CHAPTER 6. RISK ASSESSMENT& DISASTER MANAGEMENT PLAN

This Chapter provides the details about the Risk Assessment, Disaster Management Plan (DMP) and on-site emergency plan as proposed for the proposed project.

6.1. Introduction

Industrial plants deal with materials, which are generally hazardous in nature by virtue of their intrinsic chemical properties or their operating temperatures or pressures or a combination of these. Fire, explosion, toxic release or combinations of these are the hazards associated with industrial plants using hazardous chemicals. More comprehensive, systematic and sophisticated methods of Safety Engineering, such as, Hazard Analysis and Quantitative Risk Assessment have now been developed to improve upon the integrity, reliability and safety of industrial plants. In this chapter risk assessment and disaster management is mentioned the cummulative.

The primary emphasis in safety engineering is to reduce risk to human life, property and environment. Some of the more important methods used to achieve this are:

- Quantitative Risk Analysis: Provides a relative measure of the likelihood and severity of various possible hazardous events by critically examining the plant process and design.
- Work Safety Analysis: The technique discerns whether the plant layout and operating procedures in practice have any inherent infirmities.
- Safety Audit: Takes a careful look at plant operating conditions, work practices and work environments to detect unsafe conditions.

Together, these three broad tools attempt to minimize the chances of accidents occurring. Yet, there always exists, no matter how remote, probability of occurrence of a major accident. If the accident involves highly hazardous chemicals in sufficiently large quantities, the consequences may be serious to the plant, to surrounding areas and the populations residing therein.

6.2. Risk Assessment

A three 'levels' risk assessment approach has been adopted for the Samridhi Crop Chemicals (henceforth SCC) for proposed project considering approved TOR. The risk assessment levels are generally consistent with the practices encountered through various assignments for medium and large chemical complexes. The brief outline of the three-tier approach is given below:

Level 1 – Risk Screening

This is top-down review of worst- case potential hazards/risks, aimed primarily at identifying plant sites or areas within plant, which pose the highest risk. Various screening factors considered include:

• Inventory of hazardous materials;



- Hazardous Materials properties;
- Storage conditions (e.g. temperature and pressure);
- Location sensitivity (distance to residential areas / populace).

The data / information is obtained from plant. The results provide a relative indication of the extent of hazards and potential for risk exposure.

> Level 2 – Major Risk Survey (Semi - Quantitative)

The survey approach combines the site inspection with established risk assessment techniques applied both qualitative as well quantitative mode. The primary objective is to identify and select major risks at a specific location in the plant considering possible soft spots / weak links during operation / maintenance. Aspects covered in the risk usually include:

- Process Hazards;
- Process Safety Management Systems;
- Fire Protection and Emergency response equipment and programs.
- Security Vulnerability;
- Impact of hazards consequences (equipment damage, business interruption, injury, fatalities);
- Qualitative risk identification of scenarios involving hazardous materials;
- Risk reduction measures.

Selection of critical scenarios and their potential of damage provide means of prioritizing mitigative measures and allocate the resources to the areas with highest risks.

> Level 3 – Quantitative Risk Assessment (Deterministic)

This is the stage of assessment of risks associated with all credible hazards (scenarios) with potential to cause an undesirable outcome such as human injury, fatality or destruction of property. The four basic elements include:

- i. Hazards identification utilizing formal approach (Level 2, HAZOP etc.);
- ii. Frequency Analysis. Based on past safety data (incidents / accidents);
 Identifying likely pathway of failures and quantifying the toxic / inflammable material release;
- Hazards analysis to quantify the consequences of various hazards scenarios (fire, explosion, BLEVE, toxic vapour release etc.).
 Establishminimum value for damage (e.g. IDLH, over pressure, radiation flux) to assess the impact on environment.



iv. Risk Quantification: Quantitative techniques are used considering effect / impact due to weather data, population data, and frequency of occurrences and likely hood of ignition / toxic release. Data are analyzed considering likely damage (in terms of injury / fatality, property damage) each scenario is likely to cause.

QRA provides a means to determine the relative significance of a number of undesired events, allowing analyst and the team to focus their risk reduction efforts where they will be beneficial most.

SCC shall manufacture some new technical grade pesticides chemicals. Table2.6 in Chapter 2 gives the list of raw materials. Solid raw materials are stored in ware house while liquid and gaseous raw materials are stored in tank farms and covered area. The list of bulk liquid storages of raw materials is as given below:

| S. No | Material | Capacity | Remarks |
|-------|-----------------|-----------|---|
| | RAW MATERIAL | | |
| 1. | Methanol | 2X 25 MT | Underground storage in tanks |
| 2. | Sulphuric acid | 50 MT | Above ground storage in tanks |
| 3. | Nitromethane | 50 MT | In drums, Well ventilated covered storage |
| 4. | Fuel (LDO /HSD) | 5 KL each | In drums, Well ventilated covered storage |

Table 6.1 Liquid/Gaseous Bulk Storages

6.3. Risk Screening Approach

Proposed Plant: Risk screening of proposed project was undertaken through data / information provided by SCC. Data of major / bulk storages of raw materials, intermediates and other chemicals were collected. MSDS of hazardous chemicals were studied vis avis their inventories and mode of storage. Plant will be using number of hazardous chemicals and also producing pesticides chemicals – all hazardous in nature. The chemicals stored in bulk (liquid or gaseous) and defined under MSHIC Rule will be considered for detailed analysis.

Hazardous materials have been defined under MSIHC Rules (1989) - 2 (e) which means.

- Any chemical which satisfies any of the criteria laid down in Part I of Schedule I and is listed in Column 2 of Part II of this Schedule;
- 1.



• **Toxic Chemicals**: Chemicals having the following values of acute toxicity and which owing to their physical and chemical properties, are capable of producing major accident hazards:

| S. No | Toxicity | Oral Toxicity LD50 (mg/kg) | Dermal Toxicity LD50 (mg/kg) | Inhalation Toxicity LC50 (mg/l) | Remarks |
|-------|-----------------|-------------------------------|------------------------------------|---------------------------------------|---------|
| 1 | Extremely Toxic | >5 | < 40 | < 0.5 | |
| 2 | Highly Toxic | >5 – 50 | > 20 – 200 | < 0.5 – 2.0 | |
| 3 | Toxic | >50 - 200 | > 200 - 1000 | > 2 – 10 | |

2. Flammable chemicals:

- (i) **Flammable gases**; 20 ^oC and at standard pressure of 101.3 KPa are:
 - Ignitable when in a mixture of 13% or less by volume with air, or;
 - Have a flammable range with air of at least 12% points regardless of the lower flammable limits.
- (ii) **Extremely flammable liquids**: chemicals which have a flash point lower than or equal to 23^oC and the boiling point less than 35^oC;
- (iii) **Very Highly flammable liquids**: chemicals which have a flash point lower than or equal to 230C and the boiling point higher than 35 ^oC;
- (iv) **Highly Flammable Liquid**: Chemicals, which have a flash point lower than or equal to 60 °C but higher than 23 °C.
- (v) **Flammable liquids**: chemicals, which have a flash point higher than 60 ^oC but lower than 90 ^oC.

