ/ ಸಾಂಸ್ಕೃತಿಕ (4-29)	ಪ್ರಂತ	654-655- 656-657/೮	47-08	03-63	ಮಿಕ್ಕಿ	654	653	648	655	
203 204	ಛಾತ್ರ ತಂ/ ಹಣಕಾಸು ವಿಭಾಗ (4-29)	ಪ್ರಂತ	654-655- 656-657/೮	00-06(20) 47-02	03-62	ಮಿಕ್ಕಿ	654	653	648	655	
204	1) ಹಣಕಾಸು ತಂ/ ಬಲಾಚಲ (04-29) 2) ಹಣಕಾಸು ತಂ/ ಬಲಾಚಲ	ಪ್ರಂತ	654-655- 656- 657/೮		03-62	ಮಿಕ್ಕಿ	654	653	648	655	
205	1) ರಾಮಚಂದ್ರ ತಂ/ ಬಲಾಚಲ (01-07) 2) ರಾಮಚಂದ್ರ ತಂ/ ಬಲಾಚಲ (01-08) 3) ಸಾಂಸ್ಕೃತಿಕ ವಿಭಾಗ (02-14)	ಪ್ರಂತ	654-655- 656-657/೮		00-62	ಮಿಕ್ಕಿ	654	653	648	655	
206	1) ಐತರ ಅಧಿಕಾರ ತಂ/ ಹಣಕಾಸು ವಿಭಾಗ (01-07) 2) ಅಧಿಕಾರ ತಂ/ ಹಣಕಾಸು ವಿಭಾಗ (03-07) 3) ಬಲಾಚಲ ತಂ/ ಮಾರಾಟ ವಿಭಾಗ (02-26)	ಪ್ರಂತ	658	14-29	11-11	ಮಿಕ್ಕಿ	668	667	659	658	

ಕ್ರ. ಸಂ.	ಪಾವತಿದಾರರ ವಿವರ	ಅಧಿಕಾರಿ ನಾಮ	ವ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಮೊತ್ತ By/for a-roc	ಅಂತ ದಾ-ತ್ಯ	ಮಾನ್ಯತೆ ಪಡೆ	ಅಂತರ (ರೂಪಾಯಿ)				ಮೊ.	
							ಮಾರ್ಚ್	ಏಪ್ರಿಲ್	ಮೇ	ಜೂನ್		
1	2	3	4	5	6	7	8	9	10	11		
	4) ಬೆಂಗಳೂರು ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (02-26) 5) ಬಾಬು ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (03-03)											
207	1) ಪಾವತಿದಾರ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (01-06) 2) ಪಾವತಿದಾರ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (04-00) 3) ಪರಿಶೋಧನೆ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (05-04)	ಪುಷ್ಪ	659	11-10	05-63	ಮಾನ್ಯ	668	656	660	658		
208	1) ಮಧ್ಯಮ ರೂ.ಮಾತ್ರದ ಪಾವತಿ (11-38) ಪೆ.ಎಂ.ಐ-00 2) ಸಾಬ್ಜಿ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (07-07)	ಪುಷ್ಪ	660	18-17	14-34	ಮಾನ್ಯ	663	655	661	659	ಇದು ಮೇ ಮಾನ್ಯತೆ ಲೇಖ ಮಾನ್ಯತೆ 1-37 ಎಫ್ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ	
209	ಶ್ರೀ. ಎ. ಪ್ರ. ನರಸಿಂಹಾಚಾರ್ ಕುಟುಂಬದವರು	ಪುಷ್ಪ	661	16-18 0-07(40) 16-17	17-75	ಮಾನ್ಯ	663	653	662	660	ಇದು ಮೇ ಮಾನ್ಯತೆ ಲೇಖ ಮಾನ್ಯತೆ 0-04 ರೂಪ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ	
210	ಶ್ರೀ. ಎ. ಪ್ರ. ನರಸಿಂಹಾಚಾರ್ ಕುಟುಂಬದವರು	ಪುಷ್ಪ	662	17-32	19-41	ಮಾನ್ಯ	663	653	662	660	ಇದು ಮೇ ಮಾನ್ಯತೆ ಲೇಖ ಮಾನ್ಯತೆ 0-18 ರೂಪ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ	
211	1) ಪಾವತಿದಾರ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ 2) ಬೆಂಗಳೂರು ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ 3) ಅಧಿಕಾರಿಗಳಿಂದ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ 4) ಅಧಿಕಾರಿ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ 5) ಬೆಂಗಳೂರು ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ 6) ಪಾವತಿದಾರ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ 7) ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್	ಪುಷ್ಪ	663	12-49	12-25	ಮಾನ್ಯ	672	661	661	668	ಇದು ಮೇ ಮಾನ್ಯತೆ ಲೇಖ ಮಾನ್ಯತೆ 0-18 ರೂಪ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ ಮಾನ್ಯತೆ	
212	1) ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (03-33) 2) ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (03-16) 3) ಪರಿಶೋಧನೆ ತೆರಿಗೆ/ ಮಲ್ಟಿಪಲ್ ಸಾಟಿ ಚೆಕ್ಸ್ (04-00)	ಪುಷ್ಪ	664	21-11	03-77 07-17 04-88 04-87	ಮಾನ್ಯ	665	658	663	670	ಇದು ಮೇ ಮಾನ್ಯತೆ ಲೇಖ ಮಾನ್ಯತೆ 1-08 ಎಫ್	



ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಕ್ರಮ ವಿವರ	ಅಧ್ಯಯನ ಕಾಲದ ವರ್ಷ	ಒ.ಸ.ಸಂ.	ಸ್ವಯಂಸೇವಕರ ಸಂಖ್ಯೆ ಒಟ್ಟು 0-100	ಅಧ್ಯಯನ ಕಾಲದ ದಿನ-ರಾತ್ರಿ	ಪಾಠ್ಯಕ್ರಮದ ವರ್ಷ	ಫಲಾನುಭವಿ (ಸಂಖ್ಯೆ)				ಮೊ.
							ಜನರ	ಪ್ರತಿಭೆ	ಅಭಿಮತ	ದೃಢ	
1	2	3	4	5	6	7	8	9	10	11	
218	ಬಸವಯ್ಯ ಗಂ/ ಶಿವಪ್ಪ ಅಗರ್ವಾ (03-04)	ಸ್ವಂತ	669/೮		03-46	ಮಿಕ್ಕಿ	670	663	671	662	
219	ಮಲ್ಲಪ್ಪ ತಂ/ ಅರವ್ವ (02-36)	ಸ್ವಂತ	669/೮	12-08	03-95	ಮಿಕ್ಕಿ	670	663	671	662	
220	1) ಮಂಜುನಿ ಗಂ/ ಬಸವಯ್ಯ (02-00) 2) ಪಾಪನಂದನ ಶಿವ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ (04-08)	ಸ್ವಂತ	669/೨		06-94		670	663	671	662	
221	ಸಣ್ಣಮಲ್ಲಪ್ಪ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ	ಸ್ವಂತ	670	18-26	19-59	ಮಿಕ್ಕಿ	೧೫	671	673	668	
222	1) ಕೆಮ್ಮಣ್ಣ ತಂ/ ಯಲ್ಲಪ್ಪ ಪಂಪನ (02-28) 2) ಮಲ್ಲಪ್ಪ ತಂ/ ಅರವ್ವ (01-17) 3) ಪಂಪನ ತಂ/ ಅರವ್ವ (01-17) 4) ನಾಗಪ್ಪ ತಂ/ ಮಲ್ಲಪ್ಪ (02-05) 5) ಶಿವಪ್ಪ ತಂ/ ಪಾಪನಂದನ (02-05) 6) ಬಲ್ಲಪ್ಪ ತಂ/ ಸಾಂಪುಣ್ಣ (02-06)	ಸ್ವಂತ	671	11-38	03-02 03-61 01-61 07-05	ಮಿಕ್ಕಿ ಮಿಕ್ಕಿ ಮಿಕ್ಕಿ ಮಿಕ್ಕಿ	670	672	673	669	
223	ಸಣ್ಣ ಪಂಪನ ತಂ/ ಯಲ್ಲಪ್ಪ ಅಗರ್ವಾ 01-01 ಕೆಮ್ಮಣ್ಣ ತಂ/ ಅರವ್ವ 01-14 ಪಂಪನ ತಂ/ ಅರವ್ವ 01-16 ಮಲ್ಲಪ್ಪ ತಂ/ ಬಲ್ಲಪ್ಪ ಅಗರ್ವಾ 06-08	ಸ್ವಂತ	672	11-39	03-39 01-52 01-57 06-94	ಮಿಕ್ಕಿ	671	663	673	669	
224	1) ಶೈಲವ್ವ ಪಂಪನ ತಂ/ ಪಾಪನಂದನ (09-22) 2) ಮಂಜುನಿ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ (09-22)	ಸ್ವಂತ	673	19-04 0-12(ಸ) 18-32	17-49	ಮಿಕ್ಕಿ ೧೫	662	674	672		
225	1) ಮಂಜುನಿ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 02-36 2) ಮಲ್ಲಪ್ಪ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 03-10 3) ಮಂಜುನಿ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 03-10 4) ಮಂಜುನಿ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 03-32	ಸ್ವಂತ	674	13-08	02-70 06-04 03-54	ಮಿಕ್ಕಿ ೧೫	676	675	673		
226	1) ಮಂಜುನಿ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 01-38 2) ಮಲ್ಲಪ್ಪ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 01-35 3) ಮಂಜುನಿ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ 05-17	ಸ್ವಂತ	675	09-15 0-02(ಸ) 09-13	03-31 04-61	ಮಿಕ್ಕಿ ೧೫	676	೧೫	674		
227	ಪಾಪನಂದನ ತಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ	ಸ್ವಂತ	676	11-13 0-24(ಸ) 10-29	11-70	ಮಿಕ್ಕಿ	675	677	668	679	
228	ಮಂಜುನಿ ಗಂ/ ಮಲ್ಲಪ್ಪ ಅಗರ್ವಾ	ಸ್ವಂತ	678	13-23	15-54	ಮಿಕ್ಕಿ	679	650/1	644	677	



ಅ. ಸಂ.	ಪರಿಷತ್ ವಿವರ	ಅಧ್ಯಯನ ಕಾಲ	-೦.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಪಾಠ್ಯಕ್ರಮ ೦-೧೦	ಪಾಠ್ಯಕ್ರಮ	ಪರಿಷತ್ ವರದ	ಉಪಯುಕ್ತ (ಪರಿಷತ್)				ಇತರ
							ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	ಪಾಠ್ಯಕ್ರಮ	
1	2	3	4	5	6	7	8	9	10	11	
238	ಪದಕಾಲಿ ಪಾಠ್ಯಕ್ರಮ	-	688	2-31 0-07(ಎ) 2-24	2-92	ಪುಸ್ತಕ	689	680	687	690	
239	ಪದಕಾಲಿ ಕೆ/ ಉಪಕಾಲಿ (1-14)	ಪುಸ್ತಕ	689	1-14 0-03(ಎ) 1-11	1-44	ಪುಸ್ತಕ	690	688	790	691	
240	ಪದಕಾಲಿ ಕೆ/ ಉಪಕಾಲಿ ಕೆ (1-14)	ಪುಸ್ತಕ	690	2-08 00-34(ಎ) 1-14	1-00	ಪುಸ್ತಕ	689	680	688	691	
241	ಪದಕಾಲಿ (12-01)	-	691	12-01 10-21	5-18	ಪುಸ್ತಕ	692	680	690	-	
242	1) ವಿಮಲಾಚಾರ್ಯ ಗಂ/ ಅನಾಚಾರ್ಯ (5-10) 2) ಸಂವಿಧಾನದ ಗಂ/ ಪರಿಷತ್ ವರದ (5-11)	ಪುಸ್ತಕ	692	1-08(ಎ) 9-13	7-28	ಪುಸ್ತಕ	695	691	690	693	
243	1) ಗೋಪಾಲ್ ಕೆ/ ಕೆ.ಎ.ಚಾರ್ಯ (1-13) 2) ಪದಕಾಲಿ ಗಂ/ ಉಪಕಾಲಿ ಪದಕಾಲಿ (5-12) 3) ಪದಕಾಲಿ ಗಂ/ ಉಪಕಾಲಿ ಪದಕಾಲಿ (5-13)	ಪುಸ್ತಕ	693/ಆ.ಆ.	11-38 0-03(ಎ) 11-35	1-28 9-27	ಪುಸ್ತಕ	694	691	692	ಪದಕಾಲಿ ಪದಕಾಲಿ	
244	ಪದಕಾಲಿ ಗಂ/ ಕೆ.ಎ.ಚಾರ್ಯ (7-29)	ಪುಸ್ತಕ	694	7-29	4-18	ಪುಸ್ತಕ	702/2	695/1	695	ಪದಕಾಲಿ ಪದಕಾಲಿ	
245	1) ಅಪ್ಪಾಜಿ ರಾಮಾನಂದ ಕೆ/ ಅಪ್ಪಾಜಿ ಪದಕಾಲಿ (5-34) 2) ಪದಕಾಲಿ ಪದಕಾಲಿ ಕೆ/ ಪದಕಾಲಿ ಅಪ್ಪಾಜಿ ರಾಮಾನಂದ (2-37) 3) ಪದಕಾಲಿ ಕೆ/ ಪದಕಾಲಿ ಪದಕಾಲಿ (5-34) 4) ಪದಕಾಲಿ ಪದಕಾಲಿ ಕೆ/ ಪದಕಾಲಿ ಅಪ್ಪಾಜಿ ರಾಮಾನಂದ(2-37)	ಪುಸ್ತಕ	695	17-22	18-43	ಪುಸ್ತಕ	702/1	692	696	694	
246	ಅರಿವಿನ ಕೆ/ ಅಪ್ಪಾಜಿ ಪದಕಾಲಿ (3-31)	ಪುಸ್ತಕ	696	3-31 0-16(ಎ) 3-15	4-06	ಪುಸ್ತಕ	702	692	-	695	
247	1) ಪದಕಾಲಿ ಪದಕಾಲಿ ಕೆ/ ಅಪ್ಪಾಜಿ ಗಂ 2) ಪದಕಾಲಿ ಅರಿ ಕೆ/ ಅರಿವಿನ 3) ಪದಕಾಲಿ ಕೆ/ ಅರಿವಿನ	11-33	697	11-33 0-11(ಎ) 11-22	12-13	ಪುಸ್ತಕ	700	695	698	702	

ಸ. ನಂ.	ಸಾಹಿತ್ಯದ ವಿಷಯ	ಅನುಬಂಧದ ಸಂಖ್ಯೆ	D.K.No.	ಪ್ರಕಟಣೆಯ ಸಂಖ್ಯೆ Dy. No. 2-10	ಪುಟ ಸಂಖ್ಯೆ	ಮುದ್ರಣ ಸಂಖ್ಯೆ	ಮೂಲ (ಅಂಕಗಳು)				ಮಾ.
							ಮೂಲ	ಪರಿಷ್ಕರಣೆ	ಅನುವಾದ	ಪರಿಷ್ಕರಣೆ	
1	2	3	4	5	6	7	8	9	10	11	
248	ಮಾತೃಕಾ ರೂಪಗಳ ಅರ ಕಂ/ ಮಾರ್ಕೆಟಿಂಗ್ ಗೋದಾನ್ (1-15)	ಸ್ವಂತ	698/1	1-15 0-13(ಸ) 1-02	0-66	ಮೂಲ	699	702	702	697	
249	1) ಸಾಹಿತ್ಯದ ಮೂಲ ಕಂ/ ಅನುವಾದ ಗ್ರಂಥ 2) ಮಾತೃಕಾ ಅರ ಕಂ/ ಅರಿಯಲು 3) ಕಾರ್ಯದ ಕಂ/ ಅರಿಯಲು	(02-29)	ಸ್ವಂತ	698/2	2-29	2-87	ಮೂಲ	699	702	702	697
250	ಪಂಚರತ್ನ (0-33)	-	699	0-33 0-33(ಸ) 00	1-00	ಮೂಲ	700	698	700	700	
251	ಪಾಪಾಹ ಗಂ/ ಮಹಿಮೆಯ ಗೋದಾನ್ (3-35)	ಸ್ವಂತ	700	3-35 1-21(ಸ) 2-34	1-27	ಮೂಲ	80	೮೦೦ ೮೦೦	-	701	
252	ಸರಣಿ	-	701	15-03 1-13(ಸ) 13-30	16-50	ಮೂಲ	741	702/1	700	704	
253	1) ಅಭಿಮಾನ ಕಂ/ ಅರಿಯಲು ಮೂಲ 2) ಅಭಿಮಾನ ಕಂ/ ಅರಿಯಲು ಮೂಲ (1-24) 3) ಅಭಿಮಾನ ಕಂ/ ಅಭಿಮಾನ (1-23) 4) ಅಭಿಮಾನ ಕಂ/ ಅಭಿಮಾನ (2-17) 5) ಅಭಿಮಾನ ಕಂ/ ಅಭಿಮಾನ (4-01)		ಸ್ವಂತ	702/1, 2, 3, 4	9-25 0-05(ಸ) 9-20	0-80	ಮೂಲ	701	695	697	703
254	1) ಸ್ವಯಂಪ್ರೀತ ಕಂ/ ಕರ್ತೃತ್ವ ಕೊಡು (6-18) 2) ಸ್ವಯಂಪ್ರೀತ ಕಂ/ ಕರ್ತೃತ್ವ ಕೊಡು (5-36)	ಸ್ವಂತ	702/2	12-14 0-37(ಸ) 11-17	10-63	ಮೂಲ	701	695	695	703	
255	1) ಸ್ವಯಂಪ್ರೀತ ಕಂ/ ಕರ್ತೃತ್ವ ಕೊಡು (10-05) 2) ಸ್ವಯಂಪ್ರೀತ ಕಂ/ ಕರ್ತೃತ್ವ ಕೊಡು (9-17)	ಸ್ವಂತ	703	19-22 0-19(ಸ) 19-03	21-27	ಮೂಲ	709	ಮೂಲದ ಹಕ್ಕು ಗೊ	702/2	ಮೂಲದ ಹಕ್ಕು ಗೊ	
256	1) ಸ್ವಯಂಪ್ರೀತ ಕಂ/ ಕರ್ತೃತ್ವ ಕೊಡು (11-23) 2) ಸ್ವಯಂಪ್ರೀತ ಕಂ/ ಕರ್ತೃತ್ವ ಕೊಡು (6-30)	ಸ್ವಂತ	704	18-13 1-25(ಸ) 16-28	13-13	ಮೂಲ	705	703	701	ಮೂಲದ ಹಕ್ಕು ಗೊ	