Explosives: Explosive means a solid or liquid or pyrotechnics substance (or a mixture of substances) or an article.

- a) Which is in itself capable by chemical reaction of producing gas at such a temperature and pressure and at such a speed as to cause damage to surroundings;
- b) Which is designed to produce an effect by heat, light, sound, gas or smoke or a combination of these as the result of non-detonative self-sustaining exothermic chemical reaction.
 - I. any chemical listed in Column 2 of Schedule 2;
 - II. any chemical listed in Column 2 of Schedule 3;



| : Hazardous Analysis Raw materials stored in Bulk | | | | | | | |
|---|---|--|------------------------|------------------------|--|--|---------|
| S. No | Material | S. No & Threshold Quantity (TQ in MT) as per MSHIC Rules | | antity (TQ in es | Hazards Potential | | Remarks |
| | | Schedule - 1, Part-II | Schedule- 2, Part-I | Schedule- 3, Part-I | Hazards | Toxic DT->mg/Kg; OTmg/Kg; ITmg/I; (Rats) | |
| | Methanol CAS No:67-56-1 UN No:1230 A colorless fairly volatile liquid with a faintly sweet pungent odor like that of ethyl alcohol. | 377 | | | Highly Flammable; Behavior in Fire: Containers may explode. Health Hazards: Exposure to excessive vapor causes eye irritation, head- ache, fatigue and drowsiness. High concentrations can produce central nervous system depression and optic nerve damage. 50,000 ppm will probably cause death in 1 to 2 hrs. Can be absorbed through skin. Swallowing may cause death or eye damage. | ERPG-1: 200 ppm ERPG-2: 1000 ppm ERPG-3: 5000 ppm IDLH: 6000 ppm | |
| | Sulphuric Acid CAS No: 7664- 93-9 UN No: 1830 | 591 | | | Flammability: Will not burn Health Hazard: Extremely hazardous - use full protection; Reactivity: Violent chemical change possible | ERPG-1: 2.0 mg/m3 ERPG-2: 10 mg/m3 ERPG-3: 30 mg/m3 IDLH:15 mg/m3 | |
| | Nitro Methane CAS No: 75-52-5 | | | | Very hazardous in case of ingestion. Hazardous in case of eye contact (irritant). Slightly hazardous in case of | DT | |



| | inhalatio | 1 | OT—940 (Rat) | |
|--|-----------|---|--------------|--|
| Colorless Oily Liquid with disagreeable- | | | IT | |

TQ-I: Threshold quantity (for application of rules 4,5,7 to 9 and 13 to 15) TQ-II: Threshold quantity (for application of rules 10 to 12)



3. Note:

- 1. Oral Toxicity (OT) in LD₅₀ (mg/kg)
- 2. Dermal Toxicity (DT) in LD₅₀ (mg/kg)
- 3. Inhalation Toxicity in LC50 (mg/l) [4 hrs.]

SCC proposes production of new technical pesticide unit. All products are hazardous in nature and limited data are available for these. However, hazards potential (for damage) of products and other materials to plant personnel, environment and off-site area is different for different materials See Table 6.3. Among technical products only one is liquid. Among the products one product namely Chloropicrin is" highly toxic" as per MSIHC rules. None is "extremely toxic".

Though SCC will be using a number of raw materials however it will be storing nearly 2 liquid raw materials (in bulk). Bromine will not be stored. It will be used immediately on receipt in cylinders; no storage the raw materials coming under hazardous category as specified by MSIHC Rules, 2016 is given in Table 6.2 above

All pesticides products are hazardous in nature and many of them are new compounds with little data available. The products are produced as per market demand and packed and stored in saleable packing.

6.4. Hazardous Materials Storage

The solid raw materials will be received in bags or drums and will be stored in chemicals go-downs. The products (liquid or solid) will be packed in drums and stored in product go-downs as per market demand. The bulk storages of liquid hazardous materials are given in the Table 6.1.

The solid materials powder or granules spillage can result in polluting small area only. The damage to personnel can be through ingress- dermal (if individual come in contact), oral (if individual food gets infected through fugitive dust) or inhalation (fugitive dust). The main route is fugitive dust which in covered area will move to short distance only. Some of the raw materials are though stored in bulk (quantity) but in drums only.

The pesticide product will be both as liquid and solid. The product storage for liquid will be in drums and ISO containers and for solid in bags depending upon client requirement

The risk is through liquid and gaseousmaterialswhich are volatile/gaseous material (toxic) and inflammable/explosive materials. The toxic vapours due to spillage of such material can travel to some distance (as they are stored in covered go-downs) and cause damage. The liquid products will be packed in drums (Approx 200 liters drums).

6.5. QRA Approach

Identification of hazards and likely scenarios (based on Level-1 and Level-2 activities) calls for detailed analysis of each scenario for potential of damage, impact area (may vary with weather conditions / wind direction) and safety system in place. Subsequently each incident is classified according to relative risk classifications provided in Table below as Table 6.4:



Table 6.2 Risk Classification

| Stage | Description | | |
|-----------------------------------|--|--|--|
| High (> 10 ⁻² /vr.) | A failure which could reasonably be expected to occur within the expected life time of the plant. | | |
| | Examples of high failure likelihood are process leaks or single instrument or valve failures or a human error which could result in releases of hazardous materials. | | |
| Moderate $(10^{-2} - 10^{-1})$ | A failure or sequence of failures which has a low probability of occurrence within the expected lifetime of the plant. | | |
| ⁴ /yr.) | Examples of moderate likelihood are dual instrument or valve failures, combination of instrument failures and human errors, or single failures of small process lines or fittings. | | |
| Low | A failure or series of failures which have a very low probability of occurrence within the expected lifetime of plant. | | |
| | Examples of 'low' likelihood are multiple instruments or valve failures or multiple human errors, or single spontaneous failures of tanks or process vessels. | | |
| Minor Incidents | Impact limited to the local area of the event with potent for 'knock – on- events' | | |
| Serious Incident | One that could cause: Any serious injury or fatality on/off site; Property damage of \$1 million offsite or \$5 million onsite. | | |
| Extensive Incident | One that is five or more times worse than a serious incident. | | |

Assigning a relative risk to each scenario provides a means of prioritizing associated risk mitigation measures and planned actions.