ಅ. ಸಂ.	ಸಾಹಿತ್ಯಕ ಕೆಲಸ	ಅಧ್ಯಯನ ಕಾಲದ ವರ್ಷ	ಒ.ಸ.ಸಂ.	ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನ ದಿನಗಳ ಸಂಖ್ಯೆ	ಅಧ್ಯಯನ ಕಾಲದ ದಿನ-ರಾತ್ರಿ	ಅಧ್ಯಯನ ಕಾಲದ ವರ್ಷ	ಪ್ರತಿಷ್ಠೆ (ಪರೀಕ್ಷೆ)				ನಿಜ
							ಜನವರಿ	ಫೆಬ್ರವರಿ	ಉತ್ತರ	ಫೆಬ್ರವರಿ	
1	2	3	4	5	6	7	8	9	10	11	
257	1) ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ ಕಂ/ ಅಧ್ಯಯನಗಳು (3-34) 2) ಕಾವ್ಯದ ಗಂ/ ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ (4-00)	ಸ್ವಂತ	705	7-39	3-69	ಮಾನ್ಯ	735	704	739	ಮಾನ್ಯ ಹಕ್ಕಿ ಗೊ	
258	1) ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು	ಸ್ವಂತ	706	3-12	2-35	ಮಾನ್ಯ	738	707	705	708	
259	ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (3-13)	ಸ್ವಂತ	707	3-33 0-20 (ಸಂ) 3-13	1-30	ಮಾನ್ಯ	706	704	705	ಮಾನ್ಯ ಹಕ್ಕಿ ಗೊ	
260	ಸ್ವೀಕೃತವಾದ ಮಾನ್ಯವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು	ಸ್ವಂತ	708	1-37	-	ಮಾನ್ಯ	733	707	706	709	
261	ಸ್ವೀಕೃತವಾದ ಮಾನ್ಯವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು	ಸ್ವಂತ	709	1-29	-	ಮಾನ್ಯ	733	707	708	710	
262	1) ಕಾವ್ಯದ ಗಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ (5-04) 2) ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (2-19) 3) ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (2-07)	ಸ್ವಂತ	710, 712, 3	10-00 0-13(ಸಂ) 9-27	5-40 3-01 2-00	ಮಾನ್ಯ	712	ಮಾನ್ಯ ಹಕ್ಕಿ ಗೊ	709	714	
263	ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (1-22)	ಸ್ವಂತ	711	1-22	2-36	ಮಾನ್ಯ	712	710	713	715	
264	ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (3-05)	ಸ್ವಂತ	712	3-05	1-50	ಮಾನ್ಯ	727	711	751	714	
265	ಕಾವ್ಯದ ಕವಿತೆಗಳ ಕಂ/ ಅಧ್ಯಯನಗಳು (2-06)	ಸ್ವಂತ	713	2-06 00-06(ಸಂ) 2-00	2-05	ಮಾನ್ಯ	714	ಮಾನ್ಯ ಹಕ್ಕಿ ಗೊ	710	714	
266	1) ಕಾವ್ಯದ ಗಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ (0-13) 2) ಕಾವ್ಯದ ಕವಿತೆಗಳ ಅಧ್ಯಯನಗಳು (0-12) 3) ಕಾವ್ಯದ ಗಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ (0-24) 4) ಕಾವ್ಯದ ಕಂ/ ಸವಿತೆಗಳ ಅಧ್ಯಯನಗಳು/ ಮಾನ್ಯವಾದ ಅಧ್ಯಯನಗಳು (1-01) 5) ಕಾವ್ಯದ ಕಂ/ ಸವಿತೆಗಳ ಅಧ್ಯಯನಗಳು/ ಮಾನ್ಯವಾದ ಅಧ್ಯಯನಗಳು (4-09) 6) ಕಾವ್ಯದ ಕಂ/ ಸವಿತೆಗಳ ಅಧ್ಯಯನಗಳು (03-06) 7) ಕಾವ್ಯದ ಗಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ 8) ಕಾವ್ಯದ ಕವಿತೆಗಳ ಕಂ/ ಸವಿತೆಗಳ ಅಧ್ಯಯನಗಳು 9) ಕಾವ್ಯದ ಗಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ (2-30) 10) ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ ಕಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ 11) ಸ್ವೀಕೃತವಾದ ಕವಿತೆಗಳ ಕಂ/ ಸವಿತೆಗಳ ಸಂಖ್ಯೆ 12) ಕಾವ್ಯದ ಗಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು/ ಮಾನ್ಯವಾದ ಅಧ್ಯಯನಗಳು (1-04) 13) ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (0-25) 14) ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನ ಕಂ/ ಸ್ವೀಕೃತವಾದ ಅಧ್ಯಯನಗಳು (0-26)	ಸ್ವಂತ	714/ 10 ರ ವರೆಗೆ	17-28 0-10(ಸಂ) 17-38	16-93	ಮಾನ್ಯ	724	ಮಾನ್ಯ ಹಕ್ಕಿ ಗೊ	710	714	

ಕ್ರ. ಸಂ.	ವಾಣಿಜ್ಯ ಕೆಲಸ	ಅನುಷ್ಠಾನ ವಾರದ ಪರಿಣ	ಒ.ಕೆ.ನಂ.	ಸ್ವೀಕೃತವಿಧಿಯುಳ್ಳ ಡ್ರಾಸ್ಟ್ ಅ-ಸಂ	ಊರದ ದಿನಾಂಕ	ಮಾಹಿತಿ ಕೆಲಸ	ಸೇವೆಗಳು (ಸೇವೆಗಳು)				ಮಾ
							ಸೇವೆ	ಪ್ರತಿಭ	ಉತ್ತರ	ಪ್ರತಿಭ	
1	2	3	4	5	6	7	8	9	10	11	
	15) ಸ್ಥಳೀಯ ಹಣಕಾಸು ತಂ/ ಸ್ಥಳೀಯ ಕಾರ್ಯ (0-26)	ಸ್ಥಳೀಯ									
	16) ಸ್ಥಳೀಯ ಮಹಿಳಾ ಹಣಕಾಸು ತಂ/ ಸ್ಥಳೀಯ ಕಾರ್ಯ (0-26)	ಸ್ಥಳೀಯ									
267	1) ಅಲ್ಪಾವಧಿ ಮಹಿಳಾ ತಂ/ ಅಲ್ಪಾವಧಿ ಗಣಿ ಪಾಠ (9-35) 2) ಅಲ್ಪಾವಧಿ ಮಹಿಳಾ ತಂ/ ಅಲ್ಪಾವಧಿ ಗಣಿ -ಎ (0-01) ಆ (3-34) 3) ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ ಪಾಠ. ಎ(6-00) 4) ಪಾಠದ ಮಹಿಳಾ ಹಣಕಾಸು ತಂ/ ಮಹಿಳಾ ಹಣಕಾಸು (3-00) 5) ಸ್ಥಳೀಯ ಮಹಿಳಾ ಹಣಕಾಸು ತಂ/ ಪಾಠ (4-16) 6) ಮಹಿಳಾ ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಮಹಿಳಾ ಅನ್ವೇಷಣೆ (3-00) 7) ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ ತಂ/ ಗಣಿಪಾಠ ಮಹಿಳಾ ಪಾಠ (4-07) 8) ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ ತಂ/ ಗಣಿಪಾಠ ಮಹಿಳಾ ಪಾಠ (6-07) 9) ಅಲ್ಪಾವಧಿ ಮಹಿಳಾ ತಂ/ ಅಲ್ಪಾವಧಿ ರೋಪಣಾ (11-24) 10) ಮಹಿಳಾ ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ ಪಾಠ (6-00) 11) ಪಾಠದ ಅಲ್ಪಾವಧಿ ಗಣಿ ತಂ/ ಪಾಠದ ಅಲ್ಪಾವಧಿ ಮಹಿಳಾ (6-00) 12) ಪಾಠದ ಮಹಿಳಾ ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ ತಂ/ ಗಣಿ ಮಹಿಳಾ (6-00) 13) ಅಲ್ಪಾವಧಿ ಮಹಿಳಾ ತಂ/ ಅಲ್ಪಾವಧಿ ಗಣಿ ಪಾಠ (3-35) 14) ಮಹಿಳಾ ಹಣಕಾಸು ತಂ/ ಮಹಿಳಾ ಉತ್ಪಾದಕ (3-00) 15) ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಮಹಿಳಾ ಹಣಕಾಸು (3-00) 16) ಅಲ್ಪಾವಧಿ ಮಹಿಳಾ ತಂ/ ಅಲ್ಪಾವಧಿ ಗಣಿ (3-34) 17) ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ (2-18) 18) ಮಹಿಳಾ ಸೇವೆಗೊಳಿಸಿದ ತಂ. ಮಹಿಳಾ ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ (6-00) 19) ಮಹಿಳಾ ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಅಲ್ಪಾವಧಿ ಗಣಿಪಾಠ ಪಾಠ (3-00) 20) ಮಹಿಳಾ ಸೇವೆಗೊಳಿಸಿದ ತಂ/ ಮಹಿಳಾ ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ (4-16) 21) ಮಹಿಳಾ ಹಣಕಾಸು ಅನ್ವೇಷಣೆಗೊಳಿಸಿದ (29-24)	ಸ್ಥಳೀಯ	715,715/ 716, 717, 718, 719	89-12	25-06 11-49 12-52, 22-89 22-80	ಮಹಿಳಾ	723	ಮಹಿಳಾ ಹಣಕಾಸು ಗಣಿ	724	ಮಹಿಳಾ ಹಣಕಾಸು ಗಣಿ	
			ಒಟ್ಟು	2735-28 67-37(ಎ) 2671-31							