6.6. Thermal Hazards

In order to understand the damages produced by various scenarios, it is appropriate to understand the physiological/physical effects of thermal radiation intensities. The thermal radiation due to tank fire usually results in burn on the human body. Furthermore, inanimate objects like equipment, piping, cables, etc. may also be affected and also need to be evaluated for damages. Table 6.5, Table 6.6and Table 6.7(below), respectively give tolerable intensities of various objects and desirable escape time for thermal radiation.

Thermal hazards could be from fires or explosion. Fire releases energy slowly while explosion release energy very rapidly (typically in micro seconds). Explosion is rapid expansion of gases resulting in rapidly moving shock wave. Explosion can be confined (within a vessel or building) or unconfined (due to release of flammable gases).

BLEVE (boiling liquid expanding vapour explosion) occurs if a vessel containing a liquid at a temperature above its atmospheric boiling point ruptures. The subsequent BLEVE is the explosive vaporization of large fraction of its vapor contents; possibly followed by combustion or explosion of the vaporized cloud if it is combustible range.



Thermal hazards have been considered for various scenarios including:

• Fire in inflammable chemicals storage tanks.

Table 6.3 Effects due to Incident Radiation Intensity

| Incident Radiation kW/m ² | Damage Type | | |
|---|---|--|--|
| 0.7 | Equivalent to Solar Radiation | | |
| 1.6 | No discomfort on long duration | | |
| 4.0 | Sufficient to cause pain within 20 sec. Blistering of skin (first degree burn is likely). | | |
| 9.5 | Pain threshold reached after 8 sec. Second degree burn after 20 sec. | | |
| 12.5 | Minimum energy required for piloted ignition of wood, melting of plastic tubing etc. | | |
| 25 | Minimum Energy required for piloted ignition of wood, melting, plastic tubing etc. | | |
| 37.5 | Sufficient to cause damage to process equipment. | | |
| 62.0 | Spontaneous ignition of wood. | | |

Table 6.4 Thermal Radiation Impact to Human

| Exposure Duration | Radiation Energy {1% lethality; kW/m ² } | Radiation Energy for 2 nd degree burns; kW/m ² | Radiation Energy for 1st degree burns; kW/m ² |
|----------------------|--|--|--|
| 10 secs | 21.2 | 16 | 12.5 |
| 30 Sec. | 9.3 | 7.0 | 4.0 |
| | | | |

Table 6.5 Tolerable Intensities for Various Objects

| SI. No | Objects | Tolerable Intensities (kw/m ²) |
|--------|--|---|
| 1 | Drenched Tank | 38 |
| 2 | Special Buildings (No window, fire proof | 25 |



| | doors) | |
|---|--------------------------|-------------------|
| 3 | Normal Buildings | 14 |
| 4 | Vegetation | 10-12 |
| 5 | Escape Route | 6 (up to 30 sec.) |
| 6 | Personnel in Emergencies | 3 (up to 30 sec.) |
| 7 | Plastic Cables | 2 |
| 8 | Stationary Personnel | 1.5 |

6.7. Damage due to Explosion

The explosion of a dust or gas (either as a deflagration or detonation) results in a reaction front moving outwards from the ignition source preceded by a shock wave or pressure front. After the combustible material is consumed the reaction front terminates but the pressure wave continues its outward movement. Blast damage is based on the determination of the peak overpressure resulting from the pressure wave impacting on the object or structure.

As a safety measure SCC is storing highly hazardous raw materials in isolated places with full safety measures. Damage estimates based on overpressure are given in Table 6.8below:

| SI. No | Overpressure (psig / bar) | Damage | | |
|--------|------------------------------|---|--|--|
| 1. | 0.04 | Loud Noise / sonic boom glass failure | | |
| 2. | 0.15 | Typical pressure for glass failure | | |
| 3. | 0.5 - 1 | Large and small windows usually shattered | | |
| 4. | 0.7 | Minor damage to house structure | | |
| 5. | 1 | Partial demolition of houses, made uninhabitable. | | |
| 6. | 2.3 | Lower limit of serious structure damage | | |
| 7. | 5 – 7 | Nearly complete destruction of houses | | |
| 8. | 9 | Loaded train box wagons completely demolished | | |
| 9. | 10 | Probable total destruction of houses | | |
| 10. | 200 | Limits of crater lip | | |

Table 6.6 Damage due to Overpressure

6.8. Toxic Release



Hazardous materials handled and stored in bulk in complex are toxic liquids (as detailed in Table 6.1) and other raw materials as defined in MSHIC rules and indicated in Table 6.3. Some of these chemicals are stored in bulk (in tank farm).

Damage criteria: For toxic release the damage criteria considered is IDLH concentration (if data are available). In the absence of non-availability of IDLH, 'Inhalation Toxicity (IT) data for rats' are considered. 'IT' data are used for the products as IDLH are not available for these chemicals.

6.9. Data Limitations

It is also observed that very little data or information (regarding physical properties required for modelling) is available about the products.

6.10. Likely Failure Scenarios

Few likely failure scenarios have been selected after critical appraisal of raw materials and storage inventories. Failure scenarios selected are as given in Table 6.9 below:

| S. No. | Scenario | Remark |
|---------|-----------------------|------------------------|
| | Raw materials | |
| Case -1 | Methanol Spillage | Toxic Impact |
| Case -2 | Nitromethane Spillage | Toxic / Thermal Impact |

Table 6.7 Different Failure Scenarios

6.11. Weather Effect

The effect of ambient conditions on the impact of fire / heat radiation and GLC of hazardous / toxic material can be beneficial as well as harmful. A high wind (turbulence) can dilute the toxic material while stable environment can extend the reach of IDLH or IT (inhalation LC50 rats for products) concentration to long distance. Any inflammable gas / vapour release in turbulent weather will soon dilute the hazardous gases below LEL and thus save the disaster.

6.12. Incidents Impacts

The identified failure scenarios (Table 6.9) have been analysed (Using ALOHA and EFFECT Modules) for the impact zones considering damage due to thermal and toxic impacts. Similar impacts are considered for proposed units. Each incident will have Impact on the surrounding environment which in extreme case may cross plant boundary. The impact zones for various scenarios are given in Table 6.10.

Table 6.8 : Hazards Scenario Impact



| Scenario No. | Scenario | Impact Zone (m) | Remarks |
|-----------------|-----------------------|--------------------|---|
| | Scer | nario Raw Material | |
| Case -1 | Methanol Spillage | ∻ <10 | IDLH; Stability Class D; |
| Case -2 | Nitromethane Spillage | | IDLH; Stability Class D; Template- |
| | | ◆ 11 | 1 st Degree Burn Template-2 |

Templates of Scenario



Template 1.

Nitro Methane Spillage—Toxic Impact Zone (Class D)





 Template 2.
 Nitro Methane Spillage; Pool Fire—Thermal Impact Zone

6.13. Consequential Impacts

The consequential impacts from each incident scenario can be though thermal, over pressure wave and toxic route. The damage can be on plant personnel (and neighboring residents in case incident crosses boundary), property and also loss in production.

6.14. Thermal and Explosion Hazards

Incidents involving thermal hazards are mainly due to fuel fire (due to spillage). However, the material stored is drums in small quantity. The impact due to nitromethane spillage and fire (1st degree burn) is limited to ~11 m (2nd case) only (i.e. within plant boundary). However, the consequences can go to worse if the incidents lead to domino effect to other tanks.

6.15. Toxic Hazards

Toxic hazards are mainly due to Nitromethane and other toxic chemicals leakage and its impact is also within the plant boundary (< 18 m).

Other hazardous chemicals including products their impact will be limited to spillage area. The acid spillage if comes in contact with metal parts will produce hydrogen which is highly flammable gas. Any person moving in area and getting splash will get the injury. In addition, the spillage will cause pollution problem. The spillage is to be collected and neutralized for toxic contents before disposal.

6.16. General Control Measures

Since some of the substances in use at SCC are hazardous with fire potential and also toxic in nature, it is necessary to use appropriate control measures recommended for such substances:



6.17. Flammable Gas Fires

Fire control generally consists of directing, diluting and dispersing the inflammable gas/vapor to prevent contact with persons, to prevent it from infiltrating structures if the leak is out door, and to avoid its contact with ignition sources while, if possible, simultaneously stopping the flow of gas. Water in the form of spray, applied from hoses or monitor nozzles or by fixed water spray system cools the burning vapors / gas.

6.18. Process Safety System

Process & Plant Safety:

Conducting Preliminary Safety Analysis (A1), Basic Safety Review (A2), Detailed Safety Review (A3), Pre-Start-Up Safety Review (A4) &Pre-Start-Up Safety audit according to PPS directive (details mentioned in following flow diagram)

- Every change in the process, procedure, equipment, etc. will be done through robust management of change (MOC) procedure
- Pre-Start up Safety Reviews for all modification
- Pressure testing of pipelines and replacement of fragile pipelines and tanks by prevention project
- Hazardous area classification
- Internal safety rounds for P&PS
- Control P&IDs, and Lock opened (LO)/ Lock closed (LC) procedures are in place
- TOPPS (Top Performance in Process & Plant Safety) training to all employees
- Root Cause Analysis of all incidents
- Pre-Start up Safety Reviews for all modification

Occupational Safety:

- Permit to Work procedure and Monthly monitoring of all filled permit for continual improvement
- Mobilized Near- Miss Reporting and award scheme
- HSE rounds: PMT (Plant Management Team) of one plant takes HSE round of another plant. Exchange of best practices among plants
- MSDS Management
- Tool Box talk with contractors
- Central Safety Committee
- Departmental Safety Committees
- HSE Coordinator and Monitor program: Shop floor employees' participation in Safety activities
- Celebration of theme based Safety days/ weeks at site
- Safety Induction program for new joiners (both company & contract employees)

Emergency Preparedness:

• On-Site Emergency Plan for the site



- Training on On-Site Emergency Action Plan
- Regular Site Level Mock drills and Plant Specific Fire Drills and Leak, spill drills
- Availability of First aiders, Fire Fighters and Rescue members in each shift
- Maintenance of Fire hydrant system, sprinkler system and portable fire extinguishers
- Periodic testing of fire hydrant and sprinkler systems
- Fire Tenders and Ambulances kept ready

Occupational Health:

- Pre-employment & Annual Medical Examination
- Quarterly/Periodical Physical Examinations
- Canteen Employees Examination
- Fork lift operators Examination
- Recall services & Follow-Up
- Return to work assessment
- Exit Examination
- Training on Counselling, Hearing Conservation Program, Hazardous Chemical Awareness Program, Shop floor training, First-aid (Adequate numbers of Certified First Aiders/employees), etc.
- Legal records: All medical records of employees to be maintained.
- Emergency Medical services: Ambulance services, First-aid boxes, Decontamination facility etc.

Health Promotional Activities: Awareness on Medical issues, Ergonomics awareness programs, Stress management, De-addiction program, etc.

- Decontamination facility is provided
- Breathing air provision is provided at toxic chemical handling area.

Safety System for Toxic Material Handling

Following precaution Taken while handling Toxic materials

- Highly Toxic chemical is stored in storage room with lock and key.
- Inventory records are maintained.
- Toxic material is stored in well ventilation and out of sunlight
- It is stored away from incompatible chemicals.
- Keeping containers tightly & securely closed when not in use
- Toxic chemical charging is done inside the closed room in presence of shift incharge.
- Local Ventilation system is provided to avoid exposure at work place.
- Vent gas is passing through scrubber system for absorption & reduction of pollution.



Standby pump provision is available for LEV & scrubber system. Training to employees is providing for manual handling of toxic chemicals.

- First aid training also provided to concern employees.
- ✤ Antitoxic kit is maintaining inside OHC.
- Safety PPE's is providing during charging.
- First aid kit provision is available at work place area.

Eye wash/Safety shower stations are readily available nearby and are tested regularly

To avoid fire and explosion nitrogen blanketing, earthing& bonding, electrical flame proof equipment's, pressure rated equipment' are provided.

Suitable fire extinguisher and spill cleanup equipment are maintained.

Dyke provision is available where liquid toxic chemicals are stored.

• Appropriate spill control equipment and procedures is available.

MSDS is maintained inside the concern plant / department.