ಕ್ರ. ಸಂ.	ಪಾಠ್ಯಪುಸ್ತಕದ ವಿಷಯ	ಉಪ-ವಿಷಯ	ಓ.ಸ.ಸಂ.	ಪ್ರಾರಂಭದ ದಿನಾಂಕ	ಅಂತಿಮ ದಿನಾಂಕ	ಮಾಂಸ ಕಾಲ	ಪಾಠ್ಯ (ಘಂಟೆಗಳು)				ಒಟ್ಟು
							ಪಾಠ್ಯ	ಪ್ರಾಯೋಗ	ಲಭ್ಯ	ಪ್ರತಿ	
1	2	3	4	5	6	7	8	9	10	11	12
	<b>ಬೆಳಿಗ್ಗೆ: ಯಾದಗಿರಿ</b>	<b>ಪಿ: ಯಾದಗಿರಿ</b>	<b>ಮೇಲಿನಿಂದ: ಸೈಬಾನ್</b>	<b>ಗ್ರಾಮ: ಬಾಡಿಯಾಳ</b>							
1.	1) ಹಣಕಾಸು ಸಂ. ಹಣಕಾಸು ಉಪಾಧಿ ಸಾಕು ಕೃಷಿ (5-34) 2) ಮಹಾದೇವನ ಸಂ. ನಾಗರ ಕೃಷಿ (6-34) 3) ಮಲ್ಲಪ್ಪ ಸಂ. ಮದ್ದು ಉಪಾಧಿ (5-31)	ಭೂಮಿ	35/ಅ,ಆ,ಇ	18-23 0-19(ಐ) 8-04	14-00	ಮಿಕ್ಕಿ	38	ಕೃಷಿ ಲಭ್ಯ	ಕೃಷಿ ಲಭ್ಯ	36	
2.	1) ಹಾಸನ ಸಂ. ಹಣಕಾಸು ಉಪಾಧಿ (2-39) 2) ಯಂತ್ರ ಸಂ. ರಾಮಣ್ಣ ಉಪಾಧಿ (2-00) 3) ಅಂಜನೇಯ ಸಂ. ಶಿವಪ್ಪ ಹಣಕಾಸು (4-39) 4) ಶಿವರಾಜ ಸಂ. ಯಂತ್ರ ಉಪಾಧಿ (9-39)	ಭೂಮಿ	36/ಅ, ಆ	19-37 0-06ಐ 19-31	20-27	ಮಿಕ್ಕಿ	37	ಕೃಷಿ ಲಭ್ಯ	35	48	
3.	1) ಸಿದ್ದಪ್ಪ ಸಂ. ಶಿವಪ್ಪ ಮಂತ್ರಿ (7-00) 2) ಕಂಠಪ್ಪ ಸಂ. ಹಣಕಾಸು ಮಂತ್ರಿ ಕೃಷಿ (7-10)	ಭೂಮಿ	37	14-10	22-23	ಮಿಕ್ಕಿ	39	36	38	47	
4.	1) ಚಂದ್ರಪ್ಪ ಸಂ/ ರಾಮಣ್ಣ (2-20) 2) ಹಣಕಾಸು ಸಂ/ ರಂಗಪ್ಪ } (1-08) 3) ಶಿವಪ್ಪ ಸಂ/ ರಂಗಪ್ಪ } 4) ನಾಗರ ಸಂ/ ಚಂದ್ರಪ್ಪ (1-08) 5) ನಾಗರ ಸಂ/ ಮಲ್ಲಪ್ಪ ಉಪಾಧಿ ಕೃಷಿ (1-08)	ಭೂಮಿ	38	7-12	5-00 2-00 2-00 2-00	ಮಿಕ್ಕಿ	39	35	ಕೃಷಿ ಲಭ್ಯ	37	
5.	1) ಹಣಕಾಸು ಸಂ. ನಾಗರ ಕೃಷಿ (3-00) 2) ಬಸವರಾಜ ಸಂ. ನಾಗರ ಕೃಷಿ (3-00) 3) ಮಹಾದೇವ ಸಂ. ಹಣಕಾಸು (3-00) 4) ಬಿ.ಎ. ಕರಗಪ್ಪ ಸಂ. ಹಣಕಾಸು ಬೆಂಗಳೂರು ಎಸ್.ಸಿ. (3-00)	ಭೂಮಿ	39/ಅ, ಆ	12-00	6-00	ಮಿಕ್ಕಿ	40	37	ಕೃಷಿ ಲಭ್ಯ	42	
6.	1) ಮಲ್ಲಪ್ಪ ಸಂ. ಮದ್ದು (6-00) 2) ಮಹಾದೇವನ ಸಂ. ಚಂದ್ರಪ್ಪ ಎಸ್.ಸಿ. (8-00)	ಭೂಮಿ	40	14-00 00-22 (ಐ) 13-28	22-47	ಮಿಕ್ಕಿ	42	39	ಕೃಷಿ ಲಭ್ಯ	46	

ಕ್ರ. ಸಂ.	ಸಾಹಿತ್ಯಕರ ಕೆಲಸ	ಅಧ್ಯಯನ ಮಾಡಿದ ವರ್ಷ	ಪುಸ್ತಕ ಸಂ. ಸಂ.	ಪ್ರಕಟಣೆಯಾಗಿದ ವರ್ಷ	ಅಧ್ಯಯನದ ದಿನ-ರಾತ್ರಿ	ನಿರೀಕ್ಷಿಸಿದ ಕೆಲಸ	ಅಧ್ಯಯನ (ಪರೀಕ್ಷೆ)				ಮಾ.
							ಕವನ	ನಾಟಕ	ಕಥೆ	ಲೇಖನ	
1	2	3	4	5	6	7	8	9	10	11	
7.	1) ಛೇದನಾಂಕ ಕಂ. ಕವಿತಾಂಕ (1-39) 2) ಬನ್ನಪ್ಪ ಕಂದಪ್ಪ (1-39) — 3) ಮಹಾದೇವಪ್ಪ ಕಂದಪ್ಪ (1-39) 4) ಛೇದನಾಂಕ ಕಂದಪ್ಪ (1-39) 5) ಸುನೀಲ ಕಂ. ಆಕಾಶ ಮಂತ್ರ (1-39) 6) ಅಂಜನಾಂಬಿಕೆ ಗಂ. ಪರೀಕ್ಷಾಂಕ ಮಂತ್ರ (1-39)	ಸ್ಥಳ	41	13-34 18-00 (ಸಂ) 10-34	22-25	ಮೆಟ್ರಿಕ್	ನಿರೀಕ್ಷಿಸಿದ ಸ್ಥಳೀಯ ಗಿರಿ	40	37	42	
8.	1) ಬನ್ನಪ್ಪ ಕಂ. ಕಂದಪ್ಪ (3-23) 2) ಛೇದನಾಂಕ ಕಂ. ಕಂದಪ್ಪ (3-23) 3) ಮಹಾದೇವಪ್ಪ ಕಂ. ಕಂದಪ್ಪ (3-23)	ಸ್ಥಳ	42	10-29	2017	ಮೆಟ್ರಿಕ್	ನಿರೀಕ್ಷಿಸಿದ ಸ್ಥಳೀಯ ಗಿರಿ	40	41	44	
9.	1) ಕವಿತಾಂಕ ಕಂ. ಬಾಲಪ್ಪ (3-32) 2) ಅಂಜನಾಂಬಿಕೆ ಕಂ. ಬಾಲಪ್ಪ (3-32) 3) ಛೇದನಾಂಕ ಕವಿತಾಂಕ ಕವಿತಾಂಕ ಕವಿತಾಂಕ (3-29) 4) ಕುಸುಮಪ್ಪ ಕಂ. ಬನ್ನಪ್ಪ ಗಿರಿಗೆ ಬಾಲಪ್ಪ (4-00)	ಸ್ಥಳ	43/44, 45	15-08	18-02 18-02	ಮೆಟ್ರಿಕ್	ನಿರೀಕ್ಷಿಸಿದ ಸ್ಥಳೀಯ ಗಿರಿ	45	42	58	
10.	ಕಂದಪ್ಪ ಕಂ. ಮಹಾದೇವಪ್ಪ ಅಂಗಡಿ	ಸ್ಥಳ	44	7-21	11-75	ಮೆಟ್ರಿಕ್	43	40	42	45	
11.	ಮಹಾದೇವ ಕಂ. ಮಲ್ಲಪ್ಪ ಸಾಧಾರ	ಸ್ಥಳ	45	10-30	20-21	ಮೆಟ್ರಿಕ್	43	46	44	57	
12.	1) ಕವಿತಾಂಕ ಕಂ. ಕವಿತಾಂಕ (3-08) 2) ಮಲ್ಲಪ್ಪ ಕಂ. ಕವಿತಾಂಕ (3-08) 3) ಸ್ವಲ್ಪ ಕವಿತಾಂಕ ಕವಿತಾಂಕ (3-09) 4) ಮಹಾದೇವ ಕಂ. ಕವಿತಾಂಕ (3-08)	ಸ್ಥಳ	46	12-33 00-17 (ಸಂ) 12-16	25-42	ಮೆಟ್ರಿಕ್	45	47	40	57	
13.	1) ಸ್ವಲ್ಪಕವಿತಾಂಕ ಕಂ. ಮಲ್ಲಪ್ಪ 2) ಕವಿತಾಂಕ ಕಂ. ಕವಿತಾಂಕ ಸಾಧಾರ (13-04)	ಸ್ಥಳ	47	13-04	21-49	ಮೆಟ್ರಿಕ್	46	48	37	52/1	
14.	1) ಸ್ವಲ್ಪ ಕವಿತಾಂಕ ಕಂ. ಮಲ್ಲಪ್ಪ ಸಾಧಾರ (3-11) 2) ಸ್ವಲ್ಪಕವಿತಾಂಕ ಕಂ. ಕವಿತಾಂಕ ಕವಿತಾಂಕ (3-16) 3) ಲಕ್ಷ್ಮಿ ಗಂ. ಸ್ವಲ್ಪಕವಿತಾಂಕ ಸಾಧಾರ (0-22)	ಸ್ಥಳ	48/49, 50, 51, 52	9-39 0-04(ಸಂ) 09-35	6-49 6-49	ಮೆಟ್ರಿಕ್	47	ರೇಷ್ಮೆ ರೇಷ್ಮೆ	36	ರೇಷ್ಮೆ ರೇಷ್ಮೆ	

ಕ್ರ. ಸಂ.	ಸಾರಾಂಶ ಪರಿಚಯ	ಛೇದನ ದಿನಾಂಕ	ಒ.ಪ.ಸಂ.	ಸ್ವಾಭಿಮಾನದ ಕಾರಣ ಪುಸ್ತಕ - ಸಂ.	ಅಧ್ಯಯನ ದಿನಾಂಕ	ವಿವರಣೆ ಪರಿಚಯ	ಸಮಯ (ಸಂಖ್ಯೆ)				ಒಟ್ಟು
							ಪೂರ್ವ	ಪಕ್ಕಿನ	ಅಂತರ	ಒಟ್ಟು	
1	2	3	4	5	6	7	8	9	10	11	12
	4) ಲಕ್ಷ್ಮಿ ಗಂ. ಸಣ್ಣಮದ್ದೆ ಸಾಧನ (0-22) 5) ಸಣ್ಣ ಮದ್ದೆ ತಂ. ಮಲ್ಲಯ್ಯ ಸಾಧನ (1-04) 6) ಲಕ್ಷ್ಮಿ ಗಂ. ಸಣ್ಣ ಮದ್ದೆ ಸಾಧನ (0-22) 7) ಲಕ್ಷ್ಮಿ ಗಂ. ಸಣ್ಣ ಮದ್ದೆ ಸಾಧನ (0-22)										
15)	1) ಮಹಾದೇವಪ್ಪ ತಂ. ನರಸಪ್ಪ ಗುಡಿಯಾಳ (04-20)	ಭೂತ	52/1	4-20 0-06 (ಸ) 4-14	9-62	ಮಿಕ್ಕಿ	53	ರಫ್ತು ಲ್ಪಿಸ	47	ರಫ್ತು ಲ್ಪಿಸ	
16)	ನಾಗಮ್ಮ ಗಂ. ತಿಪ್ಪಣ್ಣ ಗುಡಿಯಾಳ (00-34)	ಭೂತ	52/2	00-34 0-06 (ಸ) 0-28	1-55	ಮಿಕ್ಕಿ	53	ರಫ್ತು ಲ್ಪಿಸ	47	ರಫ್ತು ಲ್ಪಿಸ	
17)	1) ನರಸಪ್ಪ ತಂ. ಭೀಮಣ್ಣ (03-19) 2) ಮಹಾದೇವಪ್ಪ ತಂ. ಭೀಮಣ್ಣ (03-19) 3) ಮಲ್ಲಪ್ಪ ತಂ. ಭೀಮಣ್ಣಯ್ಯ ಗೋಳಾಳ (03-20)	ಭೂತ	53	10-18 00-17 (ಸ) 10-01	22-26	ಮಿಕ್ಕಿ	55	52	54	ರಫ್ತು ಲ್ಪಿಸ	
18)	ಪೂಜಾರಿ ತಂ. ತಿಪ್ಪಣ್ಣ ಮಗನೂರು (04-09)	ಭೂತ	54	4-09	7-95	ಮಿಕ್ಕಿ	46	47	47	53	
19)	1) ಕಿವ್ವ ತಂ. ಭೀಮಣ್ಣ ಕಾವರಿ (04-26)	ಭೂತ	55	4-26 00-05 (ಸ) 04-21	10-73	ಮಿಕ್ಕಿ	56	53	54	ರಫ್ತು ಲ್ಪಿಸ	
20)	1) ದೇವಪ್ಪ ತಂ. ಕಾಯಪ್ಪ ಗುಡಿಯಾಳ ( 04-11) 2) ಅಂಬಾನಾಯಕ ತಂ. ಕಾಯಪ್ಪ ಗುಡಿಯಾಳ	ಭೂತ	56	8-28 0-29 (ಸ) 7-39		ಮಿಕ್ಕಿ	57	55	46	65	
21)	1) ಭೀಮಣ್ಣಯ್ಯ ತಂ. ನಾಗಣ್ಣ (5-11) 2) ಗಂಗಪ್ಪ ತಂ. ಅಣ್ಣಣ್ಣ ಭೀಮಣ್ಣಯ್ಯ (5-11) 3) ದೇವಿಯಪ್ಪ ತಂ. ಪೂಜಾರಿ ಗುಡಿಯಾಳ (2-00)	ಭೂತ	57/58, 59, 60	12-22	11-90 11-90 05-95	ಮಿಕ್ಕಿ	58	56	45	60	

ಕ್ರ. ಸಂ.	ಸಾಹಿತ್ಯಕ ಕೃತಿ	ಅವಧಿ ಮುಕ್ತ ಕಾಲ	ಪುಸ್ತಕ ಸಂಖ್ಯೆ	ಪ್ರಕಟಣಕರ ಹೆಸರು	ಪುಸ್ತಕ ಪ್ರಕಟಿಸಿದ ವರ್ಷ	ಪುಸ್ತಕದ ವಿವರ (ಪುಟಗಳು)					ಪುಟ ಸಂಖ್ಯೆ
						ಮೊತ್ತ	ಪುಸ್ತಕದ ವಿವರ	ಪುಸ್ತಕದ ವಿವರ	ಪುಸ್ತಕದ ವಿವರ	ಪುಸ್ತಕದ ವಿವರ	
1	2	3	4	5	6	7	8	9	10	11	12
22	1) ಕುವೆಂಪು ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (06-13) 2) ದೇವೇಂದ್ರ ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (6-08) 3) ಕುವೆಂಪು ಪ. ಸಾಹಿತ್ಯ ಭವನದ ಶಿಷ್ಯರು (1-30) 4) ಕುವೆಂಪು ಪ. ಶಿಷ್ಯರು ಶಿಷ್ಯರು (1-30) 5) ಕುವೆಂಪು ಪ. ಶಿಷ್ಯರು 6) ಕುವೆಂಪು ಪ. ಶಿಷ್ಯರು 7) ಪಾಠಶಾಲೆ ಪ. ಶಿಷ್ಯರು 8) ಕುವೆಂಪು ಪ. ಶಿಷ್ಯರು	ಭೂತ	38/ಅ. 100 40 100/1	17-36	9-58 9-58 2-63 2-63	ಪುಸ್ತಕ ಕವಿತೆಗಳು ಕವಿತೆಗಳು		57	43	60	
23	1) ಲಕ್ಷ್ಮಣ ಕೆ. ಶಿಷ್ಯರು ಕುವೆಂಪು (08-21)	ಭೂತ	39	8-21	20-08	ಪುಸ್ತಕ ಕವಿತೆಗಳು		60	58	63	
24	1) ಭೀಮಕವಿ ಕೆ. ಲಕ್ಷ್ಮಣ ಅಂಗಡಿ (05-35) 2) ಲಕ್ಷ್ಮಣ ಕೆ. ಲಕ್ಷ್ಮಣ ಅಂಗಡಿ ( 02-37) 3) ಕುವೆಂಪು ಕೆ. ಲಕ್ಷ್ಮಣ (02-37)	ಭೂತ	60/ಅ. 4	11-29	14-43 14-42	ಪುಸ್ತಕ	59	61	58	62	
25	1) ದೇವೇಂದ್ರ ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (02-00) 2) ಕುವೆಂಪು ಗಂ. ಸಾಹಿತ್ಯ ಭವನದ ಶಿಷ್ಯರು (02-35) 3) ಕುವೆಂಪು ಗಂ. ಸಾಹಿತ್ಯ ಭವನದ ಶಿಷ್ಯರು ( 00-15) 4) ಭೀಮಕವಿ ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (02-27) 5) ಕುವೆಂಪು ಗಂ. ಸಾಹಿತ್ಯ ಭವನದ ಶಿಷ್ಯರು (00-30) 6) ಭೀಮಕವಿ ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (01-13) 7) ಕುವೆಂಪು ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (05-17)	ಭೂತ	61/ಅ. 4	16-37	20-06	ಪುಸ್ತಕ	60	56	57	65	
26	1) ಬರಹದ ವಿವರ ಕುವೆಂಪು 2) ಬರಹದ ವಿವರ ಕುವೆಂಪು 3) ಕುವೆಂಪು ಕುವೆಂಪು 4) ಕುವೆಂಪು ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (01-23) 5) ಕುವೆಂಪು ಕೆ. ಪಾಠಶಾಲೆ ಶಿಷ್ಯರು (01-22)	ಭೂತ	62	12-27	15-59 03-90 05-90 05-90	ಪುಸ್ತಕ	63	65	60	64	

ಕ್ರ. ಸಂ.	ಪರಿಷತ್ತಿನ ಹೆಸರು	ಅಧ್ಯಕ್ಷರ ಹೆಸರು	ಒ.ಸ.ನಂ.	ಪ್ರಾರಂಭಿಸಿದ ದಿನಾಂಕ	ಅಂತಿಮ ದಿನಾಂಕ	ನಿರೀಕ್ಷಿತ ಸಂಖ್ಯೆ	ಉಪವಿಭಾಗ (ಸದಸ್ಯರು)				ಮಾ
							ಸದಸ್ಯರು	ವಿಜ್ಞಾನ	ಲಲಿತ	ರಚನೆ	
1	2	3	4	5	6	7	8	9	10	11	
	6) ಕೃಷ್ಣಪ್ಪ ಕಾಕಿಂಬಾಳ ಕುಟುಂಬ (01-22) 7) ಸರಸ್ವತಿ ಸಂ. ಲಕ್ಷ್ಮಣ ಕುಟುಂಬ ( 01-22)										
27	ಕೆ. ಗಂಗಾಧರ ಪಂ. ಸೂರ್ಯ	ಸ್ಥಳ	63	12-38 3-09 (ಸ) 9-25	23-05	ಮಿಕ್ಕಿ	ಕಡತಿಸಿದ ರಚನೆಗಳಿಗಾಗಿ	62	59	64	
28	1) ದೊ. ಗಂಗಾಧರ ಪಂ. ಚನ್ನಪ್ಪ (04-00) 2) ಸೂರ್ಯ ಪಂ. ಸಾಯಬಳ್ಳಿ (07-00) 3) ಸಾಲಪ್ಪ ಸಂ. ಪುನೀತಪ್ಪ ರಾಮಣ್ಣ ಕೋಡ (4-00)	ಸ್ಥಳ	64	15-00 01-14 (ಸ) 13-26	-	ಮಿಕ್ಕಿ	ಕಡತಿಸಿದ ರಚನೆಗಳಿಗಾಗಿ	65	62	67	
29	1) ಪುನೀತಪ್ಪ ಪಂ. ಜಗದ್ಗು (06-07) 2) ಕುಟುಂಬ ಪಂ. ಭಾರತ್ ಕೋಡಂಕಿ (05-31)	ಸ್ಥಳ	65	12-15 00-24 (ಸ) 11-31	26-91	ಮಿಕ್ಕಿ	62	ರಚನೆ ಲಲಿತ	61	ರಚನೆ ಲಲಿತ	
30	ಲಕ್ಷ್ಮಣ ಸಂ. ಪಾಪನಾಥ ಕೋಡ (07-28)	ಸ್ಥಳ	66	01-28 0-06 (ಸ) 7-22	26-91	ಮಿಕ್ಕಿ	68	ರಚನೆ ಲಲಿತ	67	71	
31	ಲಕ್ಷ್ಮಣ ಸಂ. ಪಾಪನಾಥ ಕೋಡ (03-15)	ಸ್ಥಳ	67	03-25 00-28 (ಸ) 02-27	06-13	ಮಿಕ್ಕಿ	69	66	67	66	
32	ಭೀಮನಾಥ ಪಂ. ಸರಸ್ವತಿ ಕುಟುಂಬ (12-04)	ಸ್ಥಳ	68	12-04 00-34 (ಸ) 11-17	3-33	ಮಿಕ್ಕಿ	69	71	766	70	
33	ಪರಮೇಶ್ವರ ಸರಣಿ	-	69	06-22 06-22 (ಸ) 00-00		ಮಿಕ್ಕಿ	ಕಡತಿಸಿದ ರಚನೆ	68	64	70	
34	1) ಮೈಸೂರು ಪಂ. ವಿವೇಕಾನಂದ ಮುಖಾರಾಜ (03-23) 2) ಸರಸ್ವತಿ ಪಂ. ಕೋಡಂಕಿ ಕುಟುಂಬ (01-27)	ಸ್ಥಳ	70/ಎ	14-19	05-11 05-12	ಮಿಕ್ಕಿ	-ಕಡತಿಸಿದ-	71	69	75	