- Precautionary placard is displayed nearby the work place.
- Toxic chemicals sign board is displayed on container.
- Avoiding any welding, cutting, soldering or other hot work on an empty container of toxic chemicals.
- Good housekeeping is maintaining.
- Toxic gas detector also provided at workplace.
- Toxic chemical waste is collecting in separate pit and transferring to ETP for its treatment.
- Always ensuring that the waste container used is compatible with the waste material
- Ensuring that the waste container is properly and accurately labelled.
- Unauthorized person entry is restricted.
- Restricted for eating, drinking & smoking at work place.
- Employees are trained for emergency of toxic chemicals.
- Toxic chemical spill, leak drills are conducting for awareness, preparedness & response during an emergency.
- Work place area monitoring is to be carried out for ensuring exposure at workplace.
- Process is performed in closed conditions.
- Regular pressure testing for pipelines and equipment to ensure tightness

WORKPLACE MONITORING PLAN

Work zone monitoring is carried out by HSE department every month for gaseous pollutants and dusts. Records are to be kept in standard Form as per Factories Rules. Location for samplings shall be identified. Samples are analyzed for Air borne concentration of hazardous chemicals in ppm.



The analyzed results are compared with the threshold limit values (TLV) of international organizations. The monitoring program is based on the Action Level Concentration (ALC) which is 50% of the TLV. If the analyzed concentration is < ALC, no regular monitoring is required, only occasional checks (once in a year) to ensure the acceptability of the system.

If the analyzed concentration is > ALC < TLV then the monitoring is carried out at regular interval (once in two months). Incase analyzed concentration is > TLV then corrective actions are decided by Plant Manager, General Manager - works and Engineering Manager and they are implemented. After implementation again, monitoring is carried out.

The sampling for gaseous pollutants and air pollutants are done by Air sampling pump.

Arrangement for ensuring health and safety of workers engaged in handling of toxic materials

All persons working in manufacturing units are surveyed by regular medical examinations.

Pre-employment Medical examination to be carried out for all employees prior to employment at well-known multispecialty hospital.

Checkups & tests carried out as per Factory rules / SPCB guidelines.

6.19. Safety Recommendations

6.20. Commonly Recommended Control Measures

A number of preventive control measures for hazardous occurrences have been analyzed and discussed above. Some more salient points are enumerated below:

- All storage tanks in the tank farm should be dyked. Other operation and maintenance features shall be based on established best safety practices.
- Concentration detectors for hazardous chemical vapours (e.g. Chlorine/ bromine/ other chemicals etc.) fire Smoke / heat detectors and fire alarm should be installed at all strategic locations in the plant.
- A schedule for preventive maintenance including health survey of all plant equipment should be adhered to as far as possible.
- Ensure the absence of ignition sources in storage area.
- Ensure placement of firefighting facilities, such as, carbon dioxide, dry chemical powder and foam type fire extinguishers in addition to fire hydrant system, at strategic locations. Spill control measures, such as, removal of all ignition sources from the spill area and ventilating the area as well as soaking the spilled material with paper, towel or mud and letting the volatile substance evaporate slowly in a safe area.
- Compulsory use of protective clothing, non-sparking tools and warning signs during critical operations and maintenance.
- Training / refresher courses on safety information's / norms.
- Eyewash and showers should be put up at strategic places for use during emergencies.



A group of plant personnel should be trained in first aid, rescue, firefighting and emergency control measures. These personnel will form core group/emergency squad who will fight the emergency and also act as rescue and first aid team.

In order to ensure communication from isolated places/locations Walkie-Talkie be made available to persons working in these areas. This will considerably improve the effectiveness of emergency management.

There is no substitute for training-mock drills and these must be held at regular interval keeping the following objectives in mind:

Real time mock-drill should be carried out for probable/likely hazardous situation (after the plant is successfully commissioned).

Target to be set up for various tasks and events during an emergency.

Weak links should be marked and corrective action taken to improve effectiveness during emergency.

6.21. Occupational Health and Safety

Occupational Health and Safety (OHS) are of prime importance more so in hazardous industries. Industries have various types of hazards and QRA is carried out to understand the hazards potential from various incidents. Pre-emptive steps can be planned to safeguards from likely causes. Some of the

Frequent causes of accidents

- Fire and explosion: explosives, flammable material
- Hazards from Toxic Materials
- Mechanical Hazards such as: Being struck by falling objects Caught in between machine parts Snapping of cables, ropes, chains, slings

Handling heavy objects

- Electricity Hazards
 - o Electrocution
 - Short circuits and consequential fire.
 - Poor illumination etc.
- Other Hazards: Falls from height inside industrial units or on the ground Struck by moving objects; Slipping on wet surfaces Sharp objects

Oxygen deficiency in confined spaces; Lack of personal protective equipment (PPE), housekeeping practices, safety signs

• Consequential hazards due to extreme Temperatures;



- Consequential hazards due to vibration
- Consequential hazards due to radiation;
- Many more hazards.

Hazardous substances and wastes

- Heavy and toxic metals
- Lack of hazard communication (storage, labeling, material safety data sheets)
- Batteries, fire-fighting liquids
- Welding fumes
- Volatile organic compounds (solvents)
- Inhalation in confined and enclosed spaces
- Repetitive strain injuries, awkward postures, repetitive and monotonous work, excessive workload

Ergonomic and psychosocial hazards

- Many of the hazards are as result of working environment.
- •
- Long working hours, shift work, night work, temporary employment (Long working hours, shift work, night work, temporary employment, Mental stress, human relations) which results in less attention at work place and consequential incidents and accidents.
- Lack of education and training / awareness is another prime cause of accidents.

Considering above, QRA analysis and also the nature of activities at SCC the following steps for OHS activities have been suggested:

- Employee's health check-up: pre-employment and periodic check-up during employment. The health check-up observations should be informed to employees.
- The health should include any impact due to hazards at work place including (but not limited to) due to noise, heat, illumination, dust, any other chemicals, metals being suspected in environment and going into body of workers either through inhalation, ingestion or through skin absorption and steps taken to avoid musculo-skeletal disorders (MSD), backache, pain in minor and major joints, fatigue etc.
- Training and refresher courses on safety to all employees.
- Employees should be made aware of the hazards in the plant and the preventive actions to be safe from such hazards.

Response to Injuries: Based on a survey of possible injuries, a procedure for response to injuries or exposure to hazardous substances should be established. All staff should have minimum training to such response and the procedure ought to include the following:



- Immediate first aid, such as eye splashing, cleansing of wounds and skin, and Bandage etc.
- Immediate reporting to a responsible designated person
- If possible, retention of the item and details of its source for identification of possible hazards.
- Medical surveillance
- Recording of the incident
- Investigation, determination and implementation of remedial action

6.22. Emergency Management Plan

SCC should develop an Emergency Management Plan (EMP) and regularly carry out Mock drills to check the effectiveness of the EMP. Ergonomic and psychosocial hazards

6.23. Many of the hazards are as result of working environment

Repetitive strain injuries, awkward postures, repetitive and monotonous work, excessive workload

Long working hours, shift work, night work, temporary employment (Long working hours, shift work, night work, temporary employment, Mental stress, human relations) which results in less attention at work place and consequential incidents and accidents.

Lack of education and training / awareness is another prime cause of accidents.

Considering above, QRA analysis and also the nature of activities at SCC the following steps for OHS activities have been suggested:

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- If possible, retention of the item and details of its source for identification of possible hazards.



- Medical surveillance
- Recording of the incident
- Investigation, determination and implementation of remedial action

6.24. Key Process Safety Measures

- Flameproof equipment's and fittings are provided for handling of hazardous chemicals.
- Tanks and all pump motors are earthed.
- Road tanker earthing lines have been provided near the unloading pumps.
- Dykes have been provided for hazardous chemicals storage to contain leakages. Floors of the dyke area have impervious finish.
- Housekeeping of the plant is as per prescribed norms. Floors, platforms, staircases, passages are kept free of any obstruction.
- All hazardous operations are explained to the workers. They are periodically trained on the hazardous processes.
- Dedicated supply of firewater is available in the plant.
- Only authorized persons are allowed inside the plant.
- All instrument and safety devices are checked and calibrated during installation. They are also calibrated, checked at a frequent interval. Calibration records are maintained.
- All electrical equipment's are installed as per prescribed standards.
- All the equipment's of the plant are periodically tested as per standard and results are documented. All equipment's undergo preventive maintenance schedule.
- Hydrant system is pressured with a Jockey Pump.
- Flame arrestor is provided on each tank.
- Pressure gauge is provided on each tank.

In addition to fire hydrant system, nos. of fire extinguishers are also installed at different locations within premises.

Retention basin is provided to collect the contaminated water used during firefighting.

6.25. Transportation:

- Class A petroleum products (equivalent raw materials) will be received through road tanker and stored in underground storage tank as per petroleum Act & Rules.
- Road tanker unloading procedure will be in place and will be implemented for safe unloading of road tanker.
- Static earthing provision will be made for tanker unloading.
- Earthed Flexible Steel hose will be used for solvent unloading from the road tanker.
- Fixed pipelines with pumps will be provided for solvent transfer up to Day tanks/reactors.
- Double mechanical seal type pumps will be installed.
- NRV provision will be made on all pump discharge line.

Table 6.9 Transportation, Unloading and Handling Safety Measures



| Sr.no. | Activity | Type of possible | Mitigation measures |
|--------|---|---|---|
| | | Hazard | |
| 1 | Transportation of Chemicals like, Acids&Solventsby road tanker | Leakage& Spillage | Check the source of leakage point. |
| | | | • Do not touch damaged containers or spilled material unless wearing appropriate protective clothing. |
| | | | Stop leak if you can do it without risk. |
| | | Fire, & explosion, | Use water spray to reduce vapors; do not put water directly on leak, spill area or inside container. |
| | | | • Keep combustibles (wood, paper, oil, etc.) away from spilled material. |
| | | | Isolate the area |
| | | Toxic release | Isolate the container |
| | | | • Training will be provided to driver and cleaner regarding the safe driving, hazard of Flammable chemicals, emergency handling. |
| | | | • TREM card will be kept with TL. |
| | | | Fire extinguishers will be kept with TL. |
| | | | • Flame arrestor will be provided to TL exhaust. |
| | | | Instructions will be given not to stop road tanker in populated area. |
| | | | • Clear Hazard Identification symbol and emergency telephone number will be displayed as per HAZCHEM CODE. |
| | | | Appropriate PPEs will be kept with TL. |
| 2 | Solvents transfer from storage tank | Leakage& Spillage due to Line rupture, | • Double mechanical seal type FLP type pump will be provided. |
| | to Day tank. | Fire, Explosion, Toxic | • Double on / off switch will provide at tank farm and process area near day |



| | | release. | tank. Pump auto cut off with day tank high level will be provided. |
|---|---|---|---|
| | | | Flame arrestor will be provided on day tank vent. |
| | | | Over flow will be provided for additional safety and it will be connected to main storage tank. |
| | | | NRV will be provided on pump discharge line. |
| | | | Double Jumper clip will be provided to all solvent handling pipeline. |
| | | | Double static earthing will be provided to day tank. |
| 3 | Transportation of Chemicals transfer from Day tank to reactor. | Leakage, Spillage due to Line rupture, Flange Gasket failure, Fire, Explosion, Toxic release. | • Gravity transfer. |
| | | | Total quantity of day tank material will be charged in to reactor at a time. |
| | | | Static earthing will be provided to storage tank. |
| | | | Double Jumpers will be provided to pipeline flanges. |

6.26. Emergency facilities

Emergency Management Planning (EMP) should be developed considering the likely hazards in the plant and sincerely implemented. Mock drills for various scenarios should be carried out and results of the drills should be recorded. Weal links in the mock drills should be strengthened.

6.27. Objectives

The Emergency Management Plan (EMP) is developed to make the best possible use of the resources available at SCC and the nearby agencies to provide help/assistance in case of an emergency in the plant. The activities will include:

- Rescue the victims and give them the necessary medical attention in the shortest possible time.
- Safeguard another person (evacuate them to a safer place).
- Contain the incident and control it with minimum damage to human and life and property.



• Provide necessary information to families/relatives of affected persons, outside agencies including media and statutory bodies.

6.28. Emergency Management Plan [EMP]

An outline of EMP organizational set-up necessary for chain of commands during emergency situation in the plant is as given below.SCC should develop EMP in the organization and send it statutory authorities for approval and integration in District Disaster Management Plan. A sample EMP is enclosed for reference.