ಕ್ರ. ಸಂ.	ಮಾಹಿದಾರ ಪರಿಚಯ	ಪ್ರವೇಶ ದಿನಾಂಕ	ಓ.ಸ.ಸಂ.	ಉತ್ತರೀಕರಣ ಯೋಜನೆ ಪ್ರಾಯೋಗಿಕ ಸಂ.ಸಂ.	ಉತ್ತರೀಕರಣ ದಿನಾಂಕ	ಮಾಹಿದಾರ ಪರಿಚಯ	ನಿರೀಕ್ಷಿಸಿದ (ಪರಿಚಯ)				ಮಾಹಿದಾರ ಪರಿಚಯ
							ಮಾಹಿದಾರ ಪರಿಚಯ	ನಿರೀಕ್ಷಿಸಿದ	ಉತ್ತರೀಕರಣ	ನಿರೀಕ್ಷಿಸಿದ	
1	2	3	4	5	6	7	8	9	10	11	12
	3) ಗಿರೀಶ್ ಪಂ. ಭಾವುಕಾ ಕೆವಣ್ಣ (03-32) 4) ಗಿರೀಶ್ ಪಂ. ಭಾವುಕಾ ಕೆವಣ್ಣ (03-32)				05-12 03-84						
35	ಮಹಾದೇವಪ್ಪ ಪಂ. ಕಿವಣ್ಣ ಹಾಳವಾರ (15-00)	ಸ್ಥಳ	71	15-00 01-11 (ಸಂ) 13-29	14-56'	ಮಿಕ್ಕಿ	68	ರೇಷ್ಮೆ ಶೈಲಿ	66	27	
36	1) ಮಲ್ಲಪ್ಪ ಪಂ. ಸೋಣ್ಣ (09-14) 2) ಅರವಿಂದ್ ಪಂ. ಸಾಬ್ಬಾ 3) ಪ್ರಸಾದ್ ಪಂ. ಶರಣ್ಣ (01-07) 4) ಮಲ್ಲಪ್ಪ ಪಂ. ಸೋಣ್ಣ 5) ಮಲ್ಲಪ್ಪ ಪಂ. ಸೋಣ್ಣ ಮೋಯಾ (00-10) 6) ಮಲ್ಲಪ್ಪ ಪಂ. ನರಸಿಂಹ ಮೋಯಾ (02-00)	ಸ್ಥಳ	72	07-08 00-12 (ಸಂ) 6-36	2-44 02-44 02-44	ಮಿಕ್ಕಿ	74	ಶರಣ್ಣ ರಾ	71	73	
37	1) ಶರಣ್ಣ ಪಂ. ಮಹಾದೇವಪ್ಪ (02-31) 2) ಶರಣ್ಣ ಪಂ. ಮಹಾದೇವಪ್ಪ ಸೋಣ್ಣವಾರ (02-31)	ಸ್ಥಳ	73	05-22 0-13 (ಸಂ) 05-09	7-15	ಮಿಕ್ಕಿ	74	ಶರಣ್ಣ ರಾ	72	78	
38	1) ಮಲ್ಲಪ್ಪ ಪಂ. ಸೋಣ್ಣ ಮೋಯಾ (02-00) 2) ಸೋಣ್ಣ ಪಂ. ಶರಣ್ಣ (01-25) 3) ಸೋಣ್ಣ ಪಂ. ನರಸಿಂಹ 4) ಮಹಾದೇವಪ್ಪ ಪಂ. ಕಿವಣ್ಣ 5) ಅರವಿಂದ್ ಪಂ. ಸಾಬ್ಬಾ (02-00)	ಸ್ಥಳ	74	07-09	250 1-79 3-83	ಮಿಕ್ಕಿ	75	72	70	77	
39	1) ಬಸವ್ವ ಪಂ. ನರಸಿಂಹ ಹಾಳವಾರ (00-33) 2) ಮಹಾದೇವಪ್ಪ ಪಂ. ಕಿವಣ್ಣ ಸ್ವಾಮಿ (06-05) 3) ಸಾಬ್ಬಾ ಪಂ. ನರಸಿಂಹ ಹಾಳವಾರ (00-33) 4) ಶರಣ್ಣ ಪಂ. ನರಸಿಂಹ ಹಾಳವಾರ (05-09)	ಸ್ಥಳ	75	8-25	0-85 06-60 0-85 0-85	ಮಿಕ್ಕಿ	ಶರಣ್ಣ ಸ್ವಾಮಿ ರಾ	74	70	76	
40	1) ಶರಣ್ಣ ಪಂ. ಭಾವುಕಾ ಕೆವಣ್ಣ (05-09)	ಸ್ಥಳ	76	05-09	04-71	ಮಿಕ್ಕಿ	ಶರಣ್ಣ ಸ್ವಾಮಿ ರಾ	78	75	79	

ಖ. ಸಂ.	ಮಹಾಲಯ ವಿವರ	ಅಧಿಕಾರಿ ವಿವರ	ಓ.ಸ.ಸಂ.	ಸ್ಥಾನಾಧಿಕಾರಿ ಹುದ್ದೆ	ಉದ್ಯೋಗ ಸಂಖ್ಯೆ	ಉದ್ಯೋಗ ತರಬೇತಿ	ಪರೀಕ್ಷೆ (ಫಲಿತಾಂಶ)				ಇತರೆ
							ಪ್ರಶ್ನೆ	ಉತ್ತರ	ಉತ್ತರ	ಉತ್ತರ	
1	2	3	4	5	6	7	8	9	10	11	12
41	1) ಜಾಗೃತಿ ಗಂ. ಬನ್ನೇರು ಗುಡಿಯಲ್ಲಿದ್ದು (01-16) 2) ಜಾಗೃತಿ ಗಂ. ಬನ್ನೇರು ಗುಡಿಯಲ್ಲಿದ್ದು (01-15)	ಸ್ಥಳ	77/1	2-31	1-47 1-48	ಮಿಕ್ಕಿ	76	78	74	79	
42	1) ಯಜ್ಞ ಶಂ. ಮಲ್ಲೇಶ್ವರ ಹಿರಿಯ (02-31)	ಸ್ಥಳ	77/2	2-31	3-65	ಮಿಕ್ಕಿ	76	78	74	79	
43	1) ಕೃಷ್ಣ ಶಂ. ಮಹಾಲೇಶ್ವರ (00-36) 2) ಕೃಷ್ಣ ಶಂ. ಮಹಾಲೇಶ್ವರ (00-36) 3) ಬೇಂದ್ರೆ ಶಂ. ಮಹಾಲೇಶ್ವರ ಗುಡಿಯಲ್ಲಿದ್ದು (00-32) 4) ಮಹಾಲೇಶ್ವರ ಶಂ. ಪರಶುರಾಮ ಗುಡಿಯಲ್ಲಿದ್ದು (00-32)	ಸ್ಥಳ	78/1	03-09 00-04(ಸ) 03-05	2-49	ಮಿಕ್ಕಿ	77	ರದ್ದಾ ರದ್ದಾ	73	81	
44	1) ಕೃಷ್ಣ ಶಂ. ಮಹಾಲೇಶ್ವರ (00-29) 2) ಕೃಷ್ಣ ಶಂ. ಮಹಾಲೇಶ್ವರ (00-29) 3) ಬೇಂದ್ರೆ ಶಂ. ಮಹಾಲೇಶ್ವರ (1-8) 4) ಮಹಾಲೇಶ್ವರ ಶಂ. ಪರಶುರಾಮ (1-8) 5) ಗೌರಮ್ಮ ಗಂ/ ಪಿಕ್ಕಾಟ ಮಂಡಳಿ (1-18)	ಸ್ಥಳ	78/2	5-32	1-67 1-67 1-66	ಮಿಕ್ಕಿ	77	ರದ್ದಾ ರದ್ದಾ	73	81	
45	1) ಕೃಷ್ಣ ಶಂ/ ಮಲ್ಲೇಶ್ವರ ಬೇಂದ್ರೆ (1-33) 2) ಕೇರಮ್ಮ ಗಂ/ ಕೃಷ್ಣ ಶಂ. ಮಹಾಲೇಶ್ವರ (1-36) 3) ಕೇರಮ್ಮ ಗಂ/ ಕೃಷ್ಣ ಶಂ. ಮಹಾಲೇಶ್ವರ (1-36)	ಸ್ಥಳ	79	7-25	4-39	ಮಿಕ್ಕಿ	ಬೇಂದ್ರೆಯ ಗ್ರಾಮದ ಗಣ	77	76	89	
46	1) ಅಂಬಾಳಿಯ ಶಂ. ನರಸಿಂಹ ಮಲ್ಲೇಶ್ವರ (2-03) 2) ಅಂಬಾಳಿಯ ಶಂ. ನರಸಿಂಹ (2-00)	ಸ್ಥಳ	80/1	4-03	7-35	ಮಿಕ್ಕಿ	ಬೇಂದ್ರೆಯ ಗ್ರಾಮದ ಗಣ	81	82	79	
47	1) ಮಹಾಲೇಶ್ವರ ಶಂ. ಮಲ್ಲೇಶ್ವರ (1-13) 2) ಬೇಂದ್ರೆ ಶಂ/ ಮಲ್ಲೇಶ್ವರ (1-13)	ಸ್ಥಳ	80/2	2-26	3-48	ಮಿಕ್ಕಿ	ಬೇಂದ್ರೆಯ ಗ್ರಾಮದ ಗಣ	81	82	79	
48	1) ನರಸಿಂಹ ಶಂ/ ಅಂಬಾಳಿಯ (1-21) 2) ಅಂಬಾಳಿಯ ಶಂ/ ಕೃಷ್ಣ ಶಂ } (1-21) 3) ಕೃಷ್ಣ ಶಂ/ ಬೇಂದ್ರೆ } 4) ಮಹಾಲೇಶ್ವರ ಶಂ/ ಮಲ್ಲೇಶ್ವರ ಮೂಲ (1-20)	ಸ್ಥಳ	81	4-21 0-07(ಸ) 4-14	1-54 1-54 1-54	ಮಿಕ್ಕಿ	80	ರದ್ದಾ ರದ್ದಾ	78	82	

ಕ್ರ. ಸಂ.	ಭಾವೋದ್ವೇಗ ಪಾಠ	ಅನುಭವ ಮಂದ ಪಾಠ	ಒ.ಕ.ಸಂ.	ಸ್ಮಾರಣಾಂಶ ಸಂಖ್ಯೆ Days 2-6	ಅಂಶ ದಿನ-ಶೈ	ಮನೋಭಾವ	ಪರಿಷದ್ (ಬೆಂಗಳೂರು)				ಮಾ.
							ಪಾಠ	ಪಠ್ಯ	ಅಂಶ	ದಿನ	
1	2	3	4	5	6	7	8	9	10	11	
49	1) ಲಕ್ಷ್ಮಣ ತಂ/ ಸುಬ್ರಹ್ಮಣ್ಯ 2) ಮಲ್ಲಪ್ಪ ತಂ/ ಸುಬ್ರಹ್ಮಣ್ಯ ಉಲ್ಲೇಖಗಳು } (7-11)	ಸ್ವತಃ	82	7-11 0-04(ಅ) 7-07	11-70	ಮಿಕ್ಕಿ	ಕರ್ನಾಟಕ ಗ್ರಾಮದ ಗಣ	ರತ್ನ ಲಕ್ಷ್ಮಿ	80/2	83	
50	1) ಬೊ. ಲಕ್ಷ್ಮಣ ತಂ. ರಾಮಣ್ಣ (2-17) 2) ಸ. ಲಕ್ಷ್ಮಣ ತಂ. ರಾಮಣ್ಣ (2-17) 3) ಮಹಾದೇವಪ್ಪ ತಂ. ಲಕ್ಷ್ಮಣ (4-36) 4) ಸದಸಪ್ಪ ತಂ. ಪ್ರಭುರಾಯ (4-36)	ಸ್ವತಃ	83	14-24 00-12(ಅ) 14-12	6-62 6-64	ಮಿಕ್ಕಿ	ಕರ್ನಾಟಕ ಗ್ರಾಮದ ಗಣ	ರತ್ನ ಲಕ್ಷ್ಮಿ	82	84	
51	1) ಮೌಲ್ಯವಿದಿ ಗಂ. ಮಲ್ಲದೇವ ಪಂಚರ (3-14) 2) ಮಹಿಪಾಲಯಲಿ ಗಂ. ರಾಮಣ್ಣ (3-15) 3) ಮಹಾ ಮನೋಪ ತಂ. ಮಲ್ಲದ ಸುಬ್ರಹ್ಮಣ್ಯ (6-00)	ಸ್ವತಃ	84	12-29 00-06(ಅ) 12-13	8-85 8-00	ಮಿಕ್ಕಿ	ಕರ್ನಾಟಕ ಗ್ರಾಮದ ಗಣ	ರತ್ನ ಲಕ್ಷ್ಮಿ	83	85	
52	1) ಕಿವಣ್ಣಪ್ಪ ಗಂ. ಮಹಾದೇವಪ್ಪ 2) ಬಸರೀರಮ್ಮ ಗಂ. ರಾಮಣ್ಣಪ್ಪ } (1-12) 3) ಪಾಣಜಿ ತಂ. ತಿಪ್ಪಣ್ಣ 4) ಲಕ್ಷ್ಮಮ್ಮ ಗಂ ತಿಪ್ಪಣ್ಣ ತೋರಿ (1-12) 5) ಮರೆಯೆ ಗಂ. ಸಾಗಪ್ಪ ಕೇಸರಿ (00-26) 6) ಮರೆಯೆ ಗಂ. ಸಾಗಪ್ಪ ಕೇಸರಿ (00-26) 7) ತಿಪ್ಪಣ್ಣ ತಂ. ಶಿವಪ್ಪ ಸಿಟ್ಟಣ್ಣ (00-29)	ಸ್ವತಃ	85/1 85/1/1 85/2 85/3	3-21	1-71 1-22	ಮಿಕ್ಕಿ	ಕರ್ನಾಟಕ ಗ್ರಾಮದ ಗಣ	ರತ್ನ ಲಕ್ಷ್ಮಿ	84	ಮಾಂಥ	
			ಒಟ್ಟು	496-34 20-27 (ಅ) 476-07							

## ಫೆರೋಷ್ವಾರ

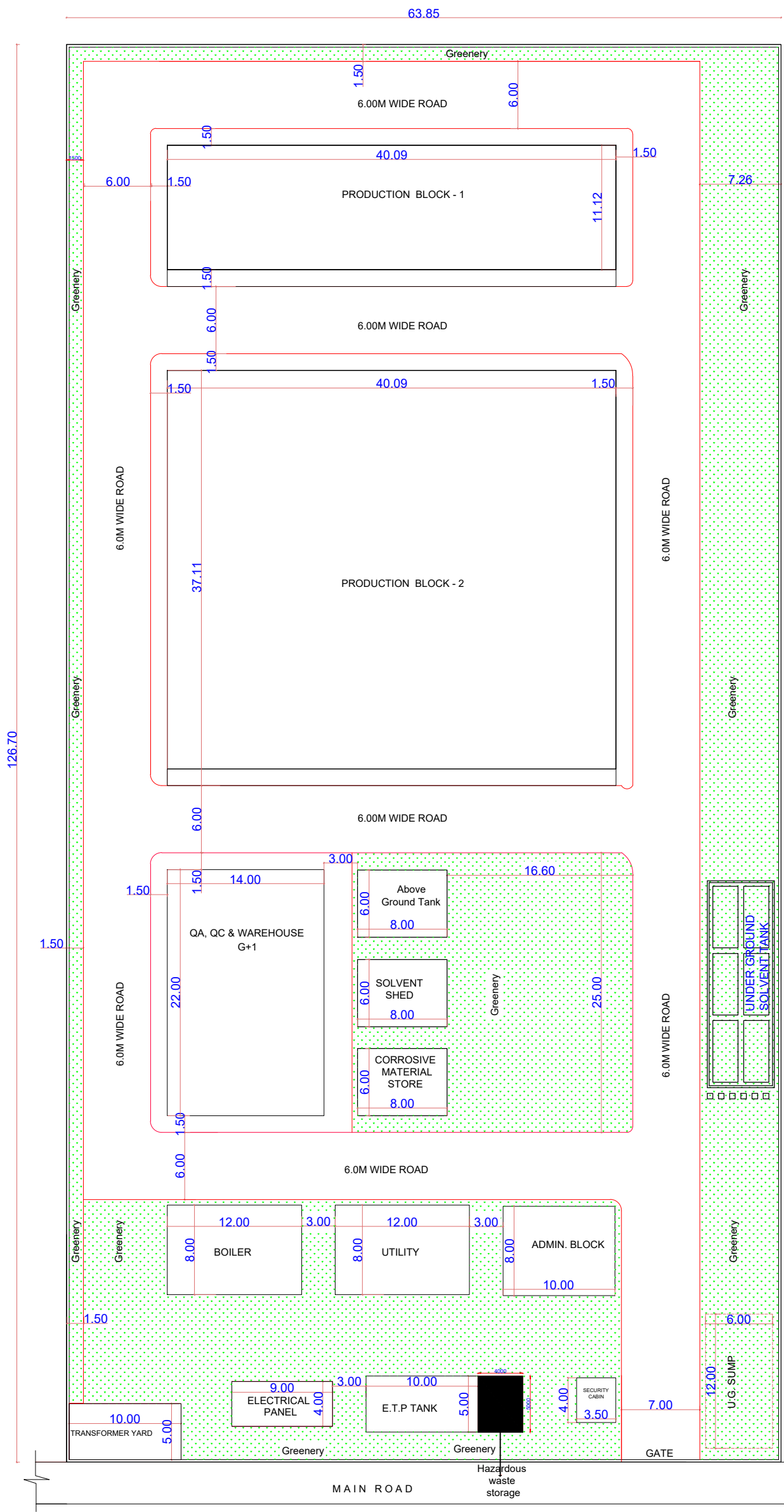
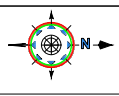
ಅ.ಸಂ.	ಗ್ರಾಮದ ಹೆಸರು	ಒಟ್ಟು ಕ್ಷೇತ್ರ	ವಿರಾಟು ಕ್ಷೇತ್ರ	ನಿವ್ವಳ ಕ್ಷೇತ್ರ
01	02	03	04	05
1.	ಕರೇಬನೂರು	2735-28	63-37	2671-31
2.	ಬಾಡಿಂಯಾಲ	496-34	20-27	476-07
	ಒಟ್ಟು	3232-22	84-24	3147-38

ಕರ್ನಾಟಕ ರಾಜ್ಯಪಾಲರ ಆದೇಶಾನುಸಾರ ಮತ್ತು ಅವರ ವೆಸರಿಂದ.