President (Operations) of the SCC is the Chief Emergency Coordinator and he shall be the main guiding person directing the emergency operations. He shall be assisted by:

| Chief Site Coordinator. | In-charge (Production) | | |
|---|---|--|--|
| | Coordinate and direct all the activities from Emergency site. | | |
| | In absence of In-charge (Prod.), Manager (Prod. I/II) will act as Chief Site Coordinator. | | |
| Chief Maintenance Coordinator Manager-Maintenance | | | |
| | Coordinate all the maintenance activities from the Emergency Control Center. | | |
| | In absence of Manager (Maint.), Asst. Manager will act as Chief Maintenance Coordinator. | | |
| Chief Service Coordinator | Manager (HR) | | |
| | Coordinate with local administration take care of transport, medical, canteen arrangements, and evacuation of people if required. | | |
| | In absence of Manager (HR), Asst. Manager (P&A) will act as Chief Service Coordinator. | | |
| Chief Material Coordinator | Manager (Commercial) | | |
| | In absence of Manager (Commercial), Asst. Manager (Commercial) will act as commercial Coordinator. | | |
| Operation Coordinator | Manager (Prod.) is the Incident | | |
| | Controller for Vehicle Control & Security | | |
| | Personnel Security Officer | | |
| | In absence of Security Officer, Security Supervisor will act for Vehicle Control & Security Personnel deployment. | | |



Fire & Safety Controller

In-charge (F&S)

In absence of In-charge (F&S), Supervisor. (F & S) will act as Fire & Safety Controller and also for first aid.

Two "Assembly Points" will be identified (based on wind direction and away from hazardous areas) and duly marked.

Chief Service Coordinator shall contact the following senior officers stationed at Bulandsahar.

6.29. Responsibilities & Role of Key Personnel

6.30. Over all In-charge – President (Operation)

On getting the information about emergency from In-Charge (Prod.) rush to incident site/. Assess the overall situation and provide guidance in critical decision-making.

6.31. Chief Site Coordinator- Manager (Prod.)

- On getting the information about emergency from Supervisor Plant, inform over all Incharge Plant (Operation).
- Rush to the emergency site to assess the situation and decide to:
 - Declare emergency based on amount/extent of hazards and water/air analysis (toxic / flammable material release) and advise in charge (F&S) for sounding emergency siren.
 - Review if plant shutting down is required to contain / control the hazard.
 - Review, evacuation from affected areas and sending the affected person to a safe place.
 - Advise Incident Controller and other key personnel to take necessary action.
 - He will interact with Chief Service Coordinator and advise him on possible effects on areas inside and outside the factory to initiate Off- Site Emergency Response Plan.
 - Remain in touch with Overall in-charge (P -O) and inform about the situation
 & actions being taken and seek his advice for the critical decisions.

6.32. Chief Maintenance Coordinator- GM (Maintenance)

- After getting information about emergency from manager concerned Plant. Inform all concerned personnel to be on alert.
- Rush to the ECC, assess the situation and facilitate Chief Site Coordinator-GM (Prod.), Maintenance support needed to tackle the emergency.
- Facilitate elect. isolation of the affected area, if required through Supervisor (E&I)



- Facilitate lighting arrangements at (a) affected locations and (b) Assembly points if required through Supervisor (E&I)
- Facilitate work-shop facilities with adequate manpower if required through Manager (Maintenance). Remain in touch with Chief Site Controller.

6.33. Chief Service Coordinator - Manager (HR)

- On getting information from the Medical Coordinator rush to the Emergency Control Centre.
- Assess the situation in consultation with Chief Site Coordinator and Incident Controller and ensure that casualties get adequate transport / medical help.
- Make arrangement to shift all the persons to the safest place if called for.
- Assess 'Law and Order' situation.
- Inform press, TV / Radio, local authorities about the severity of situation in close coordination with Chief Site Coordinator and in consultation with Over All In-charge -P (O).
- Inform the District Authority / local police station in case their help is required for evacuation of personnel / preserving law and order.
- Evacuation of adjoining areas and villages, if required.
- Remain in touch with over all In-charge P (O) and seek his advice for the critical decisions.

6.34. Chief Material Coordinator- Manager (Materials)

- Rush to the emergency control centre on receipt of the message from Chief Service Coordinator / on hearing the emergency siren and inform Supervisor. (Store) about the emergency.
- Get the stores opened for requirement of the Firefighting/safety and other materials, which may be required during emergency.
- Assess the situation in consultation with Chief site coordinator & incident controller for any material requirement /help at the affected site.
- He will be responsible for the arrangements of trucks for movement of bulk material if required.
- Remain in touch with Chief site coordinator, Incident controller, and Chief maintenance coordinator.

6.35. Incident Controller Concerned Plant -Manager Concerned Plant

• Rush to the site of emergency after getting information from Shift In-charge assesses the situation and immediately inform



- \circ GM Prod.
- Take over charge from shift in charge.
- Ensure that persons working in the area are safe and isolate source of toxic release if possible.
- Advise and assist in charge (F&S) for providing water curtains to contain toxic release with in the plant battery.
- Remain in touch with Chief Site Controller and other concerned officers.
- Coordinate with Chief Maintenance / Chief Material coordinators for assistance required at site.
- Depending upon the severity of incident, ensure that adequate emergency services like Medical/ Laboratory/ Mechanical/ Electrical etc. Are summoned.
- Preservation of evidence as far as possible without affecting the operation of emergency procedures to facilitate any subsequent inquiries into the causes and circumstances, which led to the emergency.

6.36. Shift In charge (Concerned Plant):

- Immediately proceed to the site of emergency and assess the situation:
- Emergency Control Room at 101/123 (with name and location of emergency)
- During odd hours/till arrival of Fire shift I/C should act as chief fire coordinator.
- Initiate the shutting down operations for controlling the hazard if unavoidable.
- Cordon off the area and do not allow any body to enter the affected area without respiratory protection (In case of toxic gas leakage).
- Direct rescue operations with the help of fire and safety staff.
- Open safety Almirah for the use of plant personnel.
- Have regard to the need for preserving evidence that could facilitate subsequent inquiry.
- Advise Supervisor of the plant to take roll call and account for missing personnel.
- Hand over charge of the operation to the Manager when he arrives at site.
- Ensure service agencies like Electrical, mechanical, instrumentation is mobilized to handle the emergencies.

6.37. Security Officer Vehicle Control and Security Personnel Deployment at the Locations

• Rush to the spot of emergency on getting information from Security Officer on duty and inform Manager (HR) about emergency.