ಎ.ಪಿ. ರಾಮಕೃಷ್ಣ  
ಸರ್ಕಾರದ ಆಧೀನ ಕಾರ್ಯದರ್ಶಿ (ಕೈ.ಆ.)  
ಪಾಲಿಟಿಕ್ಸ್ ಮತ್ತು ಕೈಗಾರಿಕೆ ಇಲಾಖೆ

**ANNEXURE-10**

**LAYOUT PLAN**



AREA STATEMENT.

S.No	DESCRIPTION	DIMENSIONS (mts.)		AREA Sq. M
		L	B	
01	PRODUCTION BLOCK-1 ( Ground Floor )	40.09	11.12	445.80
	PRODUCTION BLOCK-1 ( First Floor )	40.09	11.12	445.80
	PRODUCTION BLOCK-1 ( Second Floor )	40.09	11.12	445.80
02	PRODUCTION BLOCK - 2 ( Ground Floor )	40.09	37.11	1487.74
	PRODUCTION BLOCK - 2 ( First Floor )	40.09	37.11	1487.74
03	WARE HOUSE, Q.A & Q.C. ( Ground Floor )	14.00	22.00	308.00
	WARE HOUSE, Q.A & Q.C. ( First Floor )	14.00	22.00	308.00
04	BOILER	12.00	8.00	96.00
05	UTILITY	12.00	8.00	96.00
06	ABOVE STORAGE TANKS	6.00	8.00	48.00
07	SOLVENT SHED	6.00	8.00	48.00
08	E.T.P TANKS	10.00	5.00	50.00
09	ADMIN BLOCK	10.00	8.00	80.00
10	ELECTRICAL ROOM	04.00	9.00	36.00
11	H.T YARD	10.00	5.00	50.00
12	HAZARDOUS WASTE STORAGE	04.00	5.00	20.00
13	SECURITY ROOM	04.00	3.50	14.00
TOTAL BUILT UP AREA				5466.88

TOTAL SITE AREA 63.85M X 126.70M = 8089.80 SQ.M

S.No	DESCRIPTION	AREA IN SQ.M	AREA IN PERCENTAGE (%)
01	GROUND COVERAGE AREA	2725.5	33.7 %
02	GREENERY AREA	2694.3	33.3 %
03	ROADS AREA	2670.0	33.0 %
TOTAL SITE AREA		8089.80	100.00 %

SPECIFICATIONS

FOUNDATION	— R.C.C
BASEMENT	— C.R.S IN C.M
SUPER STRUCTURE	— BRICK WORK
STRUCTURE	— R.C.C
FLOORING	— FLOORING AS PER DETAIL
PLASTERING	— CEMENT MORTOR
ROOFING	— R.C.C
ELECTRICAL	— AS PER I.S.I STANDARDS

REFERENCE

PROPOSED	
EXISTING	

GENERAL NOTES:

(UNLESS OTHERWISE MENTIONED)  
ALL DIMENSIONS ARE IN METERS.

OWNER'S SIGNATURE

CONSULTANT'S SIGNATURE

CLIENT:

PROPOSED FACTORY BELONG TO  
M/s. LAUREATZ TECHNOCHEM PVT LTD  
PLOT NO.62, KIADB, KADECHUR INDUSTRIAL AREA  
YADGIR, KARNATAKA.

STRUCTURAL CONSULTANT:

**SHPL**  
SRI HARSHA CONSULTING ENGINEERS(P) LTD.  
Plot no: 13, Vishnu Acharya Nivas,  
Road No -3, Journalist Colony,  
Banjarahills, Hyderabad-500 034  
Ph: 040-23350500/23351600  
Mob: 9440350500  
Email: shpl.hydr@gmail.com

DRAWING TITLE:

LAY OUT PLAN

DRAWING NO	SHPL/PLLY/SUB/001	REV	R0
APPROVED		V.S REDDY	
SCALE		1:100	DRAWN BY VENKAT
DATE		12-03-2021	CHECKED BY V.S REDDY

This drawing is copyright and may not be copied without prior written consent. The contractor shall verify all dimensions on site before commencing any work or shop drawing. Any discrepancies occurring in this drawing must be referred to the Structural consultants before the commencement of any work.

**ANNEXURE-11**

**NABET CERTIFICATE**



# Quality Council of India

National Accreditation Board for  
Education & Training



## CERTIFICATE OF ACCREDITATION

### AM Enviro Engineers

No.14/1, Harikrupa, Patalamma Temple Street, Basavanagudi, Bangalore,  
Karnataka-560004

Accredited as Category - A organization under the QCI-NABET Scheme for Accreditation of EIA Consultant Organizations: Version 3 for preparing EIA/EMP reports in the following sectors:

Sl. No	Sector Description	Sector (as per)		Cat.
		NABET	MoEFCC	
1.	Mining of minerals - opencast mining only	1	1 (a) (i)	B
2.	Metallurgical industries (secondary – ferrous only)	8	3 (a)	B
3.	Pesticides industry and pesticide specific intermediates (excluding formulations)	17	5 (b)	A
4.	<b>Synthetic organic chemicals industry</b> (dyes & dye intermediates; bulk drugs and intermediates <b>excluding</b> drug formulations; synthetic rubbers; basic organic chemicals, other synthetic organic chemicals and chemical intermediates)	21	5 (f)	A
5.	Building and construction projects	38	8 (a)	B
6.	Townships and Area development projects	39	8 (b)	B

**Note: Names of approved EIA Coordinators and Functional Area Experts are mentioned in IA AC Minutes dated February 21, 2020 on QCI-NABET website.**

The Accreditation shall remain in force subject to continued compliance to the terms and conditions mentioned in NABET's letter of accreditation bearing no. QCI/NABET/ENV/ACO/20/1271 dated March 12, 2020. The accreditation needs to be renewed before the expiry date by AM Enviro Engineers, Bangalore following due process of assessment.

Sr. Director, NABET  
Dated: March 12, 2020

Certificate No.  
NABET/EIA/1922/IA0056

Valid till  
Dec 30, 2022

For the updated List of Accredited EIA Consultant Organizations with approved Sectors please refer to QCI-NABET website.

## Acknowledgement of Online Application for Water Supply Connection

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Application Date	16-Jun-2021	
Application No.	KIADB2021WS0183	
Name	Srihari	
Industrial Area	Kadechur I A	
Plot No.	62	
Mobile No.	9494407373	
Water Supply Details	Quantum of Water Supply Approved	136000.00
	Quantum of Water Supply Requested	84000.00
	Connections Requested Per Day	84000.00

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This is an acknowledgement of your online application for Water Supply Connection. Please note and refer the Application Number in further communications.

Please contact the Development Officer/Secretary, KIADB for further processing of the application. The contact details are mentioned below:

Officer, KIADB

---

T.H Prakash

8150848022

dokalaburagi@kiadb.in

KALABURAGI, YADGIRI, BIDAR - KIADB  
Zonal office, Kapnur Industrial Area,  
Humnabad Road, Kalaburagi-585102

## Applicant Details

### Name And Address

Applicant First Name	Srihari	Mobile No	9494407373
Applicant Middle Name		Email ID	laureatz4ec@gmail.com
Applicant Last Name	T V	Name of the	M/s. Laureatz Technochem Pvt. Ltd

### Communication Address

Address Line1	Plot No. 147, Sri Sai Nilayam
Address Line2	Pragathi Nagar, Kukatpalli, (Near JNTU),
City	Hyderabad'
State	Telangana
Pin Code	500090

### Local Address

Address Line1	Plot No. 62,
Address Line2	Kadechur Industrial area
City	Yadagir
State	Karnataka
Pin Code	585221

### Details of Water supply connection to the Unit

District	Yadgir	Industrial Area	Kadechur I A
Plot No.	62	Extent In Acre(Sq.	8089.80

# Laureatz Technochem Pvt Ltd.

Date:16.06.2021

To,

**Member Secretary, Industry - II,  
Ministry of Environment, Forest & Climate Change,  
Vayu Wing, Indira Paryavaran Bhavan,  
Jor Bagh Road, Jor Bagh, New Delhi – 110003.**

Sir,

**Sub: Declaration letter regarding usage of boiler & Thermic fluid heater primary fuel as Biomass Briquettes.**

**Ref: J-11011/143/2021-IA.II(I)**

With reference to the above subject and reference we have proposed the project "Establishment of Active Pharmaceutical Ingredients (API's)" at Plot No 62, Kadechur Industrial area, Yadagir Taluk & District, Karnataka-585221. In the application submitted, we have mentioned that the primary fuel for boiler & Thermic fluid heater will be biomass briquettes and coal will be used only as alternative. In this regard, here with we are declaring & submitting that, we will use biomass briquettes as primary fuel for boiler & thermic fluid heater. During scarcity of biomass briquettes, coal will be used as alternative fuel.

Kindly consider and issue us the environmental clearance at the earliest.

Thanking You,

Yours Faithfully,

For **M/s. Laureatz Technochem Pvt. Ltd**

Authorized Signatory