- Arrange one emergency vehicle immediately for ECC.
- Keep in touch with Chief Service Coordinator, Chief Site Coordinator and in charge (F&S).
- He will act as a special rescue Coordinator at the time of evacuation of employees and others if required.
- Alerts complete staff under his control and make it available at a known point, as per the guidance of Chief Site Coordinator / Chief Service Coordinator.
- Anticipate and arrange vehicles required at emergency site in consultation with in charge (F&S) and Chief Site Coordinator and Chief Service Coordinator.
- On request send vehicles for getting plant personnel / fire personnel required for emergency.
- Arrange vehicle in consultation with Medical Coordinator / Chief Service Coordinator for shifting injured to city hospital.
- During emergency arrange for opening of relevant gates/ barriers for easy movement of vehicles. Security Guards should be posted on these gates / barriers to prevent unauthorized entry.
- Arrange transport and temporary shelters for evacuated personnel and inform the relatives of the affected personnel if required.

6.38. Fire & Safety Controller- In charge (F&S)

- Rush to the spot of emergency after getting information from ECC and inform to Supervisor. (F&S).
- Direct rescue operations under the guidance of Chief Site Coordinator/ Incident controller if required
- Ask additional help from C.S.O. for cordoning off the area and advise fire personnel for rescue / firefighting if required
- Arrange to provide water curtains, water monitors, at affected locations if required.
- Organize and supervise fire-fighting operations if called or.
- Provide necessary respiratory equipment to plant personnel for emergency use.
- Advise Chief Site Coordinator to arrange additional help Mutual aid group / neighbouring industries if required.
- Give safety precautions to the personnel at rescue work.

6.39. Fire Control Room In-Charge

On receiving emergency message from the in charge(F&S)/ on hearing siren. Rush to ECC and take charge of Fire Control Centre from the fire operator / fire supervisor.



- Assess the situation and Call fire staff from fire barrack.
- Immediately rush fire crew to emergency spot.
- Inform Medical Centre for sending ambulance to emergency site.

6.40. Fire Supervisor should also ensure the following:

- \circ Supervisor to look for the wind direction and cordon off the area.
- Use water monitors/hydrants/water curtains in consultation with incident/Chief site controller.
- Provide respiratory equipment's to the plant personnel.
- In case of toxic spillage at site, put foam (HAZMAT)/ sand on the spillage area.
- Remain in touch with in charge(F&S).
- Chief Site Co-coordinator will instruct Fire Control Room In-charge for operation of "All Clear Siren" when the disaster is contained / controlled.
- However, regular testing of siren & emergency buzzer plant control rooms for 2 minutes on every Monday at 13.00 hrs is being done. All clear siren will sound for 2 minutes with a continuous sound.

6.41. Post Emergency Recovery

The post-emergency procedures discussed briefly below are designed to successfully manage the damage / losses of an emergency event. The focus of these procedures is to move the plant back into normal operating mode as quickly and efficiently as possible.

Immediately after the "ALL CLEAR" an emergency meeting will be held in emergency control center to assess the loss both for men & materials, where in following will be present with attendance records, details of injured, outside situation and preparation of press release (if felt necessary)

- Overall In charge
- Chief Site Coordinator
- Chief Maintenance Coordinator
- Chief Service Coordinator
- Incident Controller
- Material Coordinator
- Security
- Fire & Safety Controller



6.42. Accident Investigation

| a. | As soon as possible after the emergency is over and plant operation has become normal, the investigation and analysis are to be carried out to determine the cause of the event. |
|----|--|
| b. | Representatives from various disciplines will be members of the investigation and analysis team. |
| с. | The areas of the events are to be sealed off so that tempering or alterations of the physical evidence are not likely to occur. |
| d. | Key components are to be photographed and logged with time, place, direction etc. |
| e. | Statements are to be taken from those who were involved with the operation or who witnessed the event. |

6.43. Damage Assessment

This phase of recovery establishes the quantum of replacement machinery considered necessary for bringing back plant to normal operation; property and personnel losses accounted and culminates in a list of necessary repair, replacement and construction work.

Insurance companies will be informed of the damage and requested to pay the compensation as per claim.

6.44. Clean-up and Restoration

This phase will only begin once the investigation is complete. Reporting documentations are to be prepared and forwarded to appropriate authorities. Repair, clean up and restoration work to begin.

6.45. Conclusion & Recommendations

The hazard analysis and risk assessment incident scenario indicate that incidents mostly are not limited to plant battery limits but covers surrounding area also. There are possibilities of domino effect and the secondary scenario not predictable can be worse than the primary one. The scenarios (specifically toxic hazards scenarios) are crossing the plant boundaries. The direction of impact will be in down wind direction (wind direction and speed vary with season).

Some of the recommendations for Tank farm storage system are as given below:

- Provision of flame detectors/ thermal sensors at strategic locations in the tank farm area.
- Auto water deluge system on each bulk storage tank for inflammable liquids. The system should automatically start taking signal from flame detectors or thermal relay.



• Fixed foam system with adequate capacity.

Human Factors: Company is having well equipped fire station and also safety department – safety practices. Human factors role in safety cannot be ignored. Odd hours working and over / long hours work can drain out individual. It shows in lack of efficiency and also the lack of paper attention the modern which chemical complex demand. They are to be closely looked into and avoided.

'Safety' has unique features:

If no accident has happened so far probability of incident / accident occurring increases.

'No accident' / good safety record develops complacency inertia/ over confidence in the team. This attitude gives rise to gaps / soft spots in the system giving chances to incidents / accidents.

Safety requires novelty. Routine training practices get stale with no positive results. Look for novel scheme of training/ safety practices to build up fresh impetus in safety. Involvement of employees with refreshed outlook for safety is to be achieved.

SCC will strength their safety system by introducing SOP's, work instruction followed by mock drill with proper intervals, fire escape routes will be marked with all fire extinguishers putting in place with proper trained fire team. It is proposing to install fire hydrant system also as the storage and handling of flammable material will increase.

Above all it is attitude and practice which always help in handling the incident/ accident occurs at anywhere especially regular, fire drills and induction training program at plant before starting the day helps in avoiding the risk. It is also going to made mandatory to use PPE at site. Company has policy to achieve zero accident rewards system for employs to motivate and maintain safe environment.

The hazard potential of chemicals and estimation of consequences in case of their accidental release during storage, transportation and handling has been identified and risk assessment has been carried out to quantify the extent of damage and suggest recommendations for safety improvement for the proposed facilities. Risk mitigation measures based on MCA analysis and engineering judgments are incorporated in order to improve overall system safety and mitigate the effects of major accidents.

An effective Disaster Management Plan (DMP) to mitigate the risks involved has been prepared. This plan defines the responsibilities and resources available to respond to the different types of emergencies envisaged. Training exercises will be held to ensure that all personnel are familiar with their responsibilities and that communication links are functioning effectively.

